



Dipartimento di Ingegneria Meccanica

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Development of a Model-Based Diagnostics Tool for Solid Oxide Fuel Cells

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Presentation Outline



- Motivation, goals, approach
- Design/Control/Diagnosis oriented model for APU
- Application of the model
 - Design and Control
 - Simulation of a typical automotive auxiliary load profile
 - Diagnostics
- Conclusions



Motivations and goals



Motivations

- Developing SOFC technology to face **environmental-** and **energy-related issues**.
- High SOFC potential for both **residential** and **mobile** applications (high efficiency, cogeneration, modularity, fuel flexibility, low emissions and noise).
- Specific **short-term target**: enhance the development of **highly-efficient SOFC-APUs** destined to a wide application area (ground transportation, marine and airplane APUs).

Goals

- Development of **model-based tools** for **Fast Design, Control and Diagnosis** of SOFC systems.
- Adopt lumped **modeling approach** to meet the **trade-off** between computational burden, experimental efforts and model accuracy.



On-Field Diagnosis of SOFC Systems



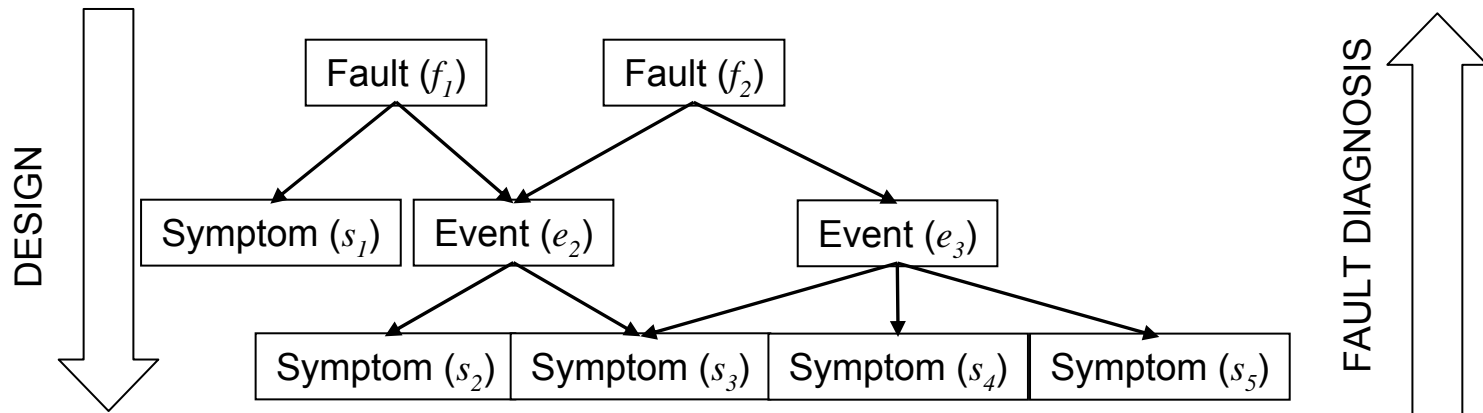
Objectives

- Prevent SOFCs from highly damaging system failures
- Monitoring SOFC operations throughout its lifetime
- Detect and manage faults

Type of faults

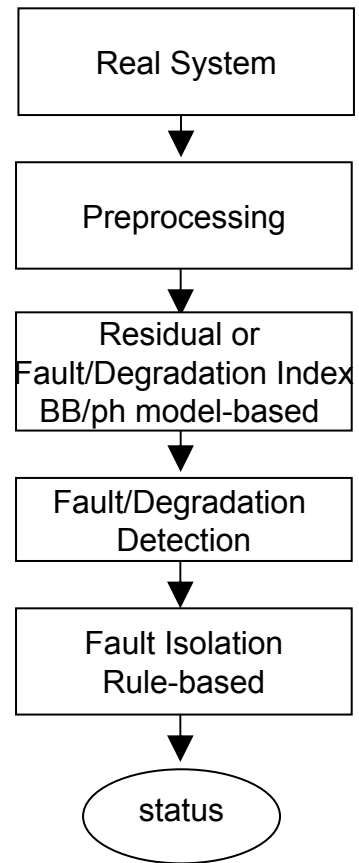
- BoP level
 - Sensors (pressure, temperature) & Actuators (electric motors, valves)
 - Auxiliaries (blower/compressor, heat exchangers, reformer)
 - Components (pipes, manifolds)
- Stack level
 - Material degradation
 - Electrodes poisoning
 - Etc.

