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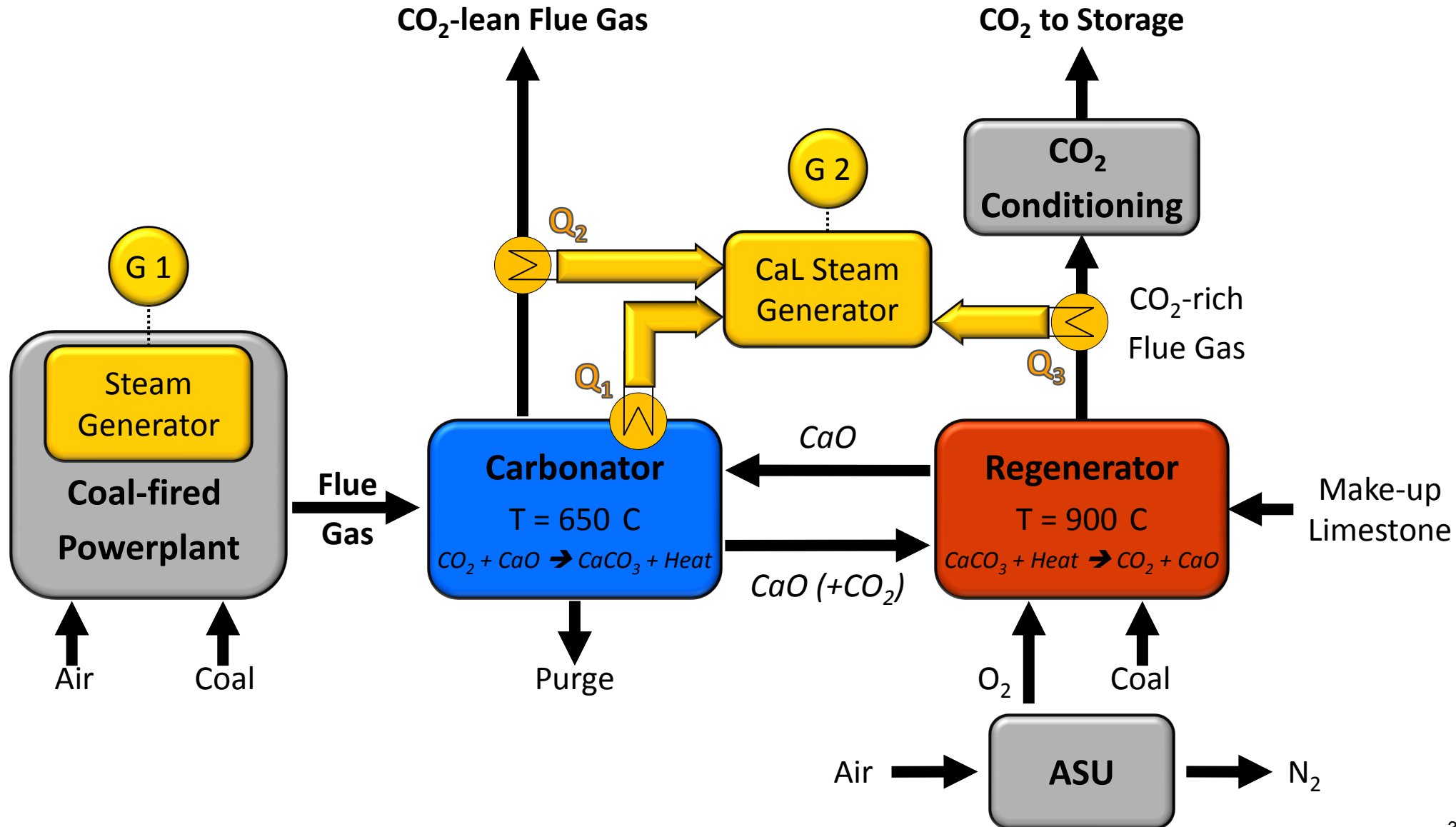
# Demonstration of the Calcium Looping Process: High Temperature CO<sub>2</sub> Capture with CaO in a 200 kW<sub>th</sub> Dual Fluidized Bed Pilot Facility

