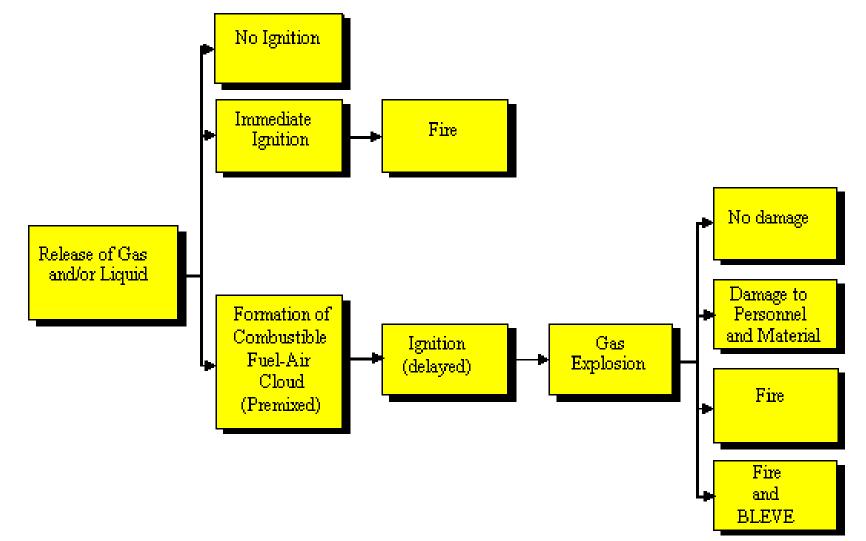
### Hydrogen Safety Basics

Kees van Wingerden



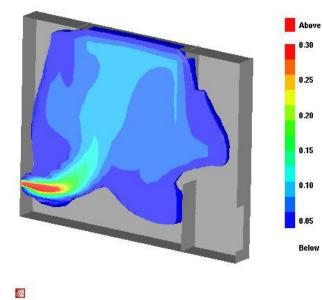
# General course of events involving release of flammable gas or liquid

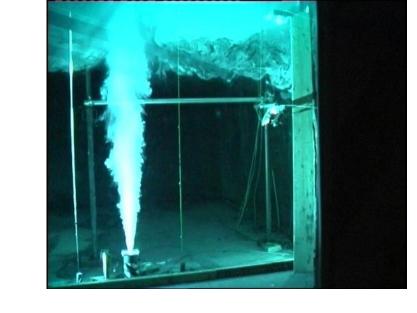


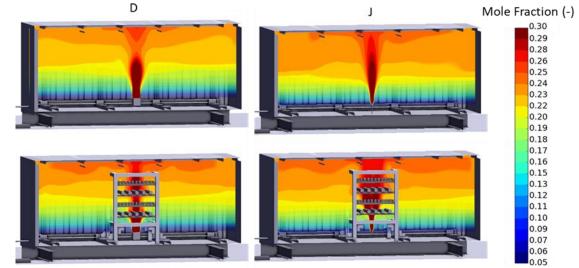
**GEXCON** 

### Hydrogen leaks

Hydrogen has a low density causing it to disperse upwards and generate flammable gas layers against the ceiling





