#### SIMULATION-BASED DESIGN OF CO<sub>2</sub> CAPTURE REACTORS

Shahriar Amini, Schalk Cloete, Mandar Tabib & Abdelghafour Zaabout

Department of Flow Technology SINTEF Materials & Chemistry Norway



Materials and Chemistry

#### Agenda

- Why simulations?
- Why CO<sub>2</sub> capture processes?
- Accelerated development
- Model development
- Model validation
- Simulation-based reactor design
- Conclusions & future work



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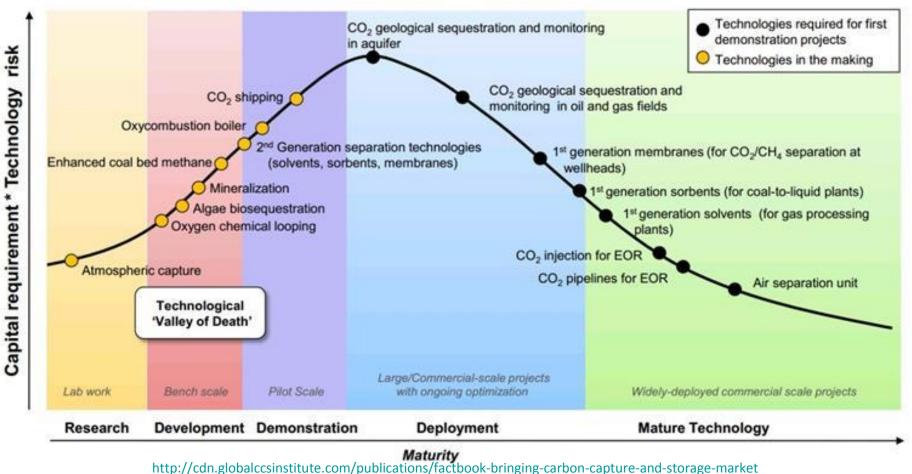
# Why simulations?

- Not subject to any physical limitations
  - Change any design/operating variable
  - Simulate real scales and operating conditions
  - Extract any flow variable from anywhere in space/time
- Ideal for:
  - Process optimization and scaleup studies
  - Prototyping of novel concepts
  - Troubleshooting of existing reactors





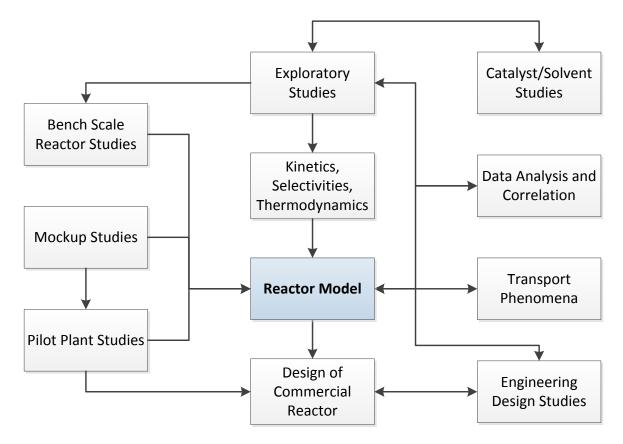
# Why simulate CO<sub>2</sub> capture systems? Relatively small amount of funding available Large number of candidate technologies Limited time to traverse the technology risk peak





#### **Classical process development**

Chemical engineers have used models for a very long timeModel is a vehicle to condense state of the art knowledge