Design and real time operation of diagnostics tools

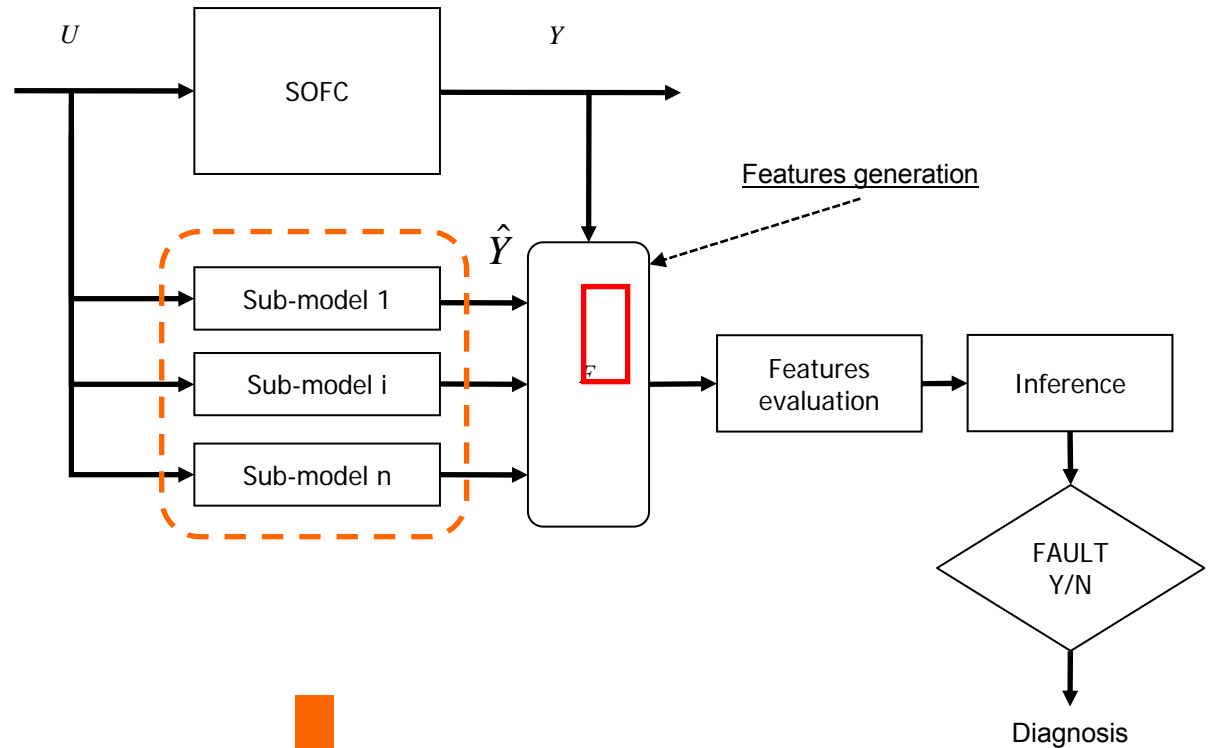




Diagnostic process



Model-based approach



It requires suited SOFC+BoP models

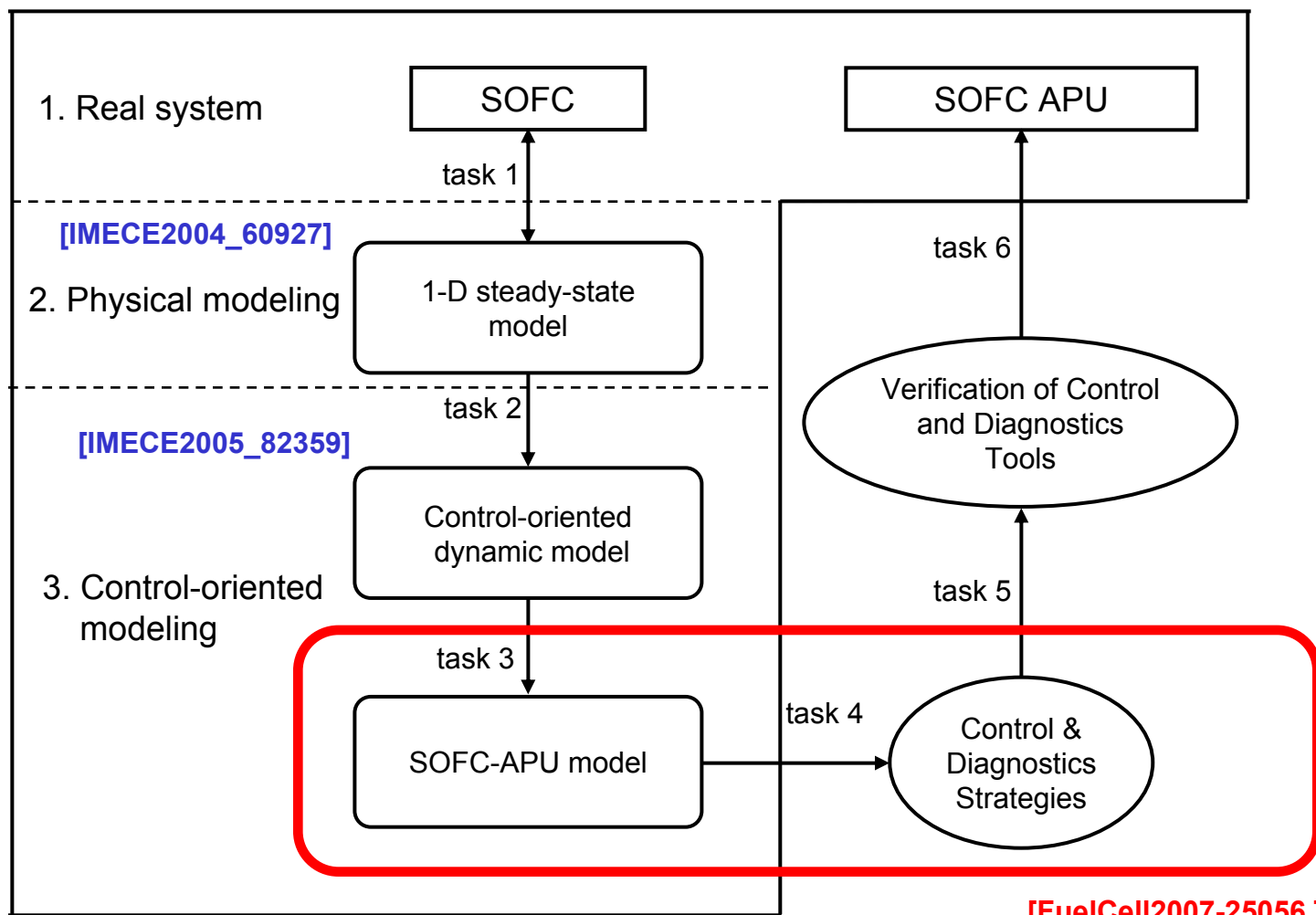
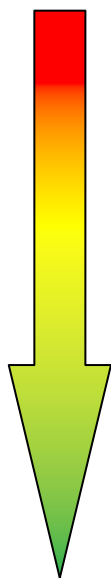


Modeling Approach



A hierarchical structure combining several models was developed to achieve accurate and fast SOFC APU dynamic model

Models' Hierarchy





SOFC APU Block Diagram

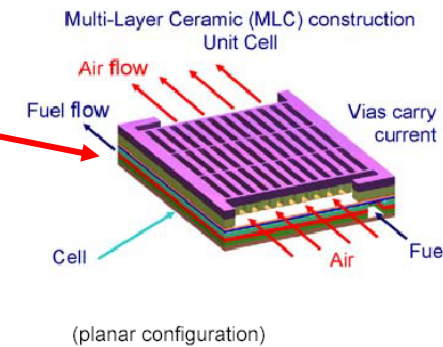
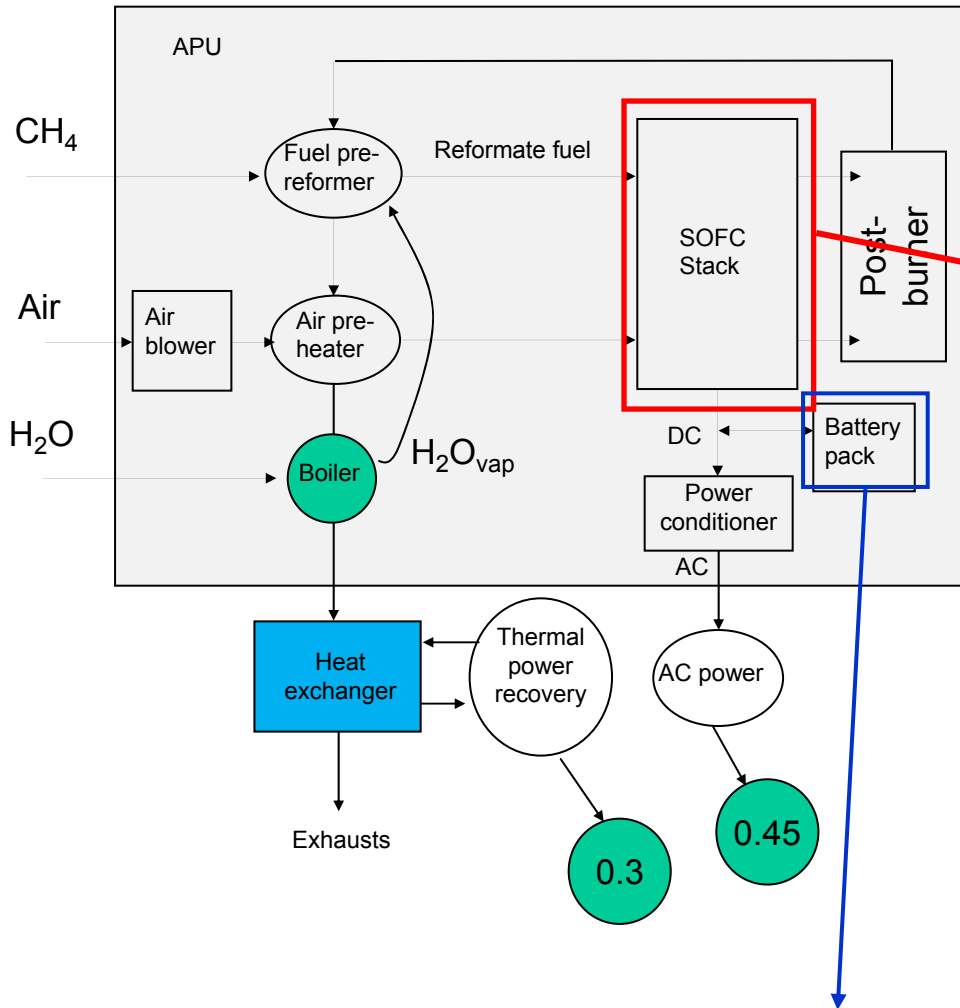


Figure 3. A 5-cell cross flow stack assembled from co-fired cells and interconnects. The air and fuel channels are seen on the two faces of the stack shown.