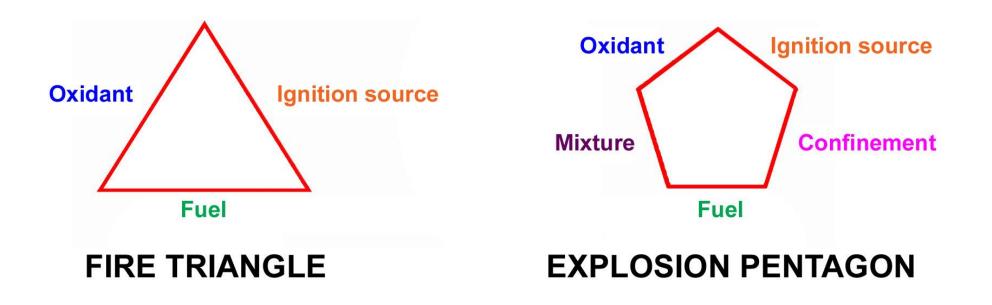


### **GEXCON**



4

#### Fire triangle and explosion pentagon

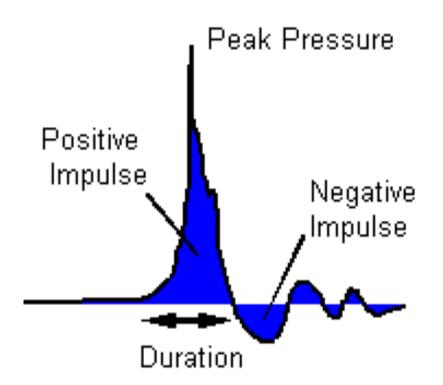




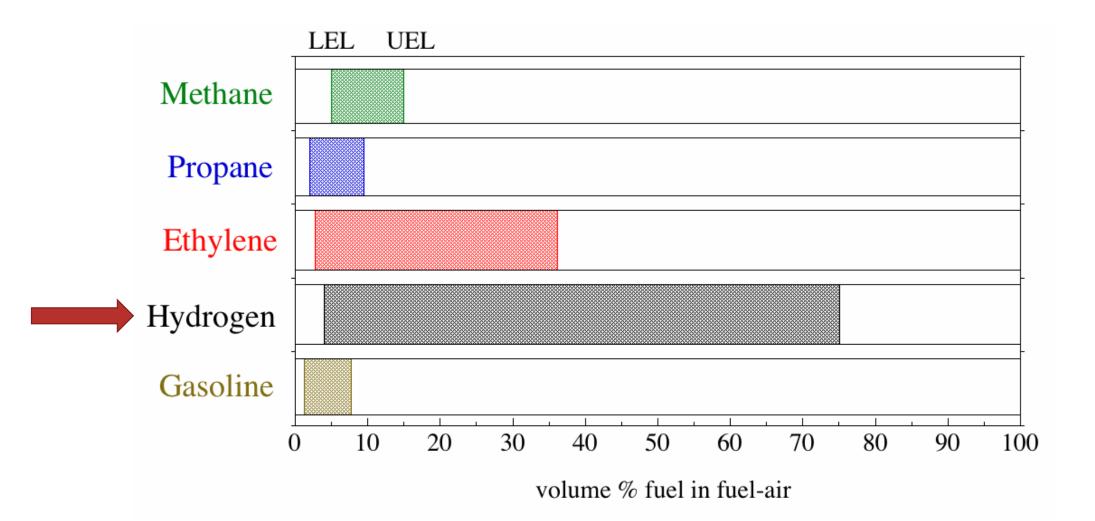
5

### **Definition explosion**

"An explosion is a chemical process which causes a very fast and considerable pressure increase"

