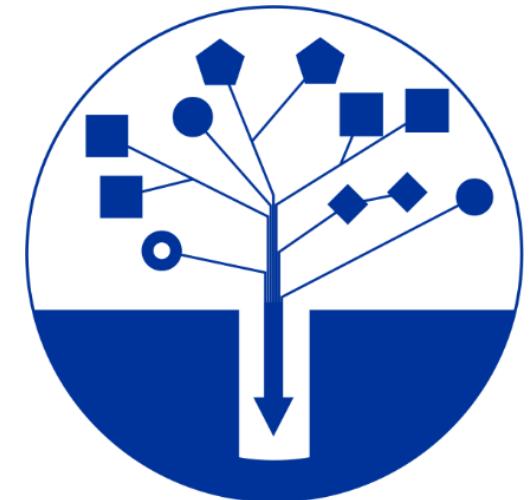


# Combining CO<sub>2</sub> streams from different emitters - a challenge for pipeline transportation



Le Quynh Hoa<sup>1</sup>, Sandra Knauer<sup>2</sup>, Dirk Bettge<sup>1</sup>, Ralph Bäßler<sup>1</sup>, Axel Kranzmann<sup>1</sup>, Heike Rüters<sup>3</sup>

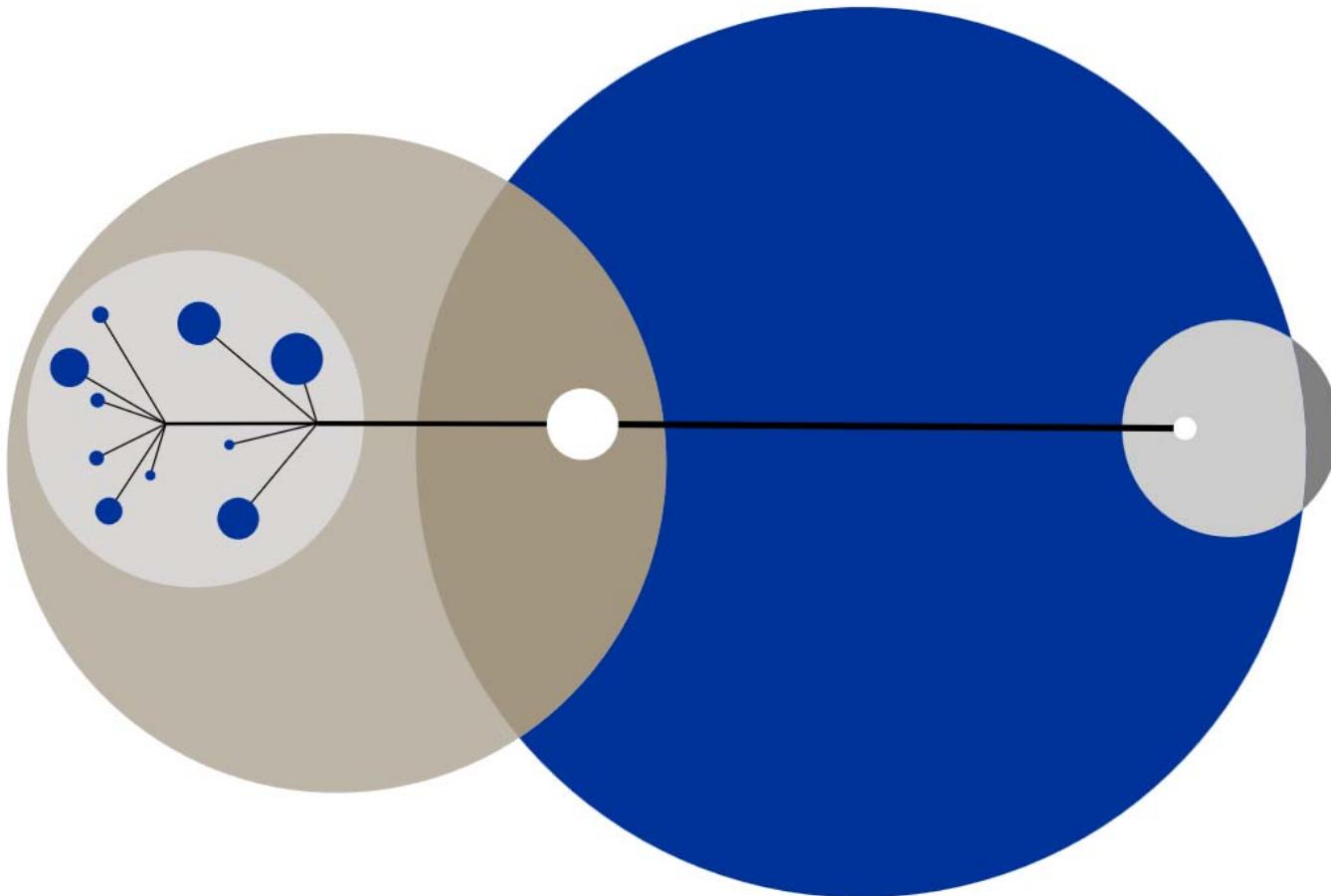
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<sup>2</sup> Eurotechnica GmbH, An den Stücken 55, D-22941 Bargteheide, Germany

<sup>3</sup> Federal Institute for Geosciences and Natural Resources (BGR), Stilleweg 2, D-30655 Hannover, Germany