Presented by: *Heiko Dieter*

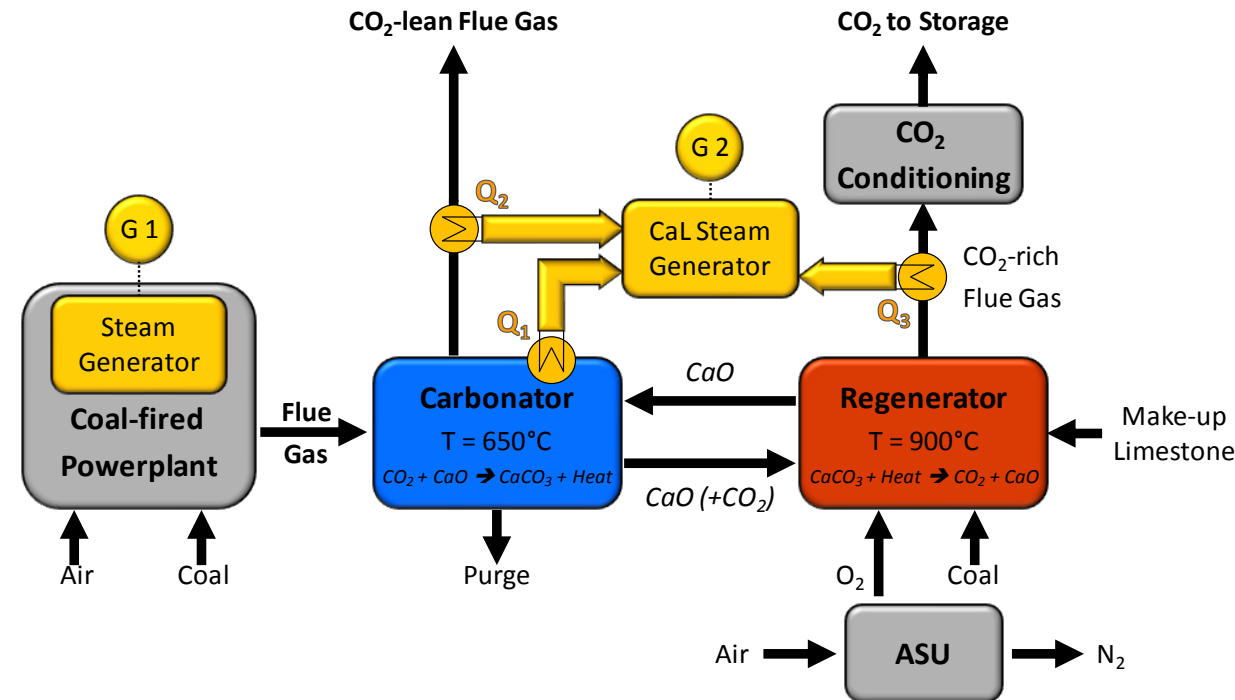
Authors: *Heiko Dieter, Craig Hawthorne*

- The Calcium Looping CO<sub>2</sub> Capture Process
- The 200 kW<sub>th</sub> Calcium Looping Pilot Plant
- Pilot Plant Results
- Conclusions and Outlook

# The Calcium Looping (CaL) Process



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## CO<sub>2</sub> Capture Costs<sup>1</sup>:

- Over 90% CO<sub>2</sub> Capture efficiency demonstrated
- CO<sub>2</sub> Avoidance Cost ~ 20 €/t CO<sub>2</sub>
- Cost of Electricity ~ 40 €/MWh
- Purged material can be efficiently utilized in cement or FGD processes