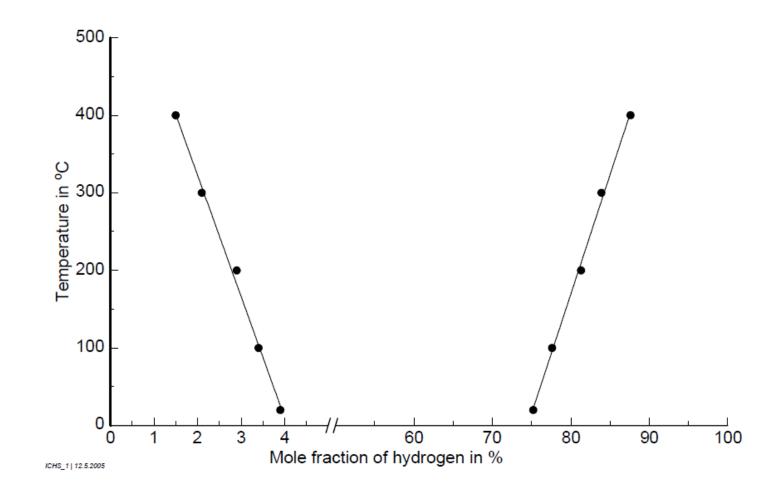


### **Explosive part of cloud**



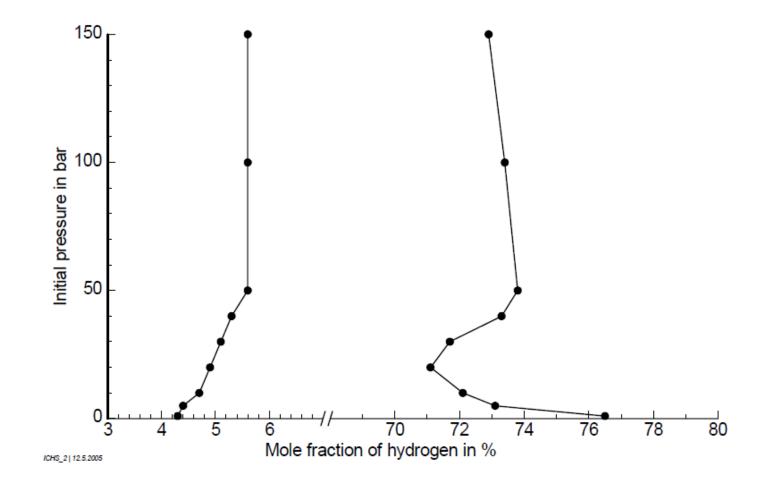


### Effect of temperature on explosion limits hydrogen





### Effect of pressure on explosion limits hydrogen

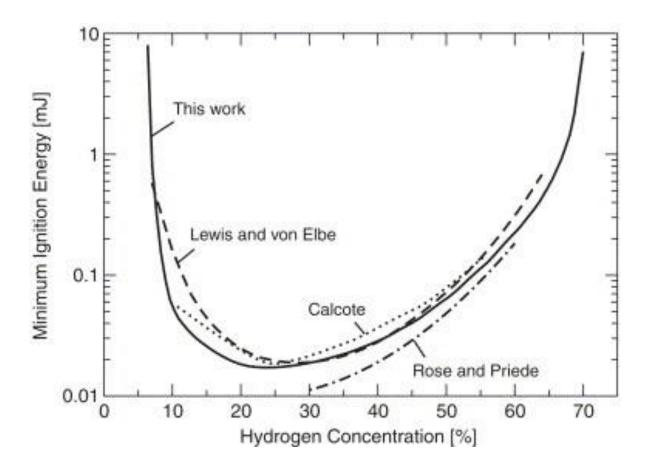




mJ

mJ

### Minimum ignition energy (electric spark)



Acetone	1.15 mJ
Methane	0.28 mJ
Butane	0.26 mJ
Ethylene	0.07 mJ
Acetylene	0.017 mJ
Hydrogen	0.011 - 0.017
Carbon disulphide	0.009 - 0.015

•

.

### **Auto-ignition temperature (hot surfaces)**

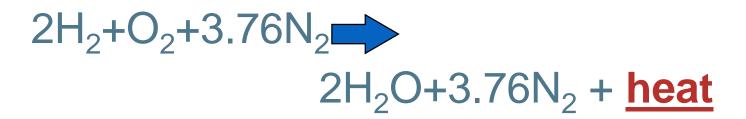


- The lowest temperature of a hot surface at which a mixture of fuel and air can ignite
  - Hydrogen 580 °C
    Methane 537 °C
    Propane 493 °C
    Acetone 535 °C
    Ethanol 363 °C
    Petrol ca 250 °C
    Diesel ca 220 °C





Simplified equation:

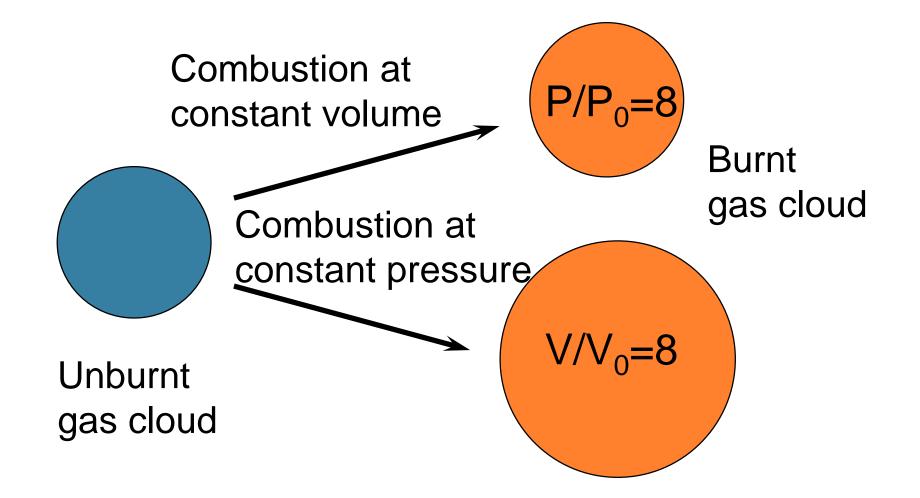


In reality: ≈57 reactions, 268 species equations

Product composition depends on mixture, temperature, pressure

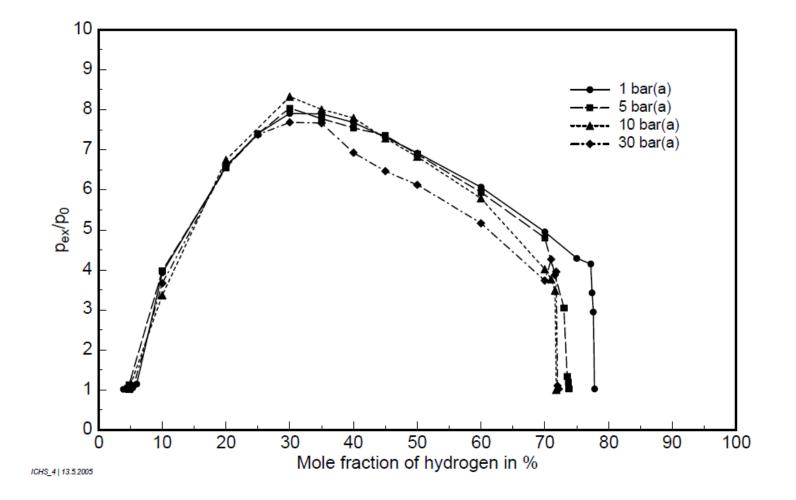


#### **Combustion at constant pressure and volume**





### **Closed vessel explosion: maximum explosion pressure**





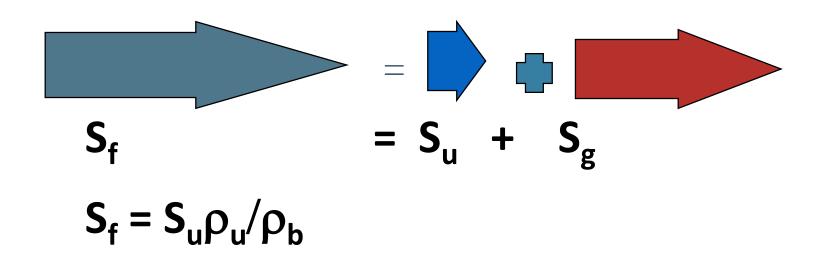
14

### Flame propagation and acceleration mechanisms

- Laminar combustion
- Flame instabilities
- Explosion generated turbulence dominated flame propagation
- Deflagration-Detonation-Transition (DDT), Detonation
- Detonation

