

# The Effect of Manufacturing Costs on the profitability of a Gas-to-Liquid Plant

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# Outline

- Introduction
- Process description
- Economical evaluation
- Scenario generation
- Sensitivity analysis
- Conclusions

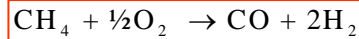
# Introduction

In the last decades, the conversion of natural gas to liquid fuels through the GTL technology, has shown to be an excellent alternative for the use of natural gas.

A typical GTL plant consists of three main units: 1) Syngas production unit, 2) Fischer-Tropsch synthesis unit, and 3) Upgrading unit.

We modelled a typical GTL plant using “UNISIM DESIGN” and performed an economical optimization to determine the optimal equipment sizes, operating conditions, and so on.

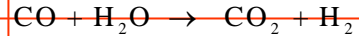
# Process description



(Partial oxidation, -71 kJ/mol)



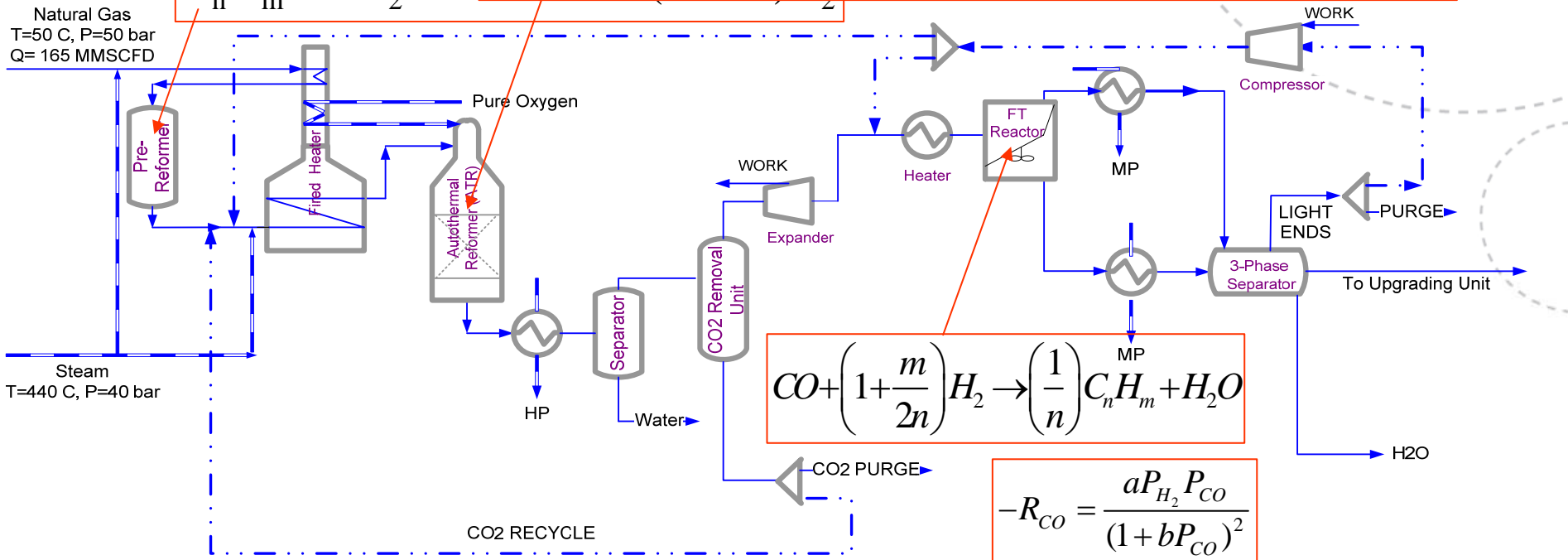
(steam methane reforming, +206 kJ/mol)



(water-gas-shift, -41 kJ/mol)



(dry reforming, +247 kJ/mol)



