



**NTNU**  
**Norwegian University of  
Science and Technology**

## **TGTC 2011**

**One step further from detailed experiments to design of heat  
exchangers for natural-gas liquefaction plants**

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# Outline

## Overview

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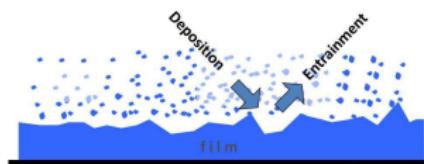
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# Motivation and approach

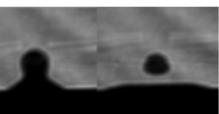
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- Focus: droplet phenomena in LNG processes.
- Importance: heat transfer, robust model.



How do we do it?

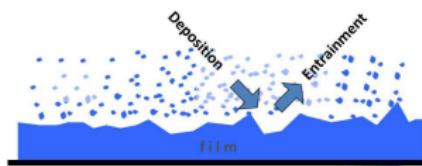
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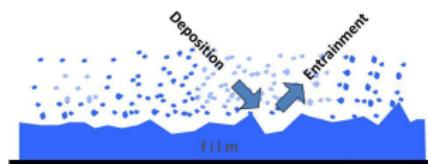
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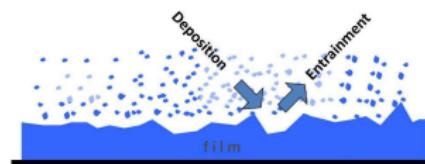
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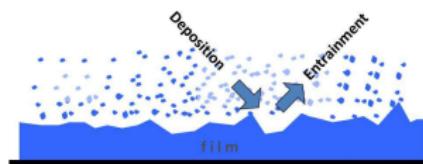
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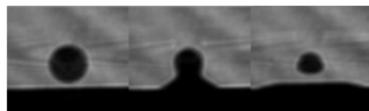
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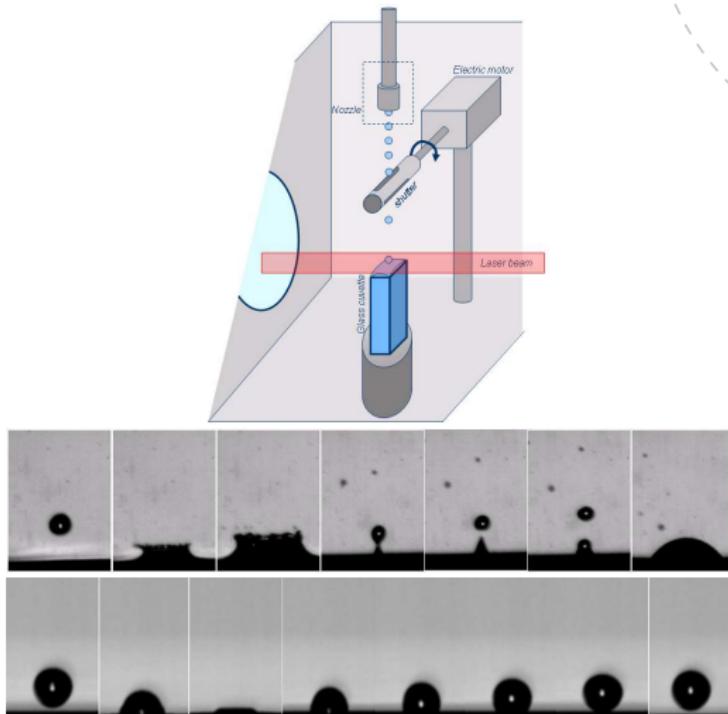
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# What were presented in TGTC 2009?



Droplet impact with a deep pool.