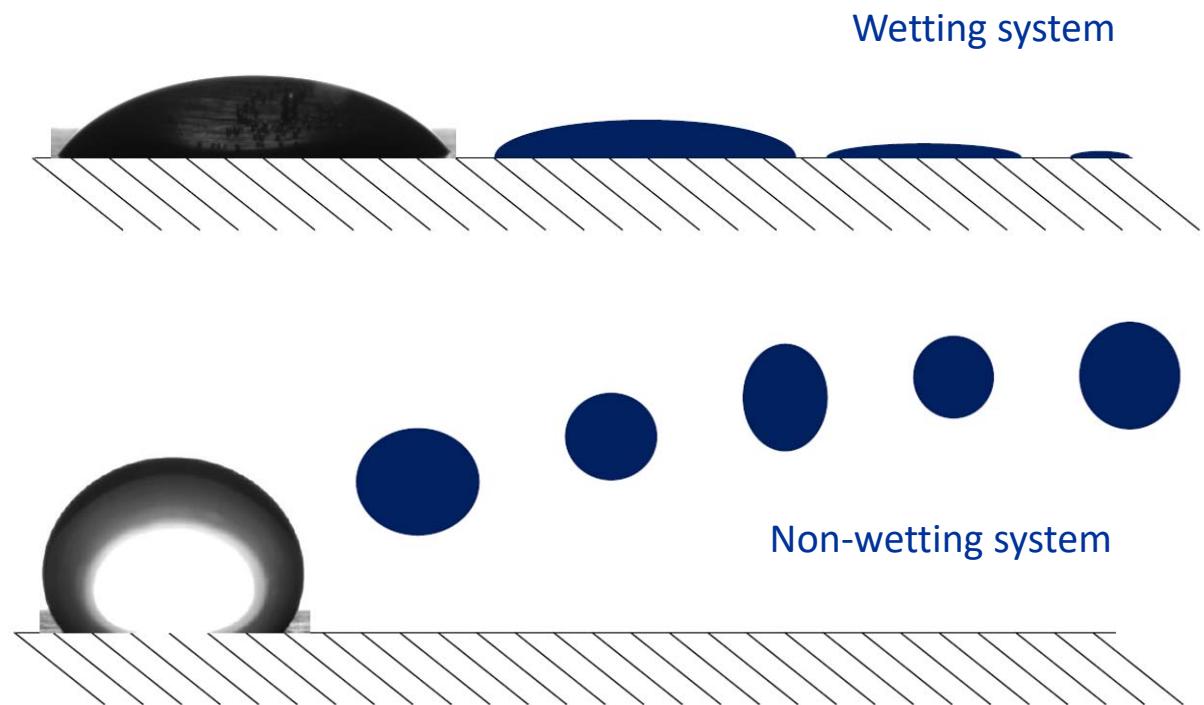
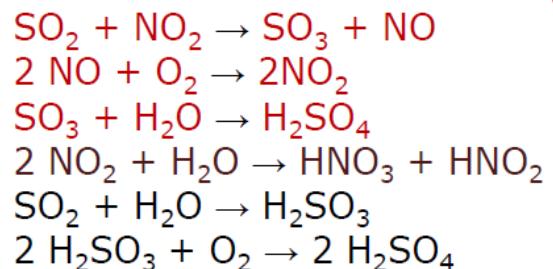