# Economical evaluation

## 1. Capital Cost Estimation

$$\log C_0 = K_1 + K_2 \log(A) + K_3 \log(A)^2$$

$C_0$  : Purchasing cost for base conditions

$K_1, K_2, K_3$  : Constants

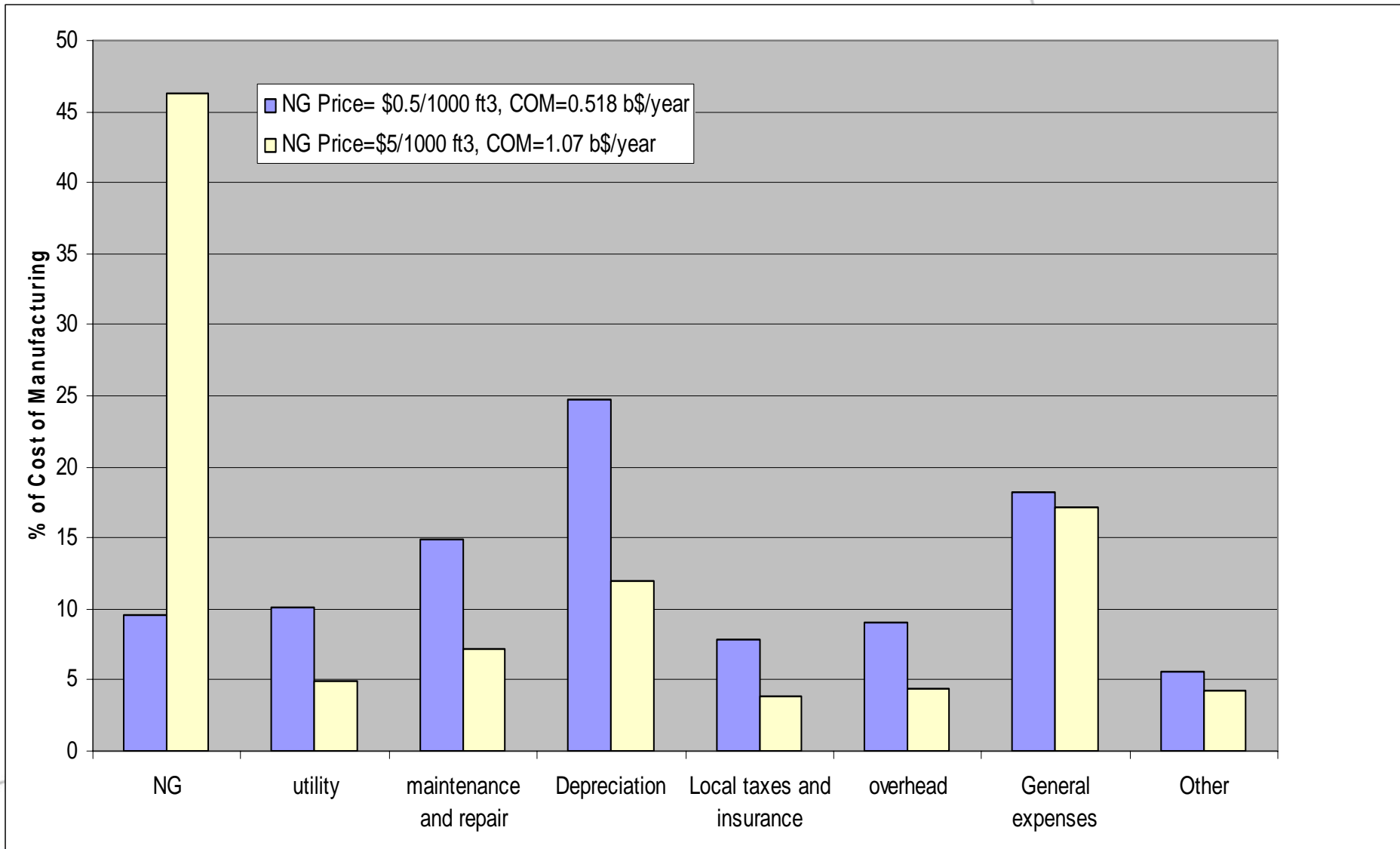
$A$  : Capacity

$$C_{BM} = C_p^0 F_{BM}$$

## 2. Estimation of Manufacturing costs

Cost item	Values used in simulation
<b>1. Direct Costs</b>	
A. Raw materials ( $C_{RM}$ )	
B. Waste treatment ( $C_{WT}$ )	
C. Utilities ( $C_{UT}$ ) <ul style="list-style-type: none"> <li>Fuel gas, oil, and/or coal</li> <li>Electric power</li> <li>Steam (all pressures)</li> <li>Process water</li> <li>Etc.</li> </ul>	
D. Operating labor	$C_{OL}$
E. Direct supervisory and clerical labor	$0.18 C_{OL}$
F. Maintenance and repair	$0.06 FCI$
G. Operating supplies	$0.009 FCI$
H. Laboratory Charges	$0.15 C_{OL}$
I. Patents and royalties	$0.03 COM$
<b>Total Direct Manufacturing Costs</b>	<b><math>C_{RM}+C_{WT}+C_{UT}+1.33C_{OL}+0.03 COM+0.069 FCI</math></b>
<b>2. Fixed Costs</b>	
A. Depreciation	$0.1 FCI$
B. Local taxes and insurance	$0.032 FCI$
C. Plant Overhead costs	$0.708 C_{OL}+0.036 FCI$
<b>Total Fixed Manufacturing Costs</b>	<b><math>0.708 C_{OL}+0.168 FCI</math></b>
