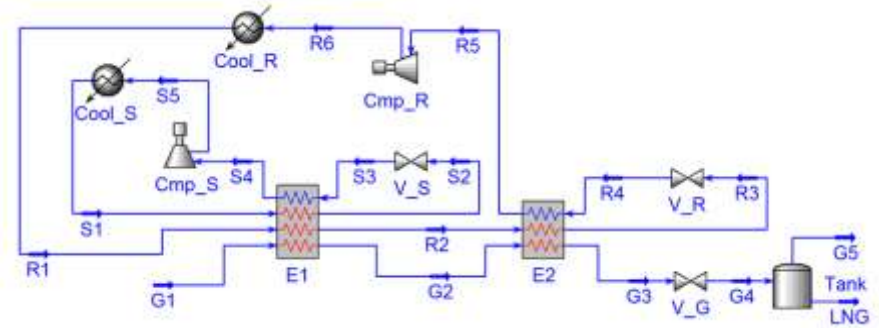




TGTC-3, Trondheim June 5th, 2014

From droplets to process: Multilevel research approach to reduce emissions from LNG processes



Sigurd Weidemann Løvseth

Ingrid Snustad

Amy Leigh Brunsvold

Geir Skaugen

Per Eilif Wahl





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M. Aa. Gjennestad



Å. Ervik



A. L. Brunsvold



A. Austegard



P. Nekså



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I. Snustad



G. A. Reigstad



T. Flåtten



A. Morin



T. Ytrehus



Ø. Wilhelmsen



P. E. Wahl



B. Austbø



S. W. Løvseth



T. Gundersen



J. Pettersen



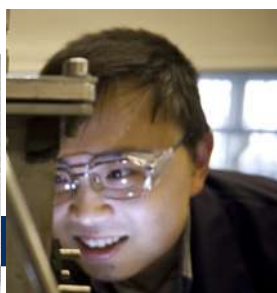
B. Müller



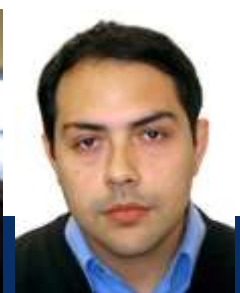
M. Hammer



K. Kolsaker



He Zhao



C. Dorao



P. K. Aursand



M. J. Mølnvik



J. Lowengrub



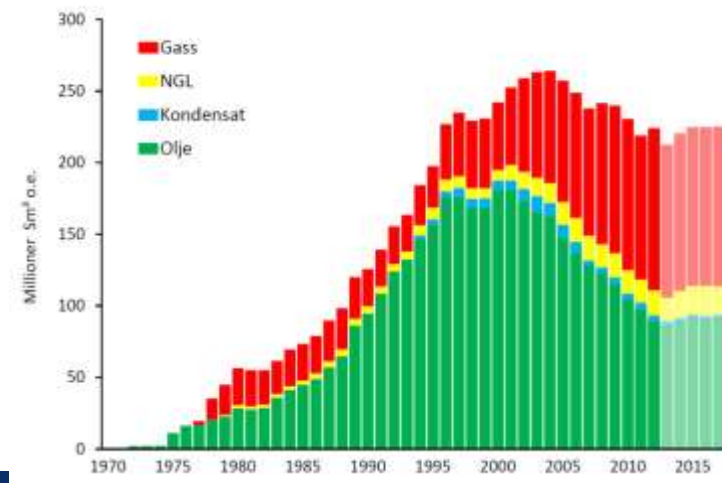
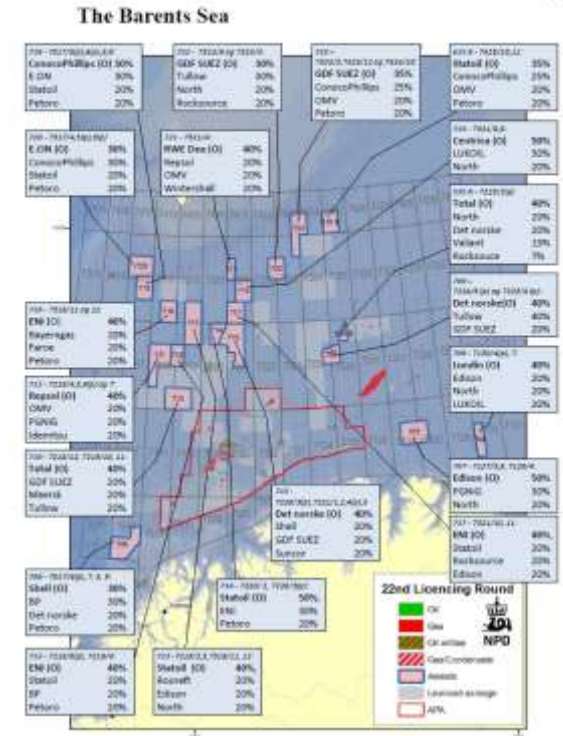
N. E. haugen

No picture:
H. T. Walnum

Motivation for research on LNG

liquefaction

- Global trends
 - LNG penetration in the energy market has increased tremendously during last decades
 - Rapid LNG growth will continue
 - Increased demand according to IEA's 2 DS
 - Large regional variation in LNG price
 - High number of LNG carriers under order
- National trends
 - Higher NG than oil production in terms of o.e.
 - Remote fields / associated gas
- LNG plants are expensive to construct and operate
 - Cost reductions and improved reliability have big impact!



Enabling Low-Emission LNG Systems



Malhaug september 2009 Photo: Eirik Lerem - Statoil

Fundamentals for multilevel modelling

- Competence building project (KMB -> KPN) with co-funding from the Research Council of Norway (PETROMAKS Programme)
- SINTEF and NTNU are research partners
- GDF SUEZ and Statoil are industrial partners
- Project duration:
 - 6 years (2009-2014)
 - Start-up Q3 2009

GDF SUEZ



<http://www.sintef.no/lelng>

Low-Emission LNG Systems

Project Goal

Facilitate sustainable production of natural gas by developing

- **knowledge**
- **competence**
- **tools**

enabling

- **evaluation**
- **design**
- **operation**

of innovative, environmentally safe, cost-effective, and energy-efficient LNG systems.



CEO Arvid Hallén, Research Council of Norway
Opening PETROMAKS Status Conference 2012-10-24

Low-Emission LNG Overview

Scale

SP3: LNG processes



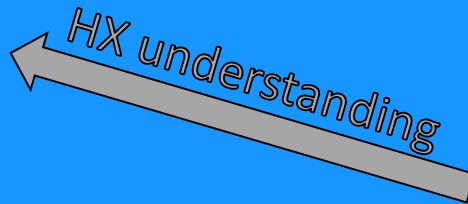
Detailed heat exchanger model



Photo: The Linde group

SP2: Heat exchanger modeling

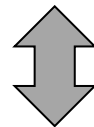
Robust modeling framework



HX 2-phase flow distr. and instabilities



Photo: The Linde group



Flow map

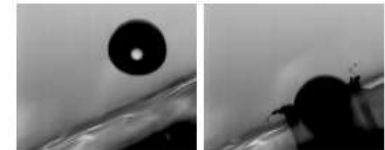
SP1: Two-phase flow phenomena

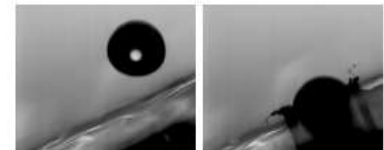
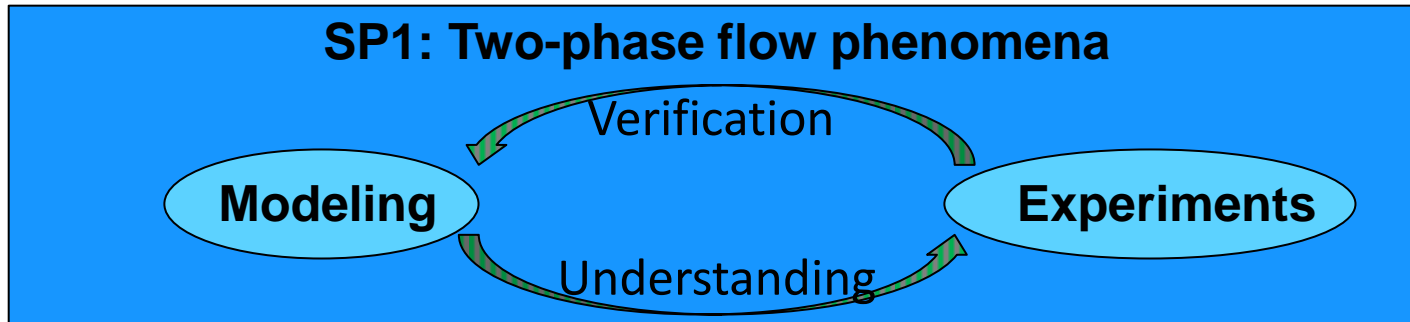
Modeling

Verification

Experiments

Understanding





Motivation: Two-phase flow phenomena

Purpose of work package

To gain insight into fundamental phenomena occurring in heat exchangers in liquefaction plants.

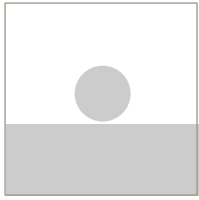
Basic hypothesis

A thorough understanding of the processes and phenomena occurring at a small-scale level in the heat exchanger is necessary to obtain an improved understanding of the heat exchanger, its design and operation.

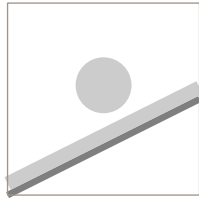
Enabling low-emission LNG systems

SP1: Two-phase flow phenomena in LNG processes

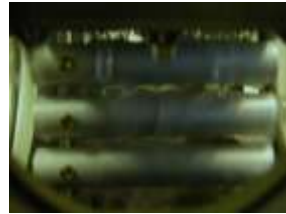
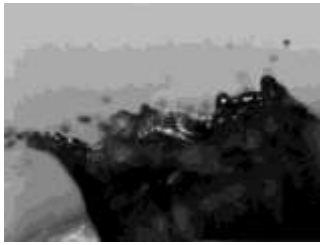
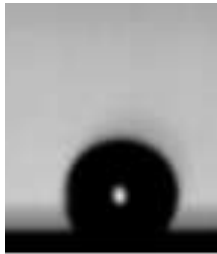
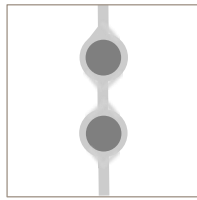
Droplet - Pool



Droplet - Flowing Film



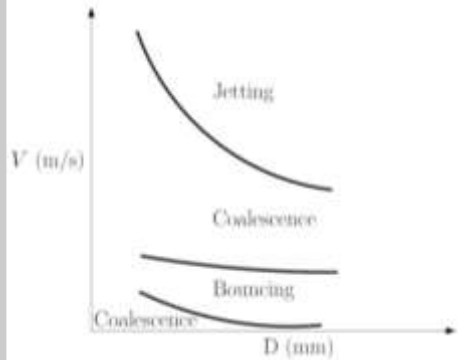
Tube bundle



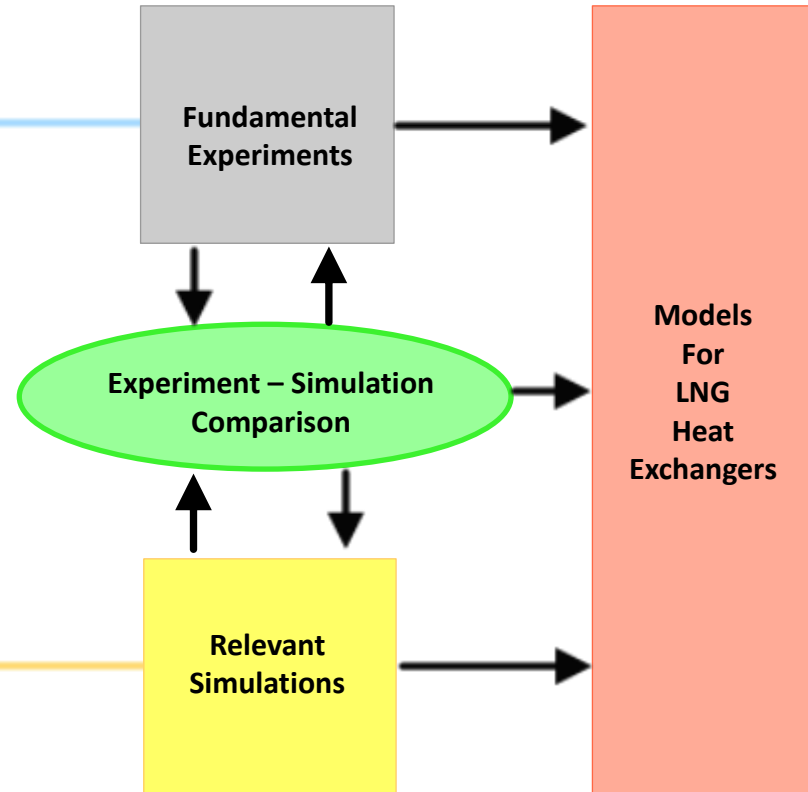
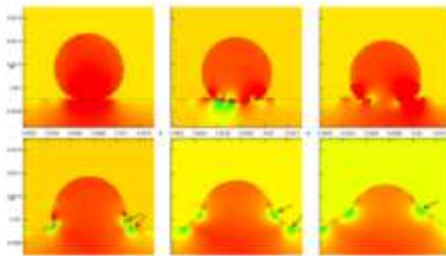
Shear flow



