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Impact of boiling liquid on fluid-vapor-wall interaction in LNG transfer systems



FLUVAWINT: A project of TNO, Delft University, Bluewater and Gutteling -






Evert van Bokhorst
Project Manager – Fluid and Structural Dynamics





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TNO – Independent contract R&D and Consultancy organization (4300 staff – 7 Themes)



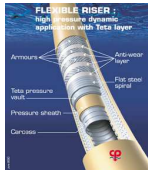
Theme Energy: Fluid & Structural Dynamics

- › Exploration and production optimisation
- › Integrity of gas transport and storage
- › Flow-induced pulsations in flexible risers
- › Pulsation and vibration analysis on process installations










Partner for LNG Development:

- › Cryogenic material behaviour
- › Fluid/structural dynamics in transfer systems and process equipment
- › Measuring and modelling of heat transfer and boil-off
- › Assessing and modelling ship structural integrity
- › Industrial and external safety



FLIBLE RISER :
 High frequency dynamic response with Tota riser
 Armour
 Receiver
 Flat steel spiral
 Total pressure
 Pressure sheath
 Carcass

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Floating LNG requires qualification of components and systems used in LNG transfer


- › Offshore FLNG configurations in STS transfer:
 - › Side-by-Side
 - › Tandem Aerial
 - › Tandem Floating

Production > liquefaction > loading > shipping > offloading > storage > regasification



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Qualification program according EN1474:

EN1474-1: Design and testing of transfer arms
EN1474-2: Design and testing of transfer hoses
EN1474-3: Offshore transfer systems

Technical challenges in risk-based qualification according EN1474-2 is not a simple check list-:

- › EN-1474-2 specifies only the baseline of qualification
- › Complex mechanical behaviour of the multi composite hose
- › Unknown material properties under cryogenic conditions
- › Pressure losses in corrugated hoses
- › Impact of possible two-phase flow (LNG + boil-off gas)
- › Unknown external loads during transfer
- › Definition of allowable levels: vibration, pressure loss, hose permeability

“Not only the test methods need to be developed, but rules need to be interpreted and requirements have to be detailed”.

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Part of the qualification for Gutteling hose: Ambient and Cryogenic LNG Flow Test in straight and STS configuration

- Inlet-, Outlet pressure
- Pressure loss across the hose
- Pulsations at inlet and outlet
- LNG Temperature at inlet and outlet
- Vibrations along the hose
- Temperatures along the hose
- Modal analysis: natural frequencies, mode shapes
- Methane gas permeability

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LNG Flow test shows a considerable variation of pressure loss with the inlet pressure of the hose:

- impact of hose elongation
- impact of profile and roughness
- vortex shedding
- Impact of boil-off gas ?

The graph shows pressure drop per meter (y-axis, 0 to 10 bar/m) versus volume flow (x-axis, 0 to 1500 m³/h). Data series include: test 1 (low pressure), test 2 (high pressure), test 3 (med. pressure), test 4 (low pressure 2), test 5 (H₂O), and a Prediction line. The H₂O test shows the highest pressure drop, reaching approximately 10 bar/m at 1500 m³/h. Other tests show lower pressure drops, generally between 2 and 6 bar/m at 1500 m³/h.




Cryogenic Flow Test

Inlet pressure:

- High 9.0 Bar
- Medium 6.0 Bar
- Low 2.7 Bar

ID = 8"
L = 15.0 m




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Lessons learned:



- › Close cooperation of supplier, certifying authority, possibly the end user and the independent research contractor is recommended because of the non-prescriptive character of the EN1474-2;
- › Specification of the requirements and allowable levels is needed: vibrations, pressure loss, permeability;
- › Combine testing with modelling to reduce amount of testing;
- › Flow tests should be carried out with LNG **over the complete operating envelope** regarding flow rates and pressure range involved in the actual operation;
- › Further fundamental investigation of flow phenomena is recommended to understand impact of internal pressure and boil-off gas on pressure loss and friction coefficient of the hoses;



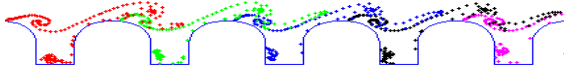
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FLUVAWINT: Impact of boiling liquid on FLUId-VAPor-Wall INTERaction in LNG transfer systems:

- › MIP project 4 years
- › Approved July 2010, started January 2011
- › Participants:
 - › **TNO** project manager: project co-ordination, progress reports to AgentschapNL, knowledge from qualification/experimental work LNG hoses, vortex shedding in corrugated piping (gas risers), test facilities
 - › **Delft University** - Aero and Hydrodynamics -Prof. Westerweel -PhD students: experimental and numerical work, modeling
 - › **Gutteling**: supply of samples, knowledge of product and materials, valorisation, economic perspective
 - › **Bluewater**: knowledge of applications/configurations, valorisation, economic perspective