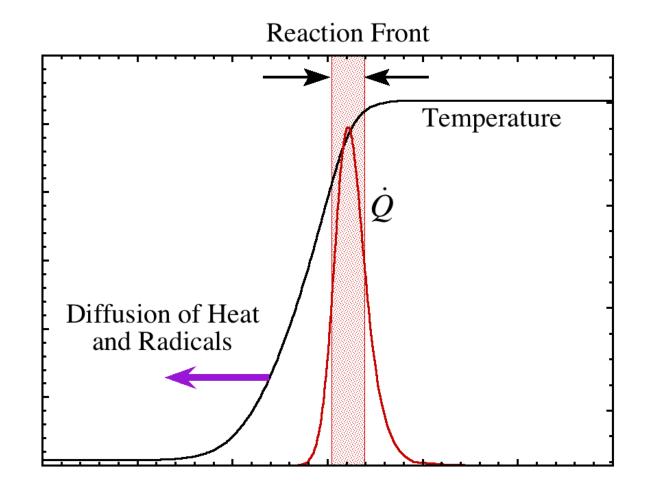
### Laminar flame propagation

- Slow process (dominated by diffusion)
- Typical velocities (burning velocities): 0.5 m/s
- Expansion velocity: total velocity becomes: 3-4 m/s



**GEXCON** 

### Laminar flame propagation



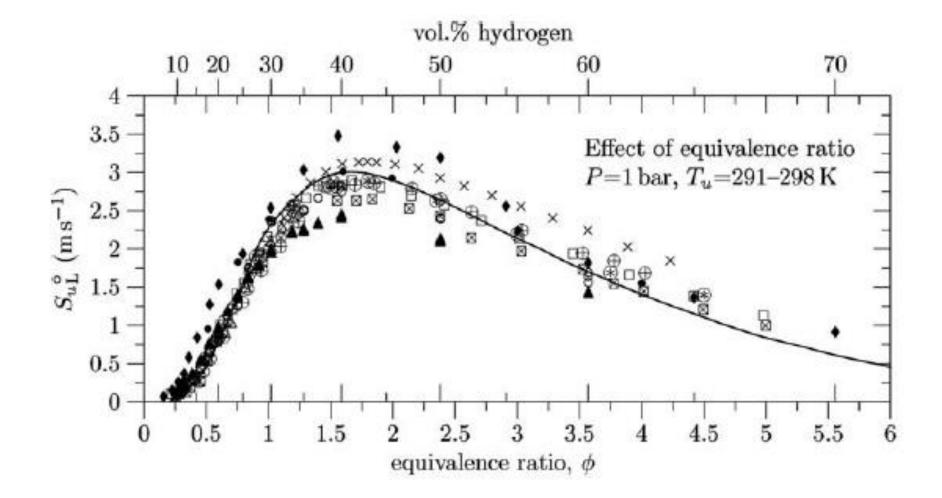
Distance



### Laminar combustion

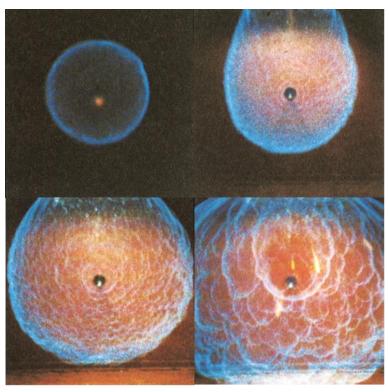
- Typical laminar burning velocities
  - methane: 0.40 m/s
  - propane: 0.46 m/s
  - ethylene: 0.75 m/s
  - acetylene: 1.55 m/s
  - hydrogen: 3.25 m/s
- Expansion ratio typically 7-10 ( $a=n_2T_2/n_1T_1$ )