Droplet-column flow

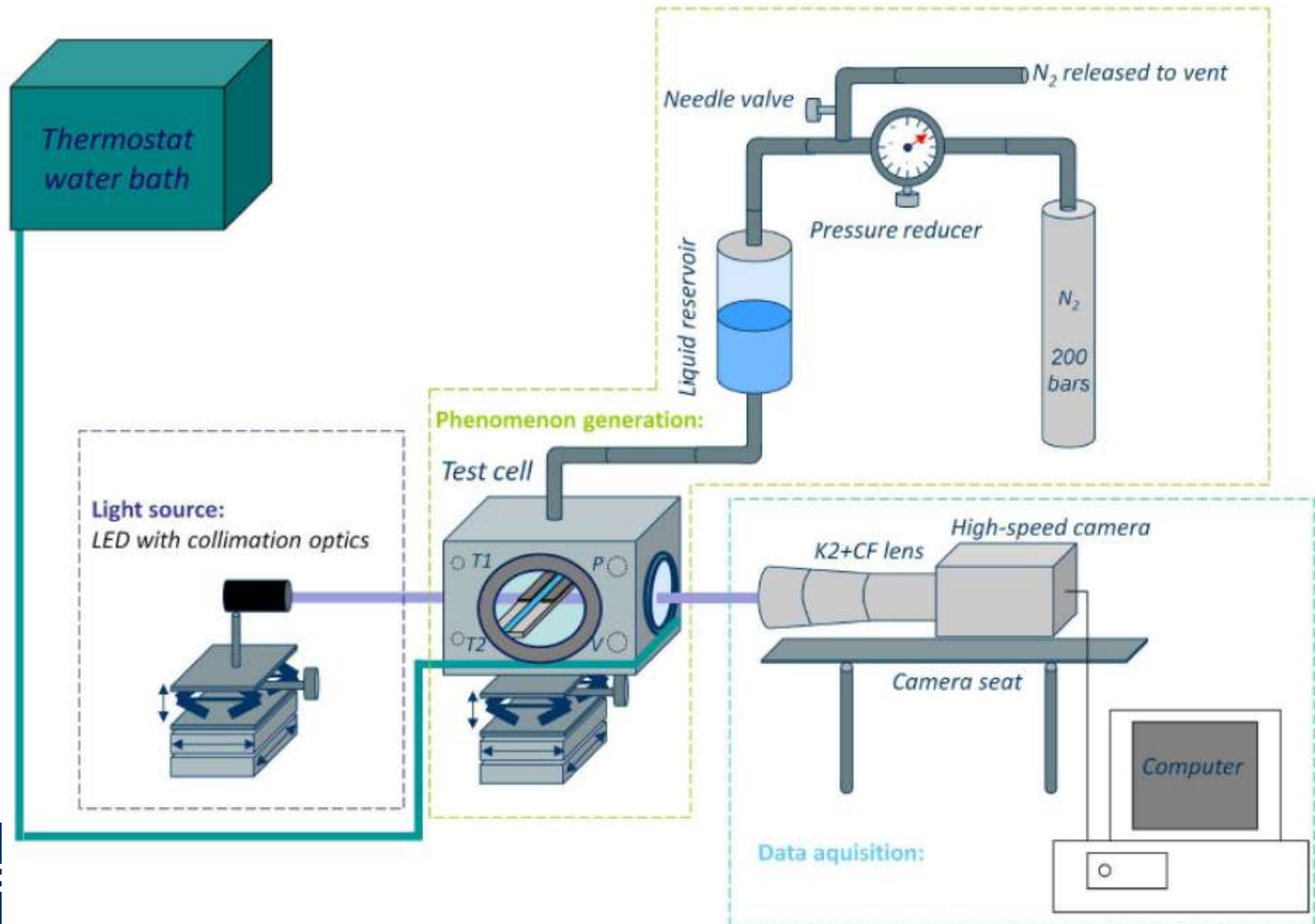


Example : water droplets on water pool



Experimental Study of detailed flow phenomena

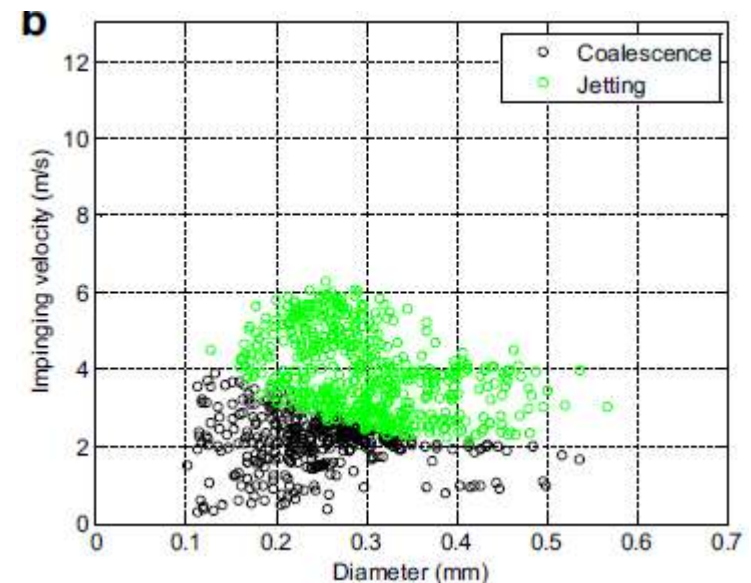
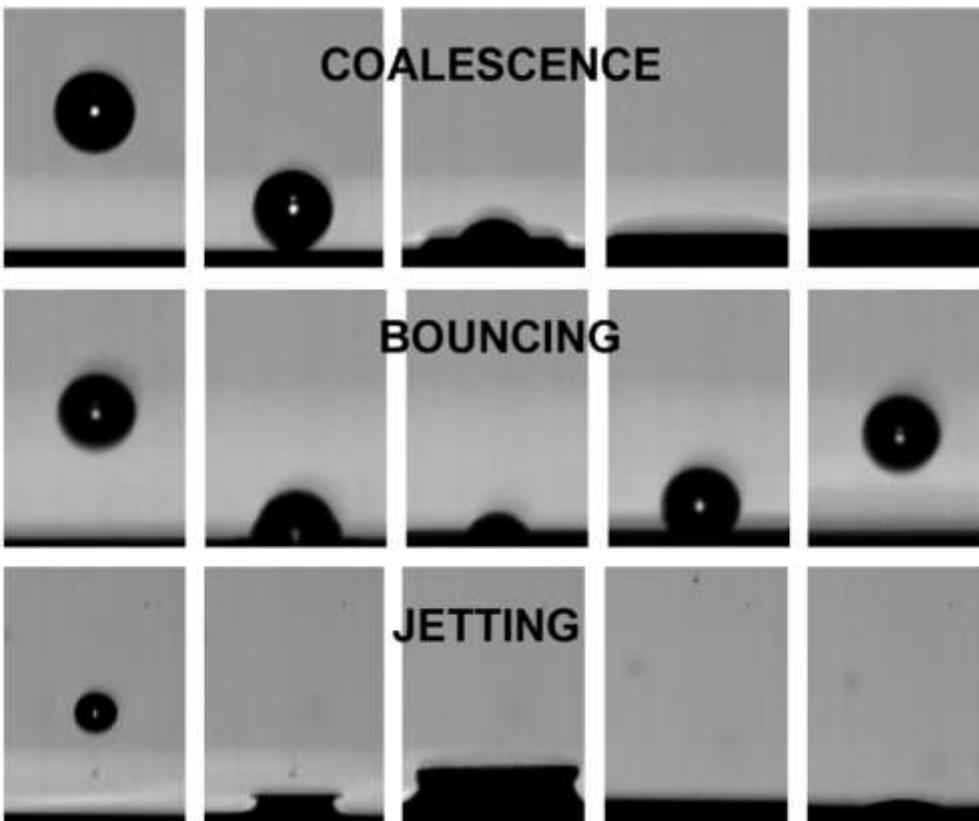
Detailed experiments necessary in order to learn the droplet / film behaviour and important for e.g. heat transfer and pressure fall. N-pentane used as a model fluid.



Experimental study of detailed flow phenomena

Detailed experiments necessary in order to learn the droplet / film behavior and important for e.g. heat transfer and pressure fall. N-pentane used as a model fluid.

- Droplet falling in deep pool



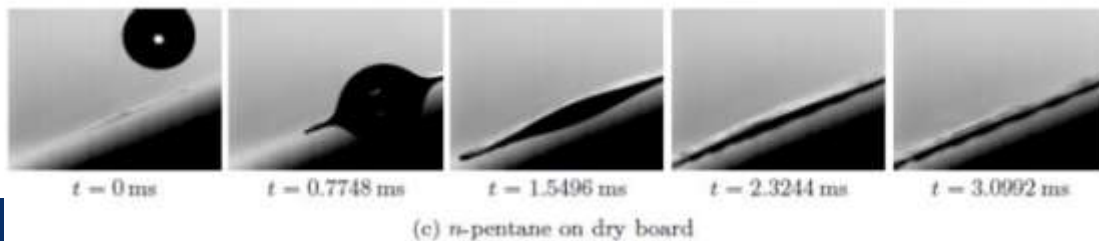
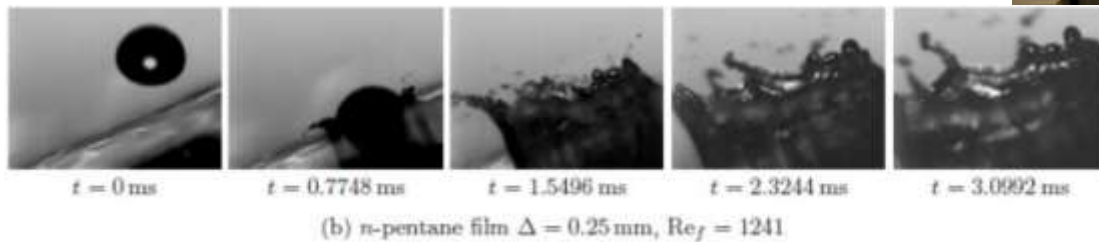
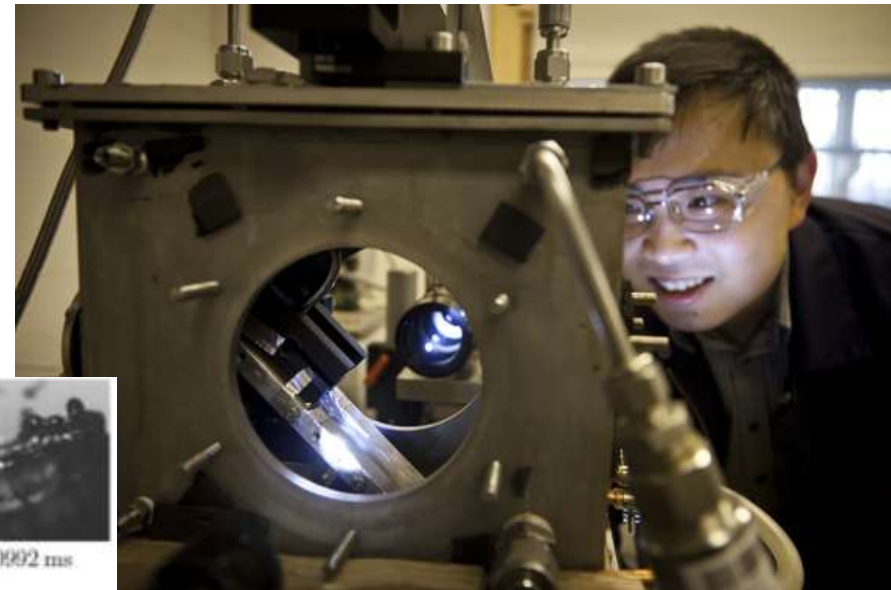
H. Zhao et al. / Journal of Natural Gas Science and Engineering 2 (2010) 259–269

Experimental study of detailed flow phenomena

Detailed experiments necessary in order to learn the droplet / film behavior and important for e.g. heat transfer and pressure fall. N-pentane used as a model fluid.