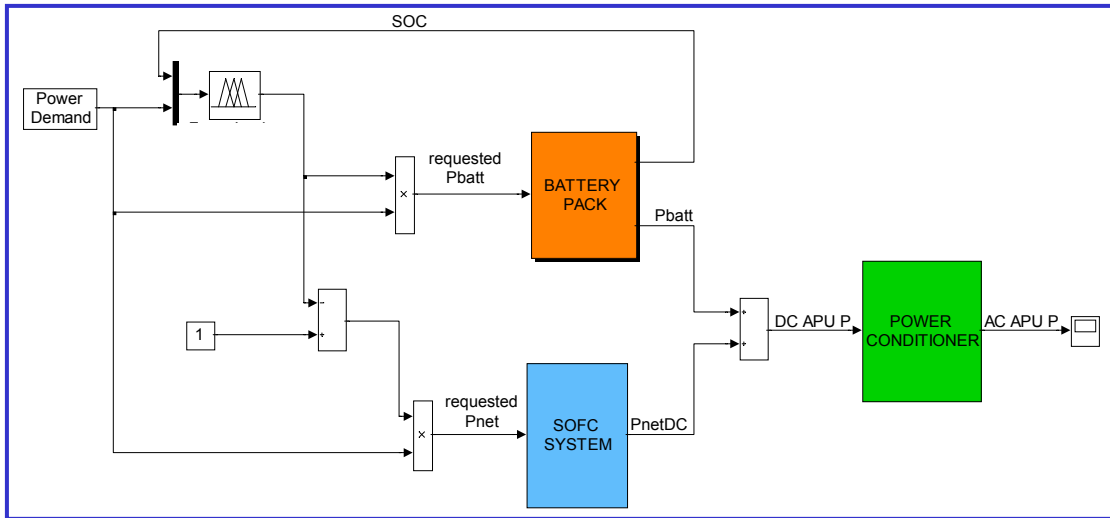
Source: SOFCo - EFS

Planar co-flow SOFC

Hybridized with battery for start-up; peak power; transients; energy storage



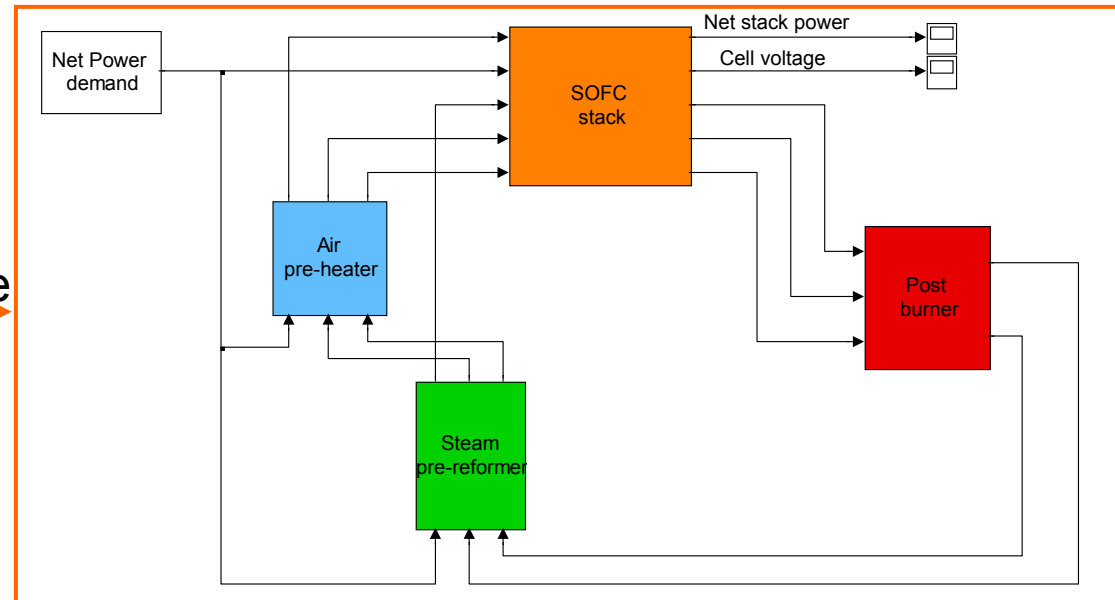
Modeling scheme



Outer APU scheme



Inner SOFC system scheme





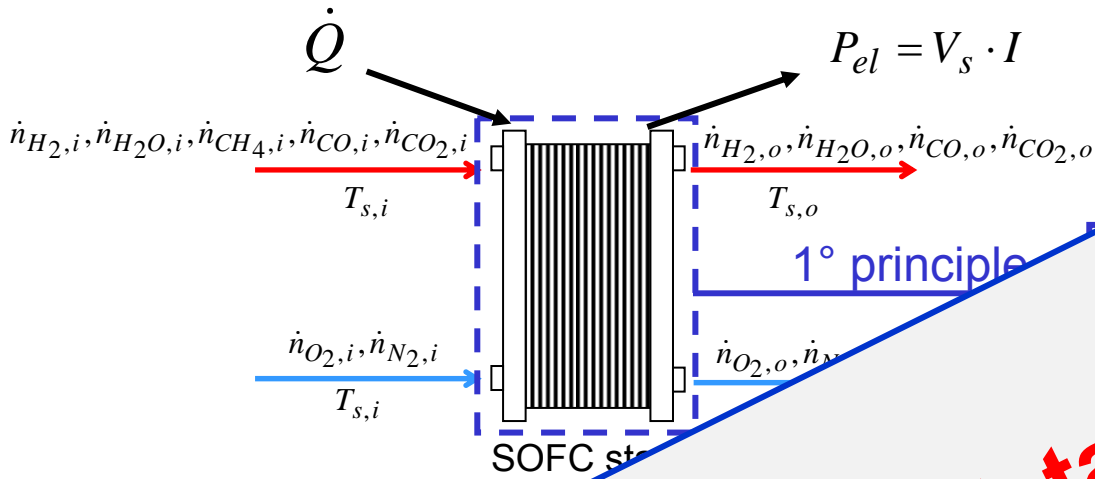
Modeling assumptions



- Spatial variations are not considered, i.e. **lumped** modeling approach.
- **Thermal dynamics is predominant**; mass transfer and electrochemistry were assumed instantaneous.
- **Lumped** heat transfer coefficients were assumed to model **heat exchangers**.
- **Adiabatic** components.
- Water gas shift reaction is considered at equilibrium.



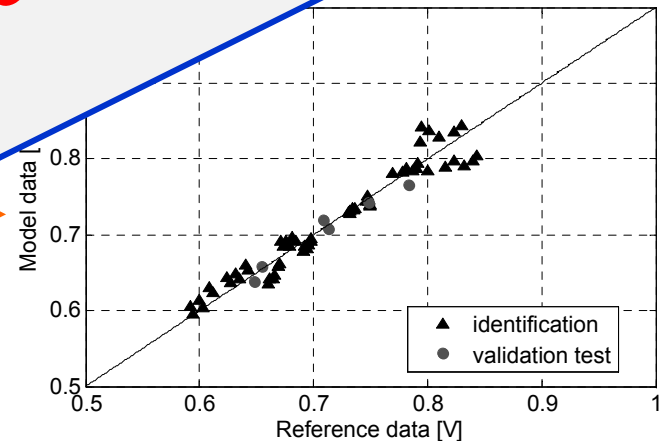
SOFC dynamic model



The outlet temperature is ...

