

Enabling technologies for pre-combustion

TCCS-6

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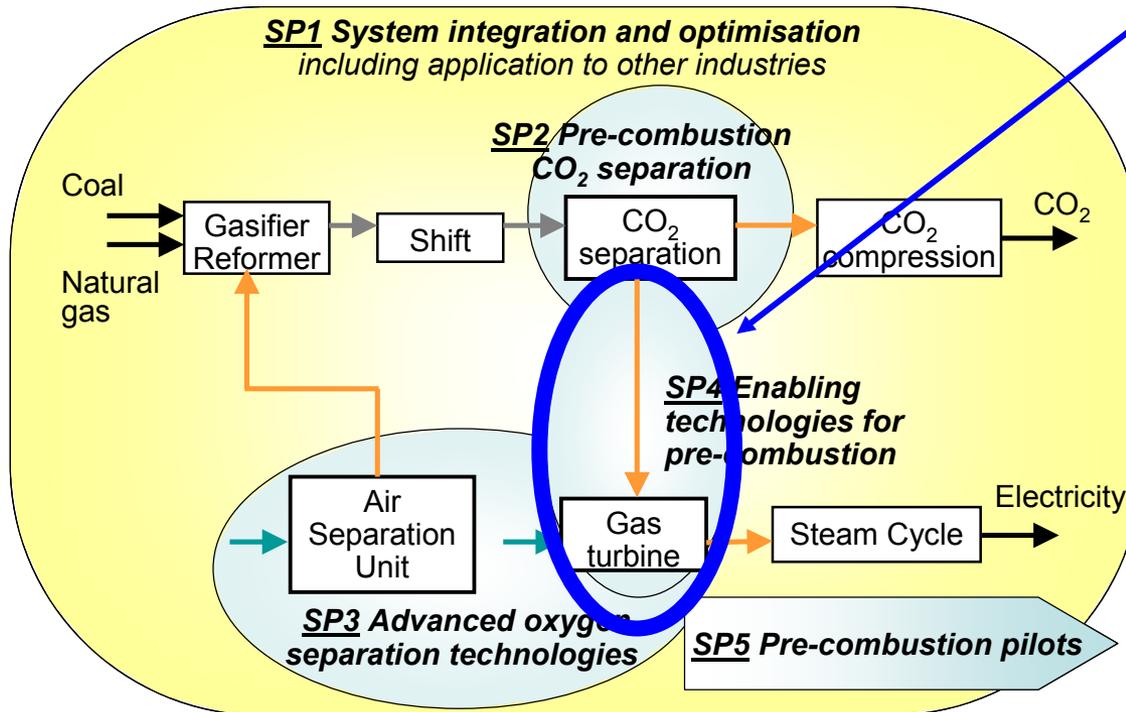
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Enabling technologies for pre-combustion