# Cluster Scenario

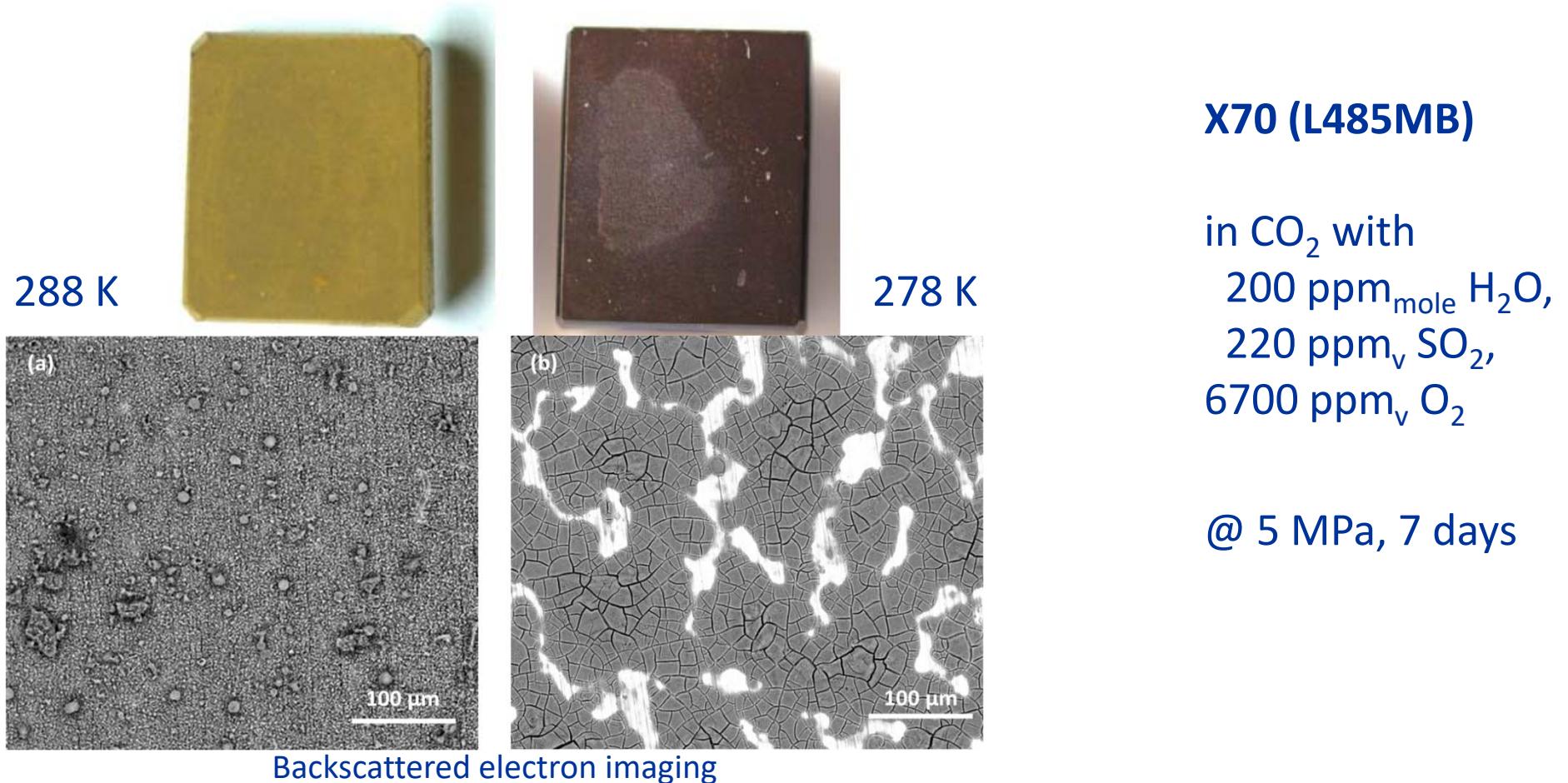


Project Homepage: [www.bgr.bund.de/CLUSTER-EN](http://www.bgr.bund.de/CLUSTER-EN)

# Reactions in CO<sub>2</sub> streams – acid formation and condensation

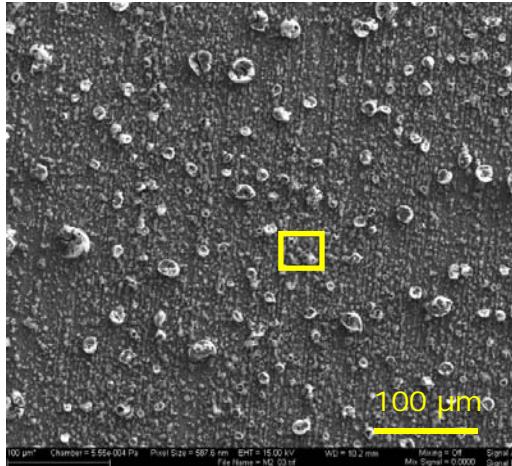


# Condensation of water and/or acids: temperature effect

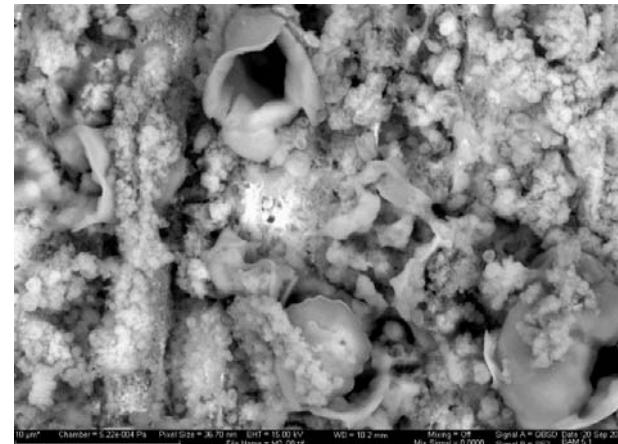
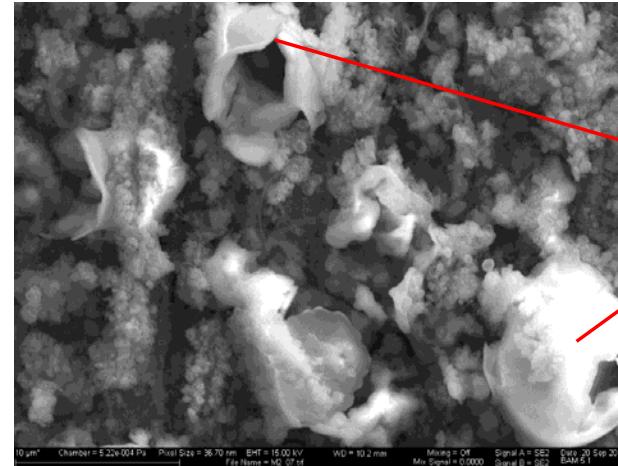
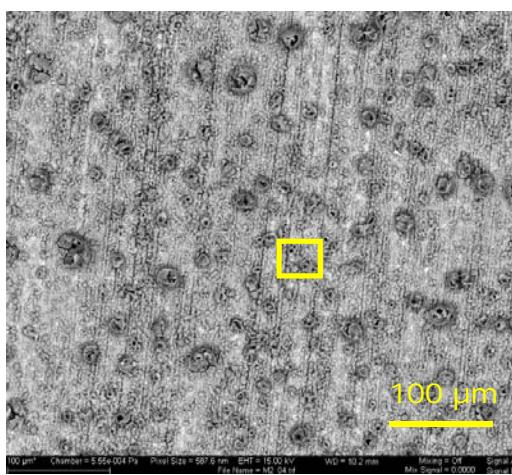