<b>3. General Expenses</b>	
A. Administration costs	$0.177 C_{OL}+0.009 FCI$
B. Distribution and selling costs	$0.11 COM$
C. Research and development	$0.05 COM$
<b>Total General Manufacturing Costs</b>	<b><math>0.177 C_{OL}+0.009 FCI+0.16 COM</math></b>

$$COM=0.3037 FCI+2.73 C_{OL}+1.23 (C_{UT}+C_{WT}+C_{RM})$$



The objective function is established as follow:

$$\text{Profit} = \text{Incomes} - \text{Cost Of Manufacturing}$$

And then this objective function has to be maximized to identify the optimal mode of operation for the plant.

$$\text{Pay Back Time} = \frac{\text{fixed capital investment} + \text{start up cost}}{\text{profit after tax}}$$



# Optimization results

For a 17000 bbl/day GTL plant we have the following results:

ATR inlet T (C)	700
Oxygen to Carbon ratio	0.55
Steam to Carbon ratio	0.5
ATR outlet T (C)	1050
CO <sub>2</sub> removed (kmole/hr)	1300
FT reactor volume (m <sup>3</sup> )	2000
FCI (billion \$)	1.282

- **Product Distribution**

LPG (C3,C4)	21.22 %
Gasoline (C5-C8)	39.07 %
Naphtha (C9, C10)	11.45 %
Kerosene (C11-C13)	11.16 %
Gas oil (C14-C20)	11.69 %
Fuel Oil (C20+)	5.37 %