Hydrogen rich fuel supply and combustion



Outline

- Numerical methods for hydrogen combustion modeling



- Development of a lean premixed hydrogen gas turbine re-heat combustor



- Optimization of hydrogen rich fuel supply system

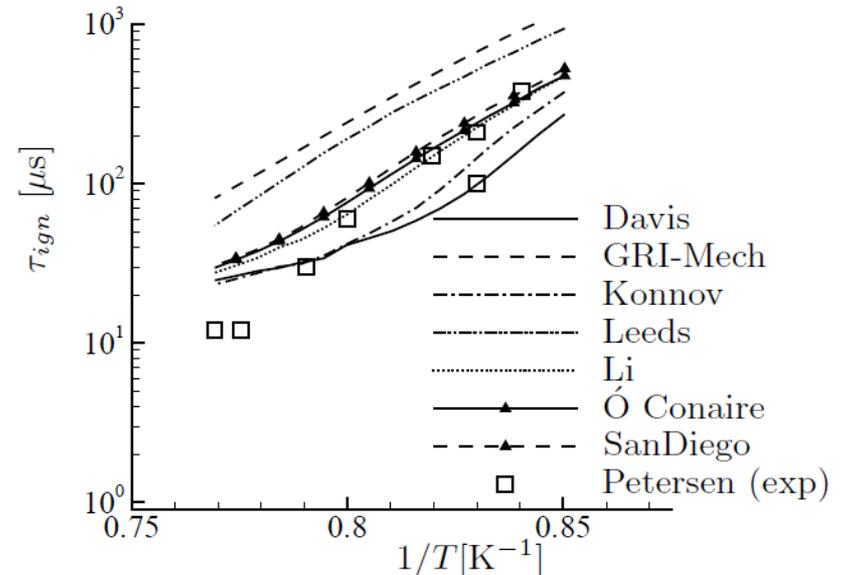


The Pencil-Code

- High order Direct Numerical Simulation (DNS) code
- Open source
 - <http://www.nordita.org/software/pencil-code/>
- Detailed chemistry combustion implemented
- No libraries required
 - Unix/linux
 - Fortran compiler
- [*Journal of Computational Physics* 230, 1-12 \(2011\)](#)
 - <http://arxiv.org/abs/1005.5301>

Chemical kinetics combustion model validated at LPM and SEV conditions

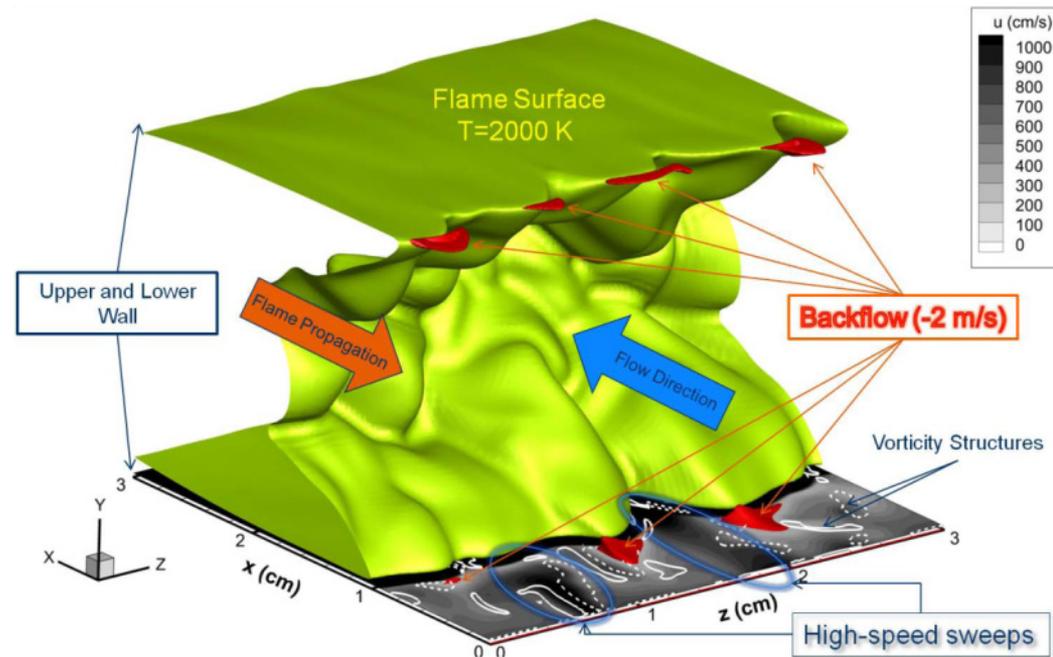
- **Background:** “Operation of SEV burners involves accurate knowledge and monitoring of both flame speed and ignition delay time.”
- **Results:**
 - H₂ chemical kinetic models have been compared and partly validated at the high temperature and pressure conditions (up to 30 bar) relevant to LPM and SEV conditions.
 - At these conditions the mechanisms that are thoroughly validated for hydrogen at lower pressures, predict a factor 3 different ignition delay times.
 - To reduce the uncertainties in predictions with hydrogen mechanisms at the high temperature and pressure condition more experiments are needed.