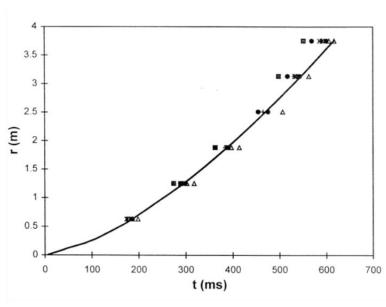
### Laminar burning velocity



### **Flame instabilities**

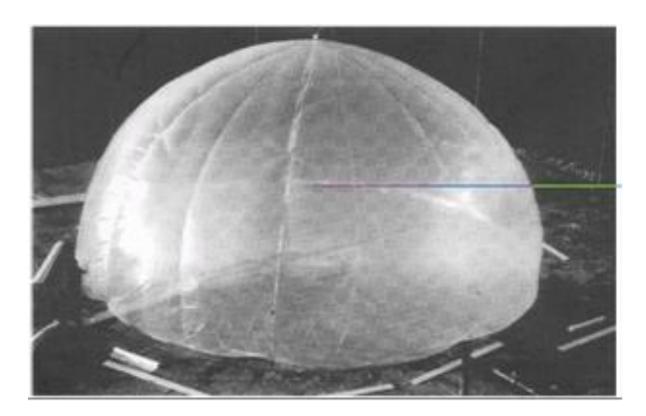
- Flame instabilities will cause laminar flames to accelerate, especially due to increase of flame area
- Example:
  - Intrinsic instability





Methane-air

### **Intrinsic flame instabilities: DDT?**



Ignition of optimal hydrogen-air mixture in 20m diameter balloon (Fh-ICT, 1982) resulted in max. 60 mbar overpressure

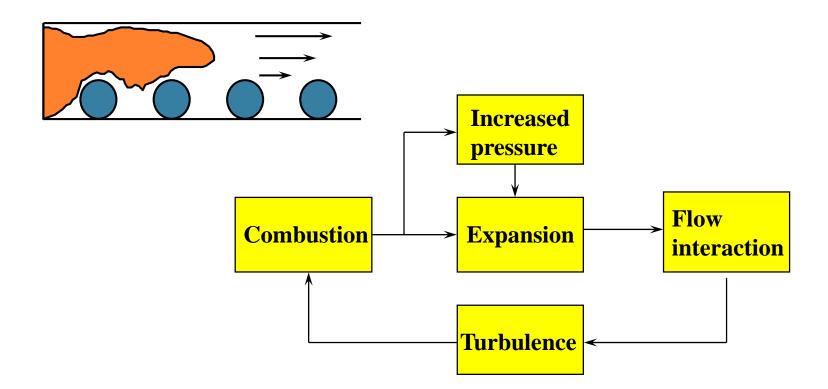


#### **Turbulent combustion**

- Turbulence causes an increase of burning velocities due to mixing of combustion products and reactants and due to an increase of the flame surface area
- Flame speeds (expansion + combustion) can vary from 5-600 m/s

## **Explosion generated turbulence**

• Positive feedback mechanism of explosion generated flow and combustion



**GEXCON** 

### **Explosion generated turbulence**

 Positive feedback mechanism of explosion generated flow and combustion









### High congestion inside module



### 12 vol.% hydrogen, high congestion





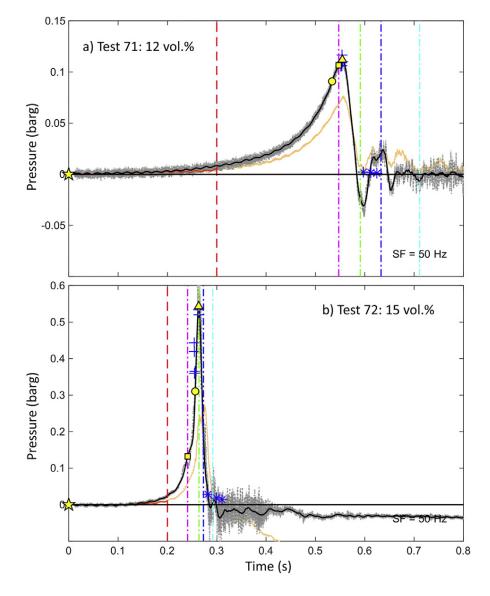
### 15 vol.% hydrogen, high congestion







### **Comparison pressure-time histories**





### **Ignition sources**

- Electrostatics
- Frictional heat and sparks
- Spontaneous ignition



#### **Different electrostatic discharges**

- Electrostatic sparks
- Corona discharge
- Brush discharge

### **Electrostatic sparks**

- Discharge occurs between two electrically conducting materials
- "All" available energy is discharged
- Yield sparks having high energy-content
- Energy can be calculated from capacitance and potential difference (E =  $\frac{1}{2}$  CV<sup>2</sup>), in practice max 1 J
- Can be avoided by grounding and bonding of equipment to same electrical potential

### **Theoretical spark energy**



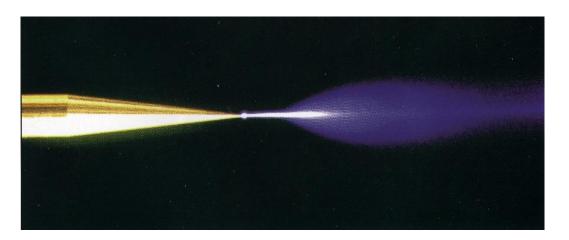
 $E = \frac{1}{2} CV^2$ 

C = capacitance and V = voltage

Object	Capacitance (pF)		1/2 CV <sup>2</sup> (mJ) at various voltages	
		10 kV	20 kV	30 kV
Single screw	1	0.05	0.2	0.45
Flange (100 mm nominal size)	10	0.5	2	4.5
Shovel	20	1	4	9
Small container (bucket, 50 litres	10-100	0.5-5	2-20	4.5-45
drum)				
Funnel	10-100	0.5-5	2-20	4.5-45
Drum (~200 litres)	100-300	5-15	20-60	45-135
Person	100-300	5-15	20-60	45-135
Major plant items (large containers,	100-1000	5-50	20-200	45-450
reaction vessels)				
Road tanker	1000	50	200	450

