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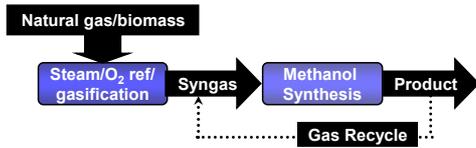
# Characterization and Performance of Pd/CeO<sub>2</sub> Catalysts as a Powder in Fixed-bed Reactor and as a Coating in a Stacked Foil Microreactor for the Methanol Synthesis

Xuyen Kim Phan<sup>1</sup>, John Walmsley<sup>2</sup>, Hamidreza Bakhtiary-Davijany<sup>1</sup>, Rune Myrstad<sup>2</sup>, Peter Pfeifer<sup>3</sup>, Anders Holmen<sup>1</sup> and Hilde J. Venvik<sup>1</sup>

1. Department of Chemical Engineering, Norwegian University of Science and Technology (NTNU), Sem Sælands vei 4, N-7491, Trondheim, Norway
2. SINTEF Materials and Chemistry, Sem Sælands vei 2A, N-7465 Trondheim, Norway
3. Karlsruhe Institute of Technology, Institute for Micro Process Engineering, D-76344 Eggenstein-Leopoldshafen, Germany

## Introduction

### Solution for Remote Natural Gas Fields or Biofuels?



Microstructured reactors have recently been proposed as alternatives to the conventional reactor technology in compact applications due to their heat and mass transfer properties

### Objectives

- Explore the properties of Pd-based catalyst coatings for methanol synthesis in microstructured reactors
  - Reaction mechanism over Pd to facilitate unconventional synthesis gas [1]
  - High activity potential with particular supports [2] ?

## Experiments

### Reactors and reaction conditions

- 14 structured and coated foils stacked and sealed inside alloy 800 housing graphite (Frentzelit) [4]



Figure 1: The stacked foil microreactor (SFMR) under operation (a), opened (b).

- SS tube fixed-bed reactor (FBR,  $\Phi=10\text{mm}$ ).
- Reduction at 1 bar and 300 °C in 10 vol.% H<sub>2</sub> in N<sub>2</sub>.
- Methanol synthesis at 220-350 °C and 80 bar (H<sub>2</sub>/CO/CO<sub>2</sub>/N<sub>2</sub> = 65/25/5/5).

### Preparation of Pd/CeO<sub>2</sub> catalysts:

- 10 wt% Pd/CeO<sub>2</sub> foil coatings:
  - CeO<sub>2</sub> sol-gel prepared from cerium ammonium nitrate<sup>2</sup>,
  - CeO<sub>2</sub> sol-gel dripped uniformly over microchannels, followed by drying (70 °C, overnight) and calcination (500 °C, 5 h, air).
  - CeO<sub>2</sub> layer dripped with PdCl<sub>2</sub> solution until 10 wt. %, dried and calcined as before.
- 10 wt% Pd/CeO<sub>2</sub> 50-120  $\mu\text{m}$  catalyst particles:
  - Deposition – precipitation, using CeO<sub>2</sub> nanopowder (Sigma Aldrich, d < 25 nm) and PdCl<sub>2</sub> solution as precursors.

### Characterization

- S<sub>BET</sub> by N<sub>2</sub> adsorption (-196 °C Micromeritics Tristar 3000).
- XRD Bruker AXS D8 Focus (CuK $\alpha$ , 20-90°, 0.03° step, 0.6s/step).
- Volumetric CO chemisorption at (313 K) of pre-reduced sample. D, %, calculated assuming Pd/CO=1
- SEM (ZEISS Ultra 20 kV) and SEM EDS (Bruker Quantax).
- TEM (JEOL 2010F, 200 kV) and TEM EDS (Oxford Instruments INCA).

## Results and discussion

### Pd/CeO<sub>2</sub> catalyst activity and stability

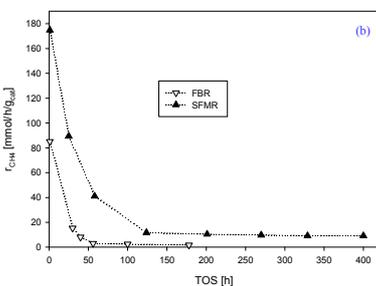
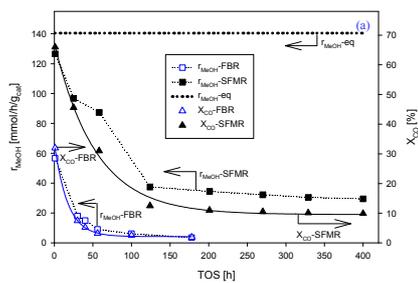


Figure 2: CO conversion and rate of CH<sub>3</sub>OH (a) and CH<sub>4</sub> by-product (b) formation with time on stream (TOS) for Pd/CeO<sub>2</sub> powder catalyst (FBR) and Pd/CeO<sub>2</sub> foil coating in SFMR. T = 300 °C, contact time W/F = 110 [ms·g<sub>cat</sub>/cm<sup>3</sup>], pressure 80 bar and syngas composition H<sub>2</sub>/CO/CO<sub>2</sub>/N<sub>2</sub> = 65/25/5/5.

