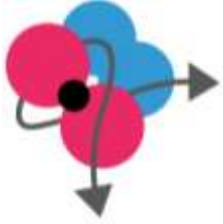


ELEGANCy

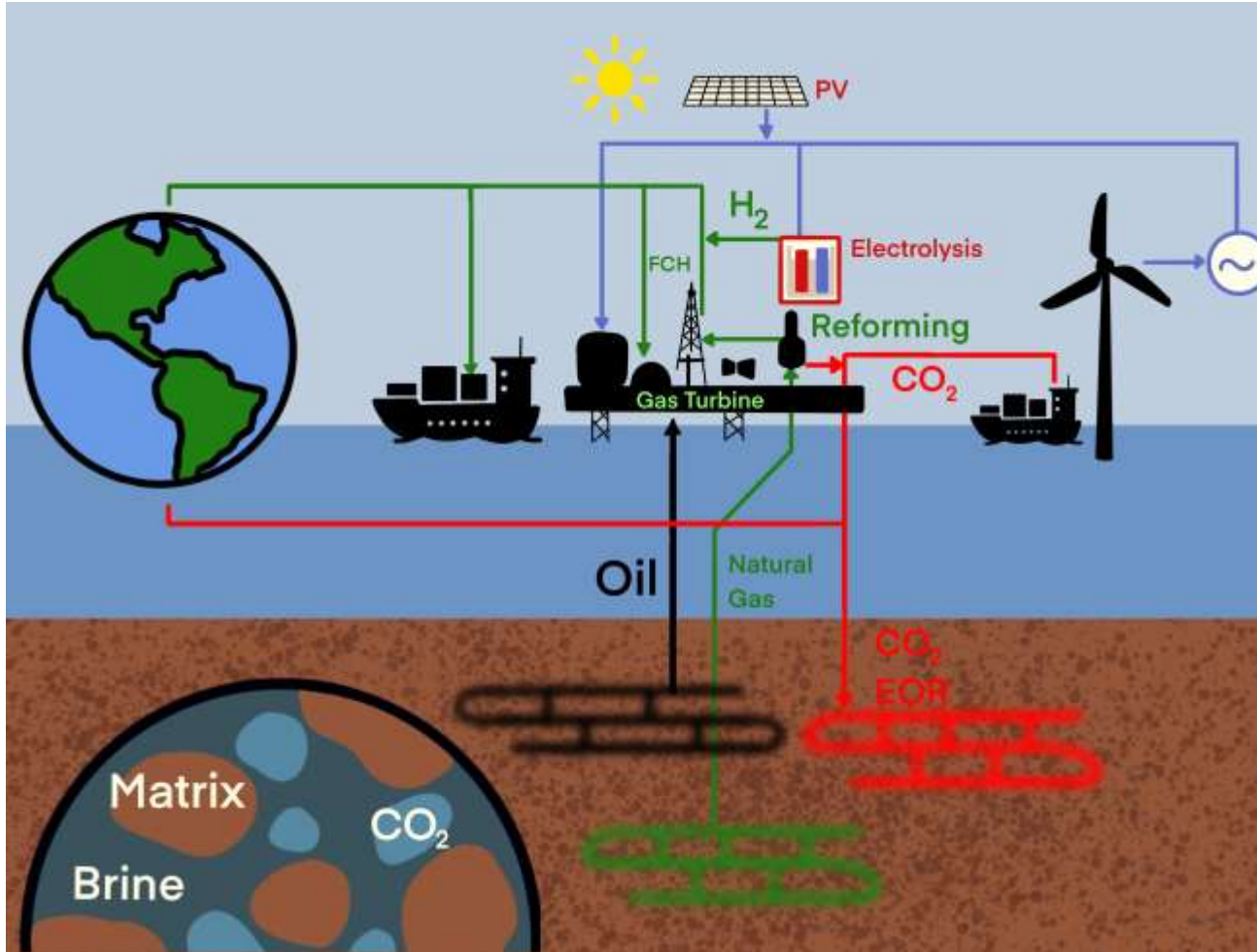
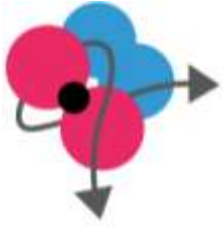
Solubility of Hydrogen in Brines Under Geological-Storage Conditions

Geraldine Torín-Ollarves

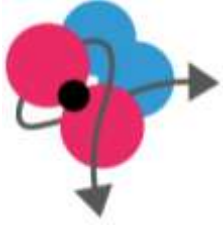
TCCS-10, Trondheim, 19th June 2019



- Motivation and background
- Experimental work
- Modelling approaches
- Conclusions and Future work

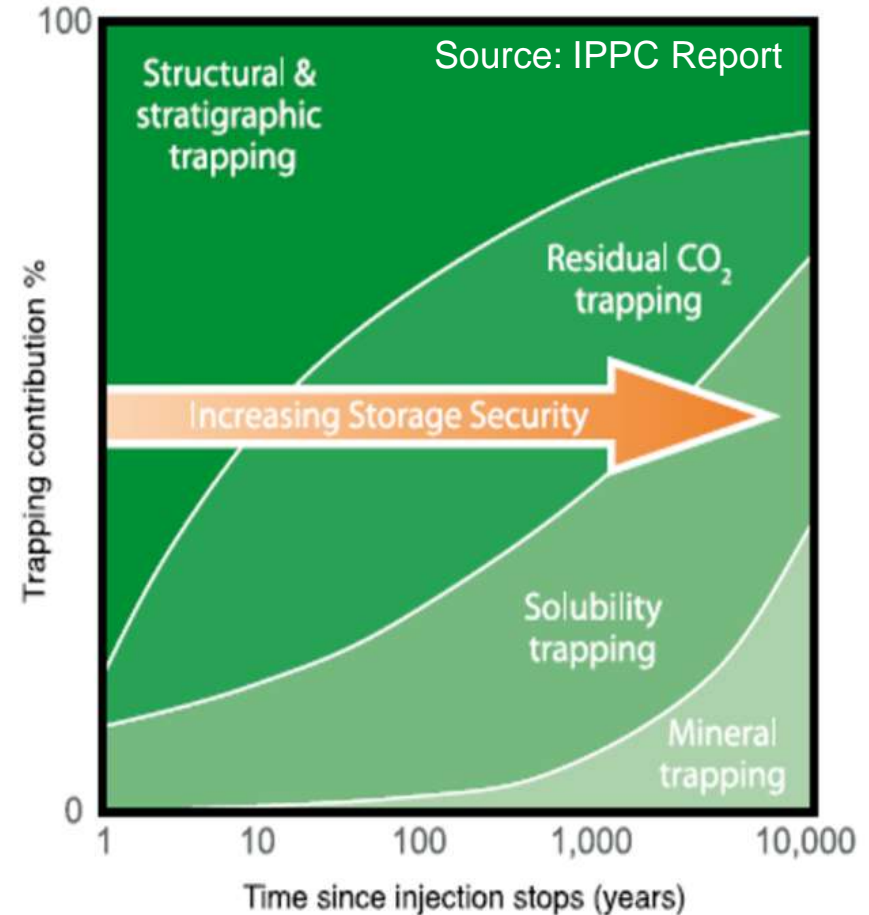


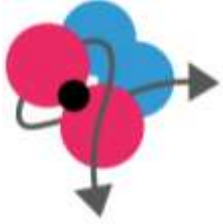
- ELEGANCY: coupling H₂ production with CCS
→ impure CO₂ for storage
- Imperfect separation processes
→ impure CO₂ for storage
- H₂ impurity especially important
- Important to understand role of impurities in transportation and **storage**