# Cross-reactions – implications for corrosion (X70)

SEM imaging



Backscattered electron imaging



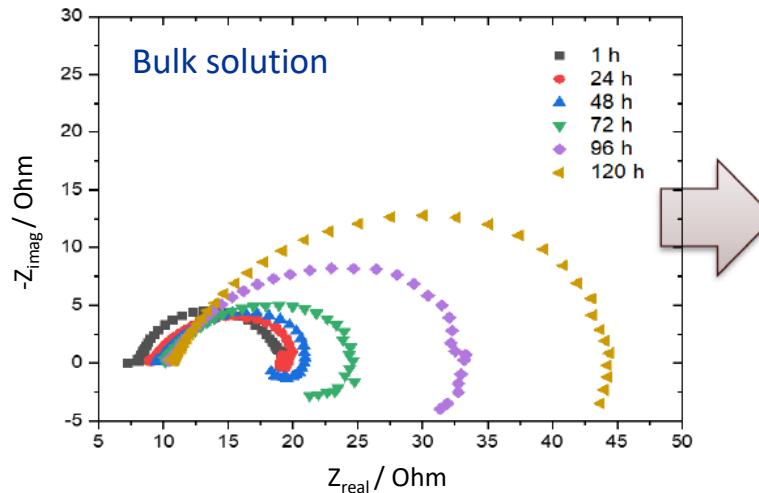
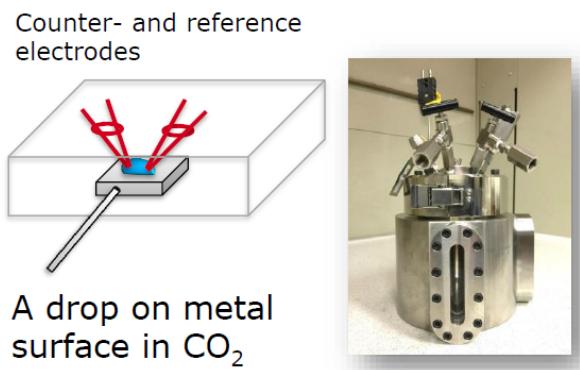
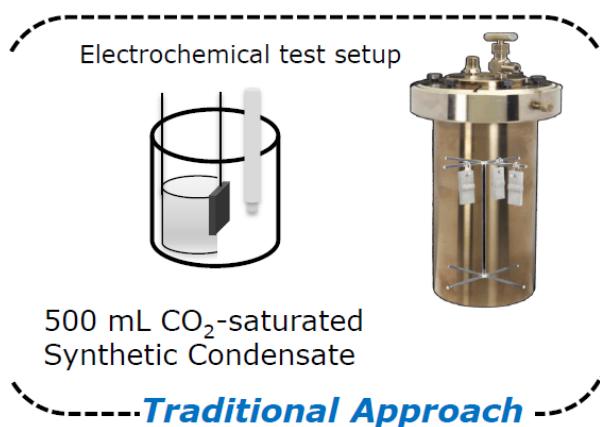
Ratio of O/S is higher cf. product formed without NO<sub>2</sub>

X70 (L485MB)

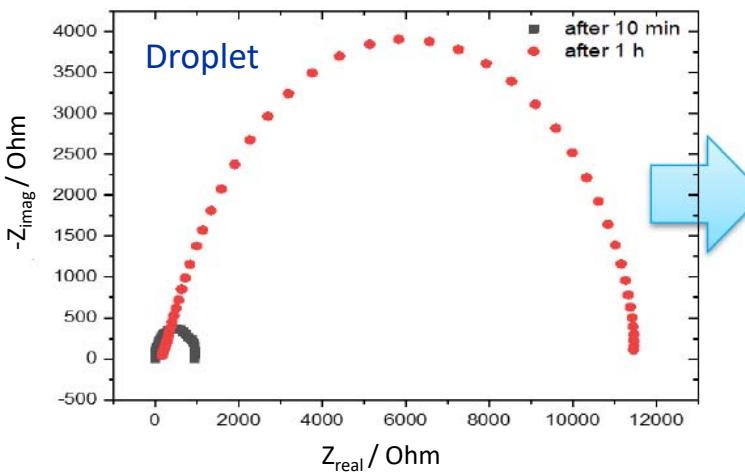
in CO<sub>2</sub> with  
200 ppm<sub>mole</sub> H<sub>2</sub>O,  
70 ppm<sub>v</sub> SO<sub>2</sub>,  
100 ppm<sub>v</sub> NO<sub>2</sub>  
and 6700 ppm<sub>v</sub> O<sub>2</sub>