The entire model (stack+BoP) is ≈ 100 time faster than real-time !!!

$$V_s = f(x, u) \Rightarrow V_s = 0.7153 \cdot \frac{T_{s,in}}{1000}$$





Model-based design



SOFC stack

Configuration	Planar
Material	Ceramic
Electroactive area	100 cm ²
Anode thickness	<u>600 μm</u>
Electrolyte thickness	50 μm
Cathode thickness	50 μm
Interconnect thickness	500 μm
<u>Heat capacity</u>	<u>8234 J/K</u>
Pressure	1 bar
Temperature in	700 °C
Temperature out	825 °C
Number of cells	150
Max DC Gross Power @ 0.8 A/cm ²	7.5 kW
<u>Max AC Net Power @ 0.8 A/cm²</u>	<u>5 kW</u>
Fuel utilization	0.7
x_{fuel} - reformat	$x_{H_2} = 0.273$ $x_{H_2O} = 0.483$ $x_{CH_4} = 0.171$ $x_{CO} = 0.019$ $x_{CO_2} = 0.054$

Air pre-heater

Type	Printed plate
Material	Ceramic
Heat transfer coefficient	200 W/m ² /K
Heat Transfer Area	0.56 m ²
<u>Heat capacity</u>	<u>588 J/K</u>

Pre-reformer

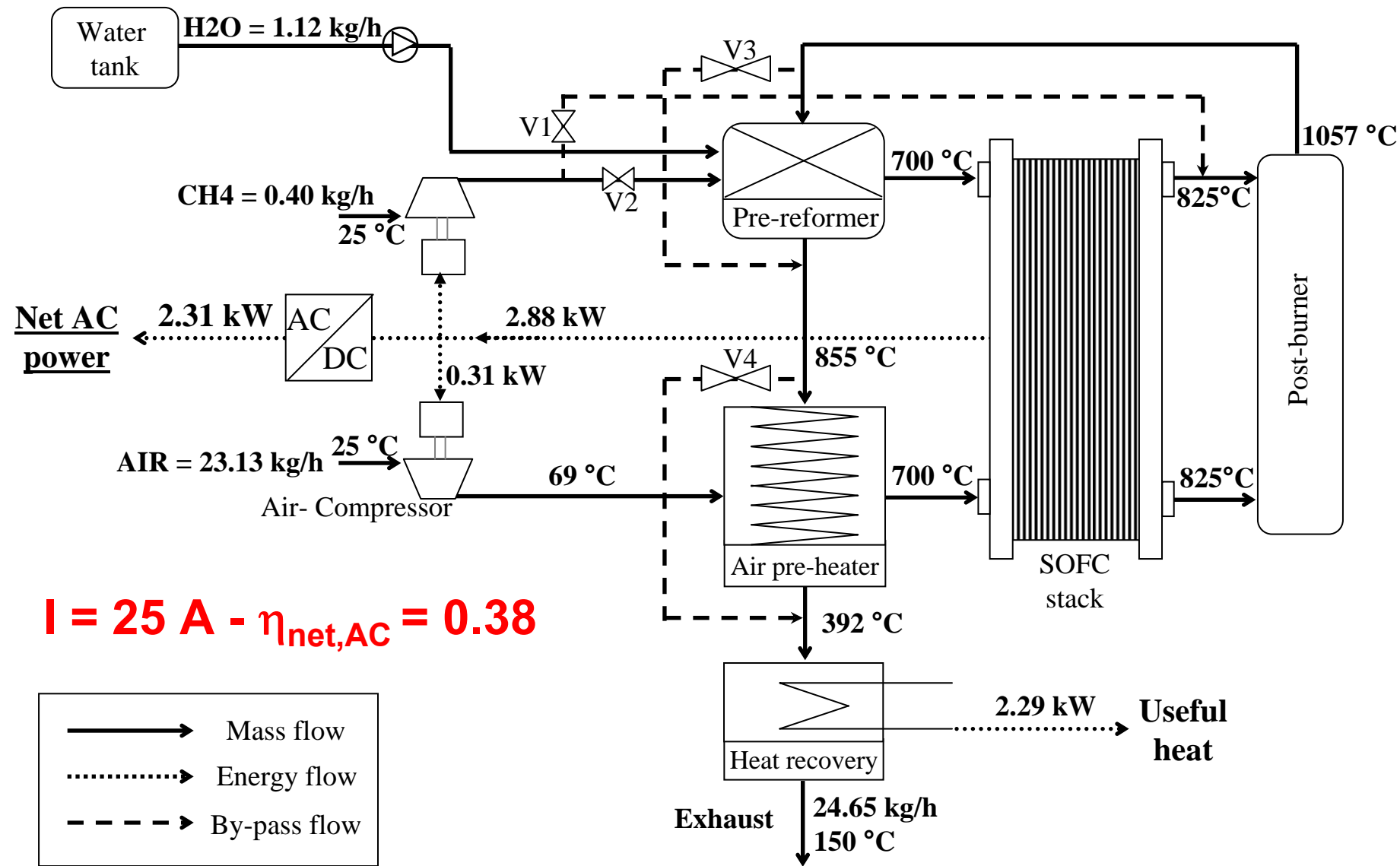
Type	Steam
Material	Ceramic
CH ₄ conversion efficiency	0.3
S/C	2.5
Heat transfer coefficient	200 W/m ² /K
Heat Transfer Area	0.04 m ²
<u>Heat capacity</u>	<u>44 J/K</u>

Battery-pack

Type	Lead-acid
<u>Number of modules</u>	<u>15</u>
Open circuit voltage	12 V
Capacity	25 Ah



SOFC system – Block diagram



$I = 25 \text{ A} - \eta_{\text{net,AC}} = 0.38$



APU control scheme



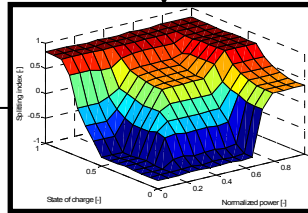
3 look-up tables (J; V3; V4)

Accessories load

Fuzzy-logic based map designed to:

- satisfy power demand;
- maximize global efficiency;
- guarantee a charge sustaining strategy for the batteries.

Supervisory Control



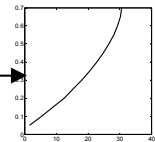
Rate Limiter

$P_{SOFC, req}$

$P_{batt, req}$

SOC

Look up table



J

SOFC System

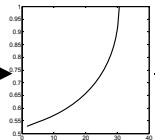
$P_{net, DC}$

$T_{s, out}$

P_{batt}

Battery

Look up table



V3

λ

PI

$T_{s, out, des}$

AC/DC

AC power demand

Low-level control aims at ensuring proper thermal management of the SOFC with:

- 2 PI controllers (cold start; warmed-up)