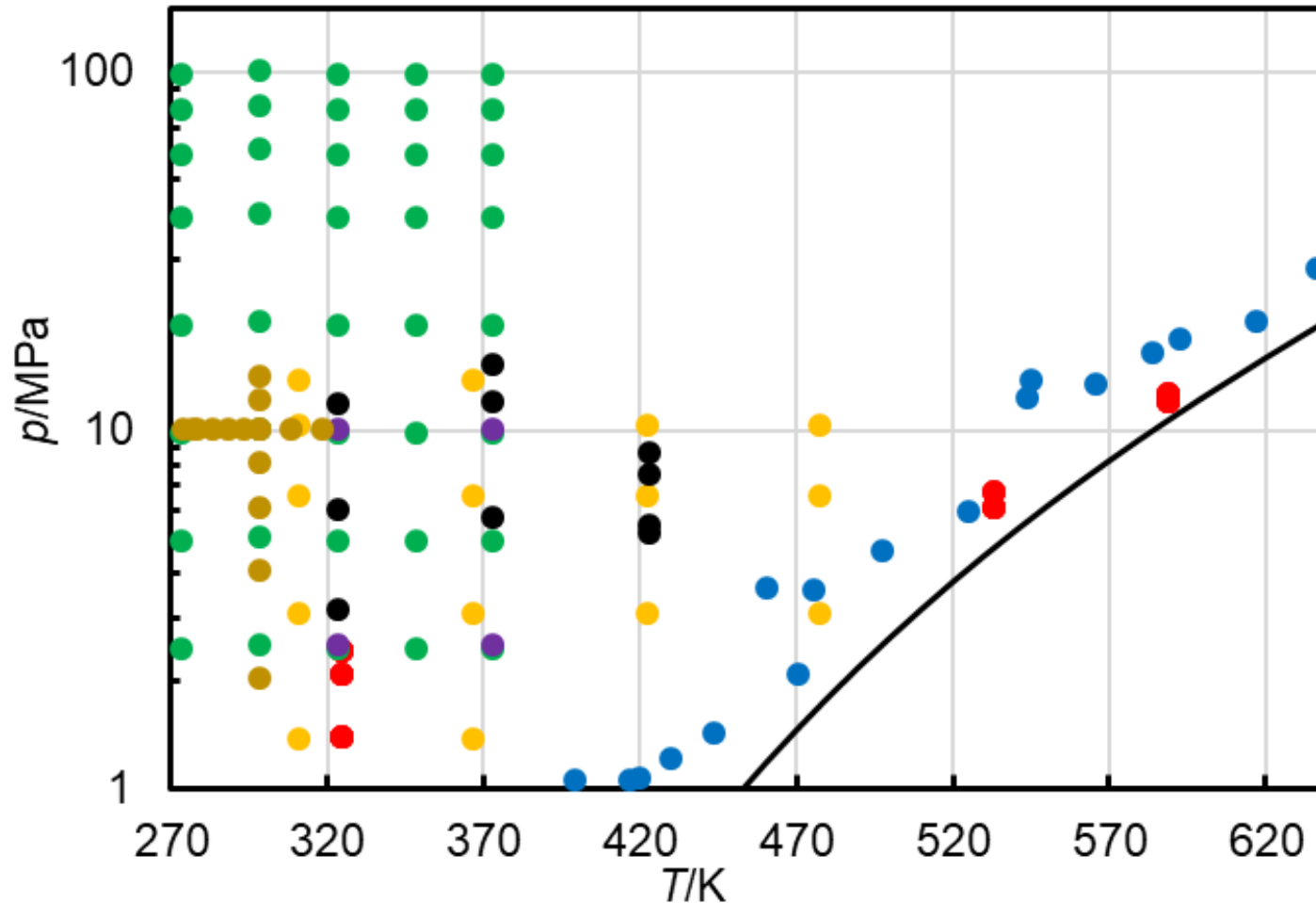
Trapping mechanisms

- Structural trapping
 - Retention of mobile CO₂ below impermeable cap-rock
- Residual trapping
 - Retention of CO₂ as dispersed micro-bubbles within the pore space
- Solubility trapping
 - Dissolution of CO₂ into the native reservoir fluids
- Mineral trapping
 - Formation of carbonate minerals by chemical reaction