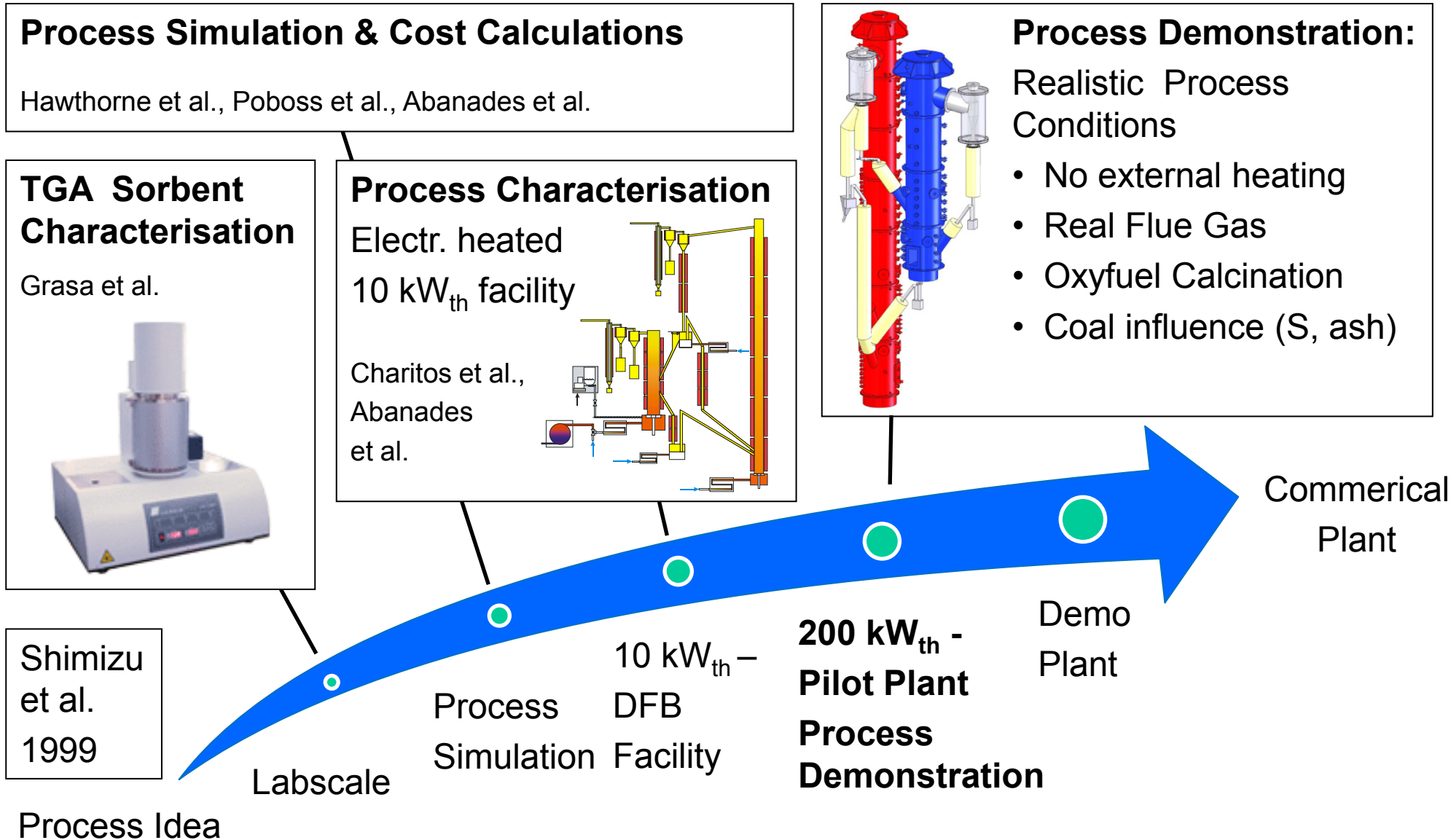
## Electricity Generation<sup>2</sup>:

- Plant electric efficiency including CO<sub>2</sub> capture and compression calculated at 39.2%
  - 6.4% penalty
- Power output increases ~ 45%

<sup>1</sup> Poboss et al., Coorettec Final Report 2008; Abanades et al., Environ. Sci. Technol., 2007