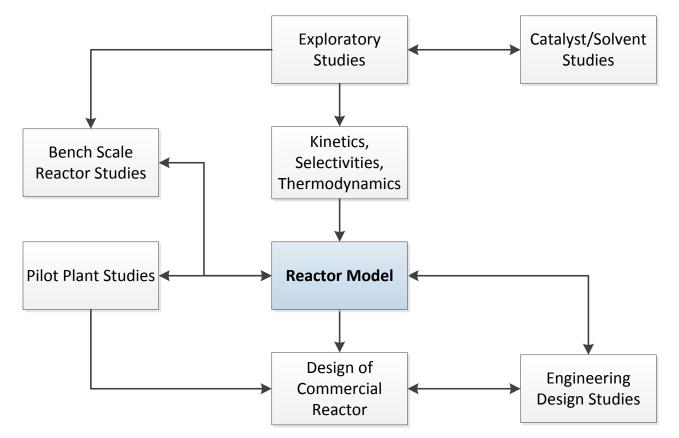


Johnsen et al. Energy Procedia 2009:1



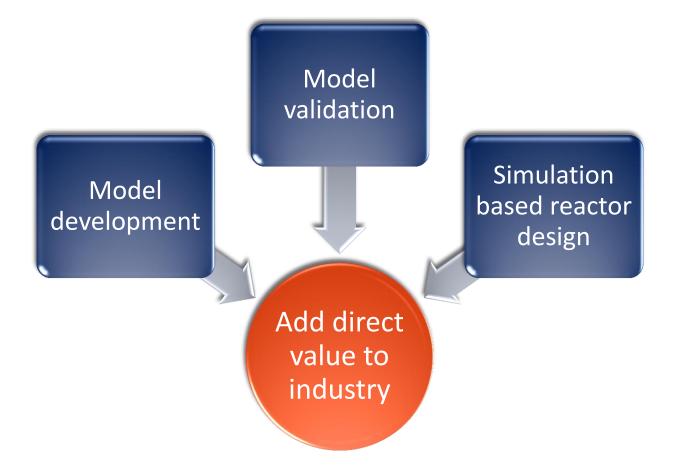
# Accelerated process developmentpotentials for low risk – high return

- More trustworthy model = larger scale-up steps
- Potential to greatly accelerate and optimize





#### **Accelerated development: Big picture**



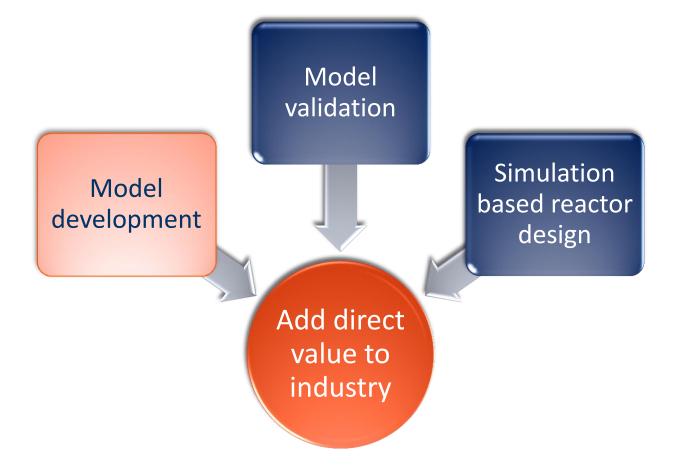


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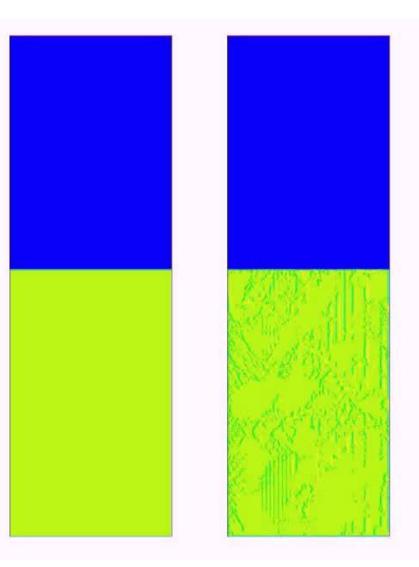
#### **Accelerated development: Big picture**





### **Model development: Fluidized beds**

- Challenge: Good accuracy required at low computational costs
- The use of super computers
- Current works on large scale models:
  - Dense Discrete Phase Model (DDPM)
  - Filtered Two Fluid Model (fTFM)





#### **Model development: Packed beds**

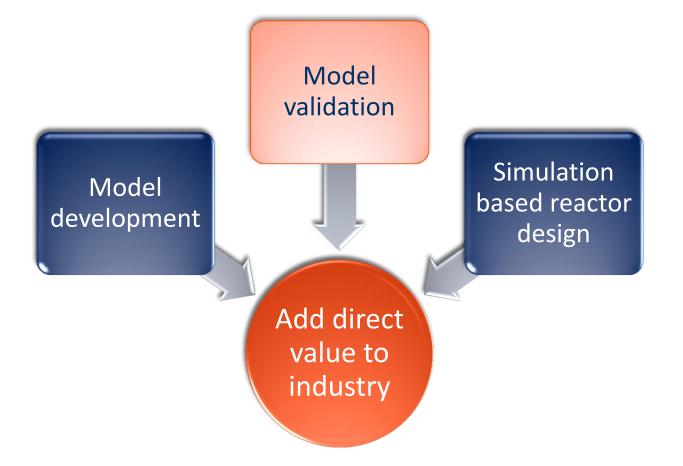
#### Simpler flow problem

- More sensitive to accurate material and kinetic data
  - Large temperature variations
  - Large chemical composition changes
  - Diffusion resistance within larger pellets must be accurately modelled
- ID models well developed ready for industrial applications (DemoCLOCK)
- Further development required:
  - Multi-dimensional models for special cases