after 7 days  
@ 5 MPa, 278 K

# Approaches to study acid corrosion

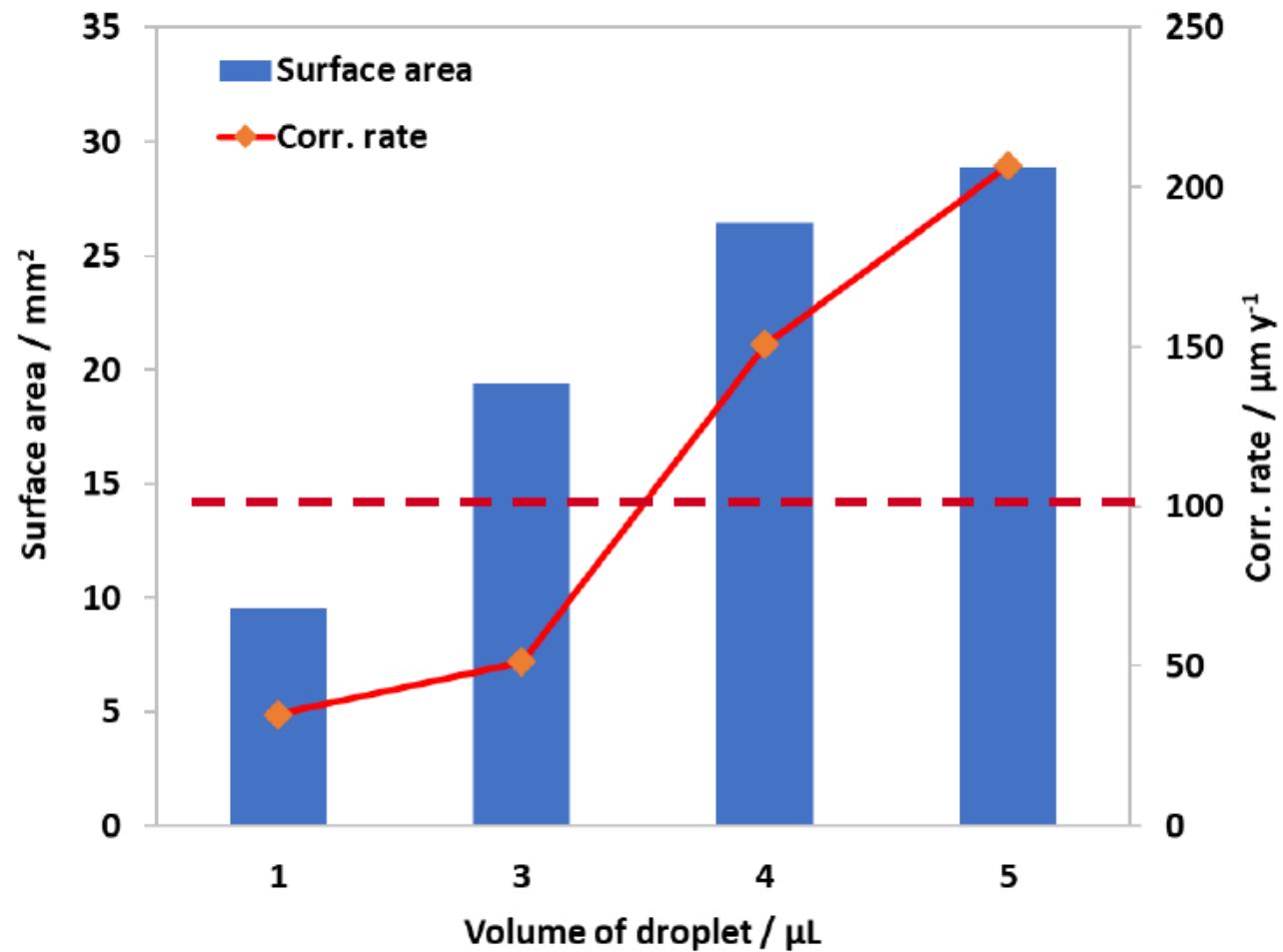


- dissolvable corrosion products
- high corrosion rate
- strong pitting



- thick, high-resistance corrosion products
- low corrosion rate

# Effect of droplet size

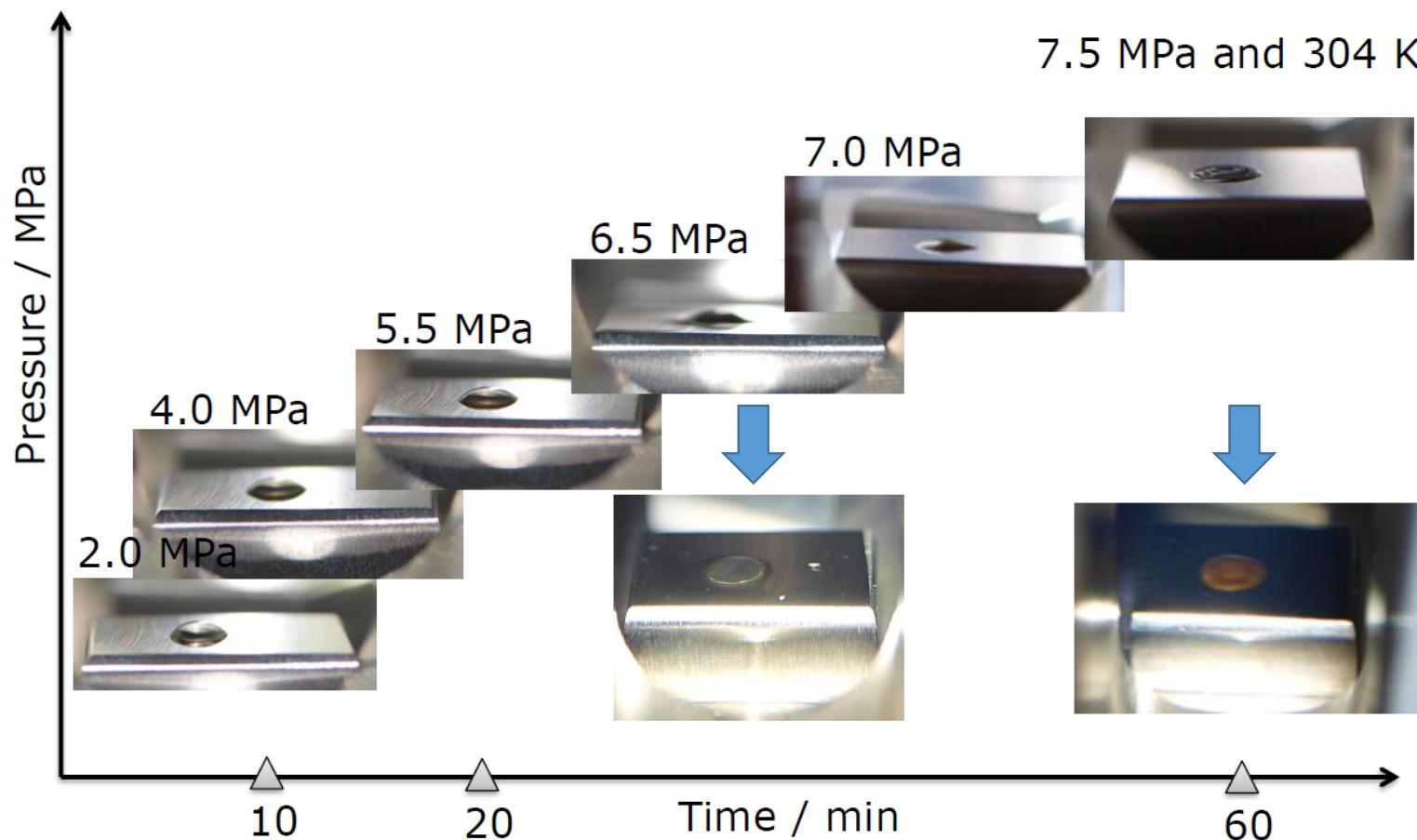


X70 (L485MB)

in  $\text{CO}_2$  with  
220 ppm<sub>v</sub>  $\text{SO}_2$  and  
6700 ppm<sub>v</sub>  $\text{O}_2$