<sup>2</sup> Hawthorne et al., Energy Procedia, 2009

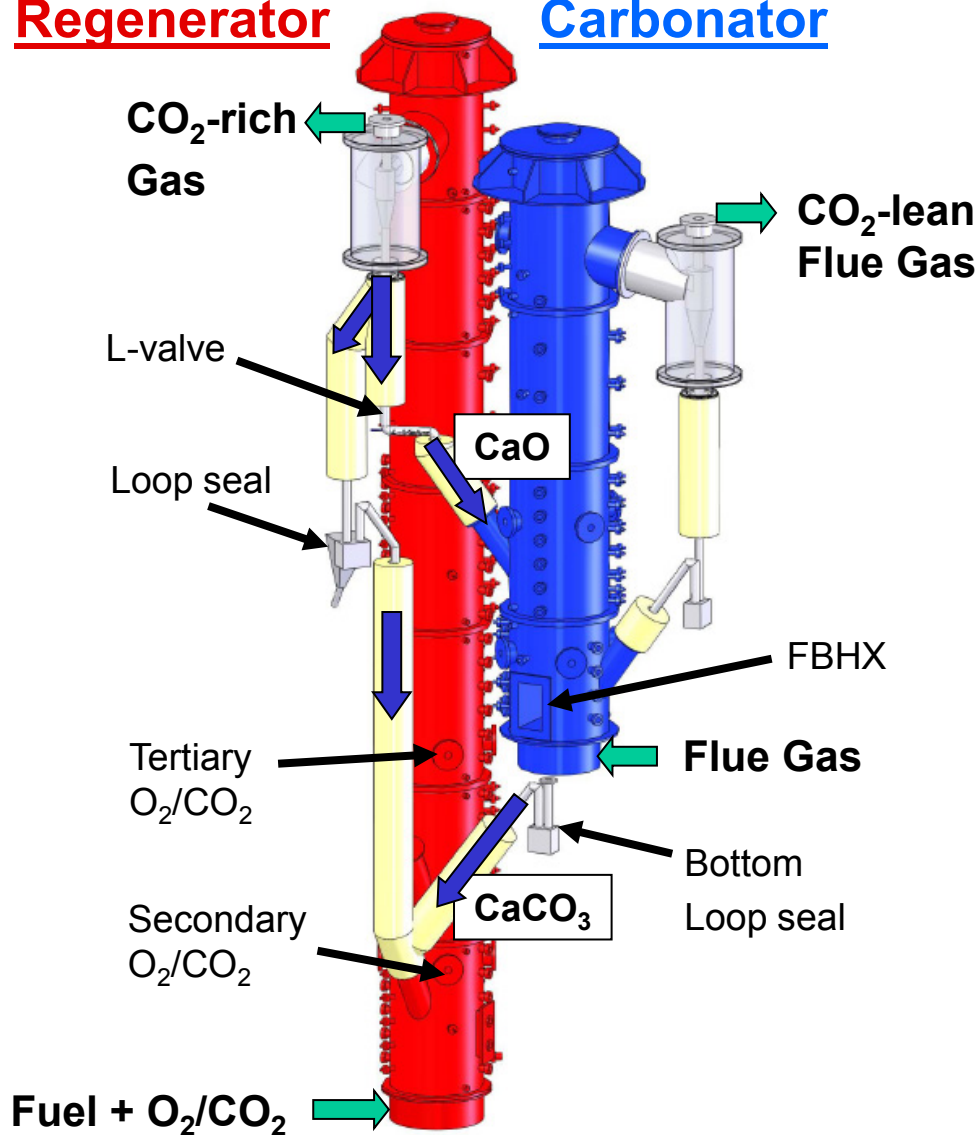
# R&D Calcium Looping Process Roadmap



# 200 kW<sub>th</sub> DFB Calcium Looping Plant

## Regenerator

## Carbonator



## Carbonator:

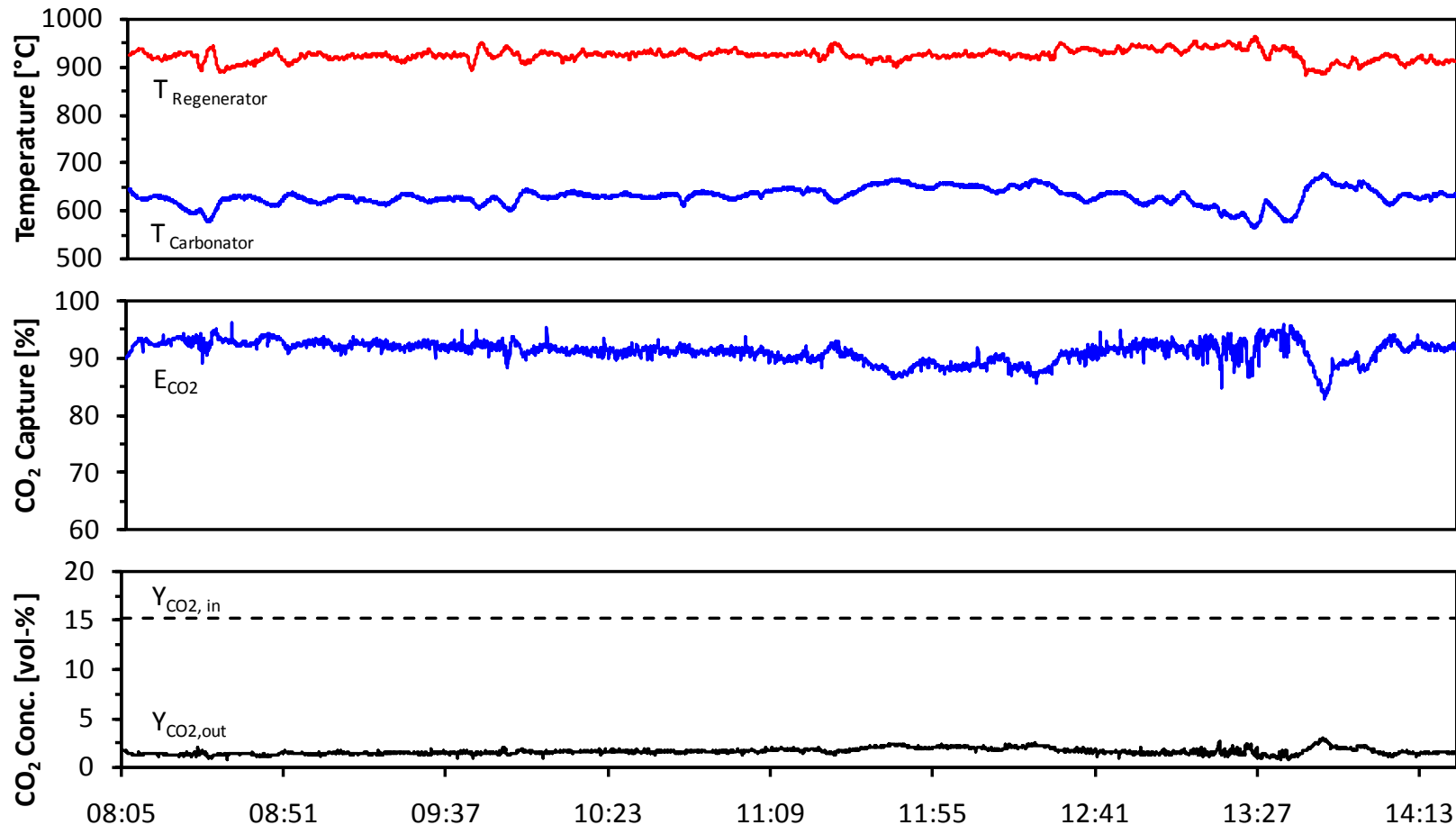
- Turbulent CFB Reactor
- Good gas-solid contact
- Lower entrainment than fast fluidized CFB
- Looping Rate controlled by L-valve
- Bottom loop seal regulates bed inventory
- Temperature controlled by Looping Rate and Fluidized Bed Heat Exchanger