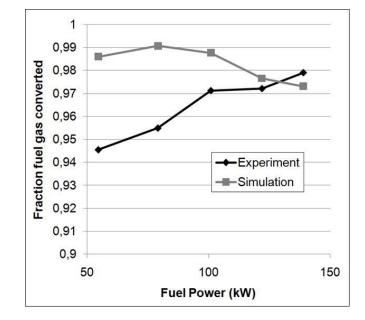
#### **Accelerated development: Big picture**





# **Model validation: Principle**

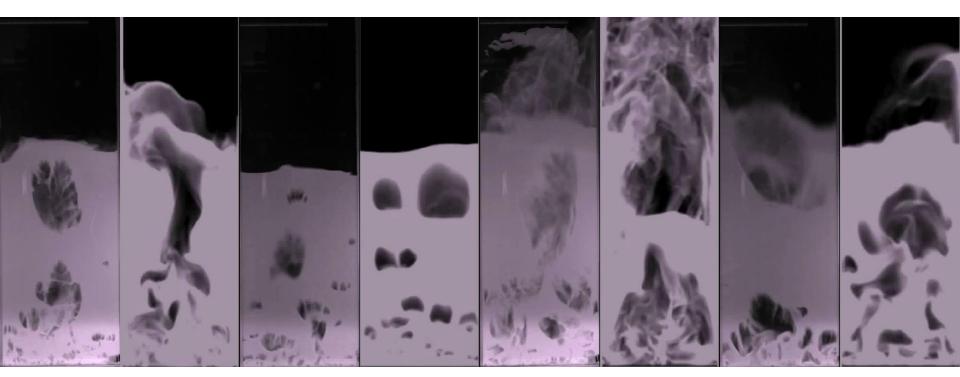
- Model generality must be explicitly demonstrated
  - Will inevitably be used far from validation conditions
  - Will be used as a basis for multi-scale modelling
  - Dedicated experimental campaigns required
    - Collect data over a wide range of flow variables
    - Collect detailed local measurements
    - Separate hydrodynamics, species transfer, heat transfer and reactions





### **Model validation: Hydrodynamics**

#### In collaboration with Eindhoven University of Technology

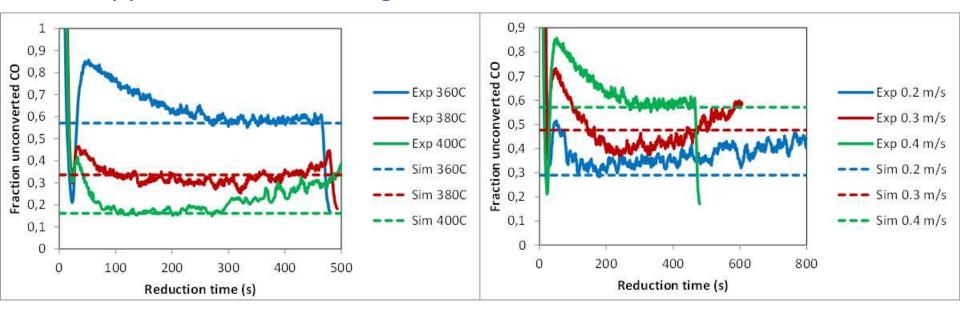


Particle size: 150 µm Fluidization velocity: 0.4 m/s Particle size: 350 µm Fluidization velocity: 0.4 m/s Particle size: 150 µm Fluidization velocity: 0.8 m/s Particle size: 350 µm Fluidization velocity: 0.8 m/s