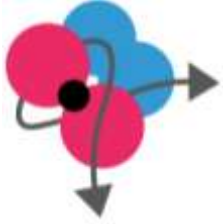




Available Experimental Data

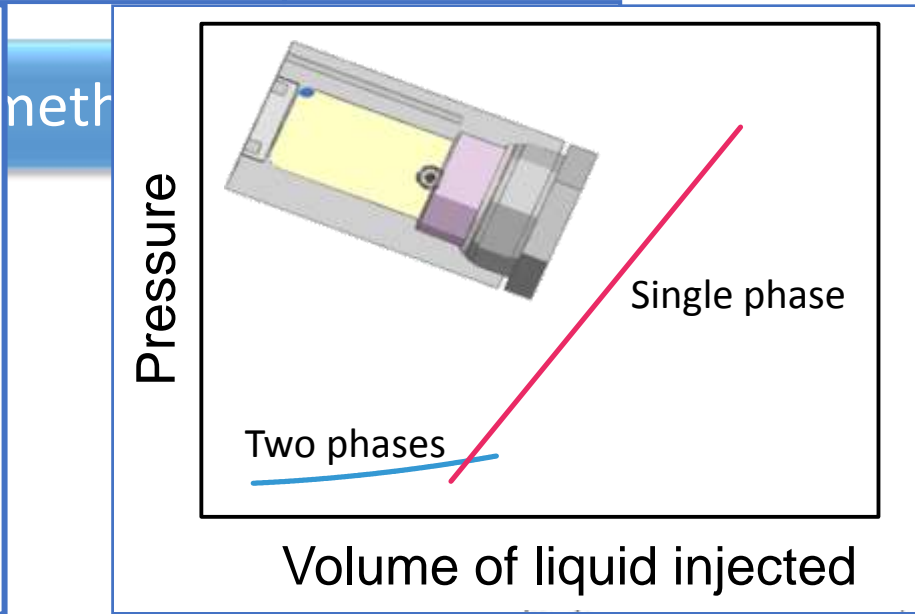
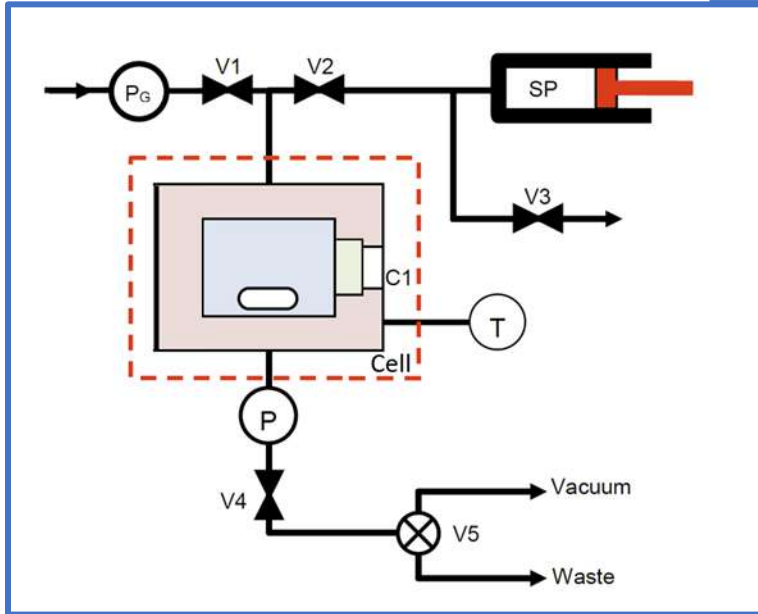


- Solubility of $\text{H}_2\text{O} + \text{H}_2$
(11 papers up to 550 K) - 1990
- Solubility of $\text{H}_2\text{O} + \text{CO}_2 + \text{H}_2$
(1 paper at 298 K) - 1939
- Solubility of H_2 in Brines
(No data)

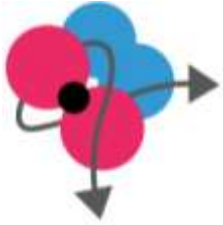


Experimental Approach

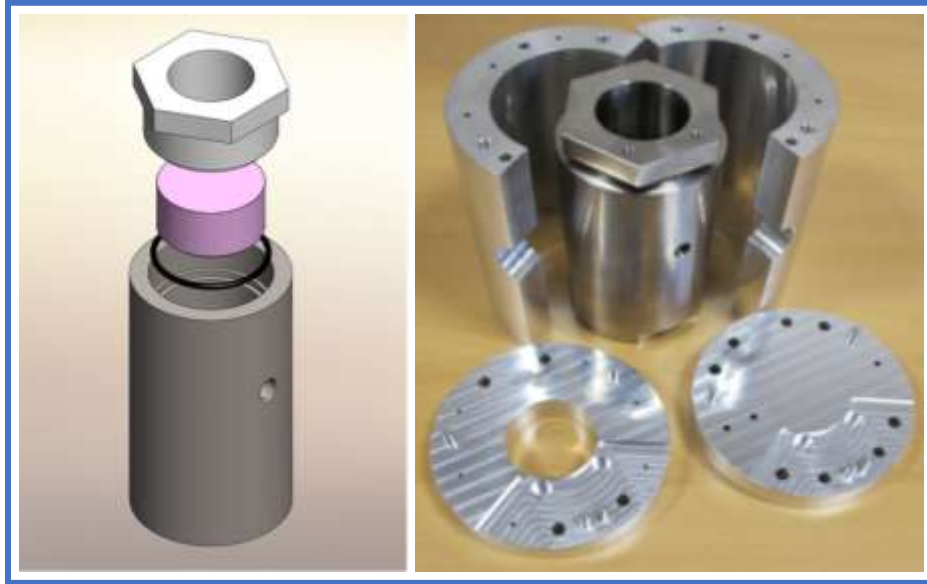
Experimental methods for high-pressure VLE



- Operation conditions: pressures ≤ 70 MPa and temperatures ≤ 473.15 K
- Fill gas \rightarrow inject liquid \rightarrow Disappearance of bubble \rightarrow PV analysis