- Droplets falling
 - in deep pool
 - on films flowing on tilted board

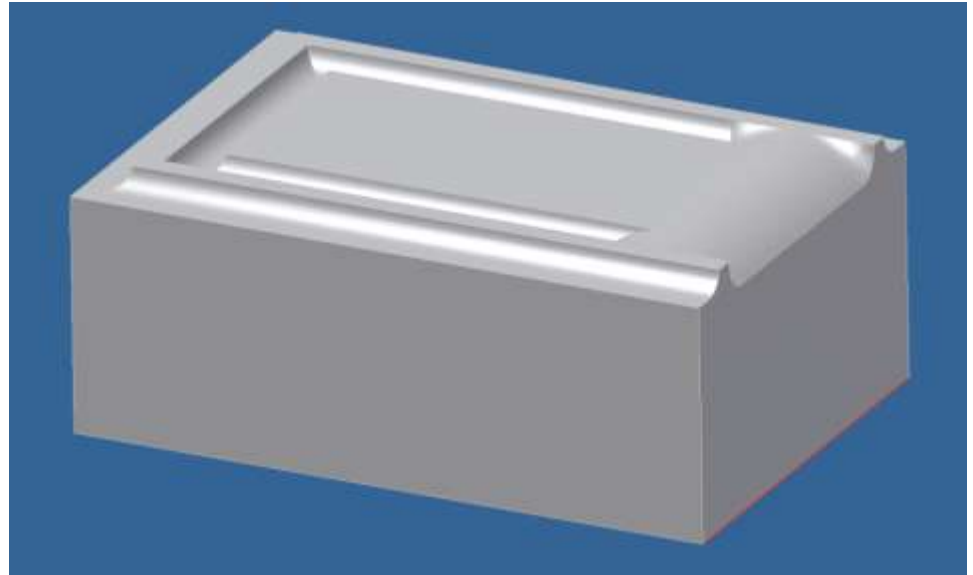
Brunsvold, A., Å. Ervik, and H. Zhao, ASME 2013 Fluids Engineering Division Summer Meeting. 2013, ASME. p. V01CT17A003



Experimental study of detailed flow phenomena

Detailed experiments necessary in order to learn the droplet / film behavior and important for e.g. heat transfer and pressure fall. N-pentane used as a model fluid.

- Droplets falling
 - in deep pool
 - on films flowing on tilted board
 - films of different thickness



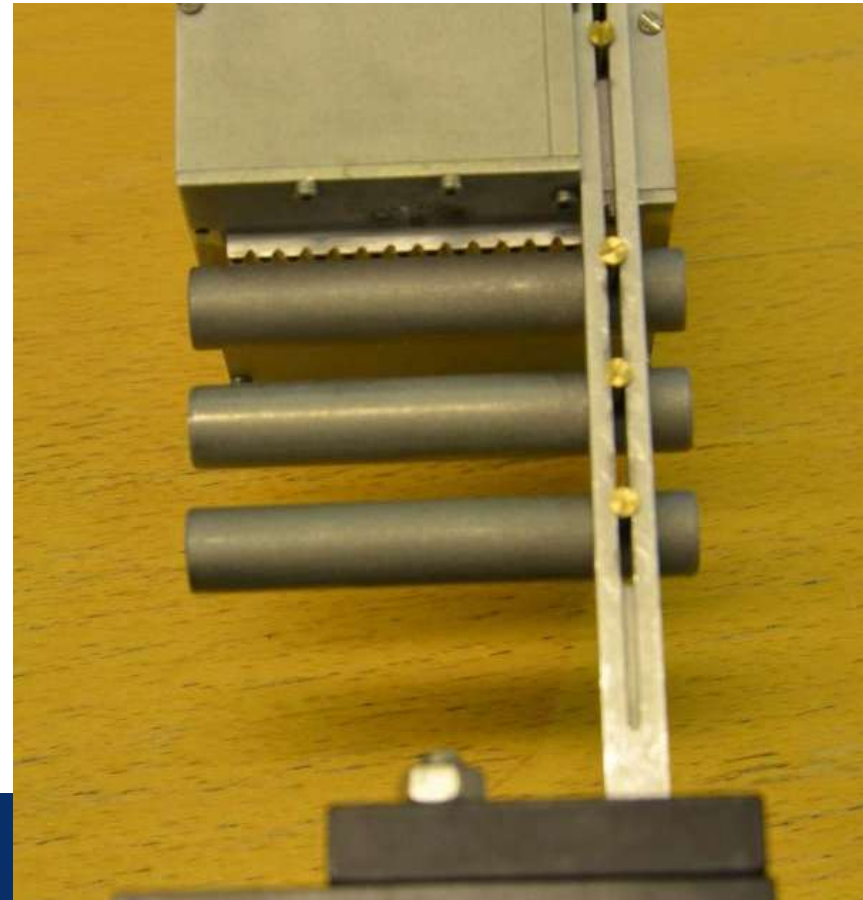
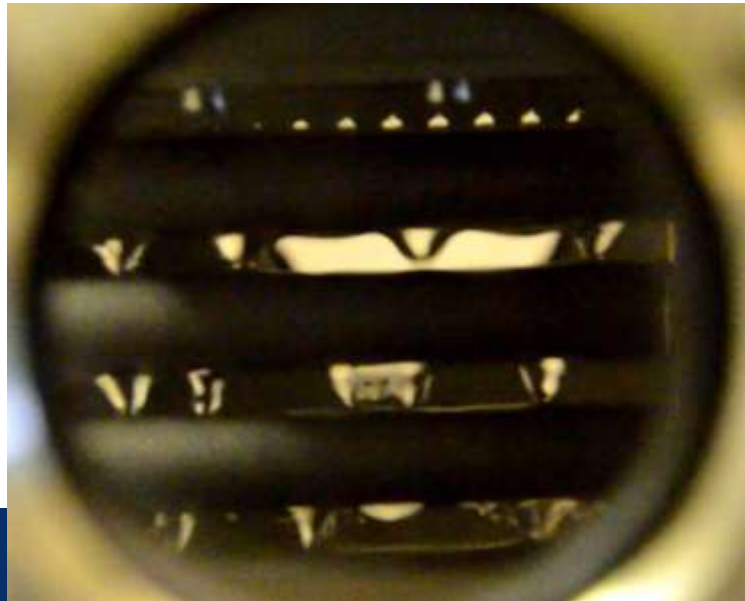
Experimental study of detailed flow phenomena

Detailed experiments necessary in order to learn the droplet / film behavior and important for e.g. heat transfer and pressure fall. N-pentane used as a model fluid.

- Droplets falling
 - in deep pool
 - on films flowing on tilted board
 - films of different thickness
- Study of different regimes of flow falling on cylinders



A. Austegard
TGTC-3
Session A2

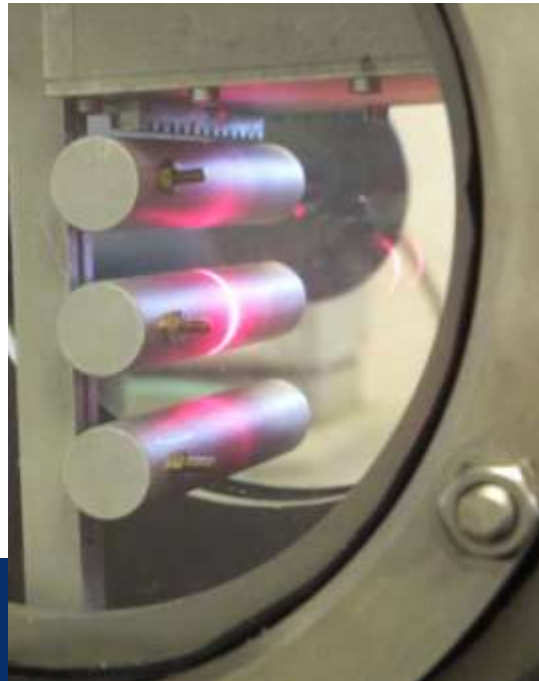


Experimental study of detailed flow phenomena

Detailed experiments necessary in order to learn the droplet / film behavior and important for e.g. heat transfer and pressure fall. N-pentane used as a model fluid.

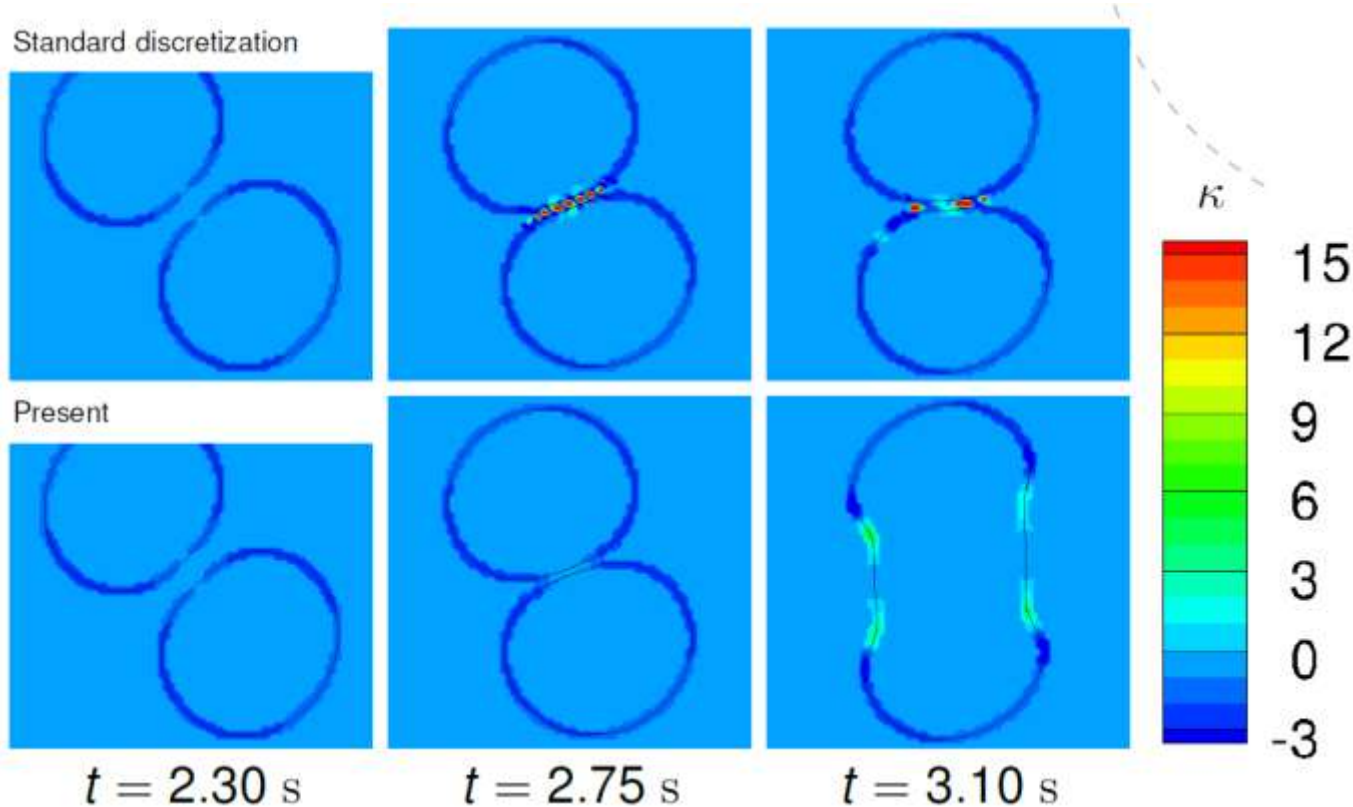
- Droplets falling
 - in deep pool
 - on films flowing on tilted board
 - films of different thickness
- Study of different regimes of flow falling on cylinders
- Film thickness measurements