### Pd/CeO<sub>2</sub> powder catalyst characterization

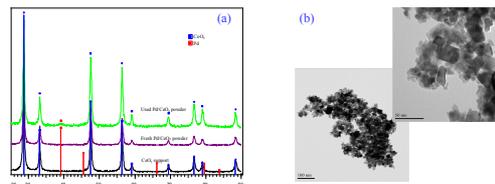


Figure 3: XRD diffractograms (a) of the CeO<sub>2</sub> support and Pd/CeO<sub>2</sub> powders before and after testing in FBR and bright-field TEM micrographs (b) of the fresh Pd/CeO<sub>2</sub> powder at different magnifications.

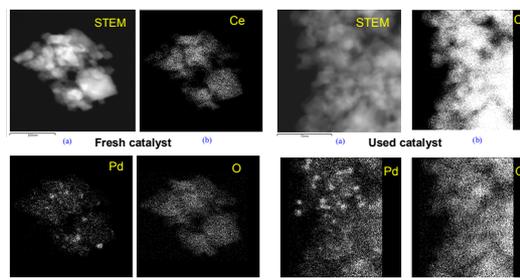
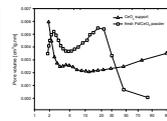


Figure 4: Dark-field STEM micrograph (a) and complementary EDS Ce (b), Pd (c), and O (d) mapping of the fresh (left panels) and used (right panels) Pd/CeO<sub>2</sub> powder catalyst.

	S <sub>BET</sub> [m <sup>2</sup> /g] <sup>a</sup>	d <sub>mes</sub> [nm] <sup>b</sup>	Pore volume [cm <sup>3</sup> /g] <sup>c</sup>	D [%] <sup>d</sup>	d <sub>p</sub> [nm] <sup>e</sup>
CeO <sub>2</sub>	32	21	0.178	-	-
Pd/CeO <sub>2</sub>	52	14	0.183	32	3.4

<sup>a</sup> BET surface area.  
<sup>b</sup> Average pore size and pore volume calculated by using BJH method.  
<sup>c</sup> Pd dispersion calculated from CO chemisorption at 313 K.  
<sup>d</sup> Pd particle size based on CO chemisorption at 313 K.

Figure 5: BET and chemisorption data



### Pd/CeO<sub>2</sub> foil coating characterization

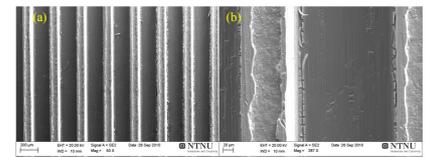


Figure 6: SEM pictures of the fresh Pd/CeO<sub>2</sub> coated foil at low (a) and high (b) magnification.

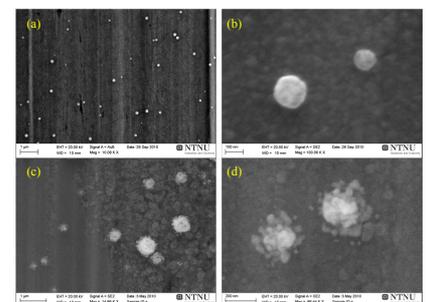


Figure 7: SEM pictures of the fresh (a-b) and the used (c-d) Pd/CeO<sub>2</sub> coated foil at 10<sup>4</sup>-10<sup>5</sup> magnification.

## Conclusions

- The Pd/CeO<sub>2</sub> catalysts show extremely high initial activity but deactivate significantly
- Transition from high S<sub>CH<sub>4</sub></sub> and low S<sub>CH<sub>3</sub>OH</sub> to decreased CH<sub>4</sub> formation and improved S<sub>CH<sub>3</sub>OH</sub> upon stabilization.
- Activity of Pd/CeO<sub>2</sub> foil coating (sol-gel synthesis) substantially better than of Pd/CeO<sub>2</sub> particles (deposition-precipitation)
- Significantly higher Pd dispersion of Pd/CeO<sub>2</sub> powder than of Pd/CeO<sub>2</sub> foil coating
- Effects attributed to the Pd nanoparticles being covered by a ceria during the preparation and subsequent reduction [6]

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