Ignition delay results with 2% H₂, 1% O₂, 97% Ar at 33atm. Comparison of predictions with various chemical mechanisms and shock tube data of Petersen et al.

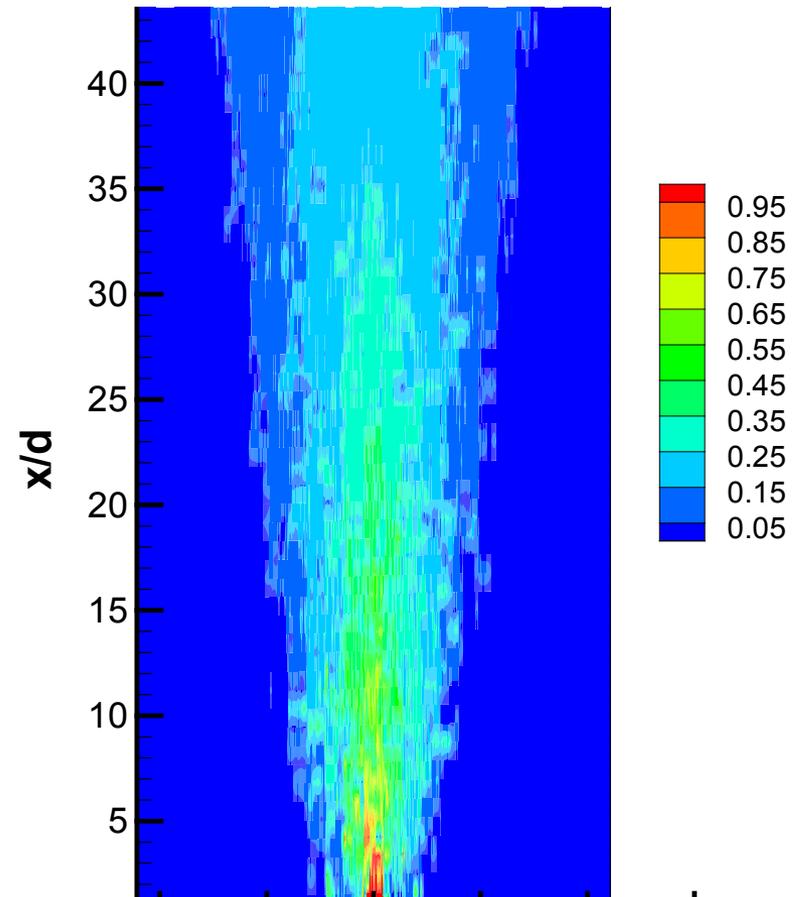
Provide fundamental combustion data for H₂-rich fuels at high temperature and high pressure

- **Background:** "Direct Numerical Simulations (DNS) may be seen as a numerical experiment as nothing except the chemical kinetics is modeled"
- **Results:**
 - DNS of flames propagating in isotropic decaying turbulence have been performed to find the dependence of the turbulence on the turbulent flame velocity
 - DNS of flame propagating in a turbulent channel flow shows the mode of propagation.