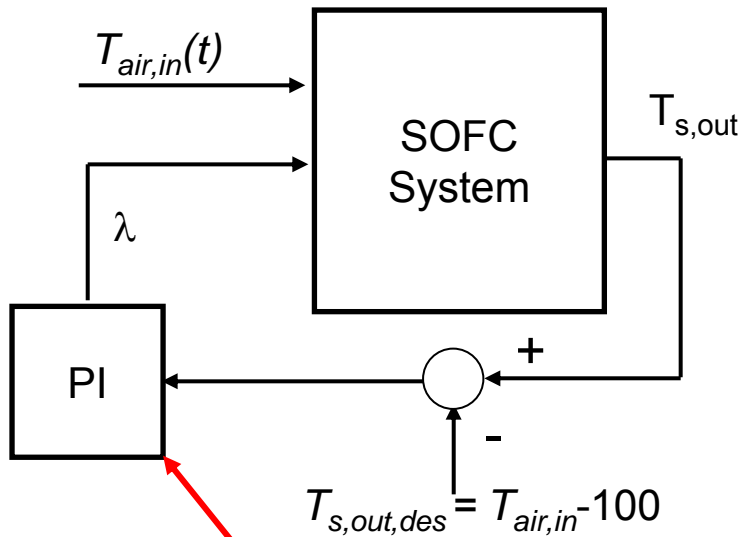
Low-level control



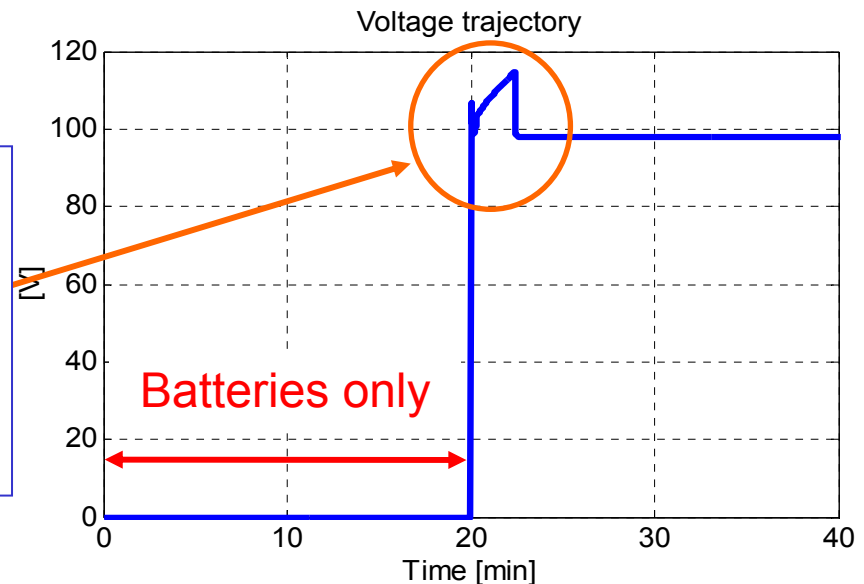
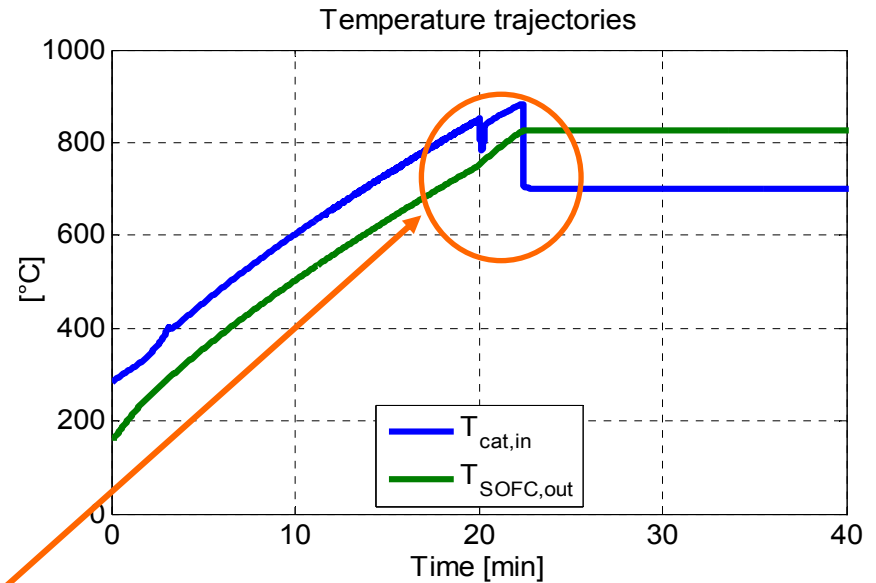
SOFC - Cold-start control



SOFC are air-cooled then λ is control variable

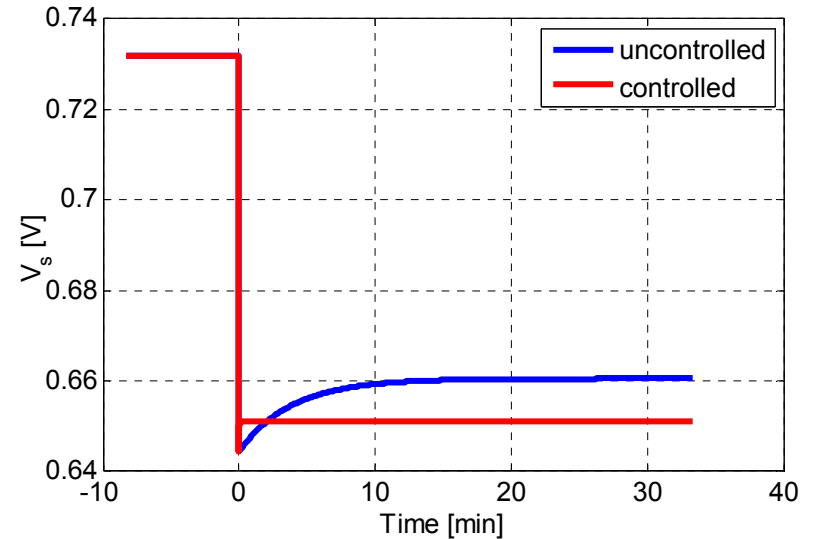
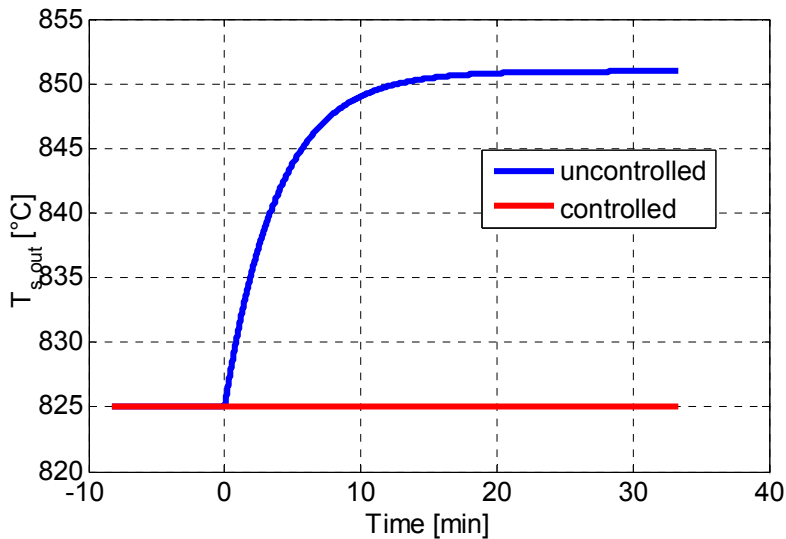
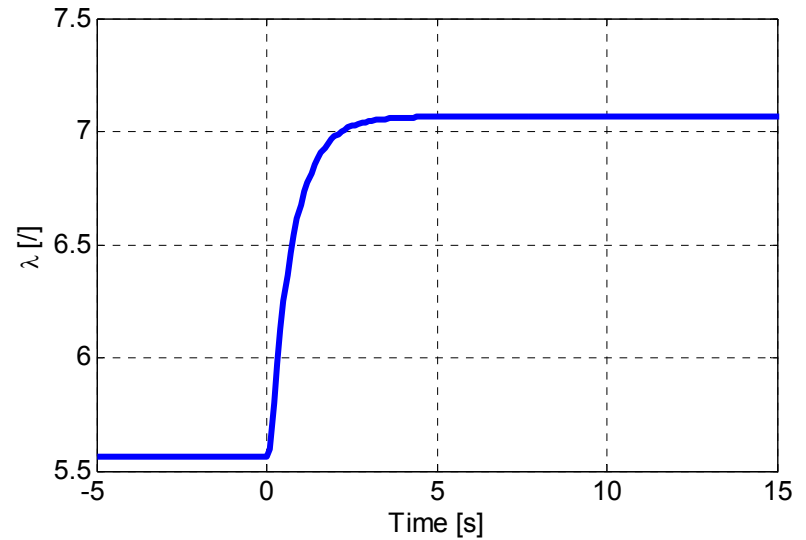
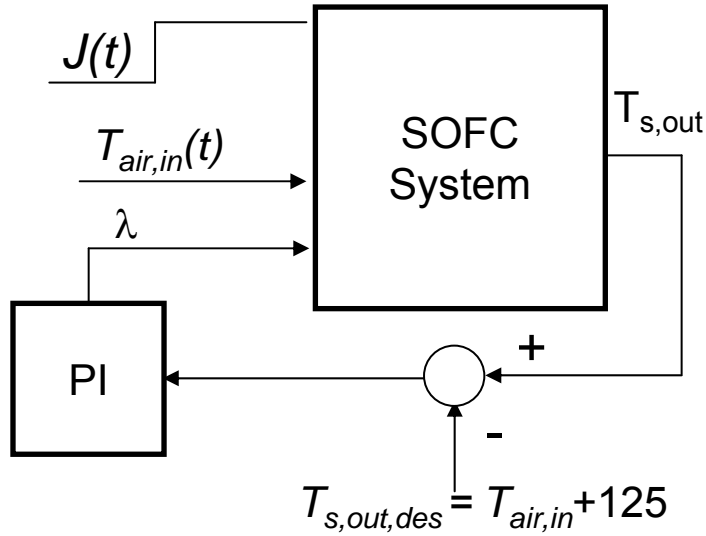


- The **PI acts** on the excess of air to limit the difference between $T_{air,in}$ and $T_{s,out}$ below 100 °C.
- **20 minutes Start-up** time was obtained.