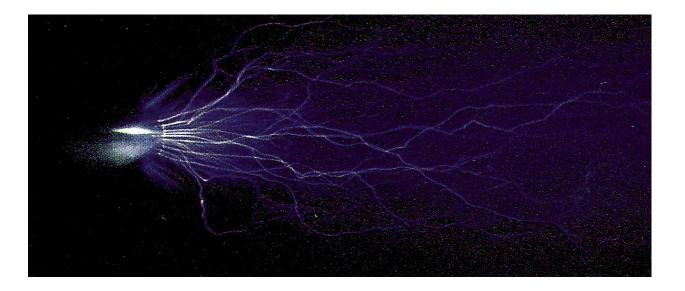
### **Corona discharge**

- Occur when sharp/pointed conducting materials approach charged non-conducting materials
- Low energy-content
- Can lead to ignition of very ignition-sensitive gases like acetylene and hydrogen
- NOT able to ignite methane/propane



### **Brush discharge**

- Usually occurs when rounded conducting materials
  approach charged non-conducting materials
- Only a limited part of the available energy is discharged
- Energy-content < 4 mJ</li>
- Can ignite hydrocarbon gases and vapours



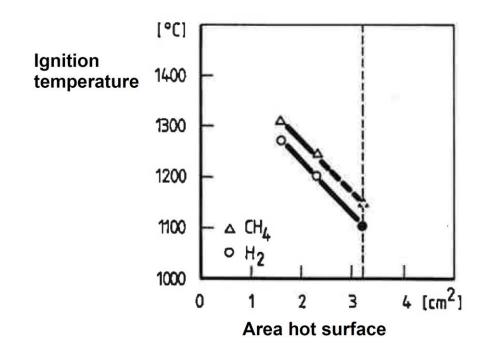


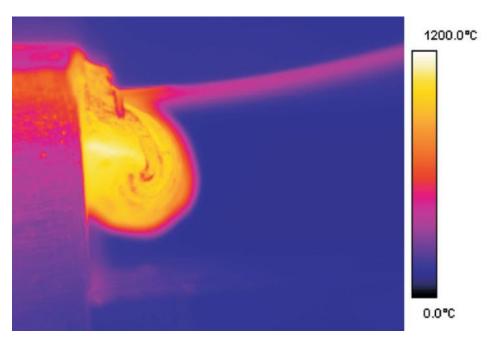
## Electrostatic discharges, summary

Type of discharge	Incendivity		
	Hydrogen MIE = 0.017 mJ	Solvents, hydrocarbon gases MIE > 0.025 mJ	
Electrostatic spark	+	+	
Brush discharge	+	+	
Corona discharge	+	-	

### GEXCON Ignition temperature of hot surfaces: influence of geometry (surface area)

• Large surface area and high temperature is more dangerous than a small surface with lower temperature