(In progress)



Modeling of detailed flow phenomena

- Based on level-set method to track interfaces
- Reformulation needed in order to account for discontinuous curvature

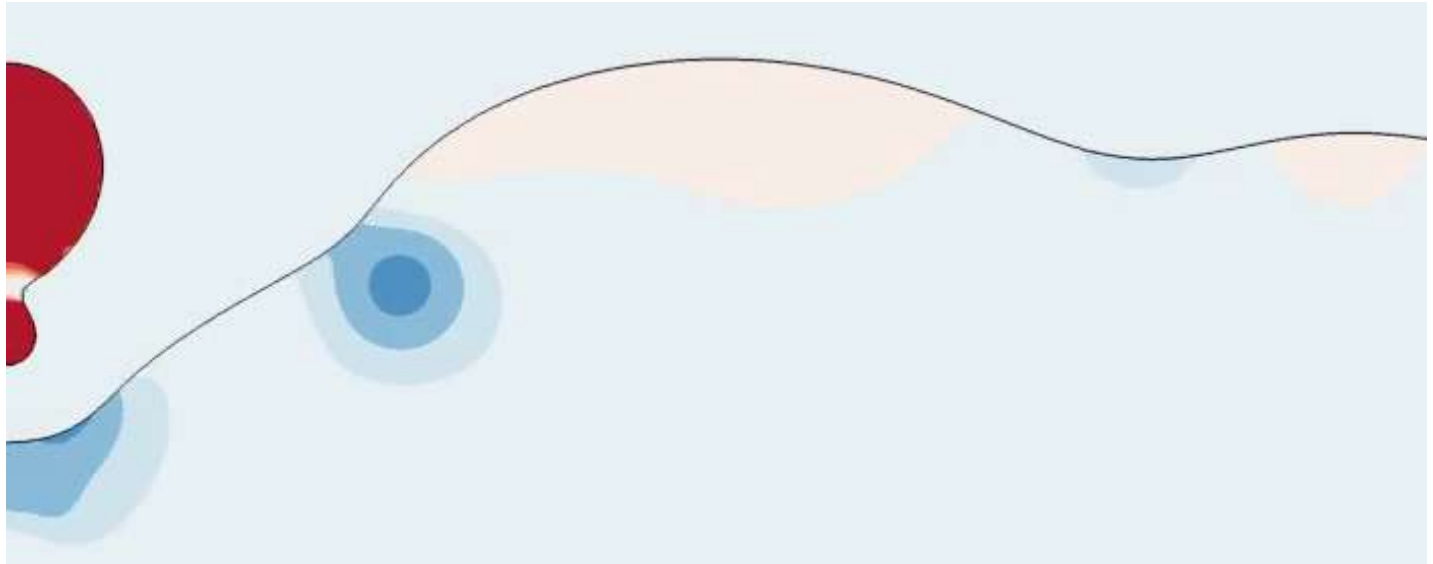


Lervåg, K.Y. and Å. Ervik, Curvature calculations for the level-set method, in Numerical Mathematics and Advanced Applications 2011. 2013, Springer. p. 209-217

Karl Yngve Lervåg, PhD, Sept 2013

Modeling of detailed flow phenomena

- Based on level-set method to track interfaces
- Reformulation needed in order to account for discontinuous curvature
- Model-experiment comparison for droplet-film coalescence possible

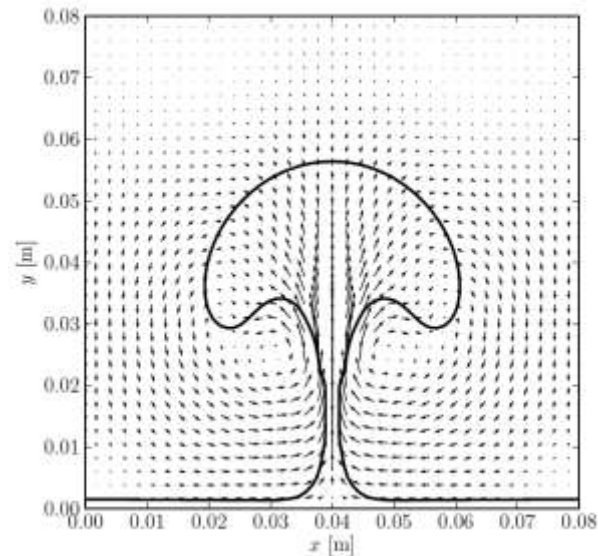


Modeling of detailed flow phenomena

- Based on level-set method to track interfaces
- Reformulation needed in order to account for discontinuous curvature
- Describes droplet-film coalescence
- Heat and mass transfer

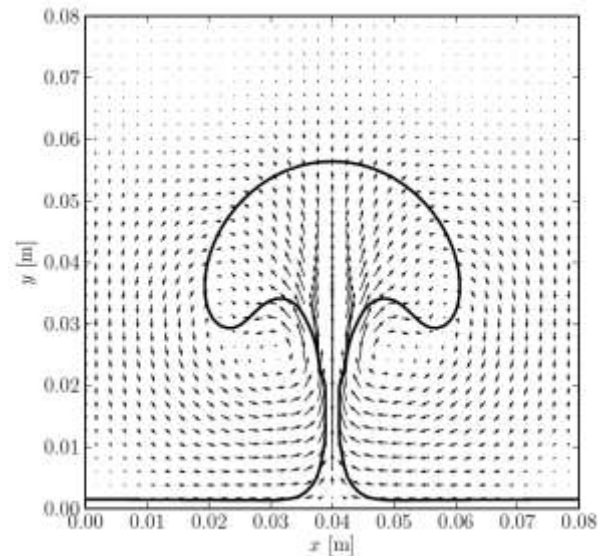


M. Aa.
Gjennestad
TGTC-3
Session A1



Modeling of detailed flow phenomena

- Based on level-set method to track interfaces
- Reformulation needed in order to account for discontinuous curvature
- Describes droplet-film coalescence
- Heat and mass transfer
 - Including heat transfer and condensation in pipes (in progress)



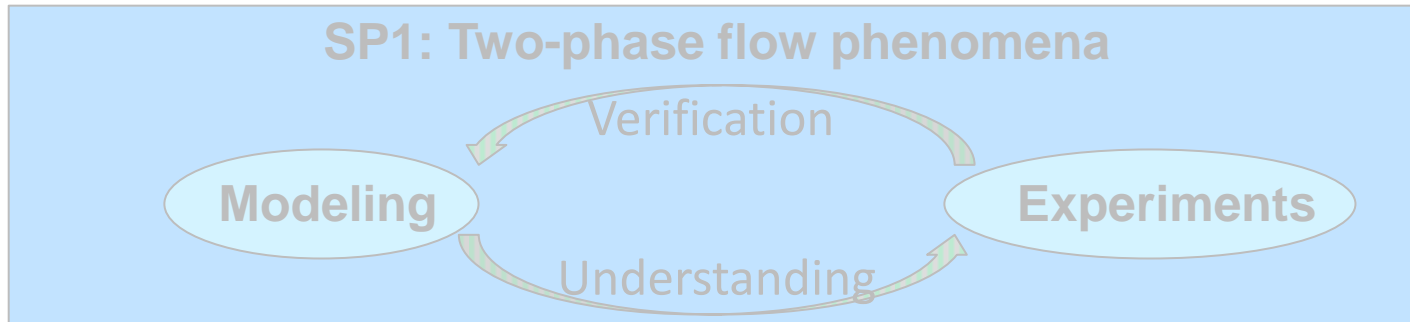
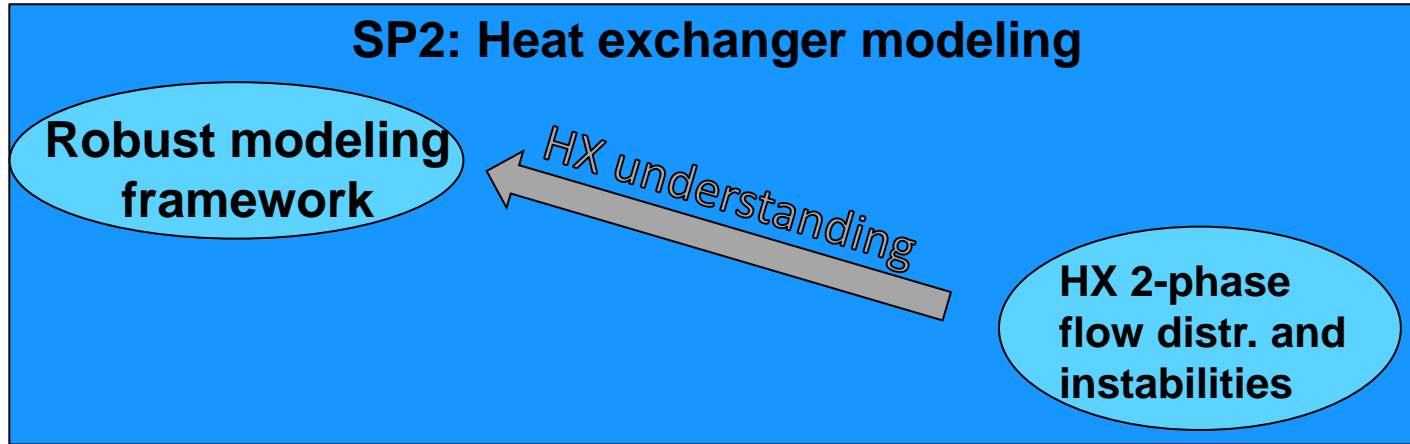
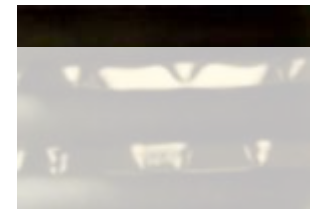
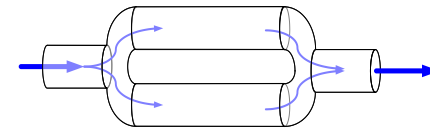


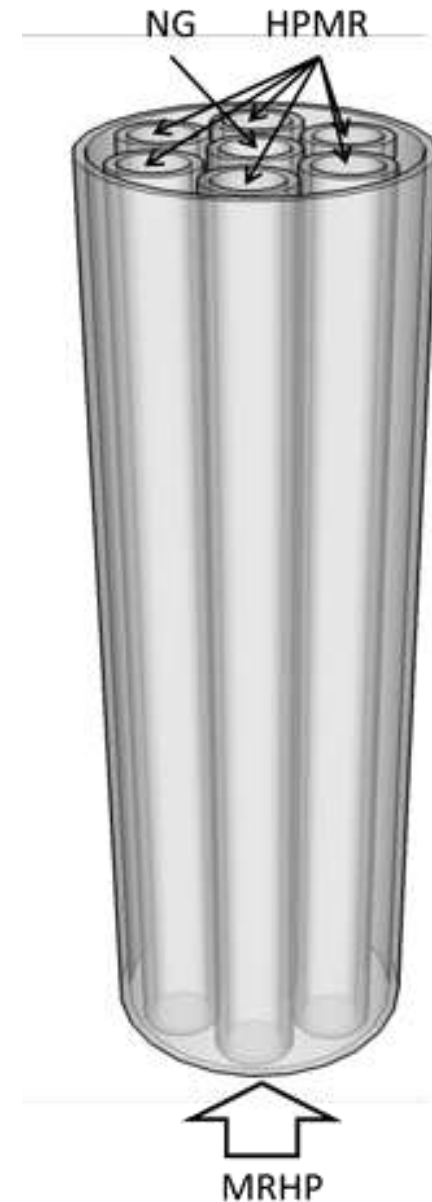
Photo: The Linde group



Heat Exchanger Modeling

FLEXHx: A Flexible Heat Exchanger Network

- Normally/ elsewhere, heat exchangers are simplified:
 - composite curve based
 - constant
 - heat transfer rates
 - heat capacities
 - constant or simplified pressure drop model.
- Geometry information is important in order to model:
 - Non-idealities
 - Dynamic behavior
 - **Realistic weight / volume => costs**