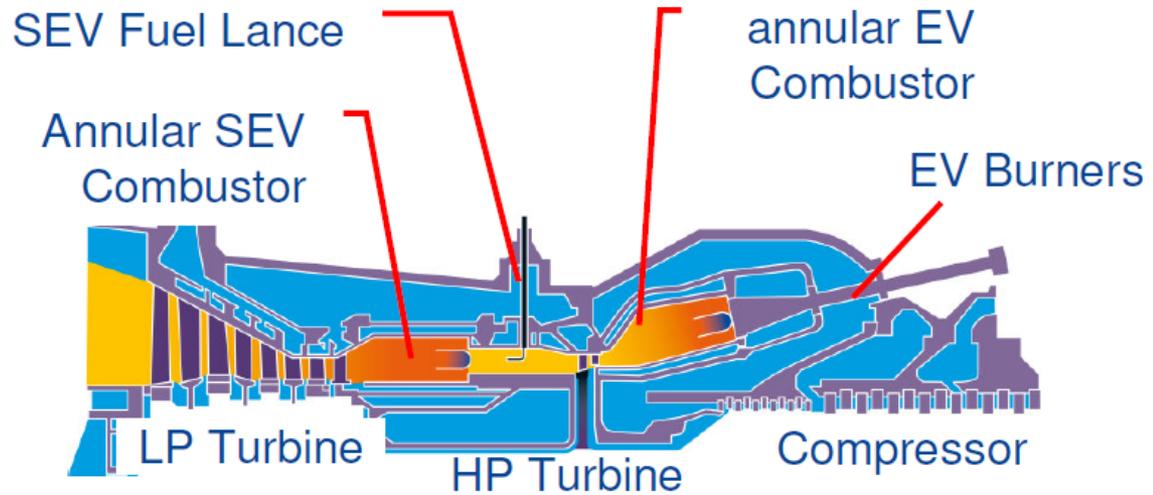
Improved combustion model: Linear Eddy Model (LEM3D) integrated with RANS

- **Background:** “LEM3D provides high fidelity resolution at a significantly lower cost than Direct Numerical Simulation (DNS)”
- **Results:**
 - The LEM3D mixing-reaction model has been coupled to the in-house CFD-code SPIDER and with FLUENT through User Defined Functions (UDFs)
 - The coupled model LEM3D-RANS has been verified against experimental data for the turbulent non-premixed jet flame denoted DLR A.

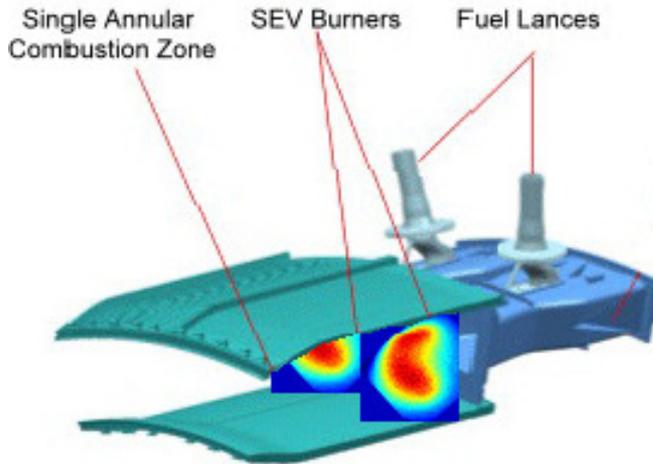


Snapshot of LEM3D-RANS simulation:
Mixture fraction contours in a non-premixed
turbulent jet flame (DLR-A)