- **Carbon efficiency**

**Case A) GTL plant without CO<sub>2</sub> removal unit**

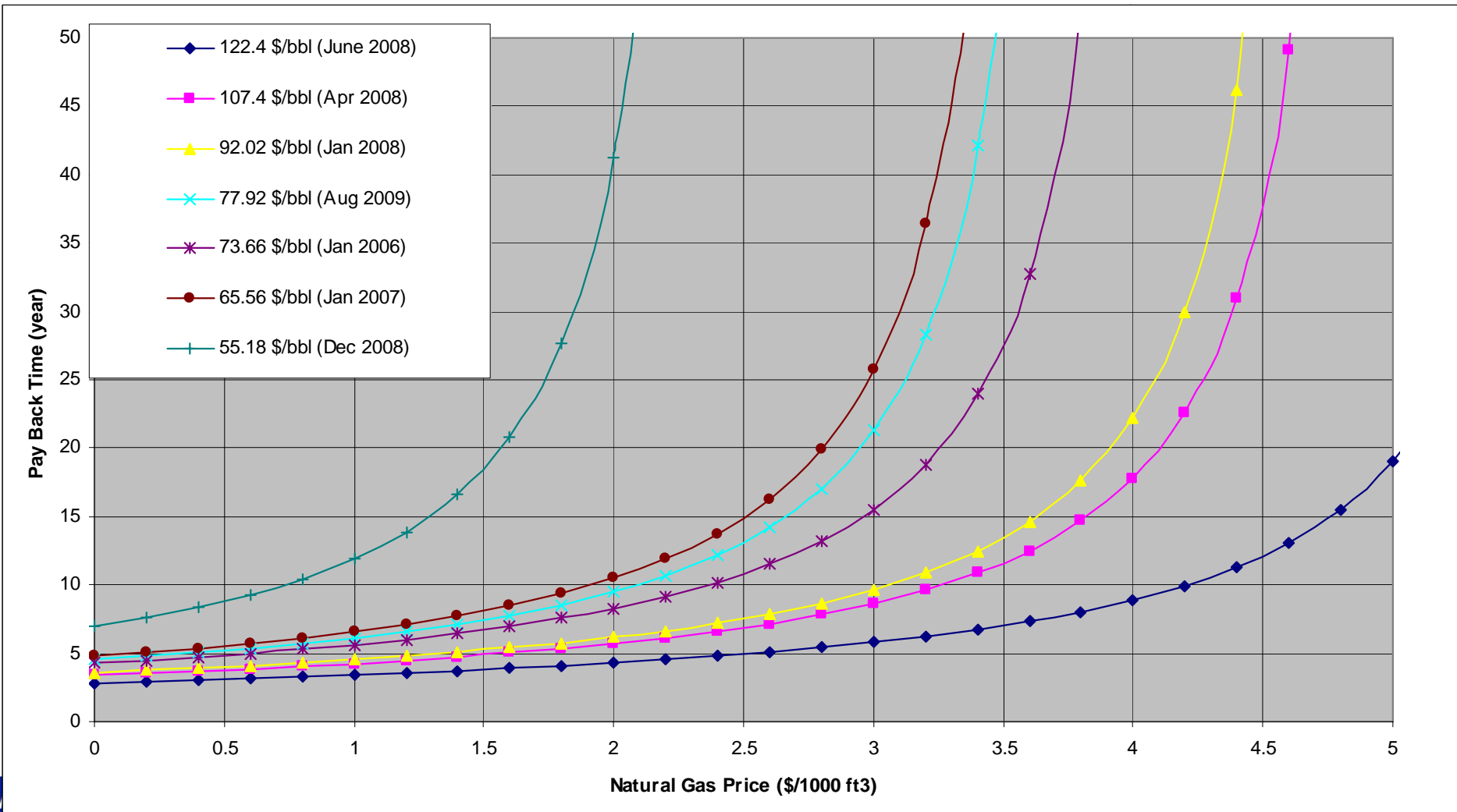
Carbon Efficiency	53 %
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**Case B) GTL plant with CO<sub>2</sub> removal unit**