Heat Exchanger Modeling

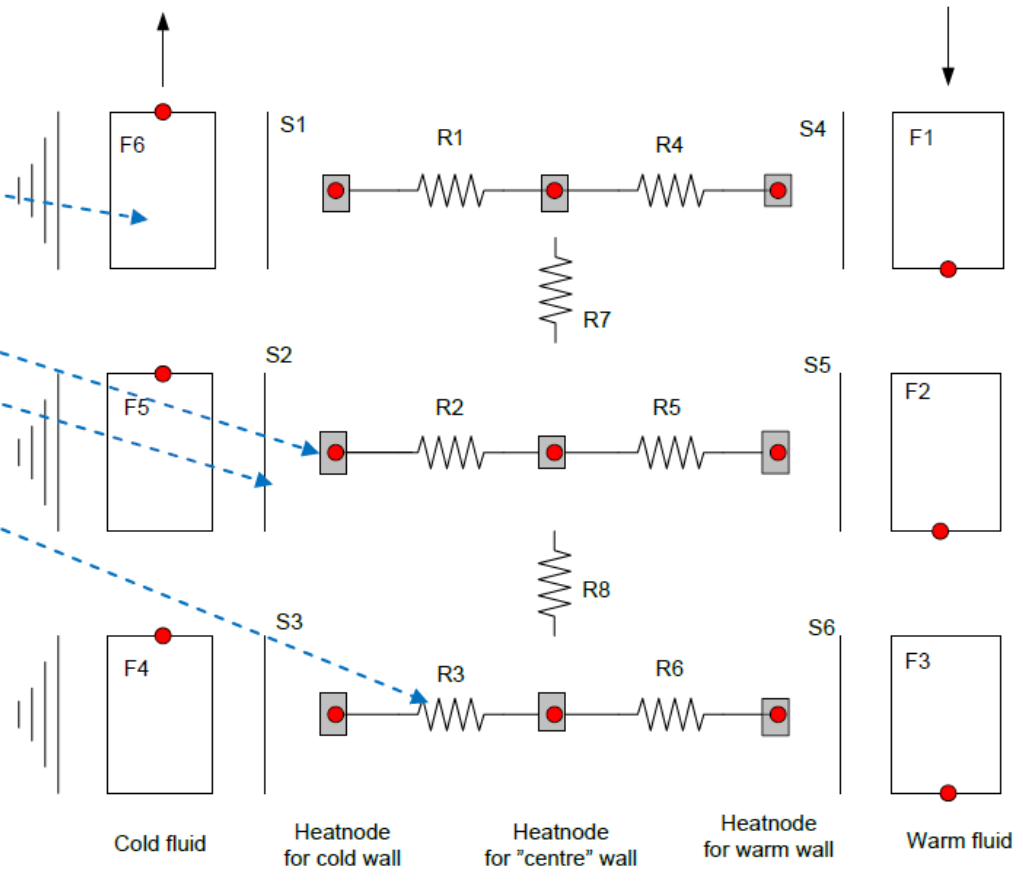
FLEXHx: A Flexible Heat Exchanger Network

Generic tool with building blocks of:

- fluid nodes
- heat nodes
- surfaces
- thermal resistors
- splitters
- mixers
- flash units
- flow restrictions

Flexible and robust data structure to handle various heat exchanger variants

Counter-flow HX with wall heat conduction



Axial and radial conduction

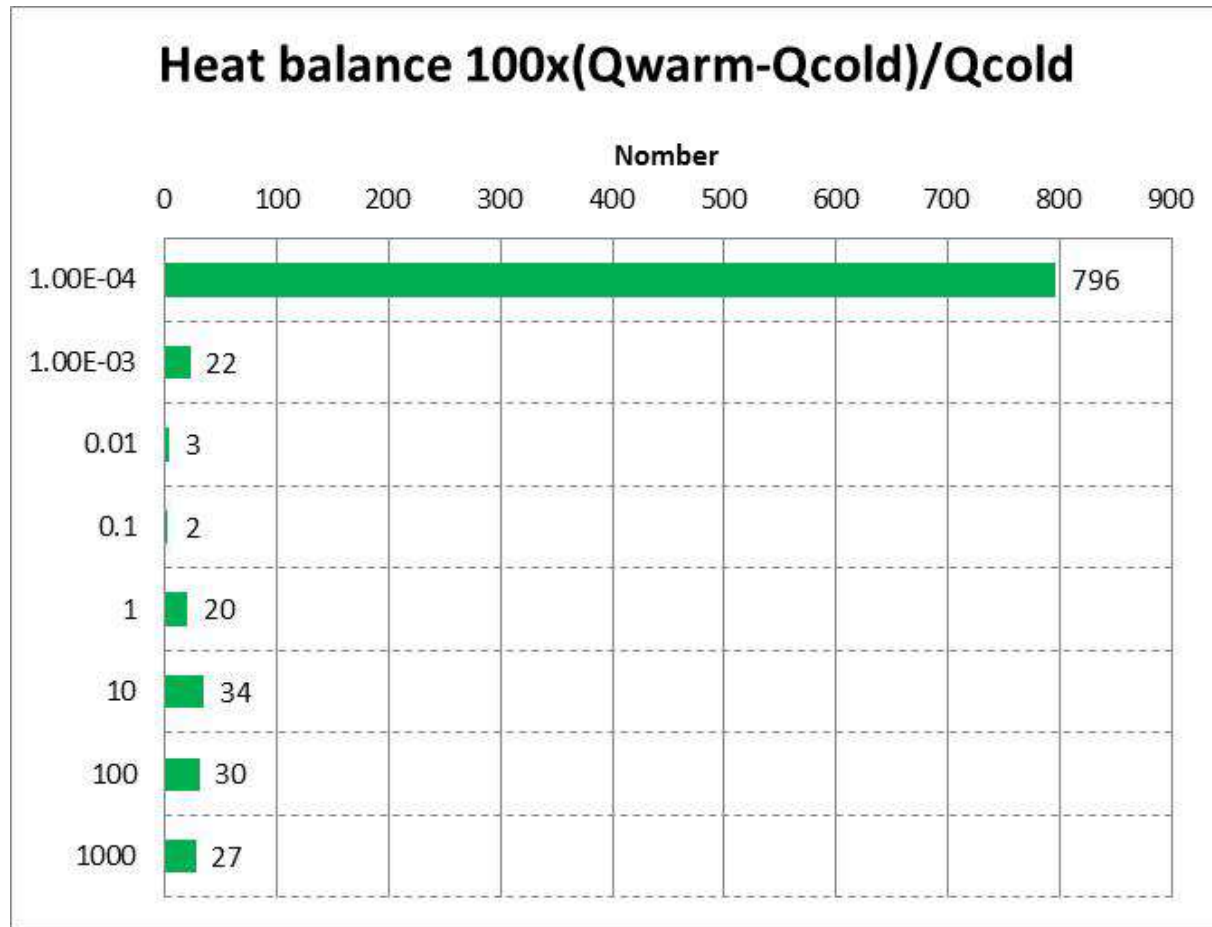
- Currently implemented: Shell & tube, plate-fin

Skaugen, G., et al., A flexible and robust modelling framework for multi-stream heat exchangers.