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<p>Objectives :</p> <ul style="list-style-type: none">› To gain a better understanding of fluid-vapor-wall interaction of a liquid in near boiling conditions› To develop a prediction model for impact of boil-off gas on pressure loss in multi-composite hoses and others› To predict and avoid cavitation (implosion of gas bubbles) by appropriate models			

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<p>Fundamental questions are:</p> <ul style="list-style-type: none">› When do vapour bubbles occur and at which location in corrugated hose or pipe ?› What is the impact of internal corrugation and wall roughness on vapour bubble occurrence ?› What are the physical properties of vapour bubbles, like size, distribution and deformability depending on local flow conditions ?› What is the impact of vapour bubbles on flow resistance ?› What are the local flow conditions to stimulate bubble formation ?			
			

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Project combines numerical and experimental investigation:

- › Observing gas bubbles in wall turbulence (experience obtained from drag reduction experiments for ships and multiphase flow in pipes)
- › Effect of gas bubbles on flow in smooth and corrugated pipes
- › Onset of boiling in flow under depressurized conditions
- › Flow visualisation studies in transparent pipes with inner corrugations similar to LNG hoses
- › Results available as function of:
 - › operating conditions (flow, pressure, temperature, LNG comp.)
 - › hose/pipe geometry (inner diameter, spiral wire diameter, roughness, pitch)
 - › physical properties of gas bubbles (size, distribution, deformation)

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Test loop in a pilot study TUD:

Pressure-gauge

Mass flow controller

Sensor

Pipe

Tank

Water pump

Flow meter

Air injection



Water flow meter

Flow direction


Water pump

V=1 [m/s]

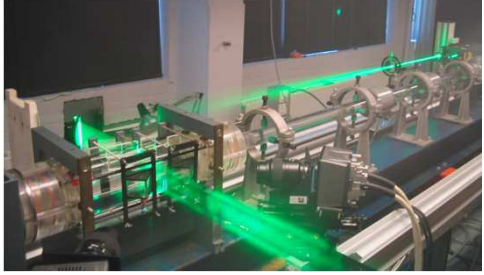
V=1.5 [m/s]

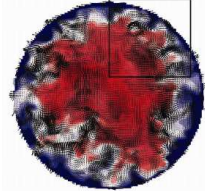



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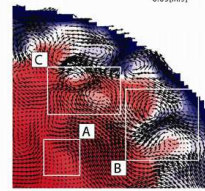


High speed stereoscopic PIV system at test section to visualize flow structures








Instantaneous flow field at $Re_m = 20,000$
(only every second vector is displayed)



Close-up of the highlighted flow field
(every vector displayed)

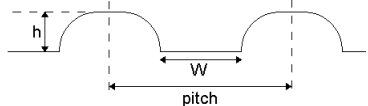



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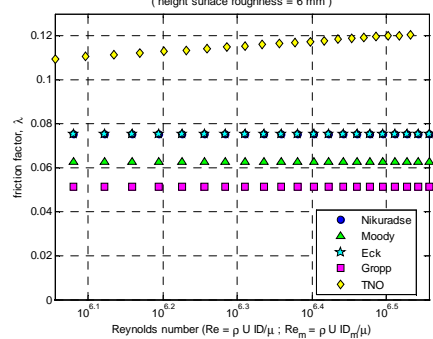
State of the art: friction factor versus Reynolds number for corrugated piping/hoses based on models:

Impact of hose profile/surface roughness



1. Nikuradse:
 $\lambda = 1 / (2.1 \log(ID_m / h) + 1.14)^2$
2. Moody:
 $\lambda = 0.0055 + 0.15 (h / ID_m)^{0.5}$
3. Eck:
 $\lambda = 0.25 / (\log(3.71 \cdot ID_m / h))^2$
4. Gropp:
 $\lambda = 0.25 / (\log(f_p \cdot \sqrt{ID_m \cdot pitch / h \cdot W}))^2$

Friction factor as function of Reynolds number
(height surface roughness = 6 mm)



5. TNO:
 $\lambda = p_1 \cdot \log(RE) - p_2$
 $p_1 = F(f)$ and $p_2 = F(f, \alpha, \beta)$
 $f, \alpha, \beta = F(\text{geometry})$

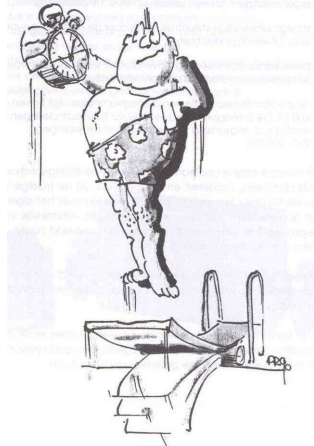
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Thanks for your attention
Questions?



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