### **Model validation: Reaction kinetics**

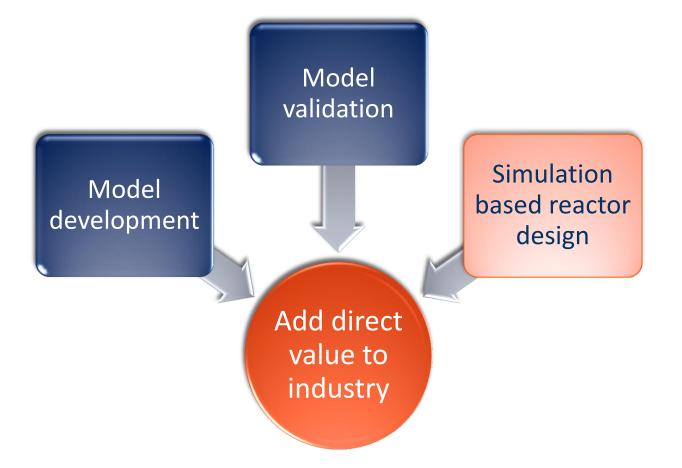
In collaboration with Eindhoven University of Technology
 Appear to be on the right track, but more work needed



- Two variables in this case: temperature and fluidization velocity
- Simulations averaged over 30 seconds



#### **Accelerated development: Big picture**





# **Simulation based reactor design: Principle**

- Develop methods on the assumption of high model fidelity
- Allows for full utilization of the fundamental advantages of simulation based reactor design:
  - Detailed <u>process behaviour</u> under any operating conditions
  - Ideal for <u>optimization</u> over a wide range of operating and design parameters
  - Complete creative freedom for <u>developing novel reactor concepts</u>
- Models will eventually live up to these expectations



#### **Process behaviour: Fluidized bed**

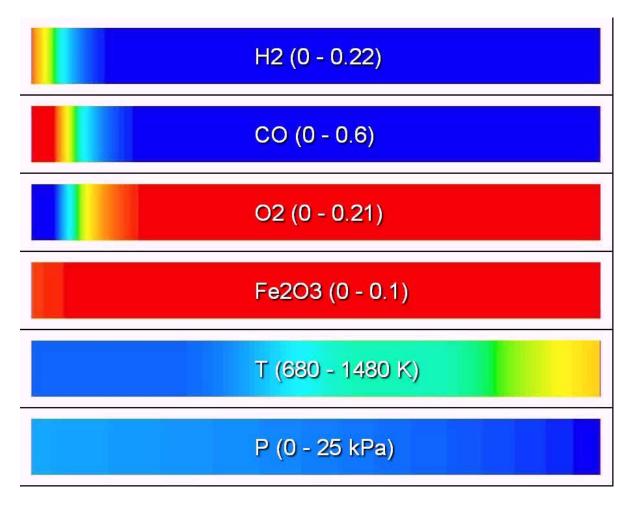
Bubbling bed CLC with periodic gas switching

VF (0 - 0.63)	T (1170 - 1178)	FeO (0 - 0.01)	H2 (0 - 0.21)	CO (0 - 0.61)	H2O (0 - 1)	CO2 (0 - 0.61)	O2 (0 - 0.21)	N2 (0 - 1)
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#### **Process behaviour: Packed bed**

#### Packed bed CLC with periodic gas switching

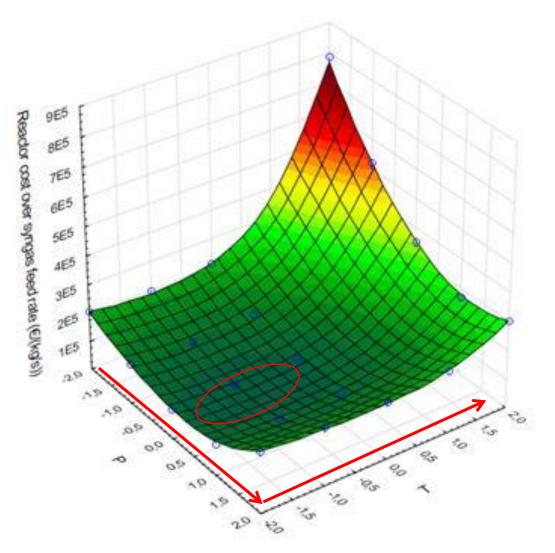




#### **Optimization:** Lowest cost operation

- Simplified example for finding lowest cost reactor P & T
- Challenge: Highly dependent on accurate cost estimates as a function of all independent variables

$$T_{actual} = 900 + 200T$$
$$P_{actual} = 5 \times 2.5^{P}$$





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#### **Conclusions & future work**

- Simulation-based reactor design shows great promise especially for application to second generation CO<sub>2</sub> capture processes
- Dedicated experimental validation is key
- Model development and more widespread utilization will follow swiftly from such campaigns

#### On the horizon for future work:

- Reactive model validation
- Reactive filtering for large scale simulations
- Representative cost-functions for optimization studies
- Increased application to real engineering problems



# Thank you