Computers and Chemical Engineering, 2013. 49(11): p. 95-104

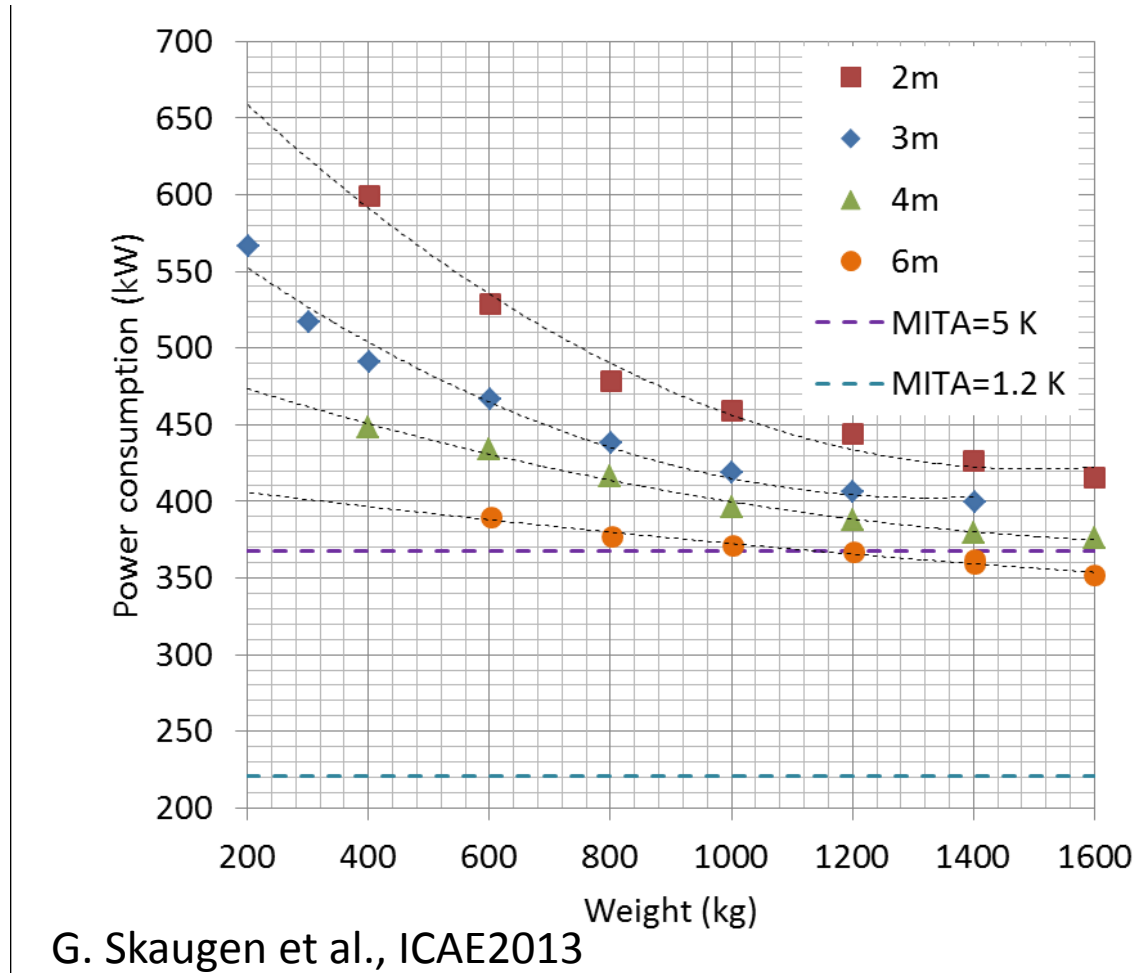
Heat Exchanger Modeling

FLEXHx: A Flexible Heat Exchanger Network - Robustness



Heat Exchanger Modeling

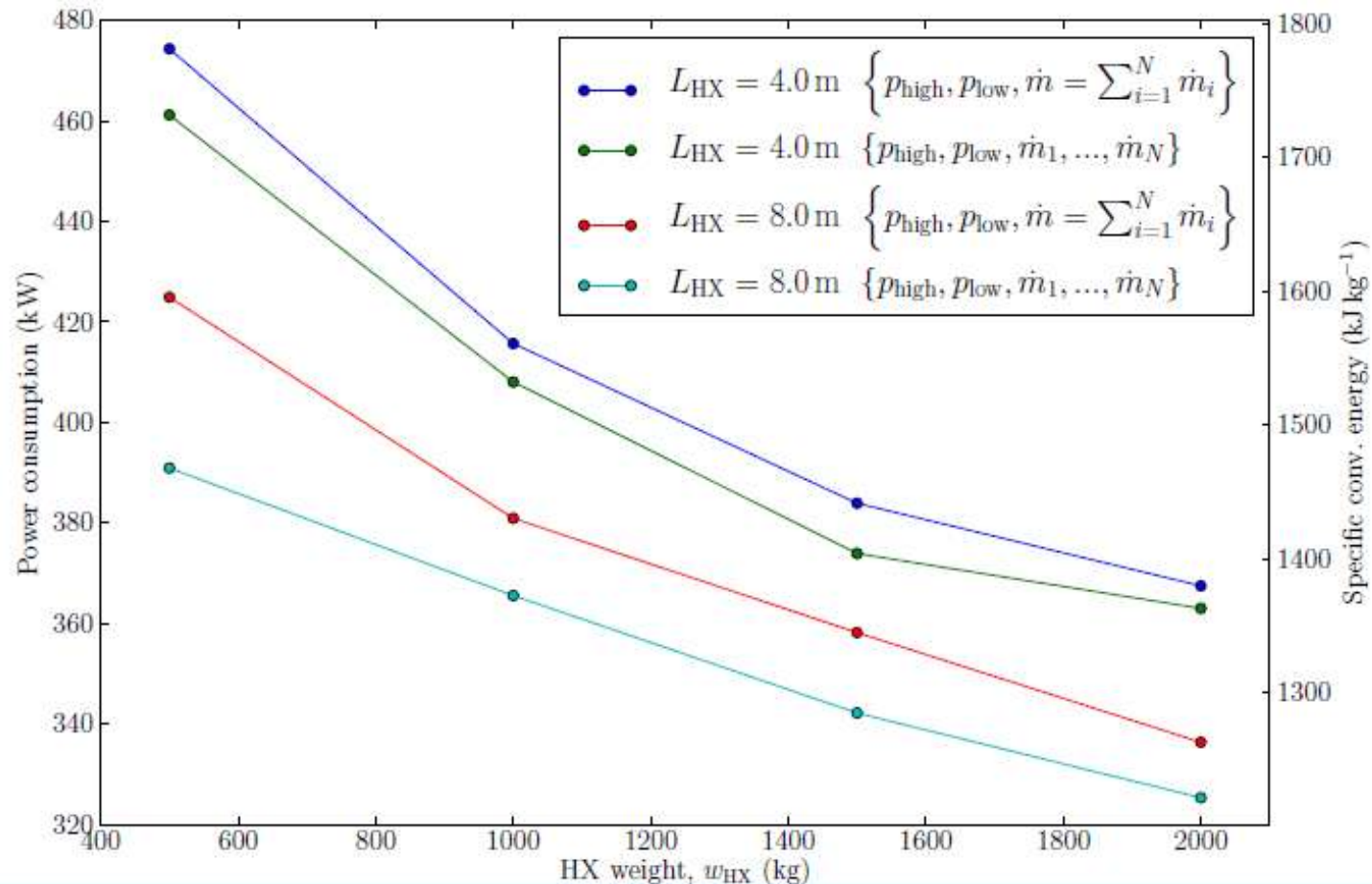
FLEXHx: A Flexible Heat Exchanger Network: Optimization of a simple single cycle LNG process with no refrigerant optimization



G. Skaugen et al., ICAE2013

Heat Exchanger Modeling

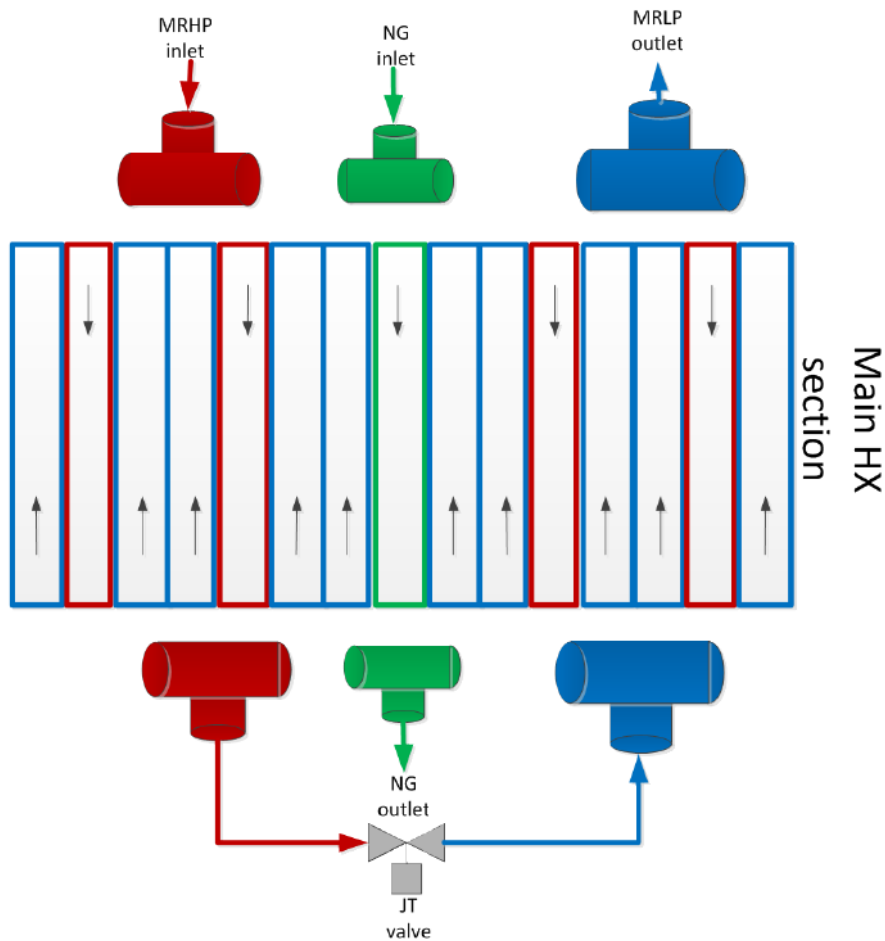
FLEXHx: A Flexible Heat Exchanger Network: Optimization of a simple single cycle LNG process with refrigerant optimization – work under progress



Heat Exchanger Modeling

FLEXHx: A Flexible Heat Exchanger Network: Instabilities

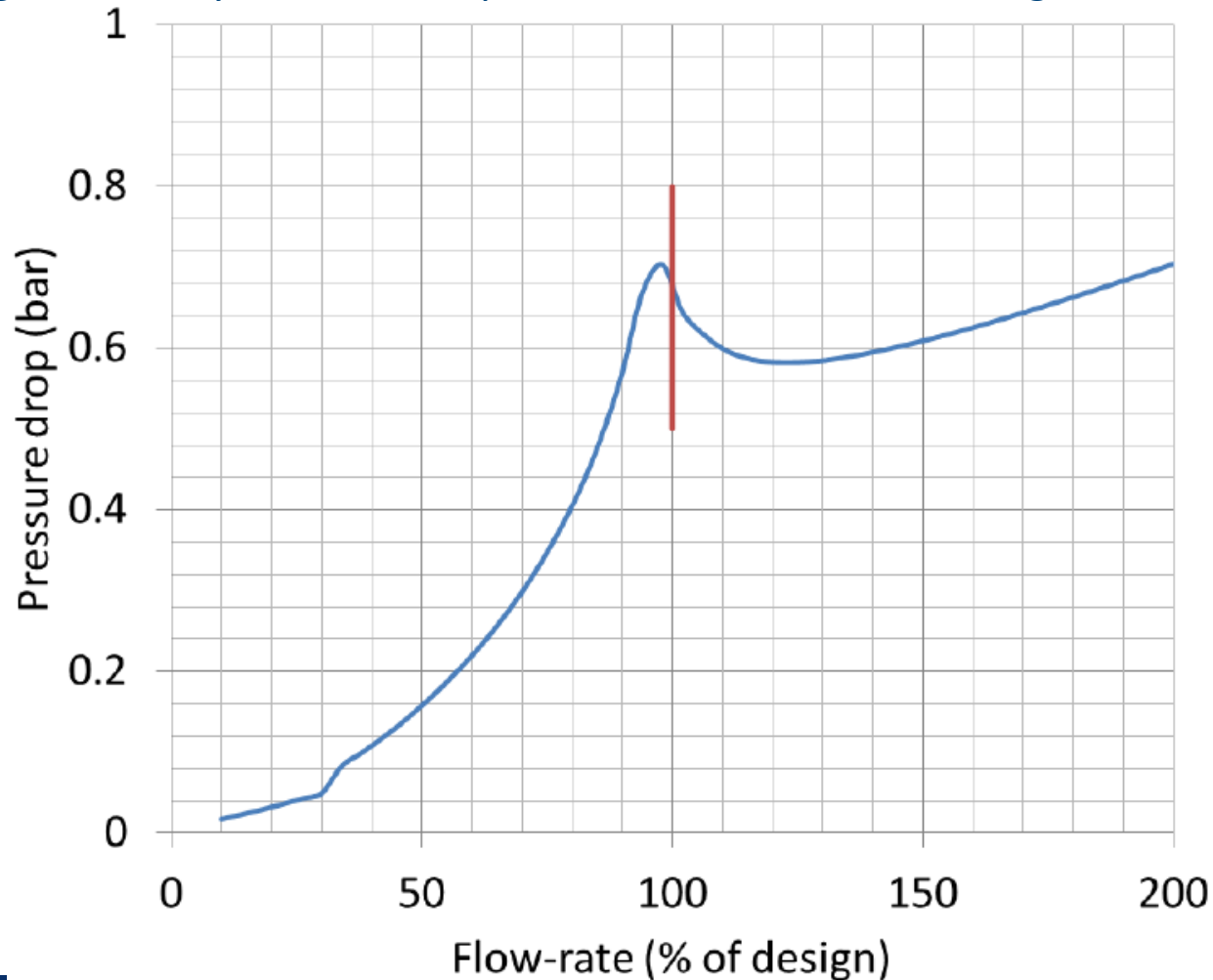
- Looking at local effects: Individual layers