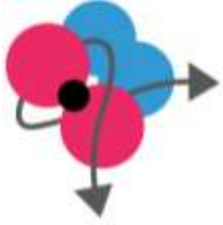
Apparatus Design



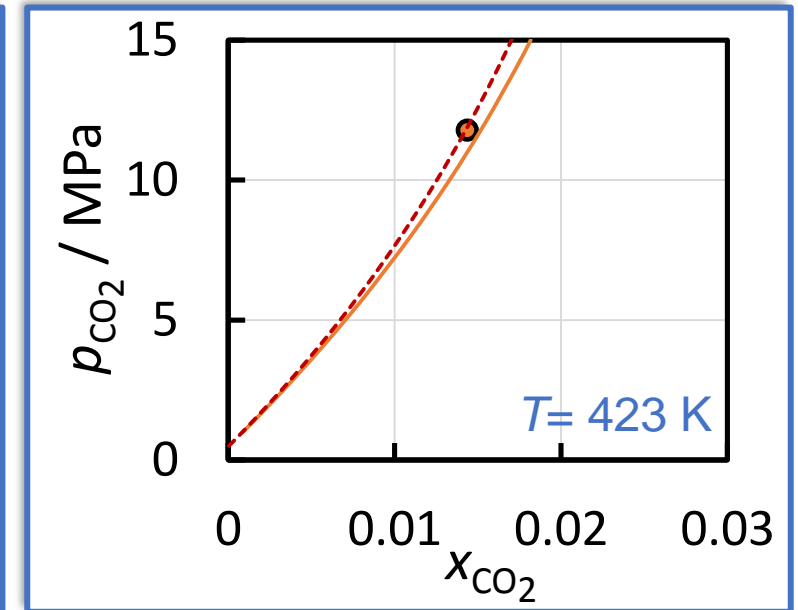
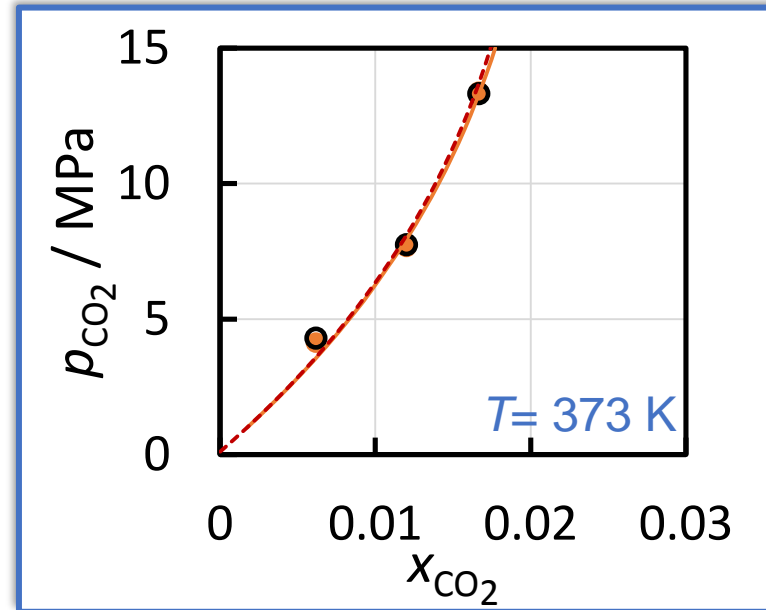
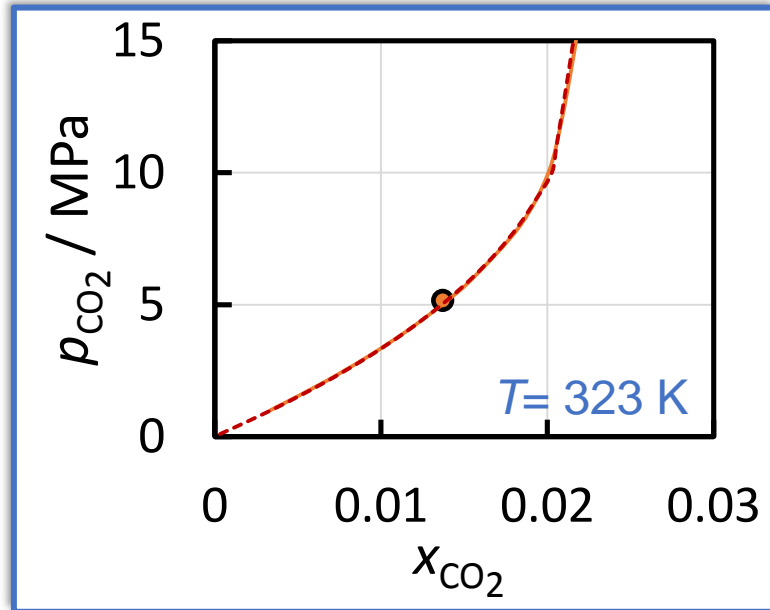
High-pressure view cell
and heated jacket



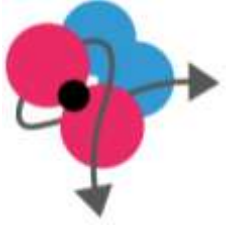
Assembled system



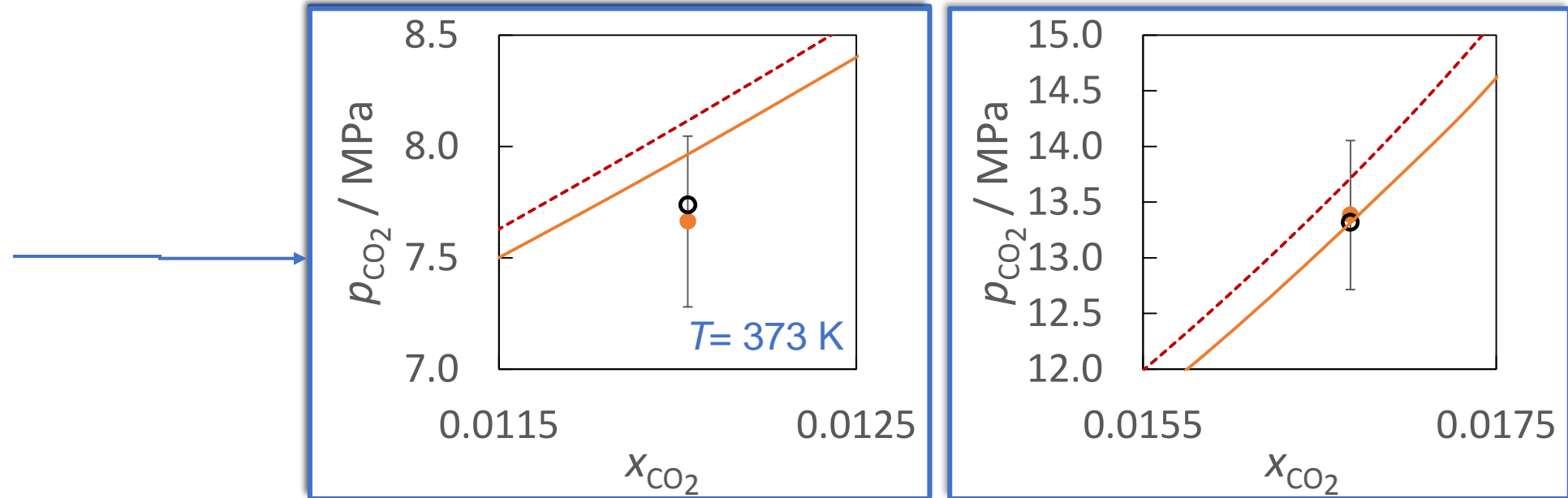
Validation: CO₂ solubility in H₂O



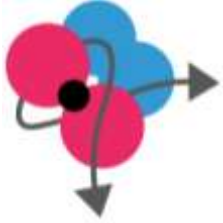
● PVT
 ○ Visual
 — Spycher-Pruess (2010)
 - - - Duan et al. (2006)