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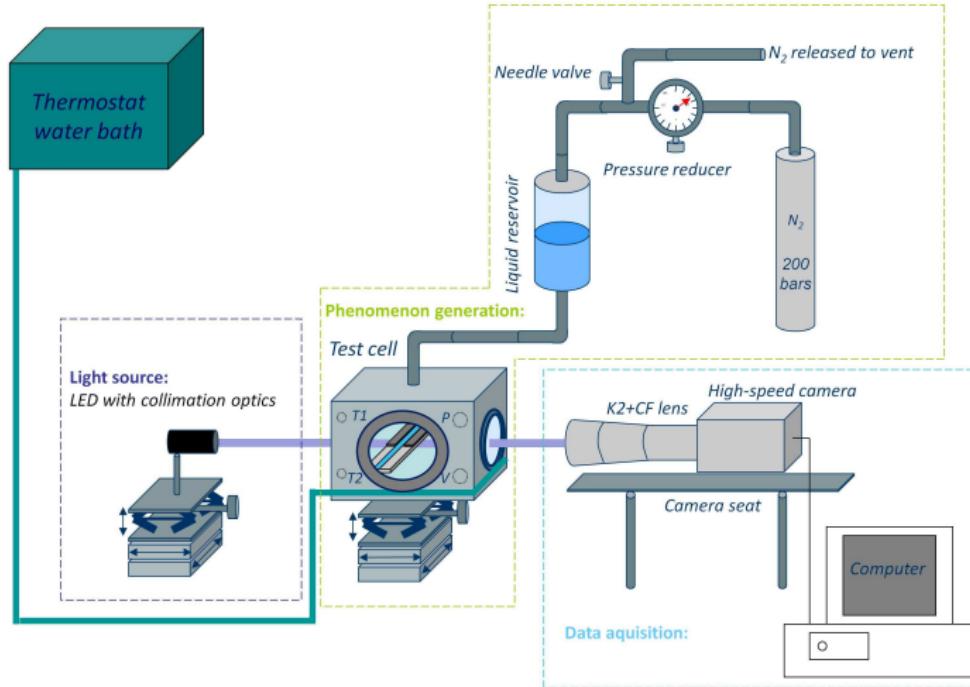
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# Experimental setup



# Material

## Physical properties of the fluids

Fluids	$\rho$ ( kg/m <sup>3</sup> )	$\mu$ ( mPa · s )	$\sigma$ ( mN/m )
Distilled water <sup>a</sup>	996.93	0.890	71.99
n-pentane <sup>b</sup>	605.69	0.1969	13.66

<sup>a</sup> Reference fluid.

<sup>b</sup> Model fluid for MR.

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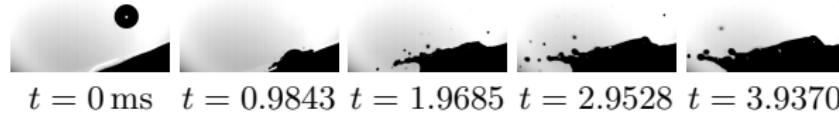
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# Film impact – water splashing 20°

Water droplet ( $D = 1.99 \text{ mm}$ ,  $V = 3.87 \text{ m/s}$ ) falling on a 20° tilted film with a thickness of 0.55 mm and mean velocity of  $\approx 0.20 \text{ m/s}$ .

# Film impact – *n*-pentane splashing 20°

*n*-pentane:  $D = 1.46$ ( mm)  $V = 2.0$ ( m/s). The following image-sequence: water drop splashing.



# Film-impact: jetting

Water droplet ( $D = 2.13 \text{ mm}$ ,  $V = 2.32 \text{ m/s}$ ).

# Film impact: Coalescence

Water droplet ( $D = 0.53 \text{ mm}$ ,  $V = 1.71 \text{ m/s}$ ).

# Bouncing

Water droplet ( $D = 0.28 \text{ mm}$ ,  $V = 1.03 \text{ m/s}$ ), bouncing droplet ( $D = 0.28 \text{ mm}$ ,  
 $V_y = -0.13 \text{ m/s}$ ,  $V = -0.51 \text{ m/s}$ ).