Heat Exchanger Modeling

FLEXHx: A Flexible Heat Exchanger Network: Instabilities

- Ledinegg: Caused by increased vapor void fraction while boiling

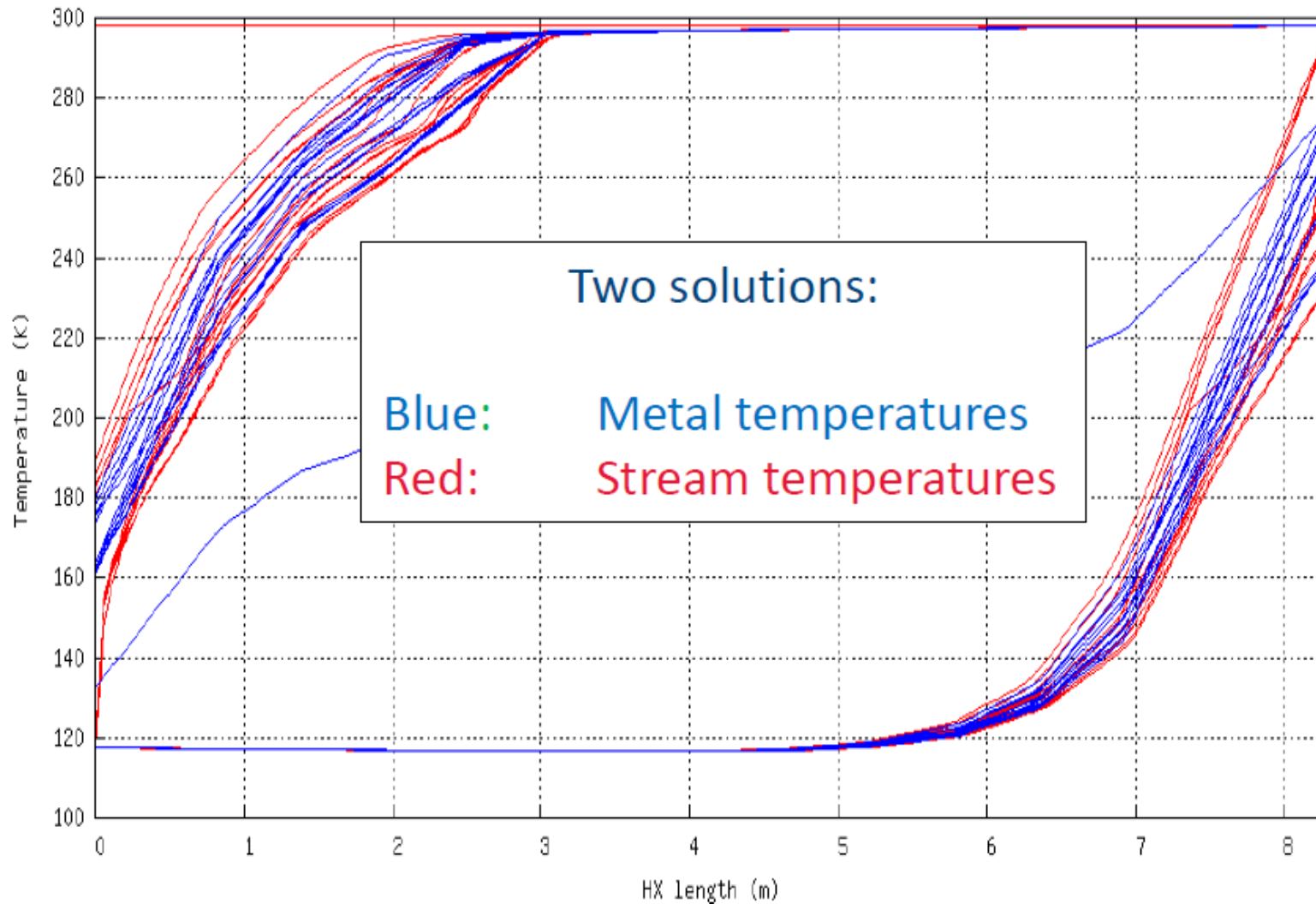


Heat Exchanger Modeling

FLEXHx: A Flexible Heat Exchanger Network: Instabilities



G. Skaugen
TGTC3
Session A5

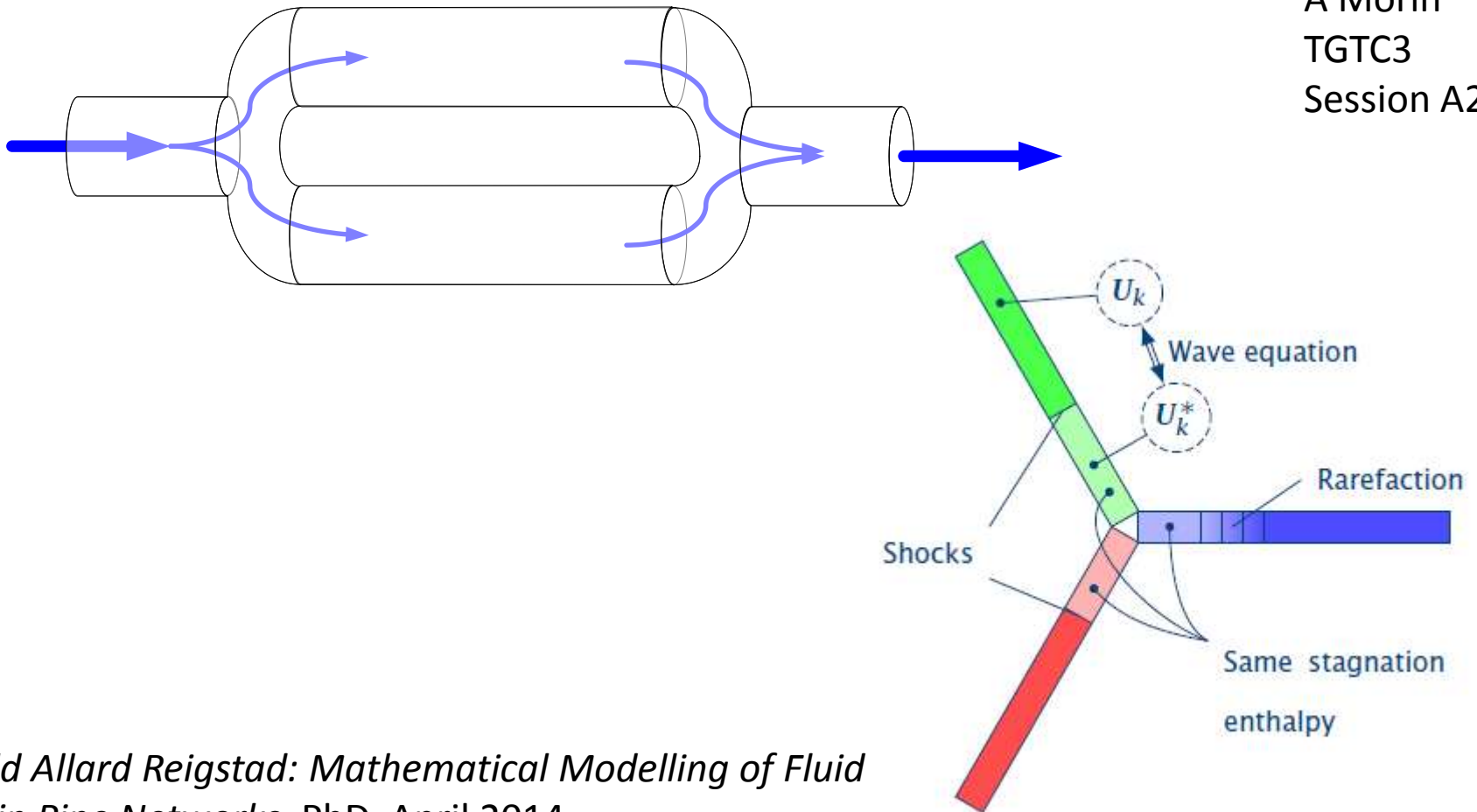


Heat Exchanger Modeling

Junction flow modeling : Looking at dynamic effects



A Morin
TGTC3
Session A2



Gunhild Allard Reigstad: Mathematical Modelling of Fluid Flows in Pipe Networks, PhD, April 2014

Low-Emission LNG Overview

Scale

SP3: LNG processes



Detailed heat exchanger model



Photo: The Linde group

SP2: Heat exchanger modeling

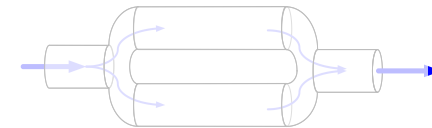
Robust modeling framework

HX understanding

HX 2-phase flow distr. and instabilities



Photo: The Linde group



Flow map

SP1: Two-phase flow phenomena

Modeling

Verification

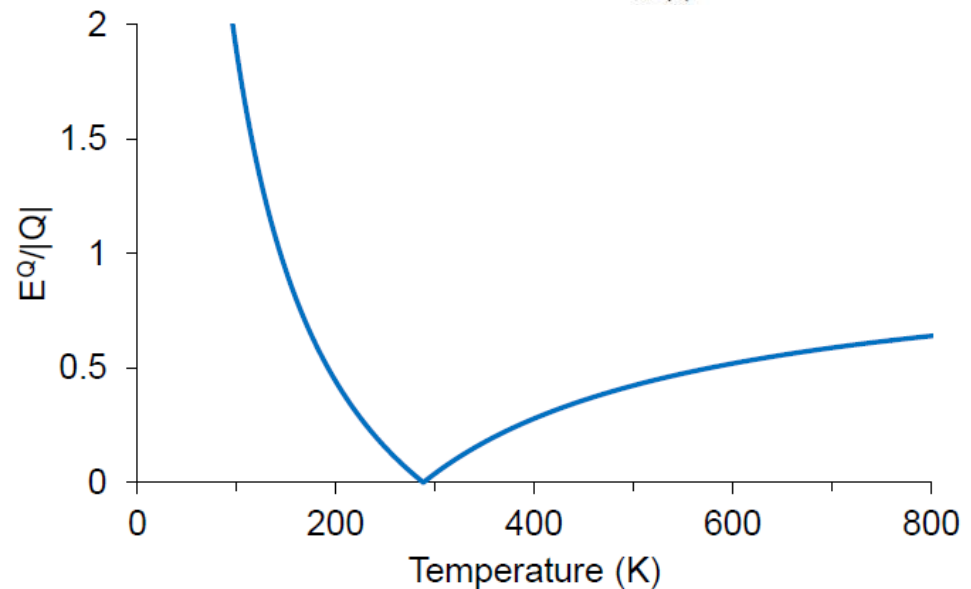
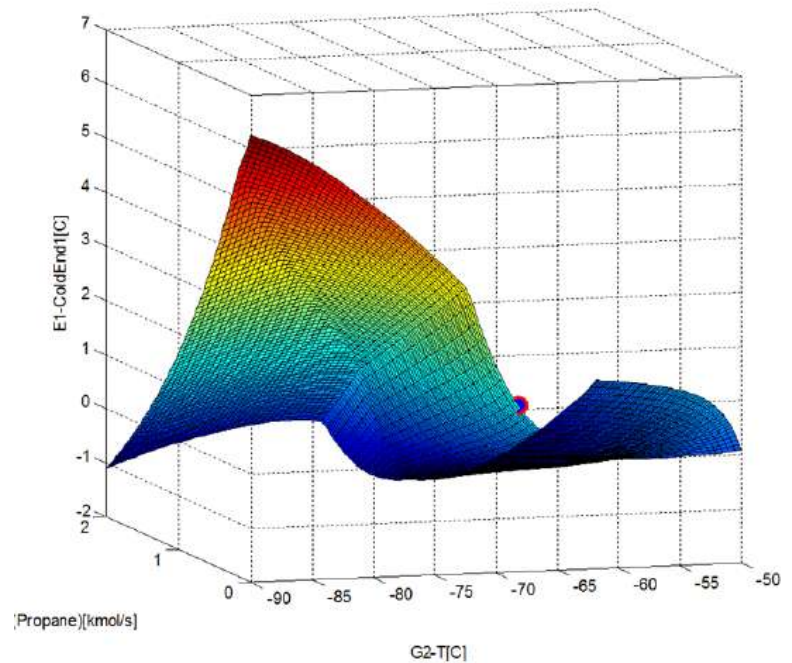
Experiments

Understanding



LNG Process optimization

- LNG liquefaction is energy expensive
- ...but difficult to optimize
 - At least 3+N-1 dimensions
 - N number of components in refrigerant
 - Non-convex
 - Non-linear constraints
 - Kinks in derivatives
 - Non analytical objective function
- Also difficult to find solution manually, especially for complex processes



LNG Process optimization

- Optimization module in tool can easily be substituted with other routines
- Results shown for **single cycle process** – trend clearer with more complex processes
- Gradient based require far fewer evaluations
- Currently working on complex processes (up to 3 cycles) with some success

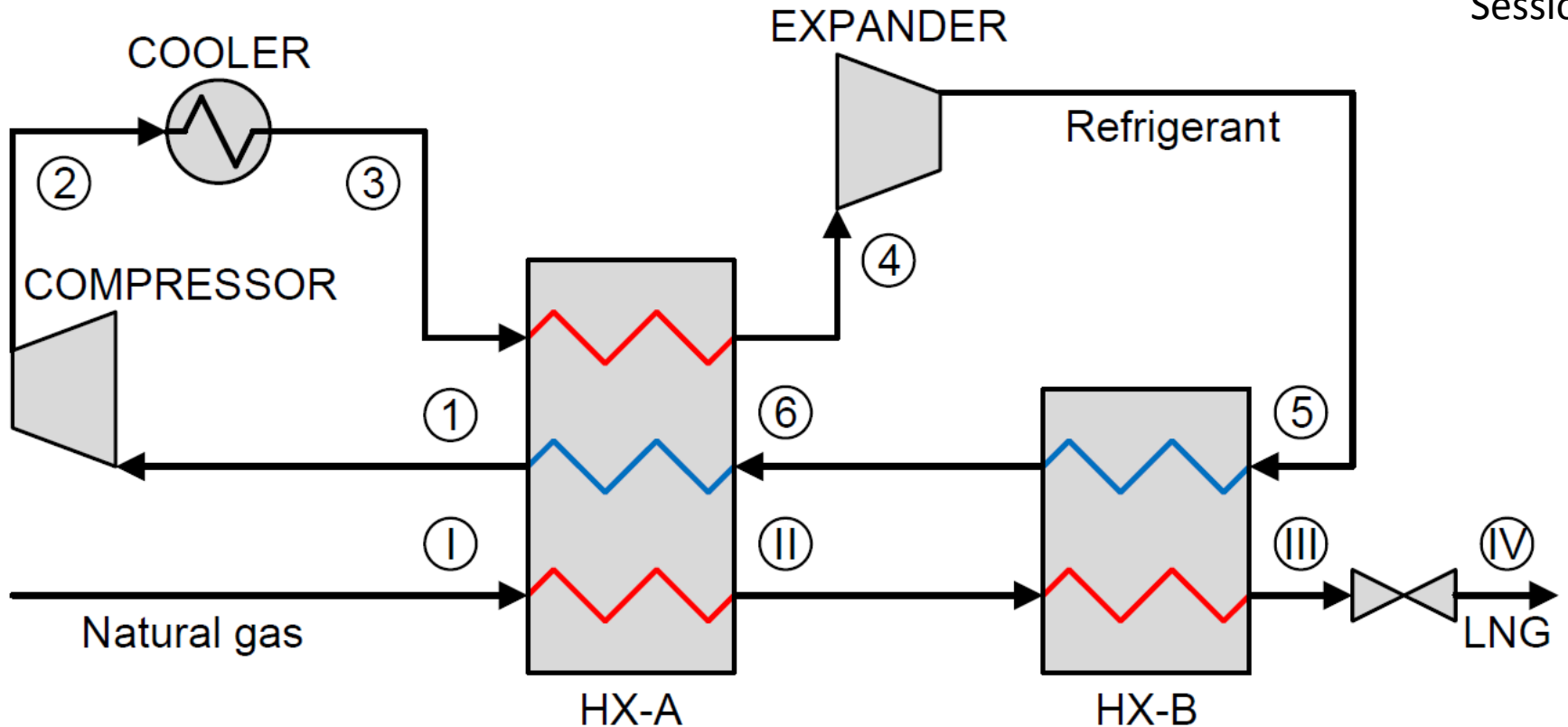
	50 %	25 %	10 %	5 %	2 %	1 %	0.1 %	0.01 %
NLPQLP	100	100	100	100	100	99	99	99
fmincon								
-SQP	100	100	100	100	100	100	98	98
-Interior-point	100	100	100	100	92	88	84	81
-Active set	100	100	100	99	98	98	95	89
LGO								
-Local search only	100	80	60	60	30	30	20	20
-Branch and Bound	100	100	90	80	60	50	40	40
-Global Adaptive Random Search	100	100	100	90	60	50	40	40
-Multi-start Search	100	100	100	100	100	100	100	100
Modified ECJ	100	100	100	100	100	100	30	0
ASA	100	100	100	100	70	30	0	0
GLOBAL (Fortran)								
-unirandi	100	60	10	0	0	0	0	0
-quasi Newton	100	100	100	100	100	80	0	0
GLOBAL (MATLAB)								
-BFGS	100	100	100	70	30	20	0	0
-unirandi	100	100	100	100	50	0	0	0
SNOBFIT	100	100	90	70	10	0	0	0
MCS	100	50	0	0	0	0	0	0