SOFC - Warmed-up control





Simulated power profile

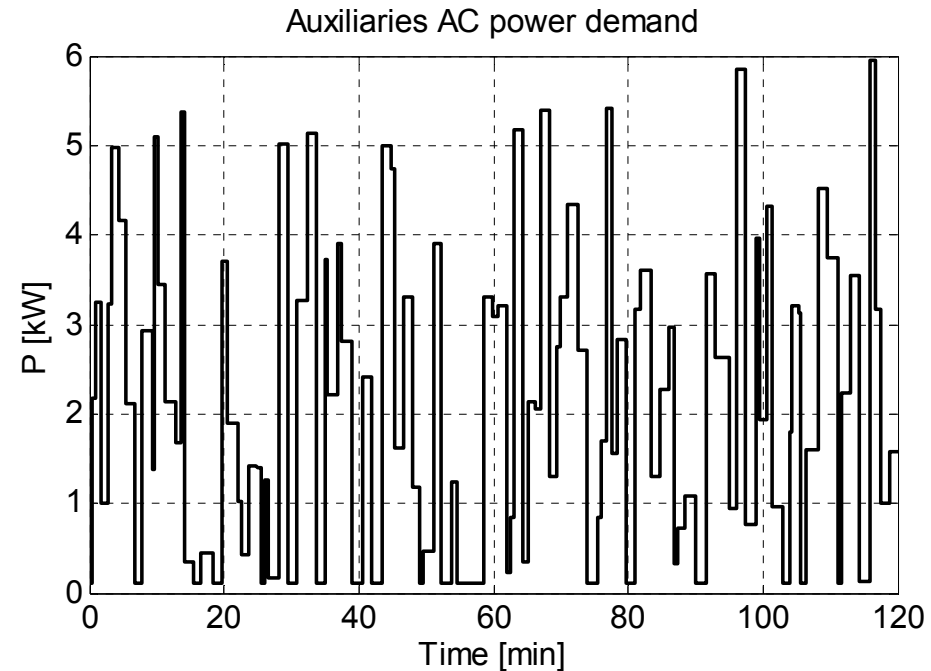


- Simulation-based testing of the SOFC-APU model.
- The reference profile, generated **randomly**, is a typical **auxiliary load** profile for commercial **trucks** in parked **idling** phase.
- Two scenarios were analyzed:

$$P_{av} = 2 \text{ kW}$$

$$P_{max} = 6 \text{ kW}$$

Case 1	with SOFC cold-start
Case 2	warmed-up SOFC

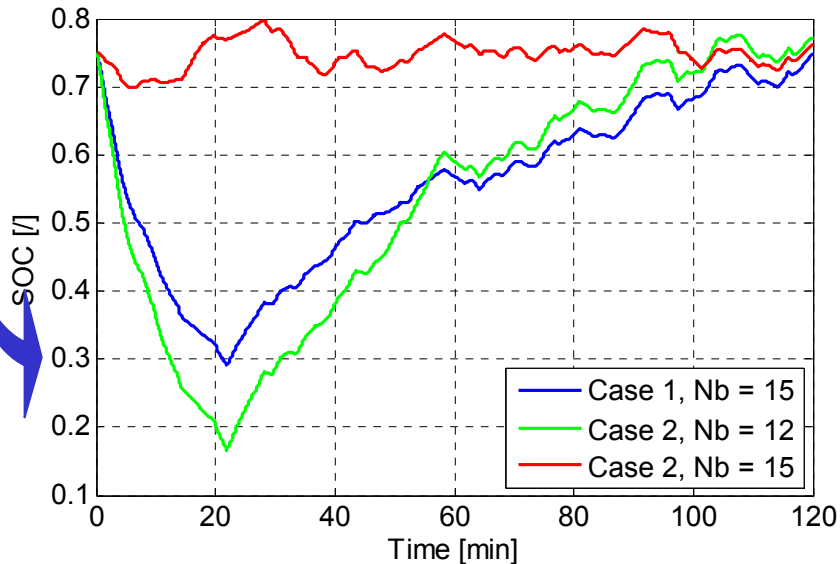




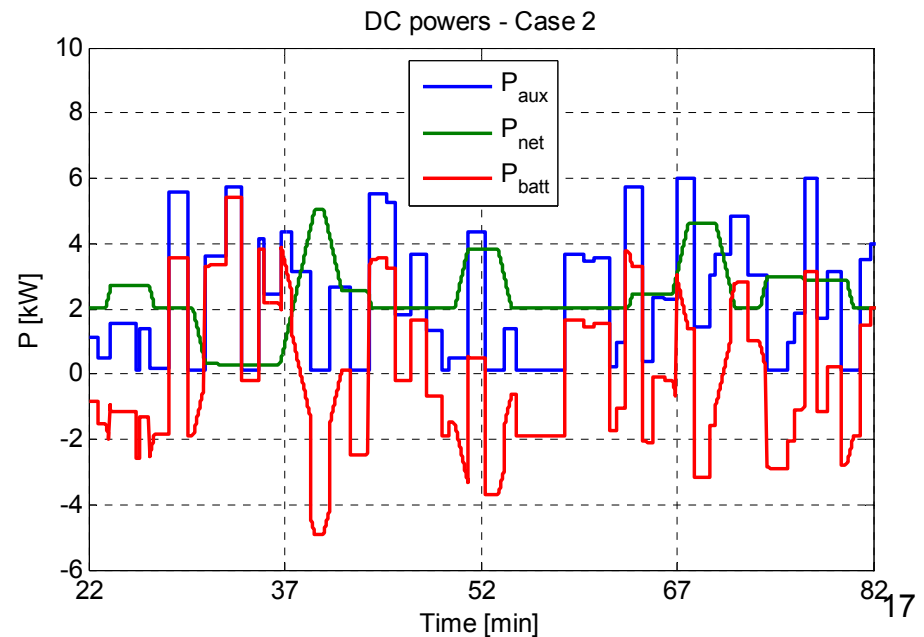
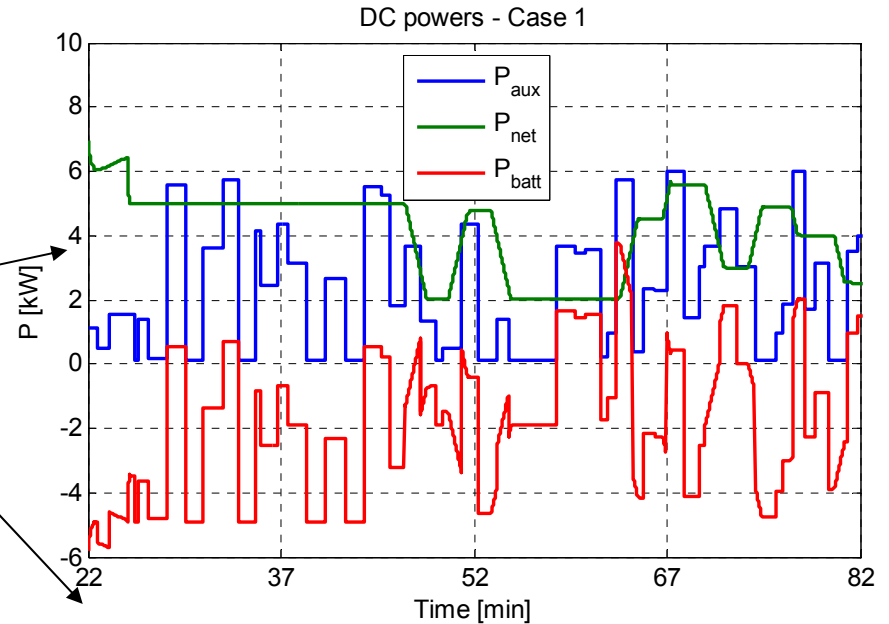
Simulation results



- The selected number of modules allows a more conservative operation of the battery pack.
- Cold-start influences SOFC power requests (case 1).