Validation: CO₂ solubility in H₂O



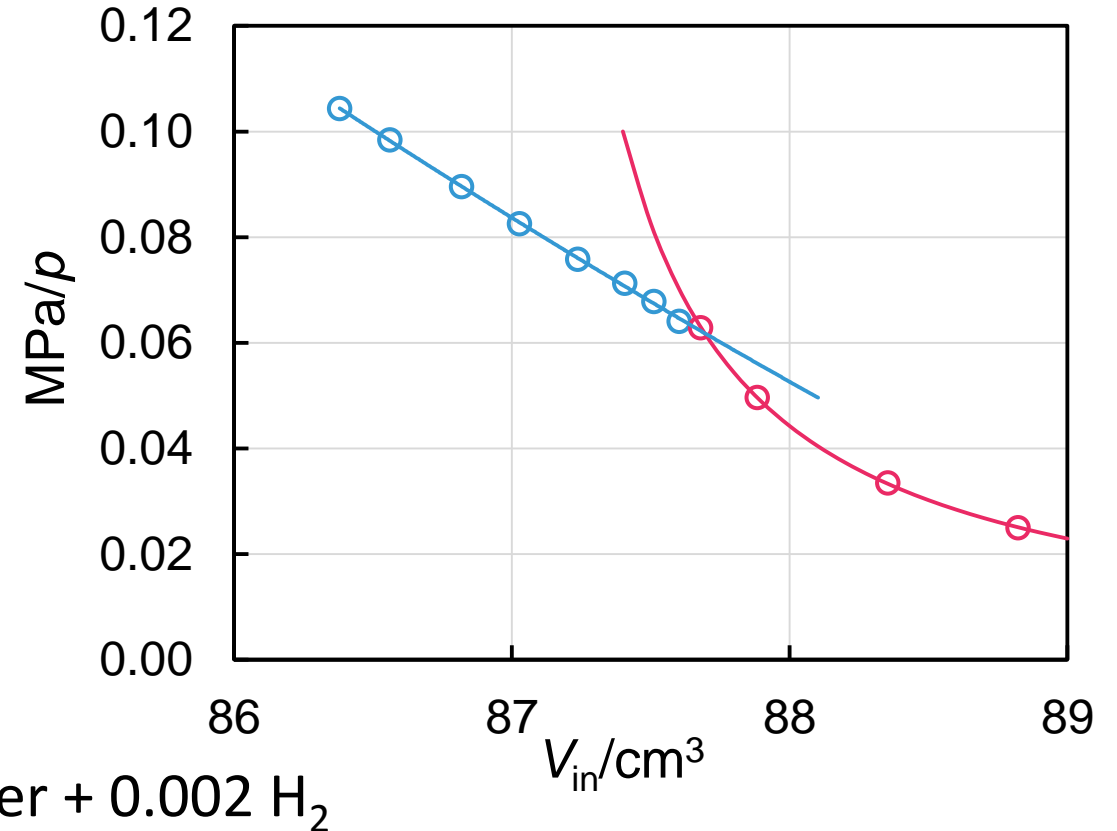
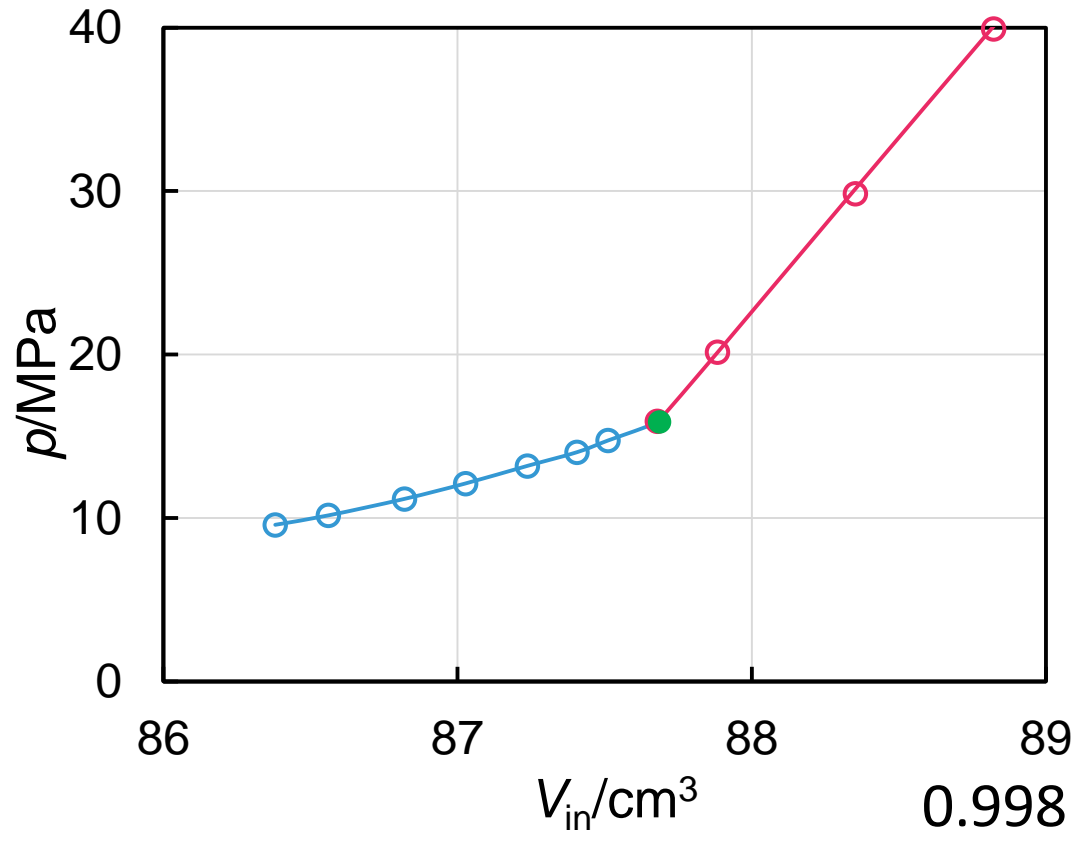
● PVT ○ Visual — Spycher-Pruess (2010) - - - Duan et al. (2006)