Carbon Efficiency	65 %
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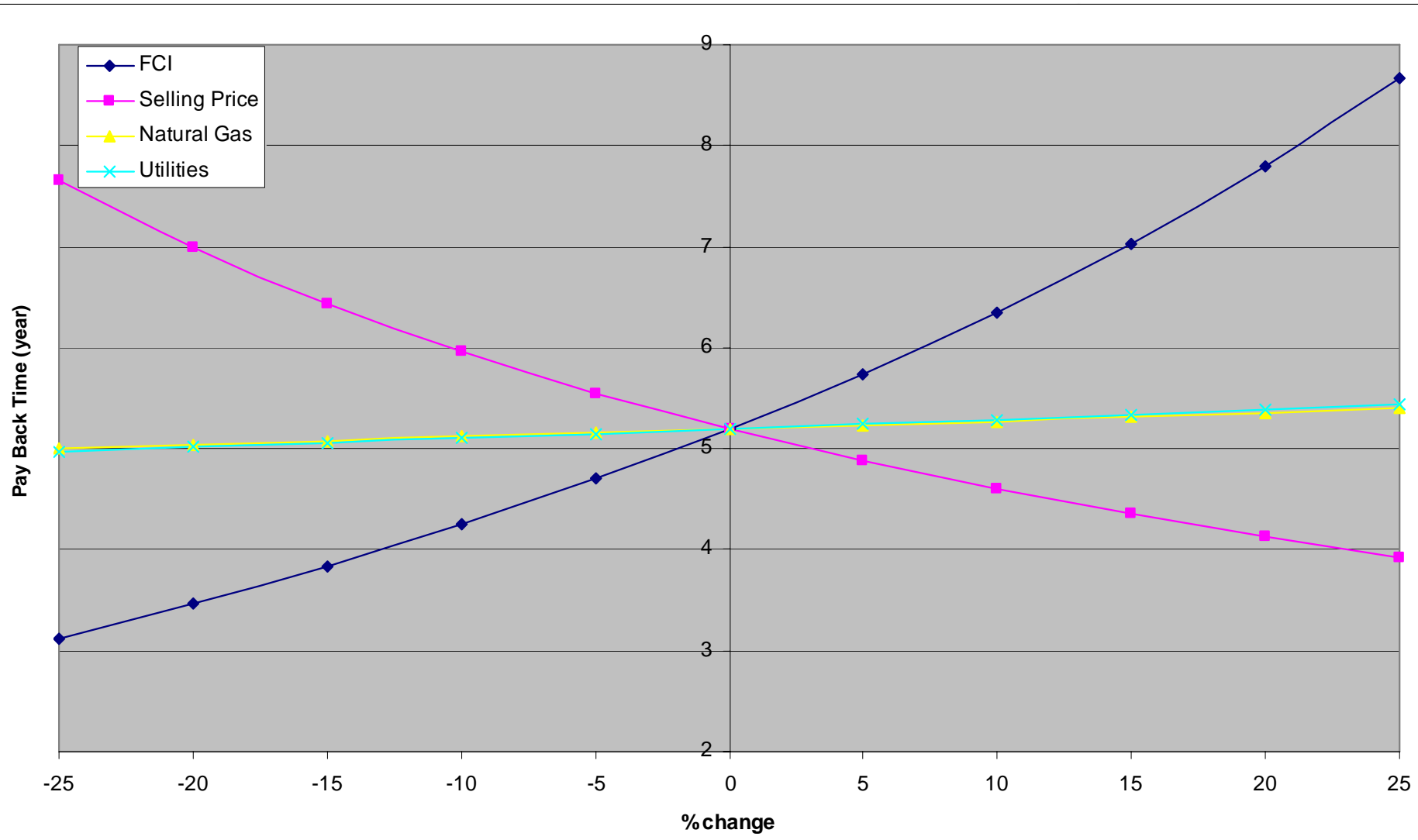
# Scenario Generation

**Objective:** Investigating the effect of “natural gas price” and “product selling price” on the “pay back time”:



# Sensitivity Analysis

FCI= 1.282 b\$, NG Price=0.5 \$/1000 ft<sup>3</sup> ,Product Selling Price= 77.92 \$/bbl



# Conclusions

1. Optimization results show that removing CO<sub>2</sub> from the synthesis gas increases the carbon efficiency of system.

For a cheap natural gas:

2. Pay back time ranges from 3 to 8 years.
3. Sensitivity analysis implies that pay back time is more sensitive to FCI and product selling price rather than natural gas price.

# Thank you for your attention