↔ Case 1 warm-up period

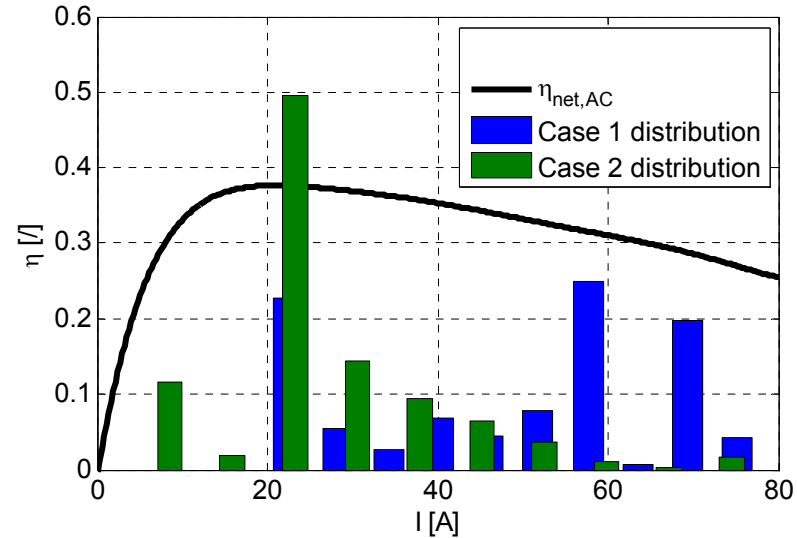




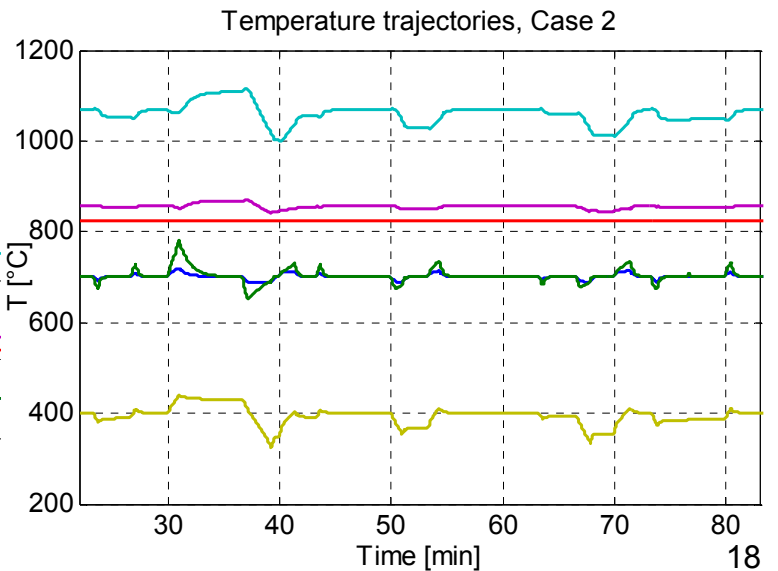
Simulation results



- Cold-start operation impacts on fuel consumption.
- Low-level control guarantees a proper thermal management.

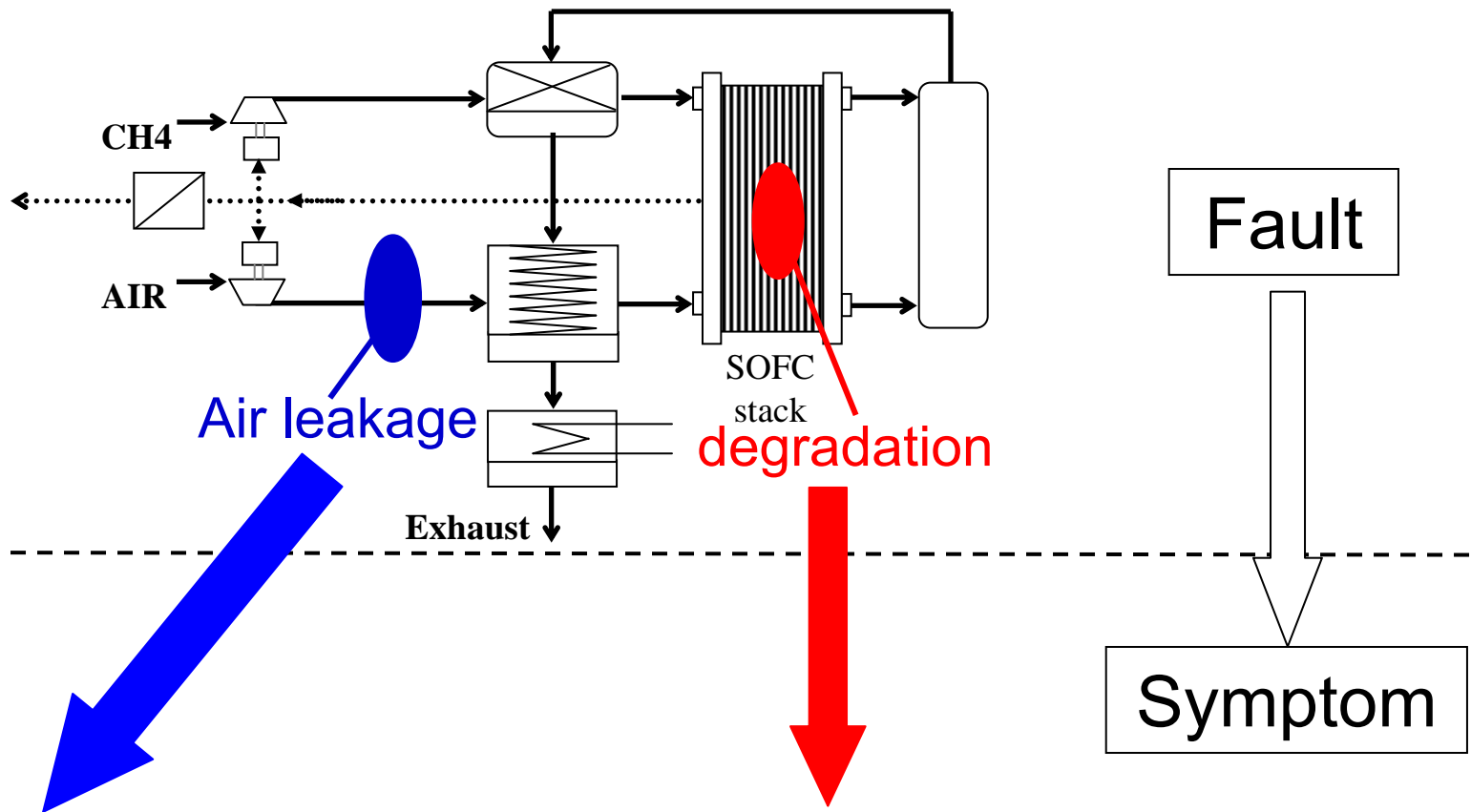


	m_{CH4} [kg]	$m_{Diesel,eq}$ [kg]	$m_{Diesel,c}$ [kg]	Fuel savings [% of $m_{Diesel,c}$]
Case 1	1.54	1.80	3.19	44
Case 2	0.84	0.98	3.19	70