LNG Process optimization:



B. Austbø
TGTC3
Session A4

- PhD work focusing on impact of formulation of problem and thermodynamics
- At TGTC3: Single expander process optimization with different thermodynamics



Enabling Low-Emission LNG Systems



CEO Arvid Hallén, Research Council of Norway
Opening PETROMAKS Status Conference 2012-10-24

Journal and proceedings publications from Low-Emission LNG

Accepted / Published

1. Skaugen, G., et al., Use of sophisticated heat exchanger simulation models for investigation of possible design and operational pitfalls in LNG processes. *Journal of Natural Gas Science and Engineering*, 2010. 2(5): p. 236-243.
2. Lervåg, K.Y., Calculation of interface curvature with the level-set method, in *MekIT'11: Sixth National Conference on Computational Mechanics*, Trondheim 23-24 May 2011. 2011, Tapir Akademisk Forlag. p. 171-187.
3. Zhao, H., A. Brunsvold, and S.T. Munkejord, Transition between coalescence and bouncing of droplets on a deep liquid pool. *International Journal of Multiphase Flow*, 2011. 37(9): p. 1109-1119.
4. Zhao, H., S.T. Munkejord, and A. Brunsvold, Investigation of droplets impinging on a deep pool: transition from coalescence to jetting. *Experiments in Fluids*, 2011. 50(3): p. 621-635.
5. Zhao, H., et al., Droplet impact on a flowing liquid film, in *PROCEEDINGS OF THE DIPSI WORKSHOP 2011 - Droplet Impact Phenomena & Spray Investigations*. 2011, Università degli Studi di Bergamo: BERGAMO, ITALY. p. 73-80.
6. Reigstad, G.A. and T. Flåtten, An Improved Roe solver for the drift-flux two-phase flow model, in *Proceedings of the 8th international conference on CFD in the oil & gas, metallurgical and process industries*. 2012, SINTEF Materials and Chemistry. p. 366-374.
7. Austbø, B., P.E. Wahl, and T. Gundersen, Constraint handling in stochastic optimization algorithms for natural gas liquefaction processes, in *23 European Symposium on Computer Aided Process Engineering*. 2013, Elsevier. p. 445-450.
8. Lervåg, K.Y. and Å. Ervik, Curvature calculations for the level-set method, in *Numerical Mathematics and Advanced Applications 2011*. 2013, Springer. p. 209-217.
9. Lervåg, K.Y., B. Müller, and S.T. Munkejord, Calculation of the interface curvature and normal vector with the level-set method. *Computers & Fluids*, 2013. 84(Sept): p. 218-230.
10. Skaugen, G., et al., A flexible and robust modelling framework for multi-stream heat exchangers. *Computers and Chemical Engineering*, 2013. 49(11): p. 95-104.
11. Wahl, P.E., S.W. Løvseth, and M.J. Mølnvik, Optimization of a simple LNG process using sequential quadratic programming. *Computers and Chemical Engineering*, 2013. 56: p. 27-36.
12. Brunsvold, A., Å. Ervik, and H. Zhao, Experimental methods for investigating the discrete droplet impact phenomena of a model fluid relevant for LNG heat exchangers, in *ASME 2013 Fluids Engineering Division Summer Meeting*. 2013, ASME. p. V01CT17A003.
13. Wilhelmsen, Ø., et al., Time efficient solution of phase equilibria in dynamic and distributed systems with DAE-solvers. *Industrial & Engineering Chemistry Research*, 2013. 52(5): p. 2130-2140.
14. Ervik, Å., K.Y. Lervåg, and S.T. Munkejord, A robust method for calculating interface curvature and normal vectors using an extracted local level set. *Journal of Computational Physics*, 2014. 257: p. 259-277.
15. Reigstad, G.A., NUMERICAL NETWORK MODELS AND ENTROPY PRINCIPLES FOR ISOTHERMAL JUNCTION FLOW. *Networks and Heterogeneous Media*, 2014. 9(1): p. 65-99.
16. Austbø, B. and T. Gundersen, Using Thermodynamic Insight in the Optimization of LNG Processes. *Computer aided chemical engineering*, 2014, accepted.

*) Shared acknowledgment with Remote Gas

Publications (more)

- 5 more scientific articles under peer-review
- **Two PhDs completed:**
 - Gunhild Allard Reigstad: *Mathematical Modelling of Fluid Flows in Pipe Networks*, April 2014
 - Karl Yngve Lervåg: *Calculation of interface curvatures with the level-set method for two-phase flow simulations and a second-order diffuse-domain method for elliptic problems in complex geometries*, September **2013**
- 22 conference publications held /accepted
- ...of which 6 will be at TGTC3:
 - *Investigation of non-ideal behavior of plate-fin heat exchangers in LNG services using optimization techniques*
 - *The Enabling Low Emission LNG Systems Project*
 - *Flow pattern transitions and hysteresis effect in falling film flow over horizontal tubes*
 - *Modeling of heat transport in two-phase flow and of mass transfer between the phases using the level-set method*
 - *Pipe networks: coupling constants in a junction for isentropic Euler equations*
 - *OPTIMIZATION OF A SINGLE EXPANDER LNG PROCESS*



Conclusion

The Enabling Low-Emission LNG Systems project has provided

- knowledge
- competence
- tools

enabling

- evaluation
- design
- operation

of improved LNG Processes

The logo for GDF SUEZ, featuring the company name in a stylized, lowercase font with a green swoosh underneath.

Acknowledgments

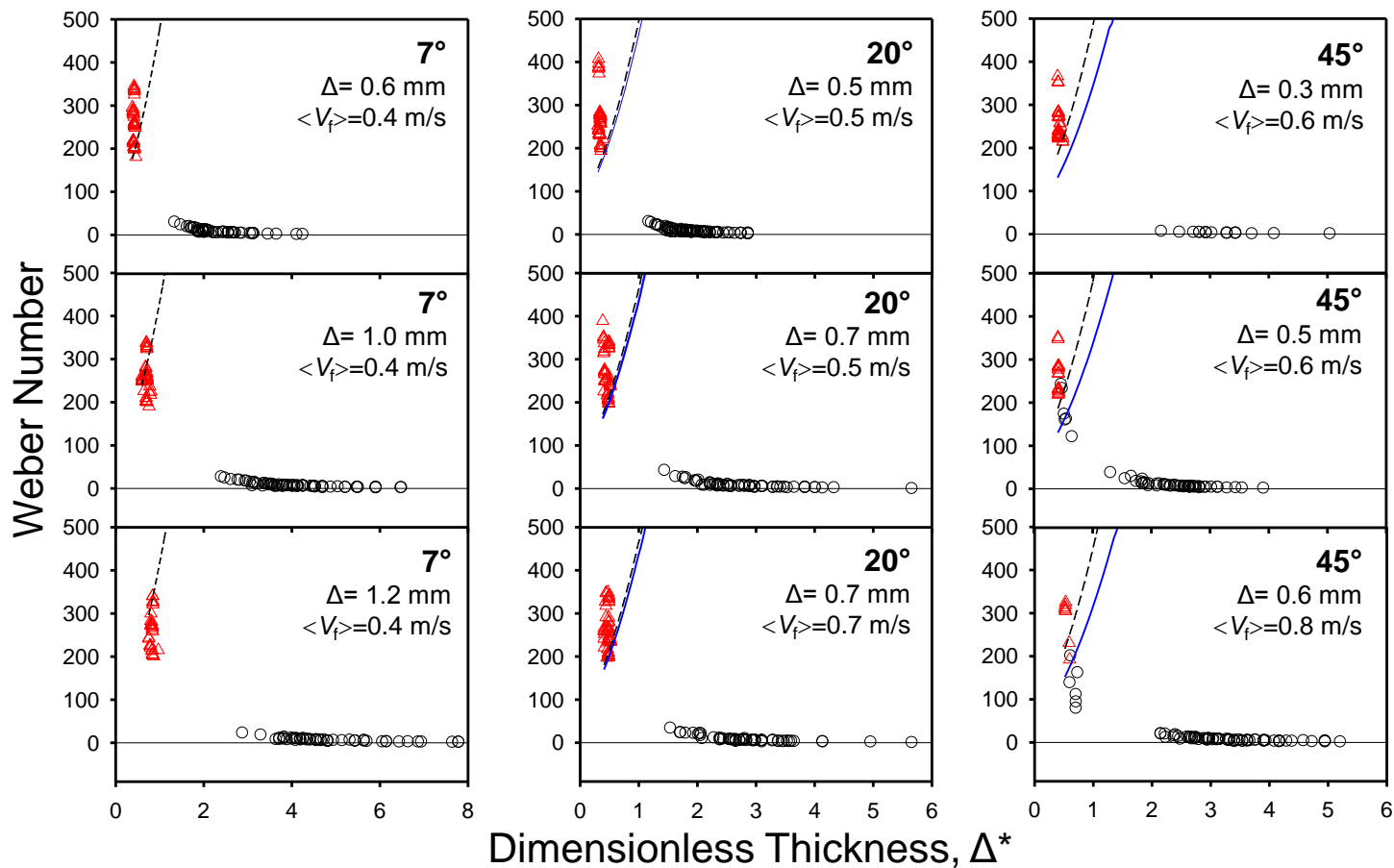
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Experimental Study of detailed flow phenomena

Detailed experiments necessary in order to learn the droplet / film behaviour and important for e.g. heat transfer and pressure fall. N-pentane used as a model fluid.

	Pentane (40°C)	Liquid methane (-162 °C, NIST[1])	Water (20°C) (NIST [1])
Density (kg/m ³)	606	422	998
Surface tension(N/m)	0.0137	0.0129	0.072
Viscosity (Pa/s)	1.97 * 10 ⁻⁴	1.12 * 10 ⁻⁴	10 * 10 ⁻⁴
Ga ^{1/4}	569	875	441
Ca (mm)	1.52	1.77	2.71

Coalescence-Splashing Threshold



$$We_c = \frac{2100 + 5800\Delta^{*1.44}}{Oh^{-0.4}}$$

- Coalescing *n*-pentane droplets
- △ Splashing *n*-pentane droplets
- Cossali c-s threshold
- Adjusted normal We corrected threshold