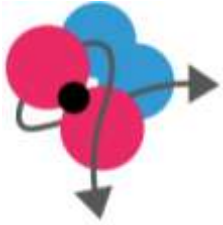
Synthetic Approach

- Visual Observation and PVT

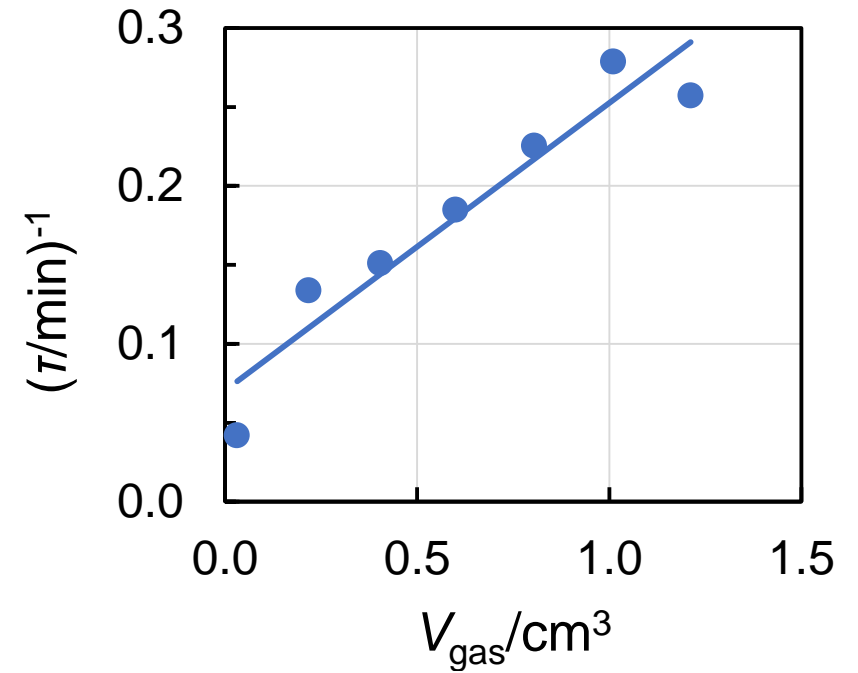
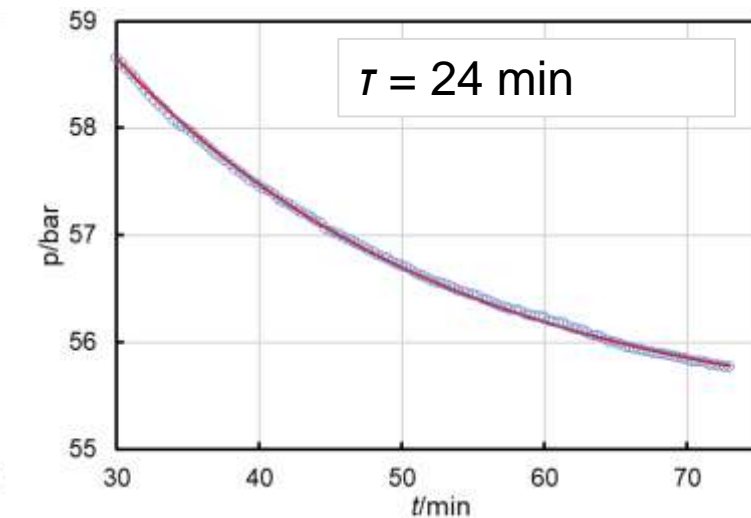
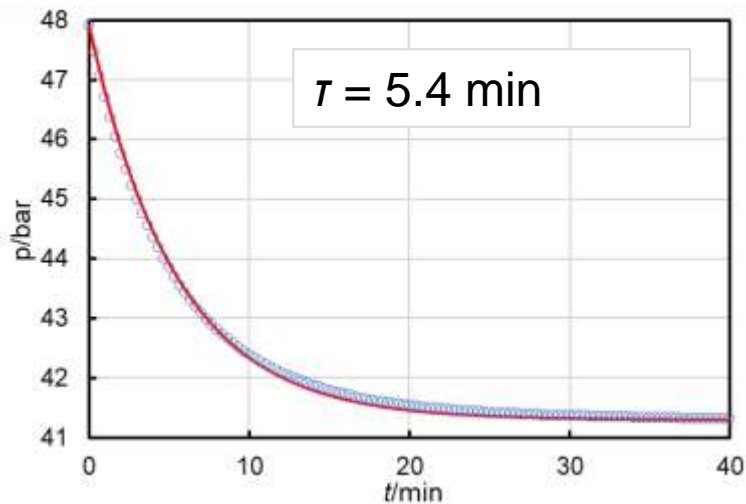
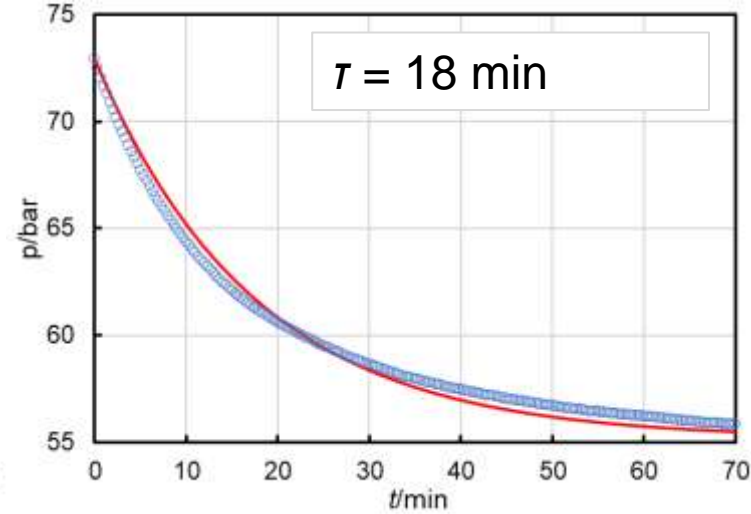
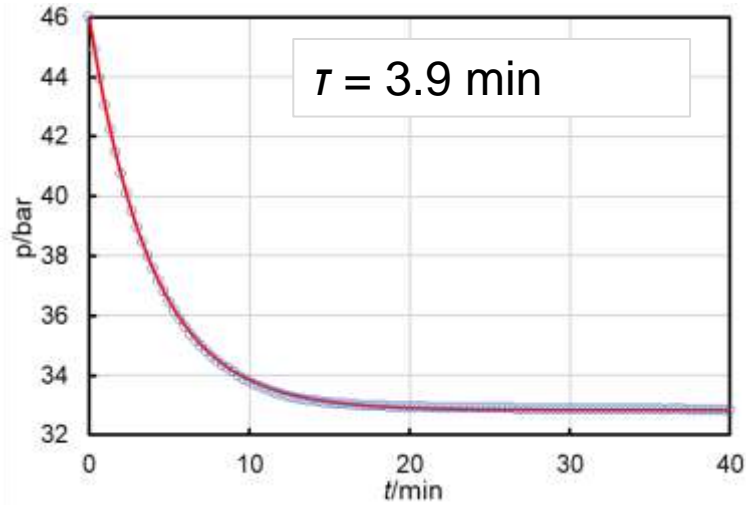
$T = 323.15 \text{ K}$



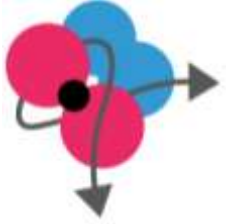
○ Experimental two phase
 ○ Experimental one phase
 — Model two phase
 — Model one phase
 ● Bubble point