## Regenerator:

- Fast fluidized CFB calciner
- Temperature controlled by oxy-combustion

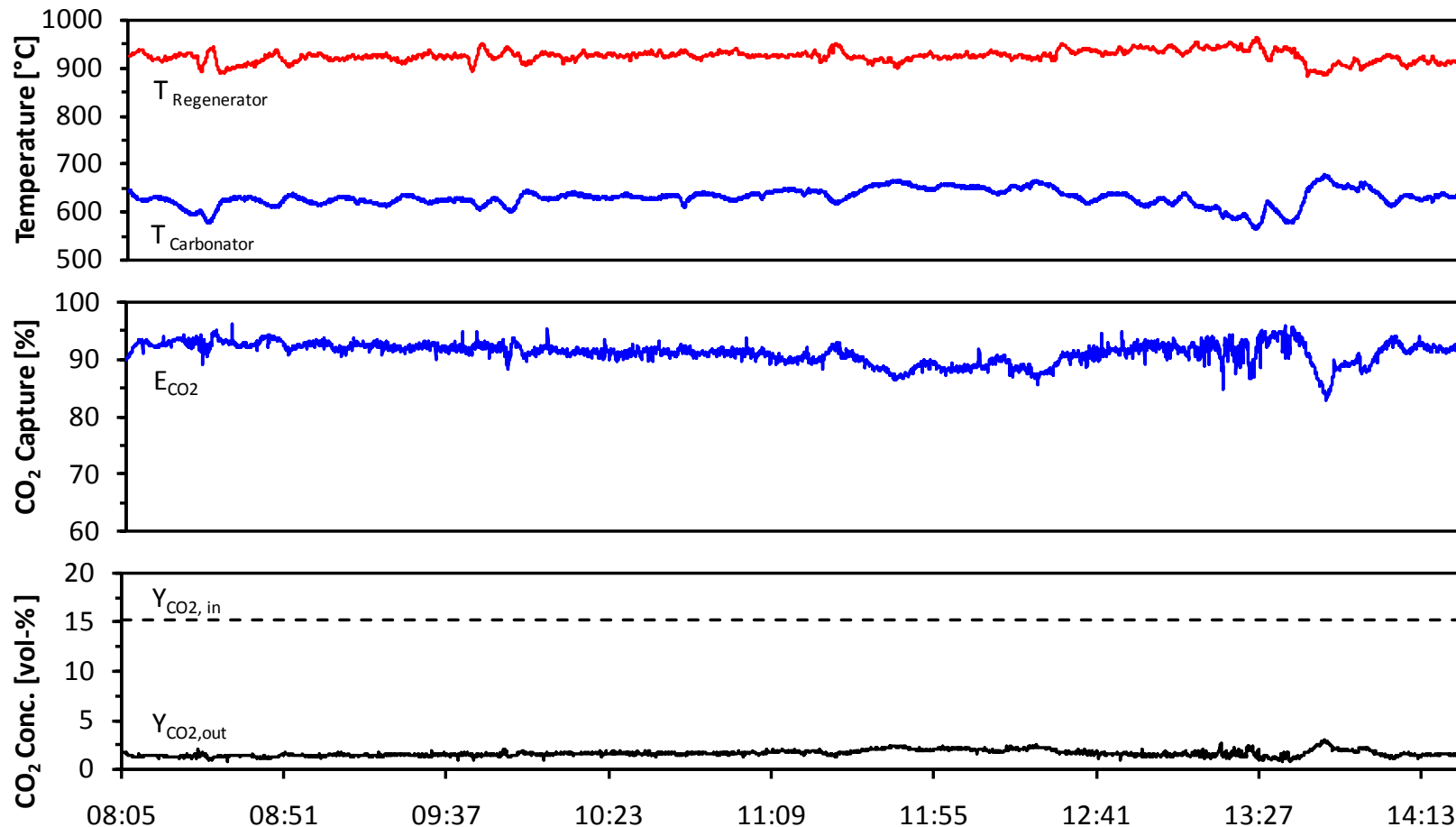
# Overview of Pilot Plant Operation

- 3 measurement campaigns completed with over 300 h of successful operation
- Dual Fluidized Bed system proved flexible and robust
  - Operated over a wide range of temperatures and looping rates
  - L-valve & loop seal system delivers stable sorbent looping rate