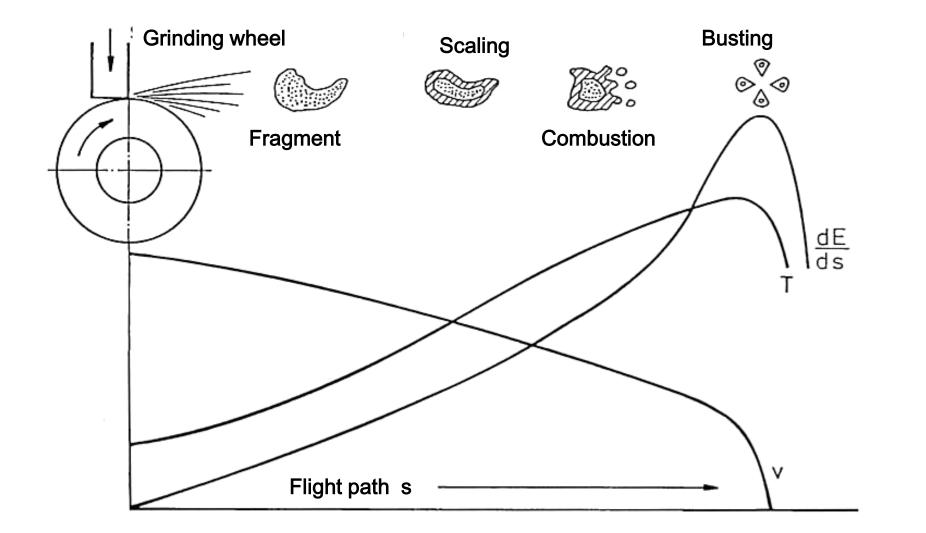




Hot burr formed on the trailing edge of a contact zone

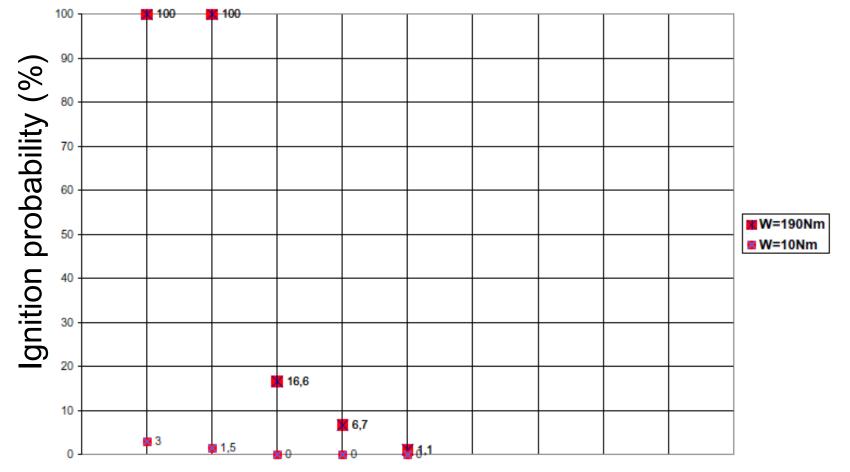
### Phenomenology

### **GEXCON**



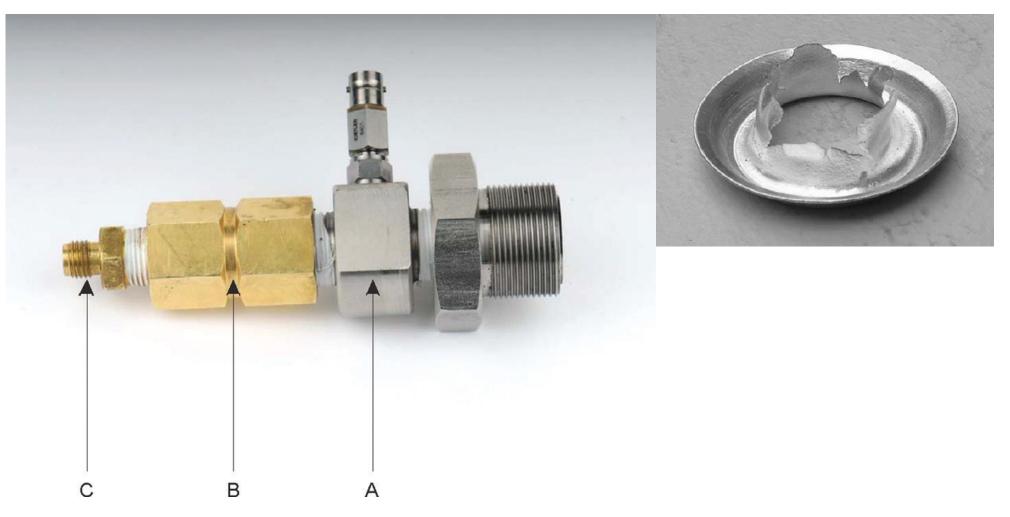
### Incendivity single impact sparks (steel-steel)





