

mechanical integrity of PFHE in LNG liquefaction process

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temperature, boiling flow, thermal stresses

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multi-domain simulation problem

- component mixtures
- vapor pressure
- multiphase flow*
- boiling flows
- heat exchange*
- flow pulsations*
- mechanical integrity*
- thermal stresses

* core expertise of the Fluid Dynamics group at TNO in Delft

knowledge investment programme at TNO, to cover all aspects of boiling heat exchanger



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Generic LNG liquefaction in PFHE





simulation of the heat flows, with fixed composition

Heat transfer: conductivity

- Fluid: limited effects in bulk, boundary effects important
- Wall: complex processes, flow related, boiling
- Aluminum: plate, fin, and axial losses

Heat transfer: capacity

• Fluid: latent heat of boiling, effect of gas density





- nucleating boiling ($\Delta T \sim 10 20K$, avoid film boiling)
- low pressure $P < P_c$ for boiling flow (Mostinski rule)
- homogenous flow and fluid temperature (no cracks or corners)

various forms of instabilities in boiling

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from nucleation, with noise, via cavitation, possible with film flow or convection cells, to bubble and slug flows

Mechanical model, unit cell

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- Brazing material as well as the material of the total structure is aluminum alloy
- There is no prestress at the brazing regions
- Mechanical properties do not depend on temperature





Effective mechanical properties

In order to calculate effective properties of the PFHE, a series of test problems (uniaxial tension and simple shear) have been solved,

as well as a set of equations from the mechanics of composites



The calculated mechanical properties of the effective orthotropic material are:

$$E_x = 2.358 \cdot 10^{10} \text{ Pa} \quad G_{xy} = 2.29 \cdot 10^9 \text{ Pa} \quad \nu_{xy} = 0.23$$

$$E_y = 1.322 \cdot 10^{10} \text{ Pa} \quad G_{yz} = 5.68 \cdot 10^9 \text{ Pa} \quad \nu_{yz} = 0.13$$

$$E_z = 3.263 \cdot 10^{10} \text{ Pa} \quad G_{zx} = 9.63 \cdot 10^9 \text{ Pa} \quad \nu_{zx} = 0.33$$
(1)

Temperature and heat flux profiles in solid part

case 1: Hot-Cold-Hot-Cold $(T_{hot} = -53C, h_{hot} = 1000W/m^2C, P_{hot} = 50bar)$ case 2: Cold-Cold-Hot-Hot $(T_{cold} = -73C, h_{cold} = 4000W/m^2C, P_{cold} = 5bar)$ (2)

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Local stresses with and without internal pressures Case Hot-Cold-Hot-Cold

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Calculation of global deformations





Stress dependencies on design parameters



design and operational margins

- use small channels: higher pressure, but more area, more stable
- avoid sharp corners in design: no local film boiling
- mean temperature gradient smaller than maximum gradients
- hot-end up: stable shutdown
- lower mass flow or increase pressure to avoid film boiling
- mixed refrigerant (i.e. less volatile components) soften boiling

Conclusions

- Complete simulation of LNG liquefaction process
- Temperature profile and stationary operational conditions for the PFHE have been derived.
- Stationary thermal stresses substantial (for constant operation)
- Effective mechanical properties have been calculated
- Geometry of the PFHE can be now optimized to avoid stress concentrations in the brazing region

Outlook and invitation

- Boiling oscillations yield thermal variations and cyclic stresses
- Fatigue due to cyclic stresses likely with current stress levels and locations
- Variation in design and operation can be treated with the current model, including prestress and manufacturing imperfections
- Looking for industrial partners in validation and optimization phase of the research



temperature profiles indicating different conditions