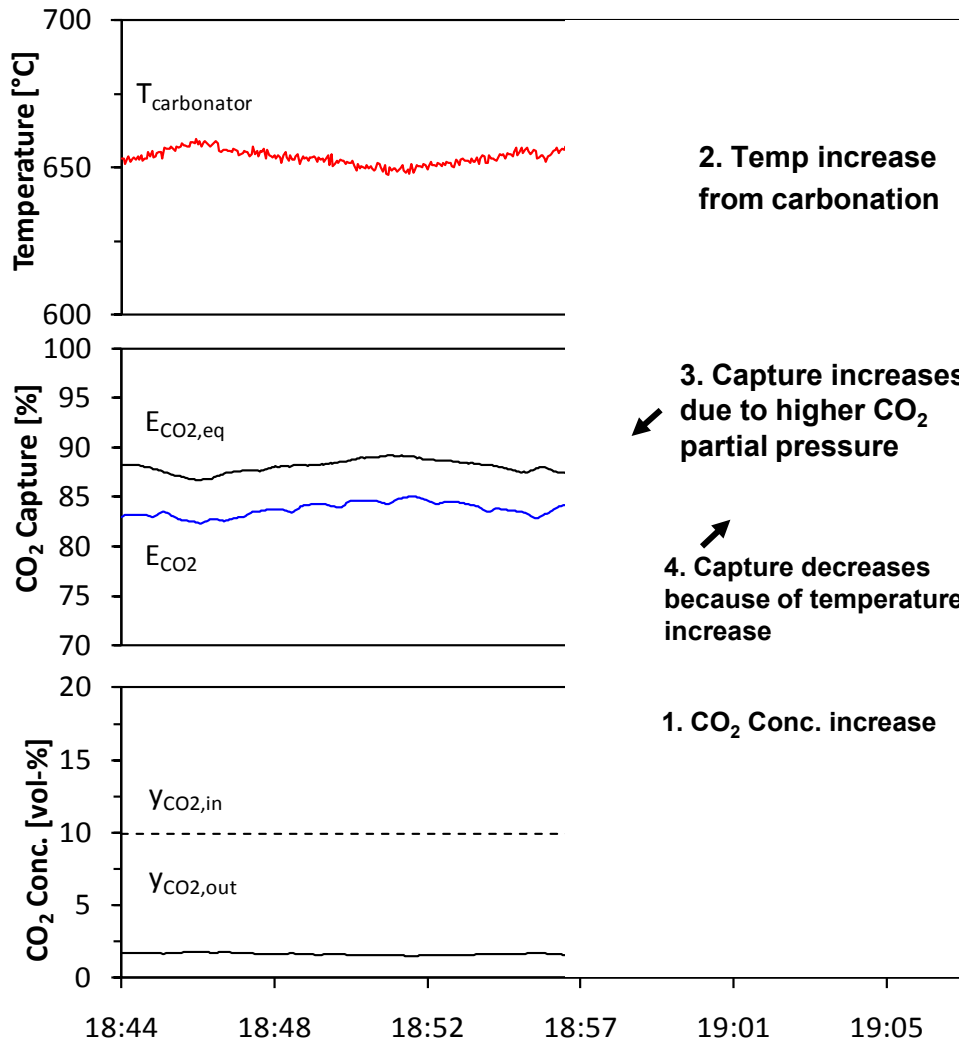
# Overview of Pilot Plant Operation

- **Over 90% capture efficiency** achieved over a wide range of operating conditions
- Oxyfuel Regenerator performed well as a combustor:
  - High fuel burnout (low CO), good controlability and uniform temperature profiles
  - Complete calcination of incoming carbonated sorbent and make-up  $\text{CaCO}_3$