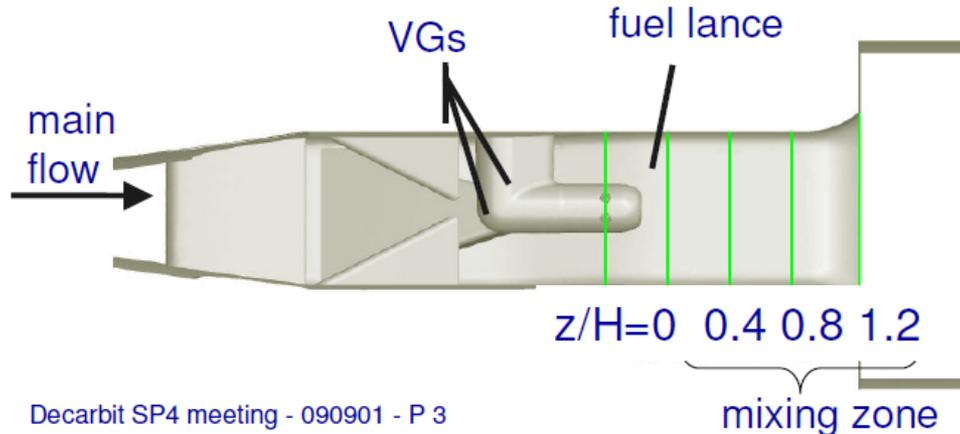
Alstoms GT24/GT26



EV = **EnV**ironmental
SEV = **Se**quential **EnV**ironmental



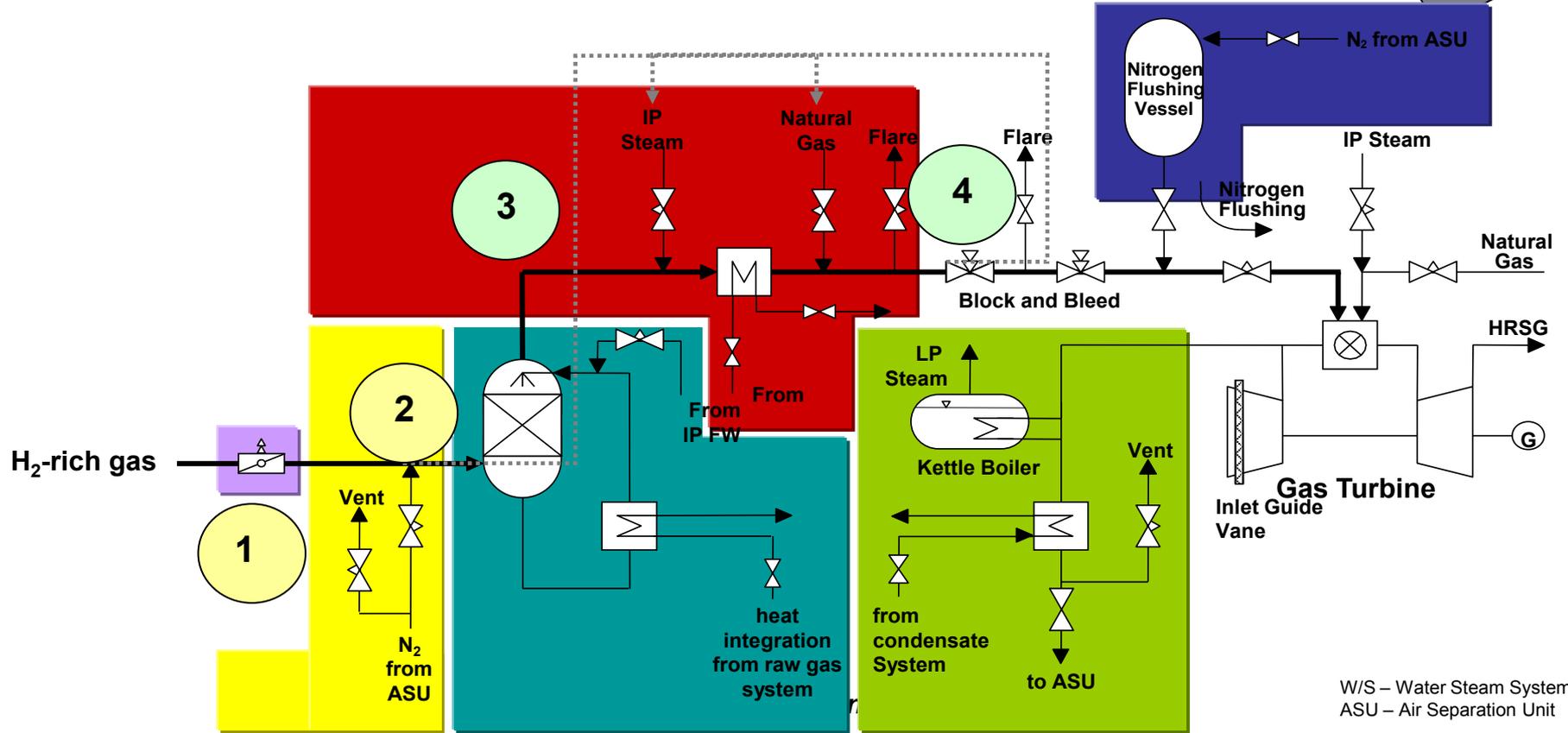
VG: Vortex generator



Decarbit SP4 meeting - 090901 - P 3

Modular Fuel System for IGCC-CCS

To avoid corrosion, plant has to be drained and conserved with inert gas after shut down.