Approach to Equilibrium

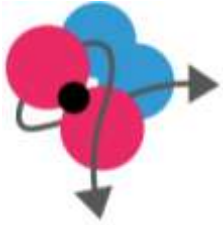


τ : Exponential decay constant

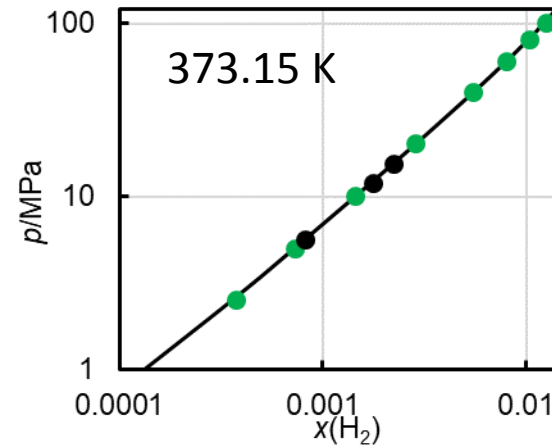
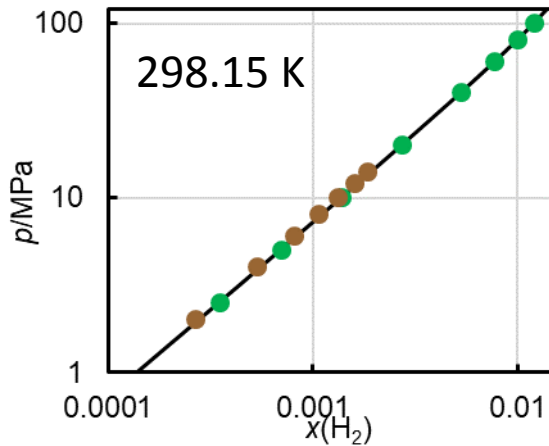
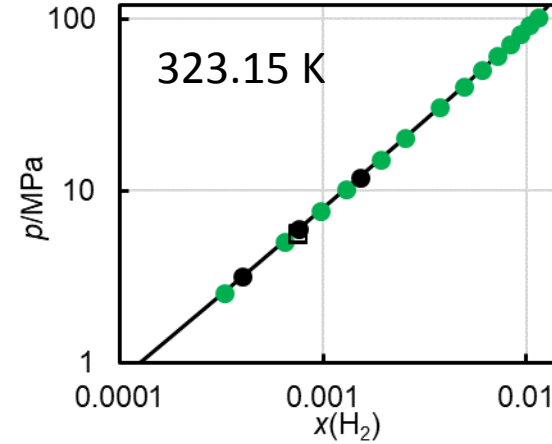
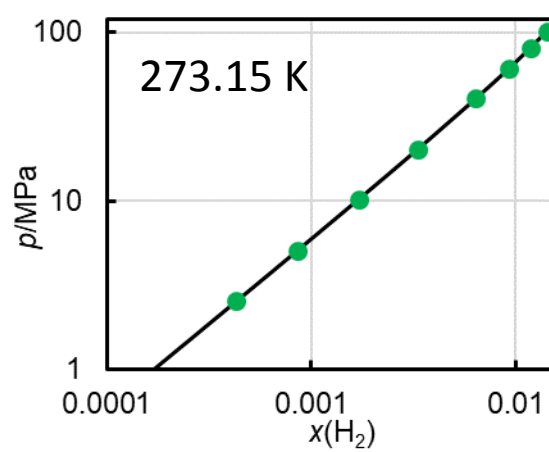


ELEGANCY: Thermodynamic Property Models

- Thermodynamic property models for injection and storage
 - To account for H₂ and other impurity gases
 - To account for salts in the aqueous phase
 - Experimental phase equilibria and phase properties required as inputs
- Model development: Ruhr-Universität Bochum
- Experimental measurements: Imperial College London

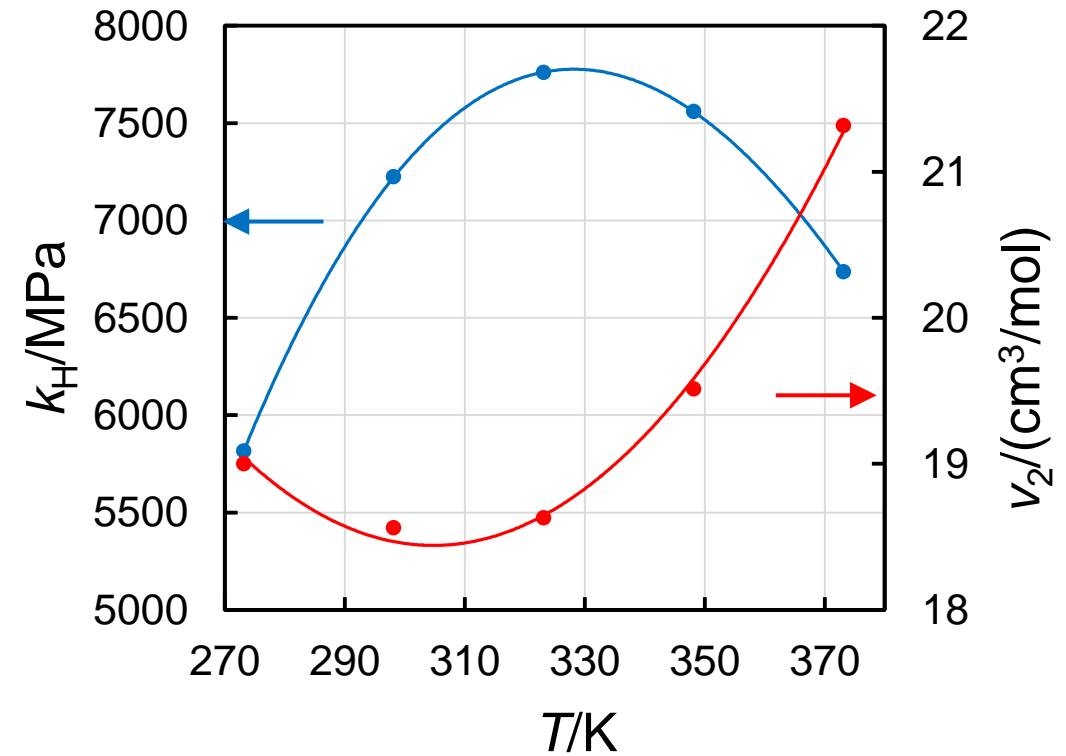


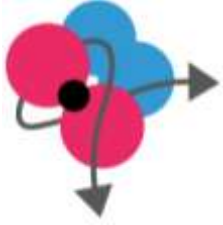
Modelling of H₂ solubility in H₂O: fitting H_{12} and v_1