@ 278 K, 5 MPa,  
7 days

# Acid formation by impurity diffusion into CO<sub>2</sub>-saturated water drop

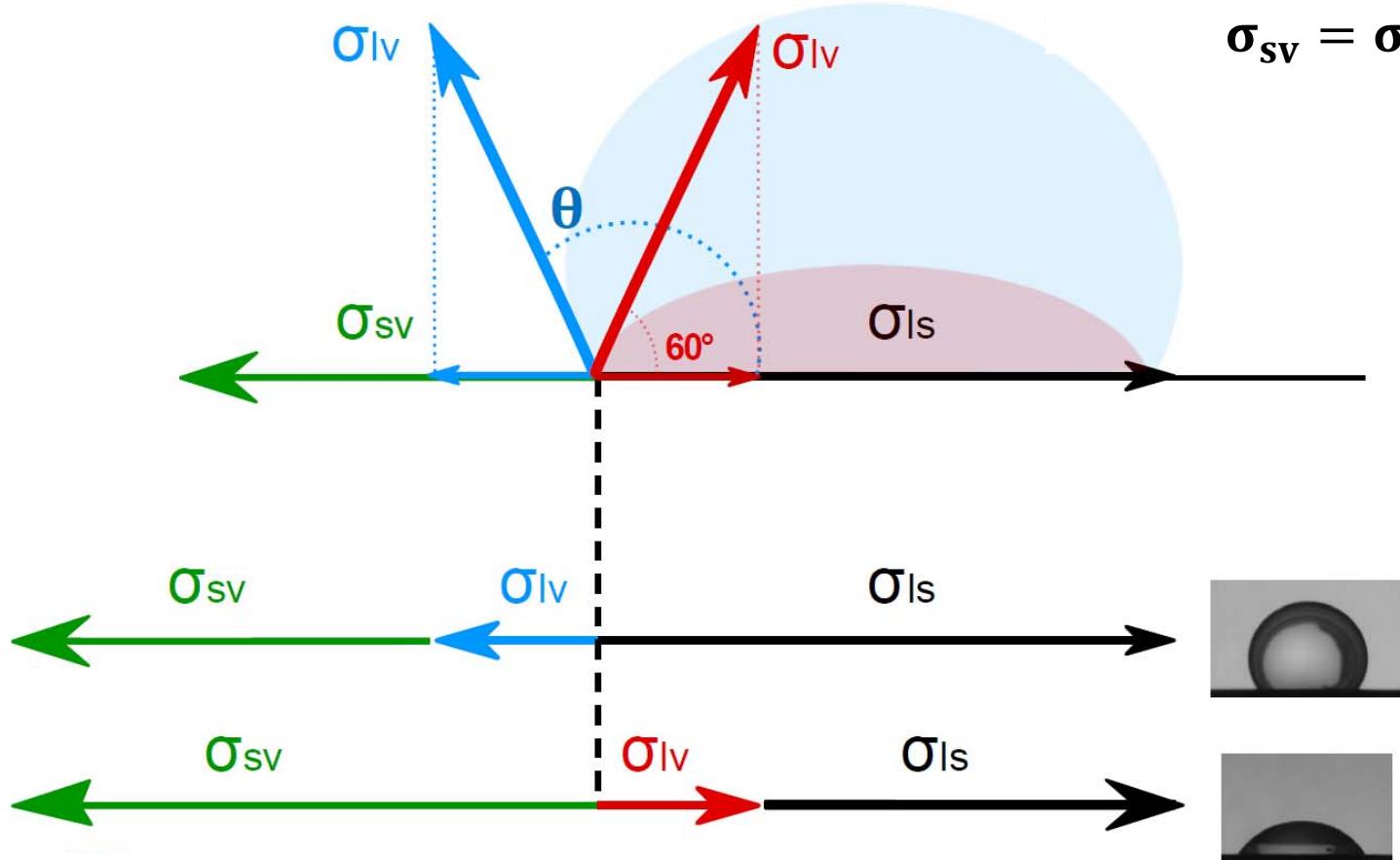


X70 (L485MB)

in CO<sub>2</sub> with  
220 ppm<sub>v</sub> SO<sub>2</sub> and  
6700 ppm<sub>v</sub> O<sub>2</sub>