Selection of piping and sealing materials

- Material Selection for Section 1 and Section 2: carbon steel 1.5415 / 1.0425 / 1.0345. CO has no effect on carbon steel due to low T, no H₂O.
- Section 3: Austenitic stainless steel necessary: 1.4571 / 1.4404 since condensed water can not be avoided (dissolution of CO₂ in H₂O)
- Section 4: Austenitic stainless steel favorable: 1.4571 / 1.4404. H₂O condensation and formation of H₂CO₃ can occur at start up or shut down

		1	2	3	4
		Clean syngas at entry Syngas Fuel System	after Waste-N ₂ admixing	after saturation by water	Diluted and saturated Syngas after overheating
Composition [vol %]	H ₂	85,32	46,34	42,54	42,54
	N ₂	8,37	49,45	45,40	45,40
	Ar	1,04	0,69	0,64	0,64
	H ₂ O	-	-	8,20	8,20
	CO	4,76	2,59	2,37	2,37
	CO ₂	0,50	0,27	0,25	0,25
	CH ₄	0,01	0,01	0,00	0,00
	O ₂	-	0,65	0,60	0,60
	others	-	-	-	-
p [bar(a)]		25,25	25,25	25	24,5
T [°C]		28	86,4	119,1	200
m_punkt [Kg/s]		20,508	100,83	110,895	110,895
LHV [MJ/kg]		36,436	7,411	6,796	6,796

Selection of piping and sealing materials (2)

- Hydrogen embrittlement is no substantial problem since H₂ partial pressures and maximum temperatures are too low
- In the presence of CO, carbon steel (section 1&2) can suffer from Carbonyl formation (Fe(CO)₅), S is catalyst, Carbonyls less problematic for IGCC-CCS
- Inconel Alloy 82 (or similar) as joining (carbon – austenitic)

Auto-oxidation effects and self ignition

- Auto-oxidation experiments with plug-flow reactor made of stainless steel 1.4517 (selected material) at atmospheric pressure
 - For residence times in a realistic modular fuel system (ca. 4 s) only 3% of the residual oxygen (3 vol%) will be consumed by auto-oxidation
 - Only traces of ammonia are found due to the presence of about 2 % carbon monoxide that acts as a catalyst poison for this reaction. Equilibrium composition of a typical syngas contains more than 9 % ammonia; cannot be neglected for pre-combustion concepts with very high rates of carbon capture.
- Experimental self ignition tests up to 50 bar for 3 vol%, 4 vol% and 5 vol% oxygen in the syngas
 - No risk of self-ignition if oxygen < 3 vol% and $T < 400^{\circ}\text{C}$ (for typical pressure and syngas composition)

Optimised design of the fuel system

- Redundant pumps at saturator recommended (“saturator failure”)
- High packing size in saturator recommended (“saturator failure”)
- Moving steam admixing upstream of heat exchanger recommended (“saturator failure”)
- Moving NG admixing closer to gas turbine (“gasifier failure”)
- Ensure fast-switch-back function of gas turbine (“waste N2 failure”)

Conclusion

- Two high fidelity simulation methods previously only used for academic applications; Direct Numerical Simulations (DNS) and the three dimensional Linear Eddy Model (3D-LEM), have proven useful for guidance in development of industrial applications
- SIEMENS has studied safety, availability and material issues for the Hydrogen fuel supply system and have used the results to design an optimized fuel supply system.

The End

- Thank you for your attention!