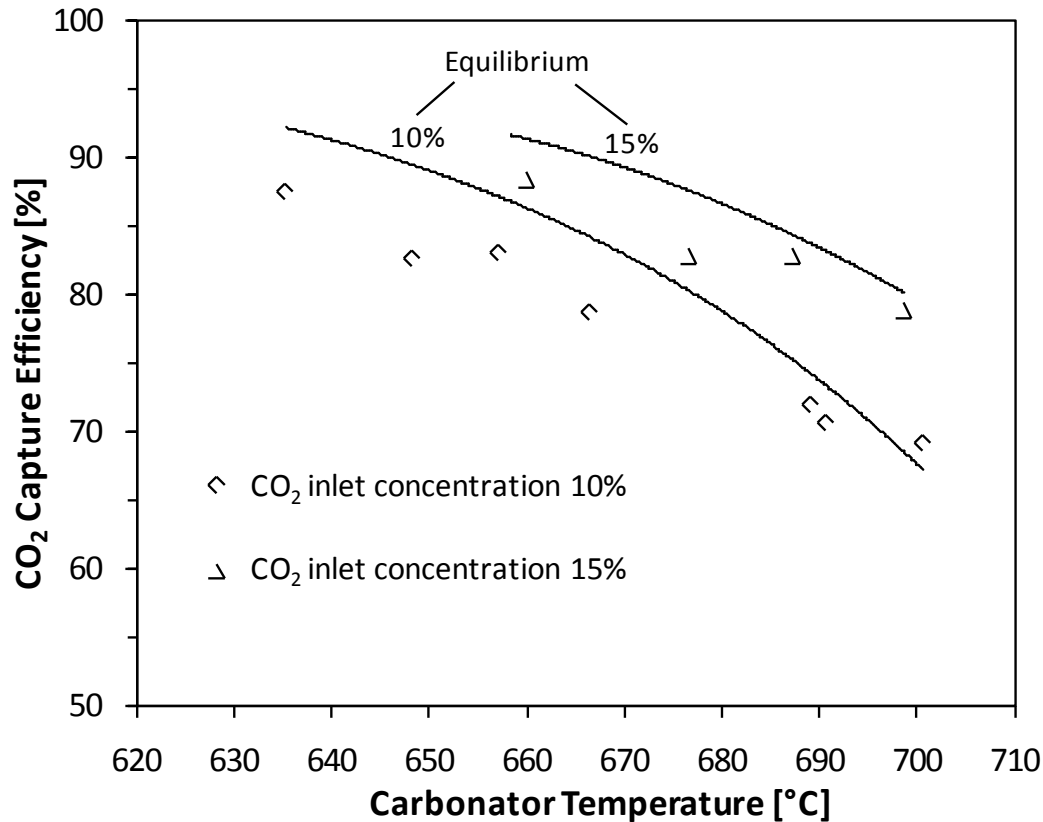
# System Response: Change in Inlet CO<sub>2</sub> Conc.



## Pilot plant operates as designed:

- Facility responds quickly to set point changes, e.g. inlet CO<sub>2</sub> vol.-% concentration
- Capture efficiencies are constant over time once system stabilized
- CO<sub>2</sub> capture close to equilibrium

# Results Summary: Effect of Temperature



**Every data point is a steady state where**

- Solid samples taken & analyzed
- Circulation rate measured
- CO<sub>2</sub> capture measured

**All capture efficiencies are close to maximum equilibrium value**

**Highest CO<sub>2</sub> capture achieved between 635-660°C for inlet concentrations of 10-15 Vol.-% CO<sub>2</sub>**

➤ **Over 90% capture efficiency in steady state pilot operation**

## **Calcium Looping process successfully demonstrated on a 200 kW<sub>th</sub> pilot facility:**

- CO<sub>2</sub> capture efficiency over 90 % achieved
- Plant showed robust performance and flexibility over 300 h of operation
- Full sorbent calcination in oxy-fired regenerator achieved
- Low sorbent loss due to attrition, i.e. ~ 5 wt.% bed/h

## **Recently obtained results and upcoming R&D topics:**

- Influence of Make-up and steam content in flue gas on CO<sub>2</sub> capture efficiency
  - Tests completed and will be published in the near future
- Influence of sulfur and coal ash on sorbent activity and pilot operation

# Acknowledgements

The results from the 200 kW<sub>th</sub> Calcium Looping pilot plant were produced as part of a joint university-industrial research & development project funded by EnBW Kraftwerke AG.