$V_{\text{drop}} = 5 \mu\text{L}$

# Wettability: Contact angle



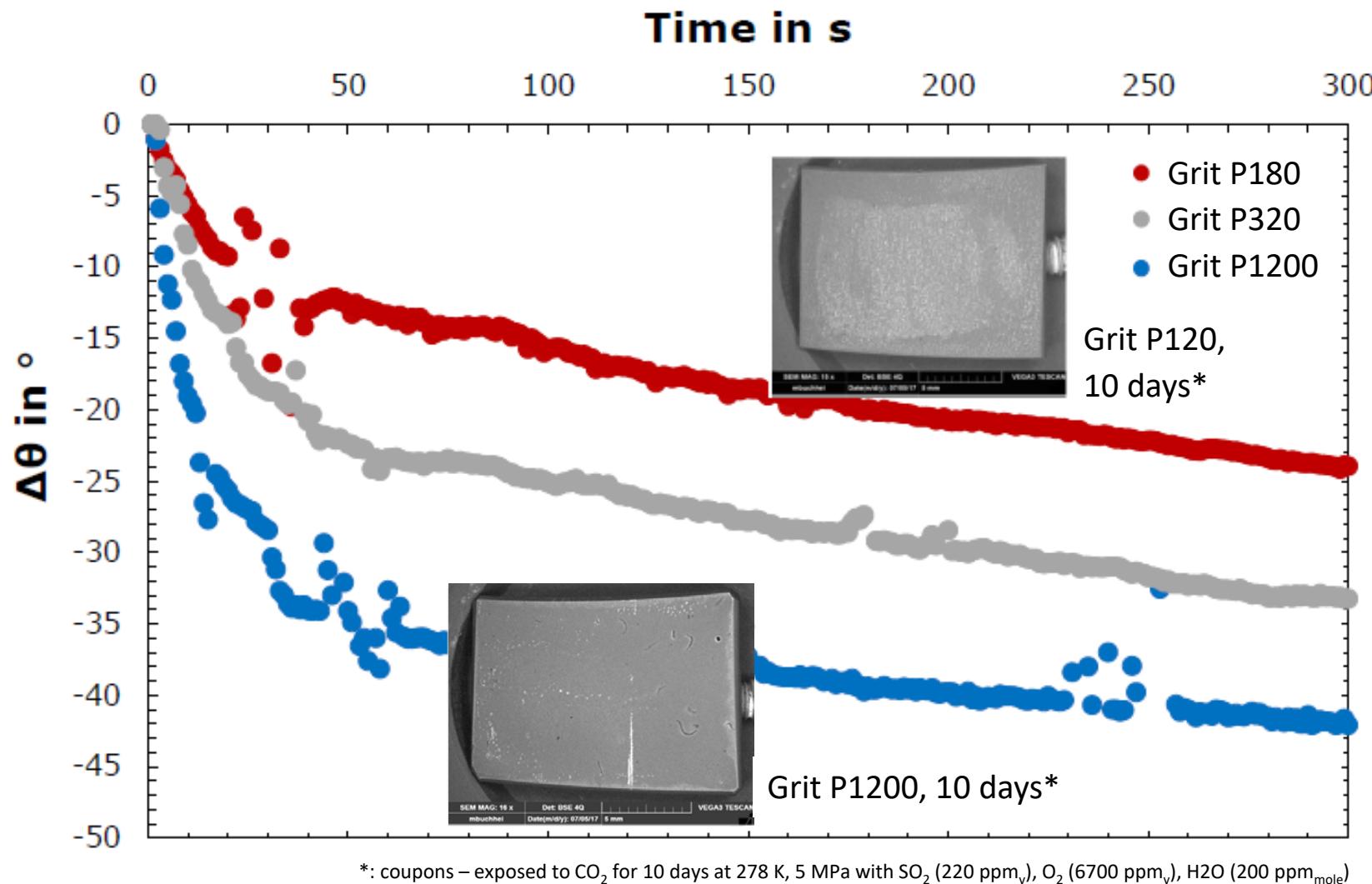
Young equation:

$$\sigma_{sv} = \sigma_{sl} + \sigma_{lv} \cdot \cos(\theta)$$

$\theta > 90^\circ$   
Non-wetting system

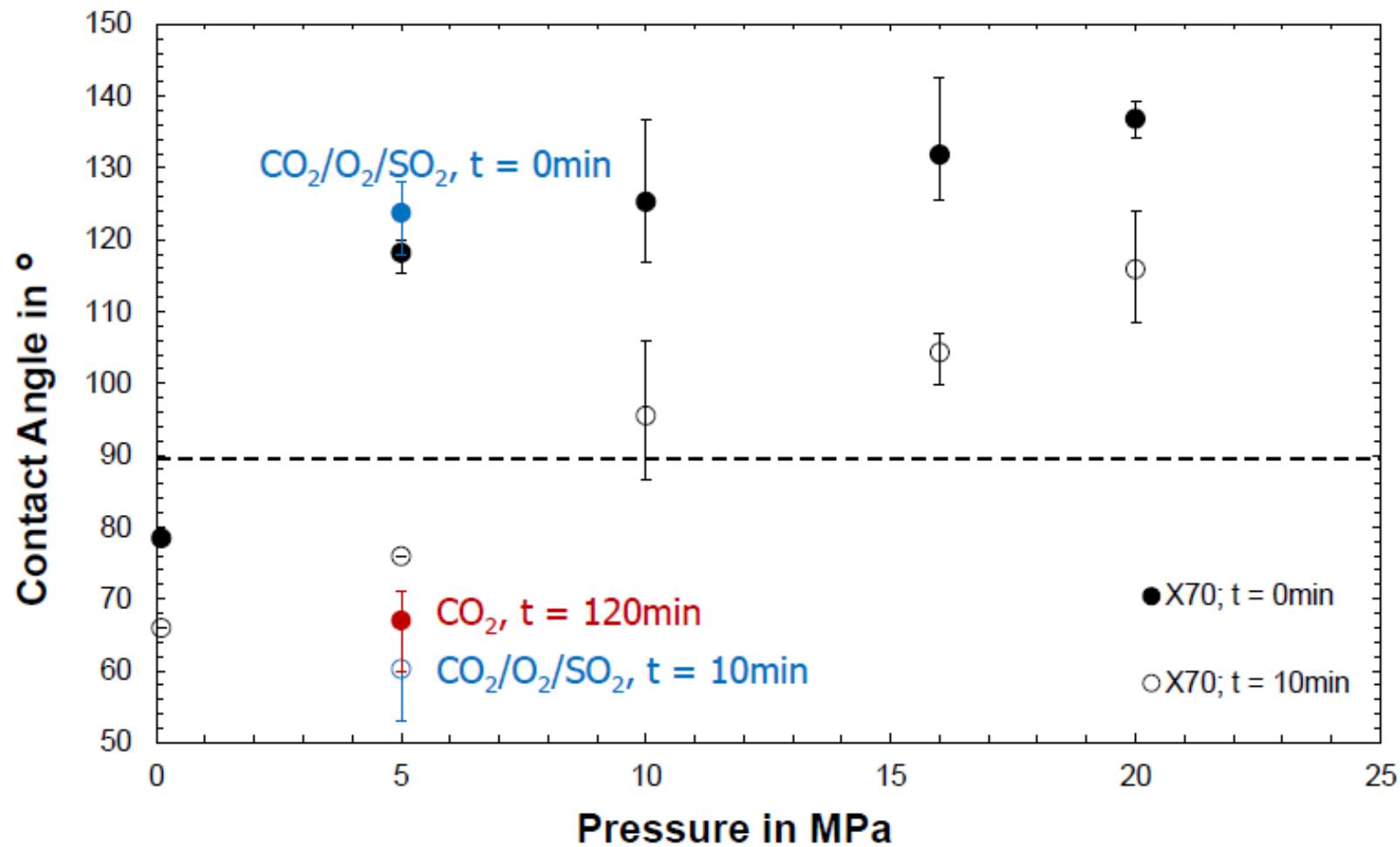
$\theta < 90^\circ$   
Wetting system

# Contact angle difference ( $\Delta\theta$ ) as f (surface roughness)



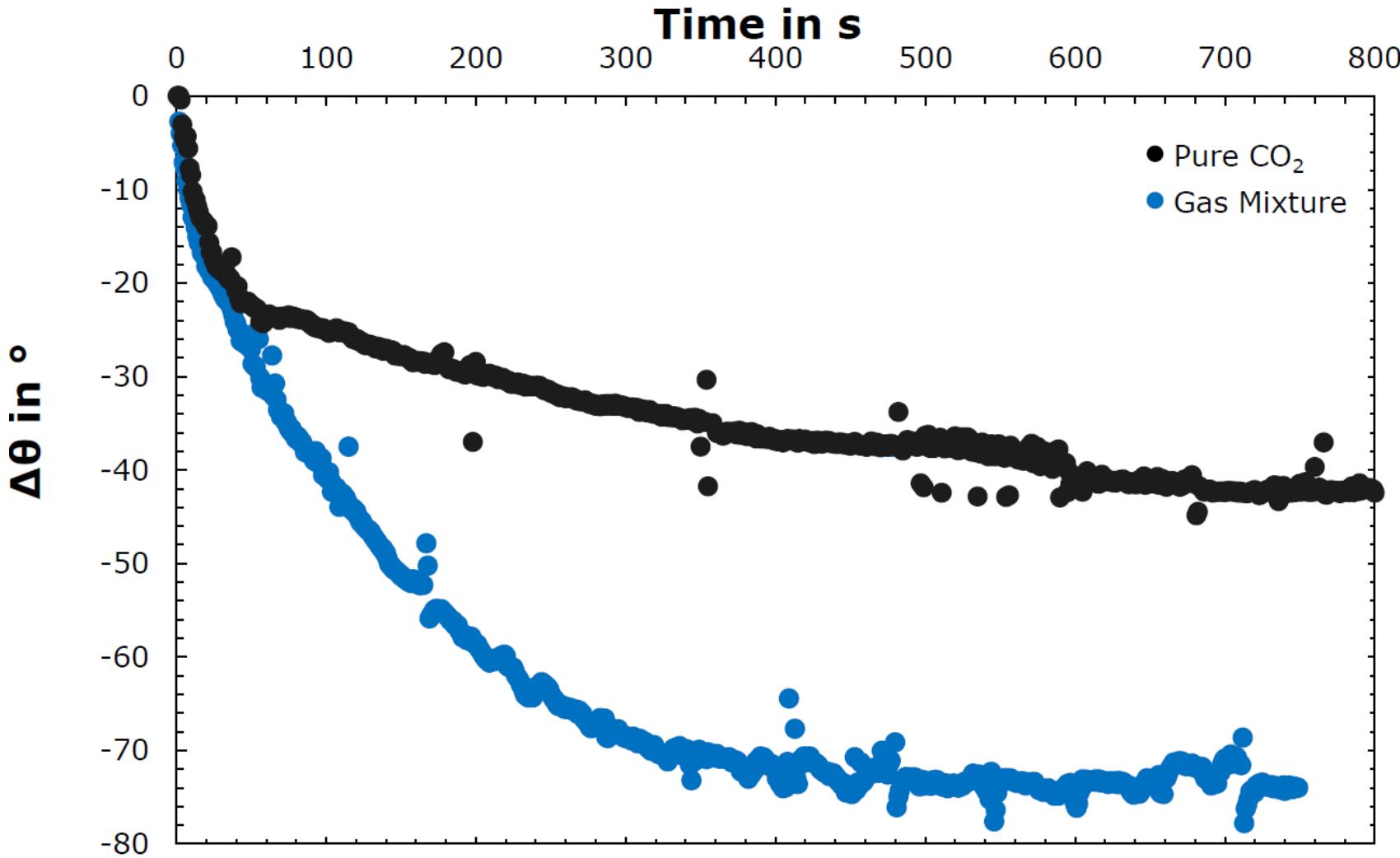
X70 (L485MB)  
in  $\text{CO}_2$   
@ 278 K,  
5 MPa

# Contact Angle as f (p, impurities)



X70 (L485MB)  
in  $\text{CO}_2$   
with  
 $220 \text{ ppm}_v \text{ SO}_2 /$   
 $6700 \text{ ppm}_v \text{ O}_2$   
@278 K  
(Grit P320)

## Contact angle changes – reactive wetting (X70)



X70 (L485MB)  
in CO<sub>2</sub> (with  
220 ppm<sub>v</sub> SO<sub>2</sub>,  
6700 ppm<sub>v</sub> O<sub>2</sub>)

@ 278 K, 5 MPa

(Grit P320)

# In summary

Contact angle decreases

- ....with decreasing pressure,
- ....with time due to formation of corrosion products,
- ....faster on smoother surfaces,
- ....faster in case of higher corrosion rate  
(e.g. in presence of O<sub>2</sub>, SO<sub>2</sub>)

resulting in better wetting and thus potentially in ...

- .....larger contact area droplet/steel,
- .....droplet mobilization being less likely,
- ..... droplet accumulation being more likely,
- ..... potentially more severe corrosion.





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