

Solvent Reclaiming by Sulfate Precipitation

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Abstract

An important issue in post-combustion CO₂ capture is the accumulation of impurities in the lean amine solvent. In particular, trace amounts of sulfur dioxide (SO₂) can react with the amine to form a heat stable salt containing sulfate ions, which can accumulate and hinder the absorption and stripping capacity of the amine. Thus, sulfate removal is necessary to re-use the amine more efficiently. Crystallization reclaiming by precipitation of the sulfate is being studied for this purpose. K₂SO₄ solid solubility experiments were carried out for 2 m to 8 m PZ between temperatures of 25 °C and 80 °C, and an empirical model was developed for the solubility of K₂SO₄:

$$\ln(K_{sp}) = 5.55 \cdot I_{0.3} - 1.17(\text{eq. mol amine}) - 4630/T + 8.96.$$

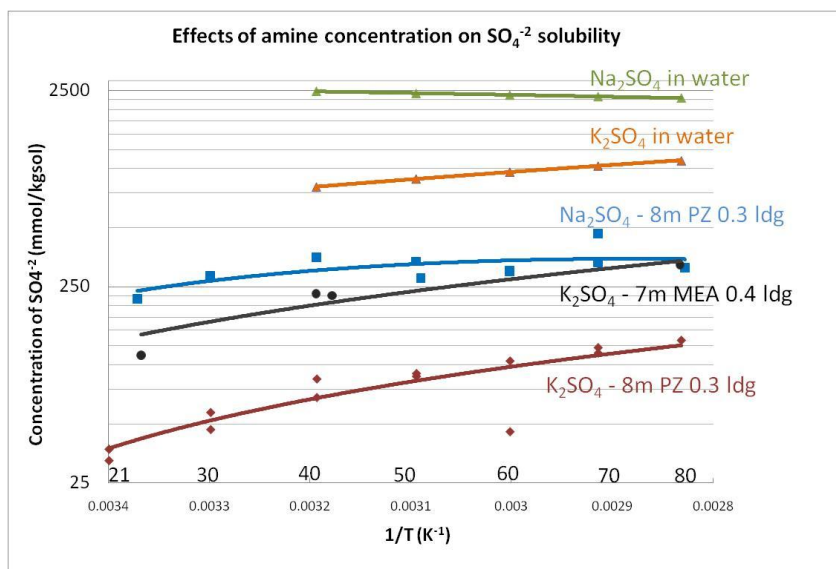
A similar equation for the solubility of Na₂SO₄ in PZ is also developed.

Excess salt was added to the PZ solution. The temperature of the solution varied between room temperature and 80 °C. Solution was sampled using a filtered syringe and diluted in DDI water to prevent crystallization. Experimental samples were analyzed for Na⁺, K⁺, SO₄⁻², CO₂, and PZ concentrations in the cation chromatograph, anion chromatograph, and TIC.

As shown in Figure 1, Na₂SO₄ is more soluble in PZ than K₂SO₄.

For both salts, the solubility has a greater dependence on amine concentration than temperature. If SO₄⁻² is the main impurity in the CO₂ capture system, the amine removed for reclaiming can be concentrated to high

Figure 1 Comparison of Na₂SO₄ and K₂SO₄ solubility in 8 m PZ



PZ concentrations at high temperatures (without affecting the solubility of SO_4^{-2} in PZ). This way SO_4^{-2} along with the other heat stable salts present can be removed together in a single thermal reclaiming procedure.