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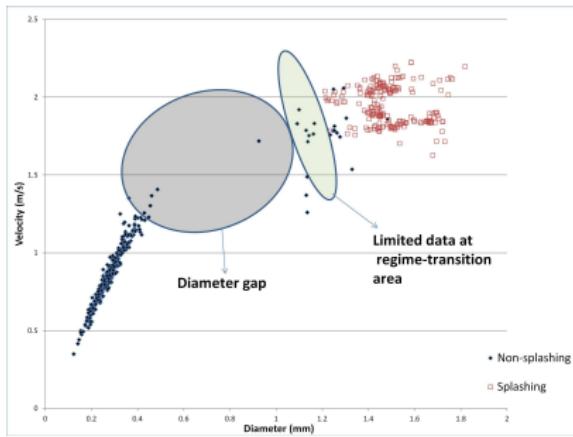
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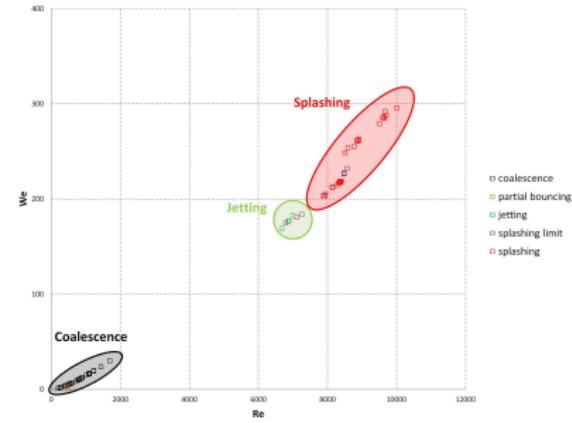
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# Flow regime characterization



V-D for all flow rates and angles.

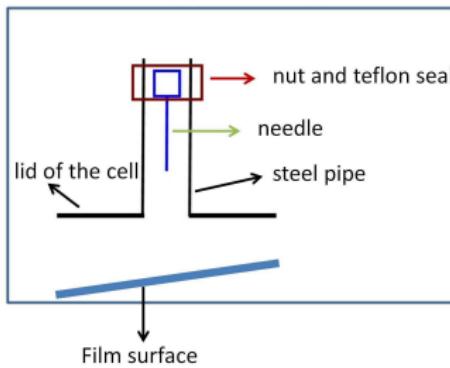


We-Re for film at 2.4 ml/s and 7°.

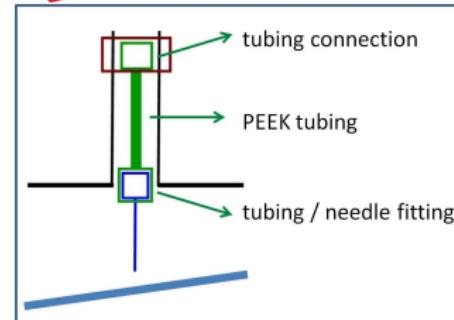
► *Bouncing of n-pentane*

# Dropper setup modification

*Old dropper setup*



*New dropper setup*



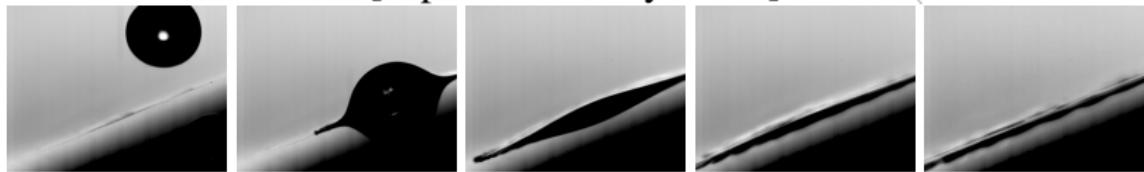
# Film impact – bouncing $7^\circ$

*n*-pentane:  $D = 0.34(\text{ mm})$   $V = 0.75(\text{ m/s})$   $V_b = 0.28(\text{ m/s})$   $V_{by} = 0.20(\text{ m/s})$ .

► *V-D with the old dropper*

# Board impact – deposition dominant

[*n*-pentane on dry board]



$t = 0\text{ ms}$     $t = 0.7748\text{ ms}$     $t = 1.5496\text{ ms}$     $t = 2.3244\text{ ms}$     $t = 3.0992\text{ ms}$

[water on dry board]



$t = 0\text{ ms}$     $t = 0.7748\text{ ms}$     $t = 1.5496\text{ ms}$     $t = 2.3244\text{ ms}$     $t = 3.0992\text{ ms}$

**Figure:** Similar droplet parameters:  $D = 1.7\text{--}2.0\text{ mm}$ ,  $V = 2.0\text{ m/s}$  impinging on a dry board at  $20^\circ$ .

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## Conclusion

- A well-functioning setup.
- Different flow regimes identified.
- Low-inertia impact possible for *n*-pentane.

## Future work

- Finishing low-inertia impact for *n*-pentane.
- Flow regime diagram and threshold model.

## Acknowledgement

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The Research Council  
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**Thank you for your attention!**