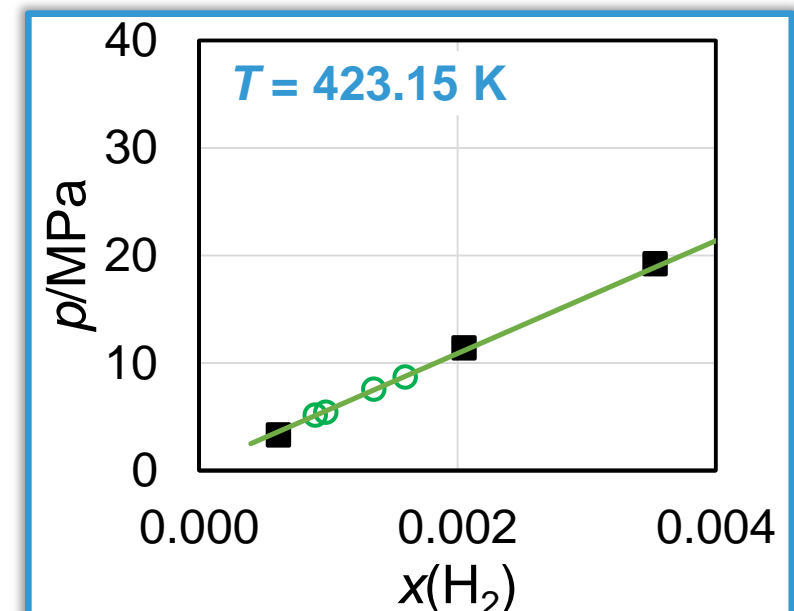
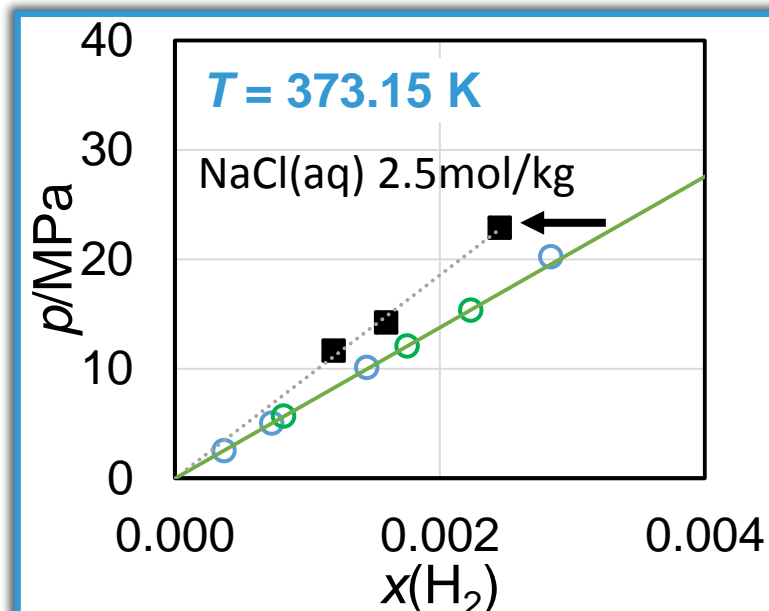
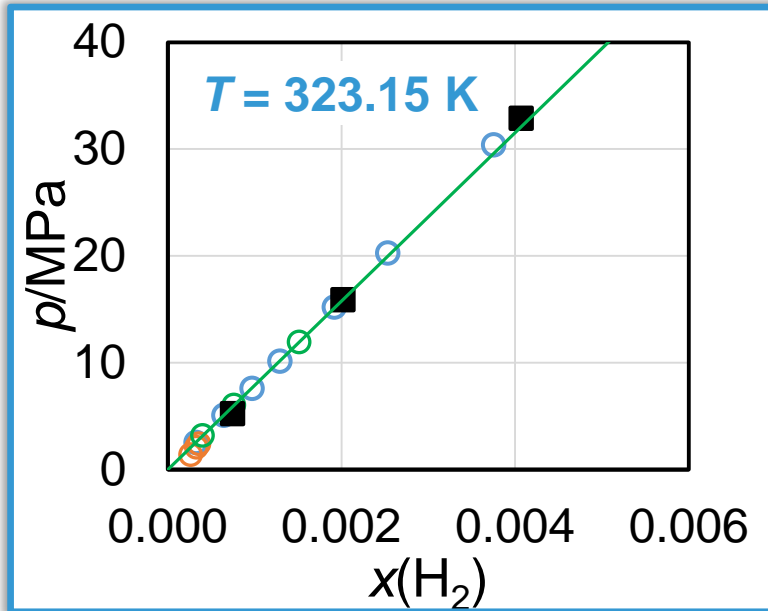
Krichevsky–Kasarnovsky equation

$$\ln(f_1/x_1) = \ln H_{12} + V_1^\infty(p - p_{\text{ref}})/(RT)$$





Experimental results: H₂ solubility in H₂O and brines

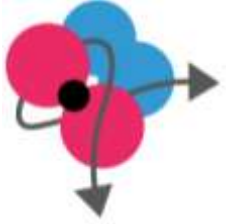


○ Wiebe & Gaddy (1934)

○ Pray et al. (1952)

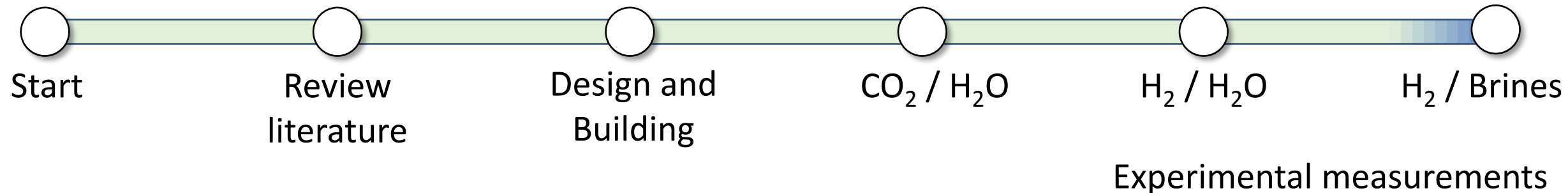
○ Kling & Maurer (1991)

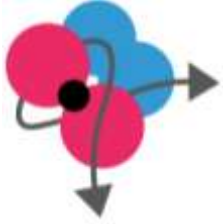
■ This work



Conclusions and Future work

- Validation of the system with CO_2 solubility in H_2O
- Experimental measurements on H_2 solubility in H_2O
- Measurements on solubility of H_2 in brines (NaCl 2.5 mol/kg) shows a salting out effect of 25%.





Acknowledgement

ACT ELEGANCY, Project No 271498, has received funding from DETEC (CH), FZJ/PtJ (DE), RVO (NL), Gassnova (NO), BEIS (UK), Gassco AS, Equinor and Total, and Statoil Petroleum AS, and is cofunded by the European Commission under the Horizon 2020 programme, ACT Grant Agreement No 691712.