Acetylene Hydrogen Ethylene Propane Methane

### Spontaneous ignition: Experiments by HSL (Hooker et al., 2011)

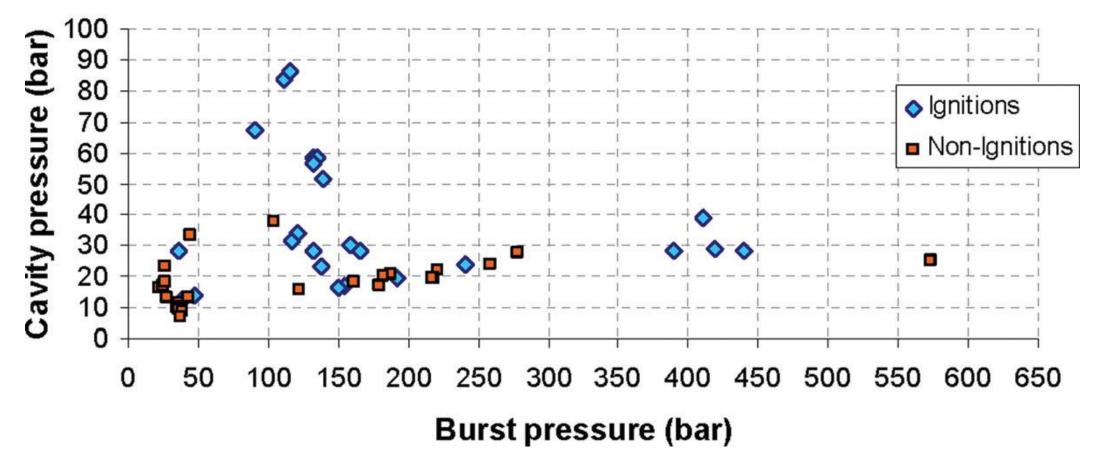


ID = 18.3 mm Length > 300 mm **GEXCON** 



### **Conditions resulting in ignition/no ignition**

### Cavity pressure against burst pressure

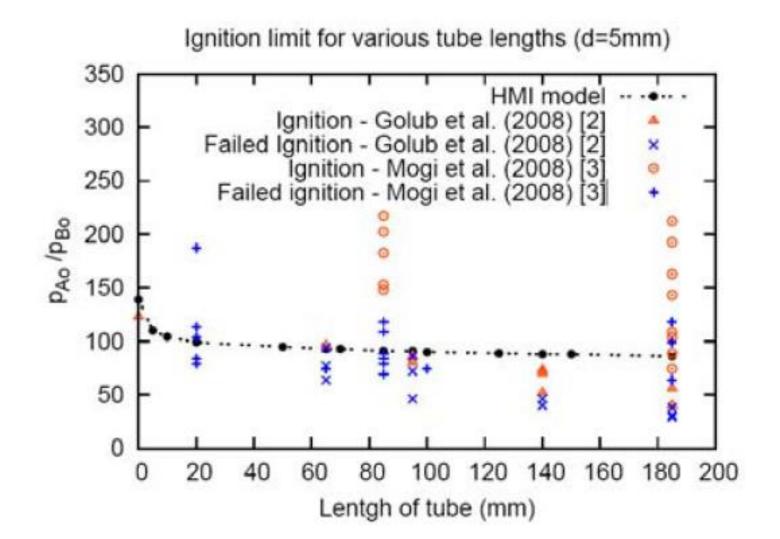




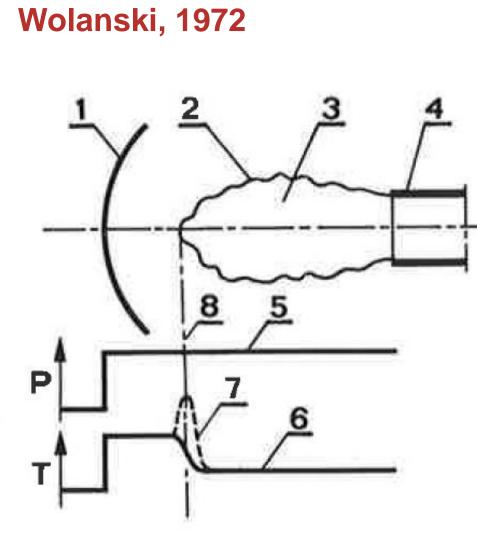
### Findings

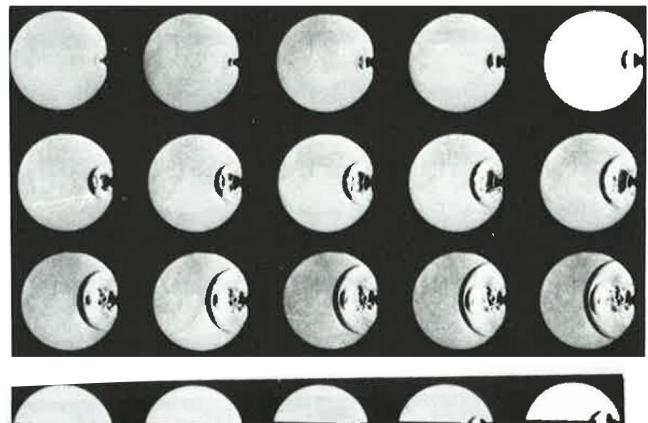
- With no fittings to restrict or reflect the flow, there was no ignition up to 831 barg
- The lowest disc burst pressure at which an ignition was obtained was 35.5 bar

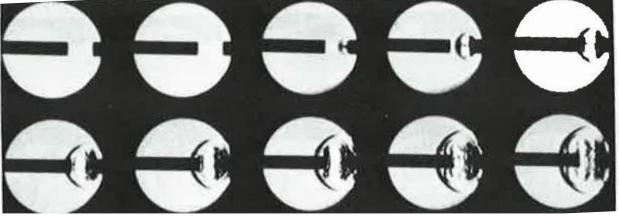
### Maxwell, 2009











### Conclusions

- Light gas: reducing likelihood of generating large gas clouds in the open (unless liquified)
- Wide explosive range
- High reaction rate
- Easy to ignite by electrostatic sparks/discharges
- Relatively easy to ignite by mechancial sparks
- Less easy to ignite by hot surfaces
- «Spontaneous ignition» only possible in case of presence of obstructions in vicinity of leak position



Thank you very much for your attention

kees@gexcon.com













**Visiting Address** Fantoftvegen 38 NO-5072 Bergen Norway

**Postal Address** P.O. Box 6015 NO-5892 Bergen Norway

Gexcon.cor