Diagnostics Application



$$\lambda \uparrow \rightarrow P_{cp} \uparrow \left. \vphantom{\lambda \uparrow \rightarrow P_{cp} \uparrow} \right\} P_{net} \downarrow$$
$$P_{gross} =$$

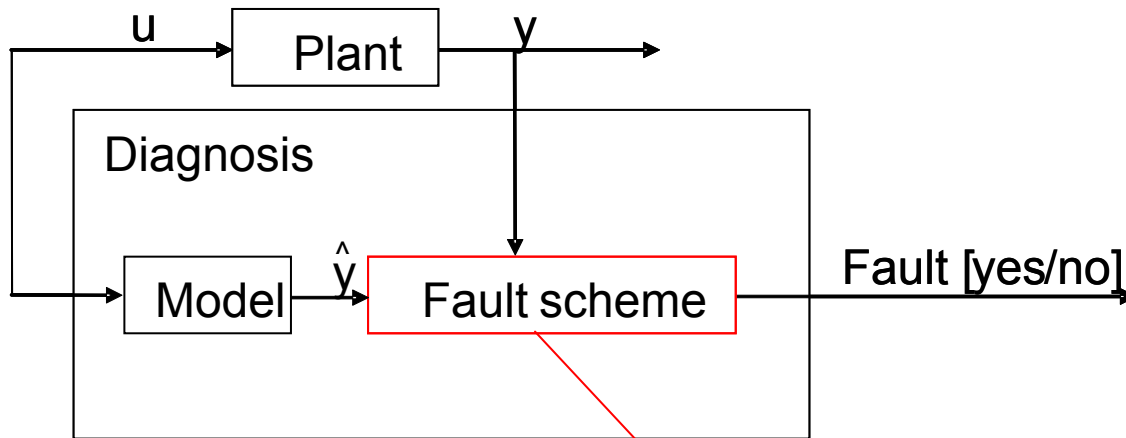
$$P_{gross} \downarrow \left. \vphantom{P_{gross} \downarrow} \right\} P_{net} \downarrow$$
$$\lambda \uparrow \rightarrow P_{cp} \uparrow$$



Diagnostics scheme



Detection of **air leakage (i)** and **stack degradation (ii)** with Parity-equation based diagnostics method:



$$R1 = |P_{net,p} - P_{net,m}|$$

$$R2 = |P_{gross,p} - P_{gross,m}|$$

$$R3 = |P_{cp,p} - P_{cp,m}|$$

Inference from symptoms

Fault	R1	R2	R3
i) Air leakage	1	0	1
ii) Increased Ohmic losses	1	1	1

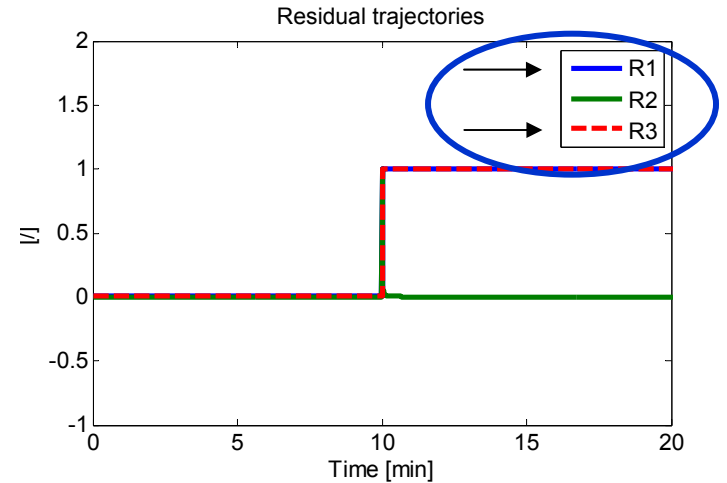
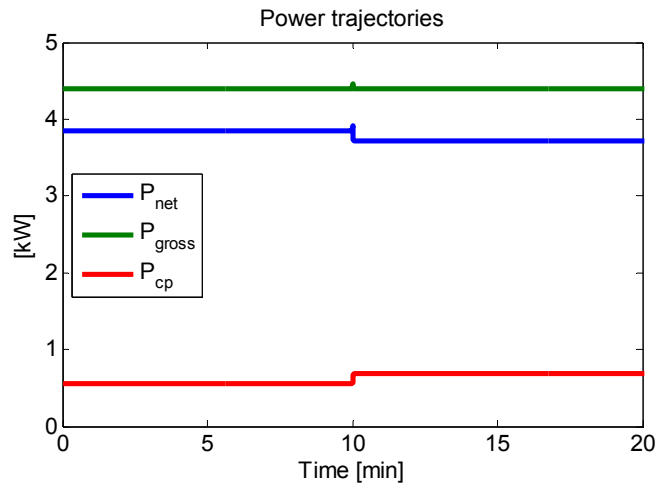
} redundancy



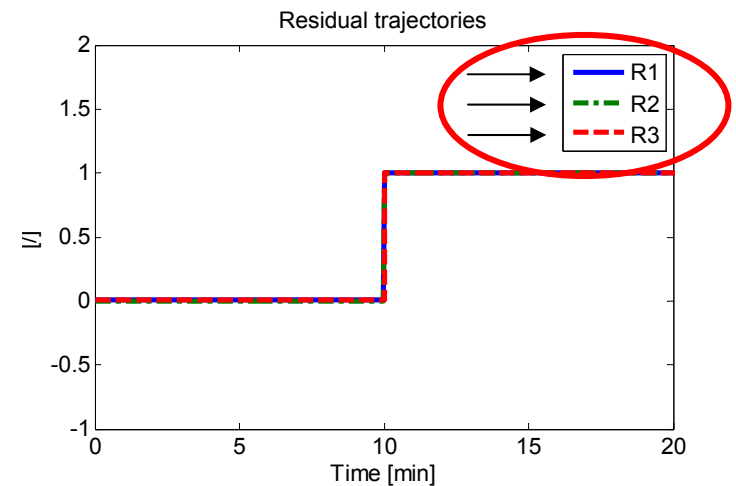
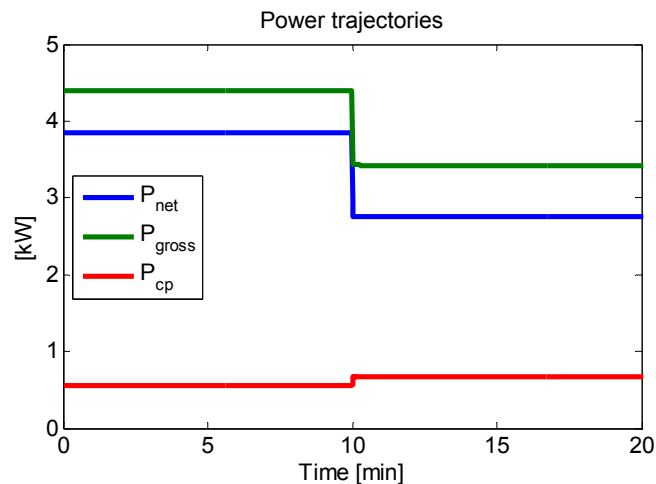
Fault detection



i) Stepwise Air leakage



ii) Stepwise Stack degradation





Conclusions

- **Modeling methodologies** were proposed to develop **control-/diagnostic-oriented** models of **SOFC cells/stacks**.
- Model-based design of suited **control strategies** to ensure optimal energy and thermal management.
- The developed model and related control strategies were tested via simulation of a typical **auxiliary power demand profile for commercial heavy-duty trucks**.
- **Model suitability** for developing appropriate **diagnostics strategies/architecture**.
- Future work will focus on **diagnosing the whole SOFC system** and perform **experimental testing** of control and diagnostic strategies.