

# Towards improved guidelines for cost evaluation of CO<sub>2</sub> capture technologies

Simon Roussanaly<sup>1,\*</sup>, Edward Rubin<sup>2</sup>, Mijndert Van Der Spek<sup>3</sup>, Niels Berghout<sup>4</sup>, George Booras<sup>5</sup>, Tim Fout<sup>6</sup>, Monica Garcia<sup>7</sup>, Stefania Gardarsdottir<sup>1</sup>, Michael Matuszewski<sup>8</sup>, Sean McCoy<sup>9</sup>, Shareq Mohd Nazir<sup>10</sup>, and Andrea Ramirez<sup>11</sup>

<sup>1</sup> SINTEF Energy Research

<sup>2</sup> Carnegie Mellon University

<sup>3</sup> ETH Zürich

<sup>4</sup> International Energy Agency

<sup>5</sup> Electric Power Research Institute

<sup>6</sup> National Energy Technology Laboratory

<sup>7</sup> IEAGHG, Cheltenham

<sup>8</sup> AristoSys, LLC, Contractor to NETL

<sup>9</sup> University of Calgary

<sup>10</sup> Norwegian University of Science and Technology

<sup>11</sup> Delft University of Technology

Corresponding author: [Simon.Roussanaly@sintef.no](mailto:Simon.Roussanaly@sintef.no)

# Towards improved guidelines for cost evaluation of CO<sub>2</sub> capture technologies

---

- There are many challenges in establishing reliable cost estimates for CCS technologies
- Several groups (for e.g. IEAGHG cost network) have been working over the past decade on improving cost evaluation of CCS
  - However, key challenges still remain and there is room for improvement
- We initiated a collaborative effort aiming to develop improved cost guidelines on three areas of Techno-Economic Analyses (TEA)
  - Evaluation of CO<sub>2</sub> capture technologies that are not yet commercial, and the evolution of CO<sub>2</sub> capture costs beyond demonstration projects
  - Need for transparency, data quality and uncertainty evaluations of both the data and models used in CCS cost analysis
  - Evaluation of CO<sub>2</sub> capture, transport and storage costs for non-power industries

# Collaborative effort between different organisations dealing with TEA

Research institutes



Intergovernmental organisations



Governmental laboratories



Universities



# Targeted areas of improvements

Focus of this presentation

Group 1: Cost evaluation of CO<sub>2</sub> capture technologies that are not yet commercial, and the evolution of CO<sub>2</sub> capture costs beyond demonstration projects

Bottom-up estimates for (hypothetical)  
N<sup>th</sup>-of-a-Kind (NOAK) plants

Cost estimates of First-of-a-Kind  
(FOAK) commercial plants

Evolution of cost beyond  
demonstration

Better account for technology  
current maturity

Group 3: Cost evaluation of CO<sub>2</sub> capture, transport and storage from (non-power) industrial sources

Electricity and steam costs

Retrofitting costs

CO<sub>2</sub> transport and storage  
costs

Transferability of experience  
from the power sector

Technology maturity

Metrics

Benchmarking basis

Group 2: Quality assurance and uncertainty evaluations of both the data and models used in CCS cost analysis

TEA quality assurance  
guidelines

Review and examples of  
existing uncertainty evaluation  
methods

Guidelines on when to use  
which method in TEA

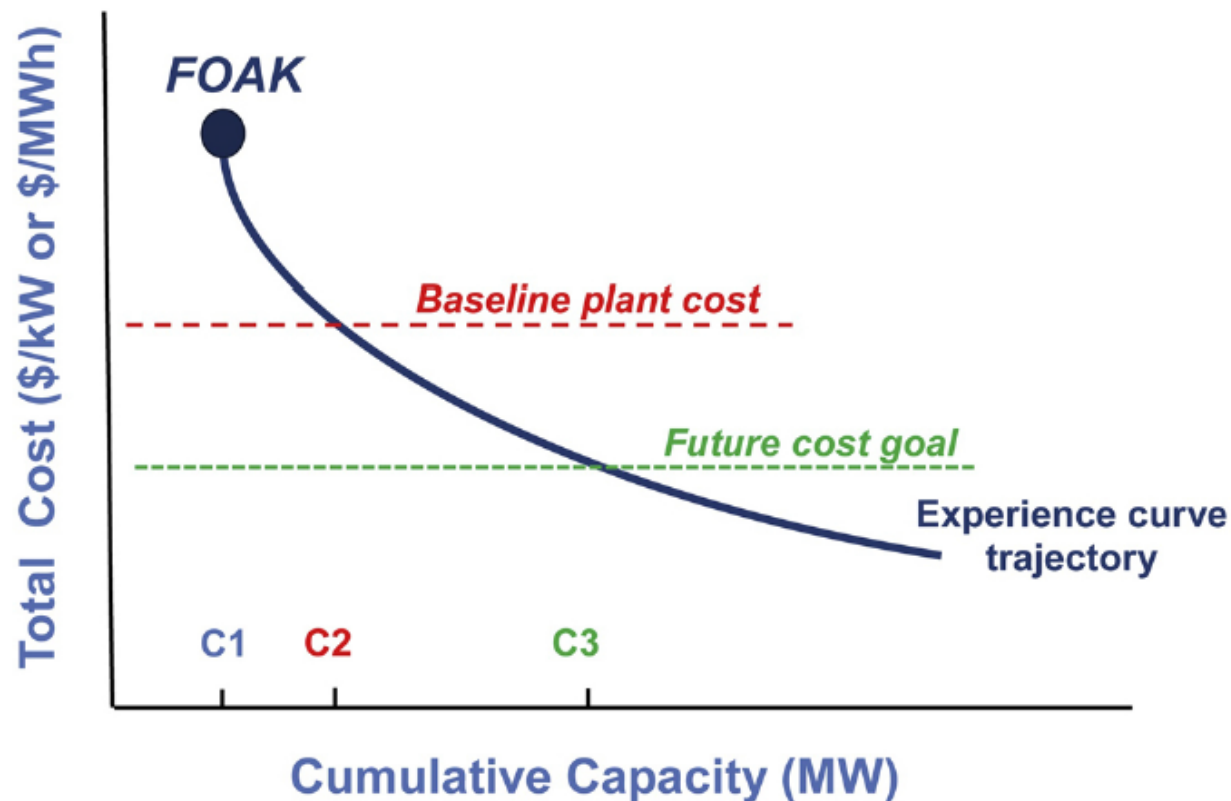
# Improving cost estimates for NOAK plants

---

- Current “bottom-up” approach to cost evaluation of NOAK plants is adapted for "what if" questions and comparisons involving the performance and cost of proposed new technologies or process designs that are still in early stages of development
- However, this method is *simply not appropriate* or intended for estimating the *actual* or *likely* future (NOAK) cost of an advanced technology that is not yet commercial
- A proposed hybrid method for advanced technology cost
  - First use the traditional “bottom-up” method to estimate the *FOAK* cost of an emerging technology based on its current state of development
  - Then use a “top-down” model based on learning curves to estimate future (NOAK) costs as a function of cumulative installed capacity (and other factors, if applicable)
  - From this, estimate level of deployment needed to achieve an NOAK cost goal (e.g., an X% lower LCOE)
    - This approach explicitly links cost reductions to commercial experience

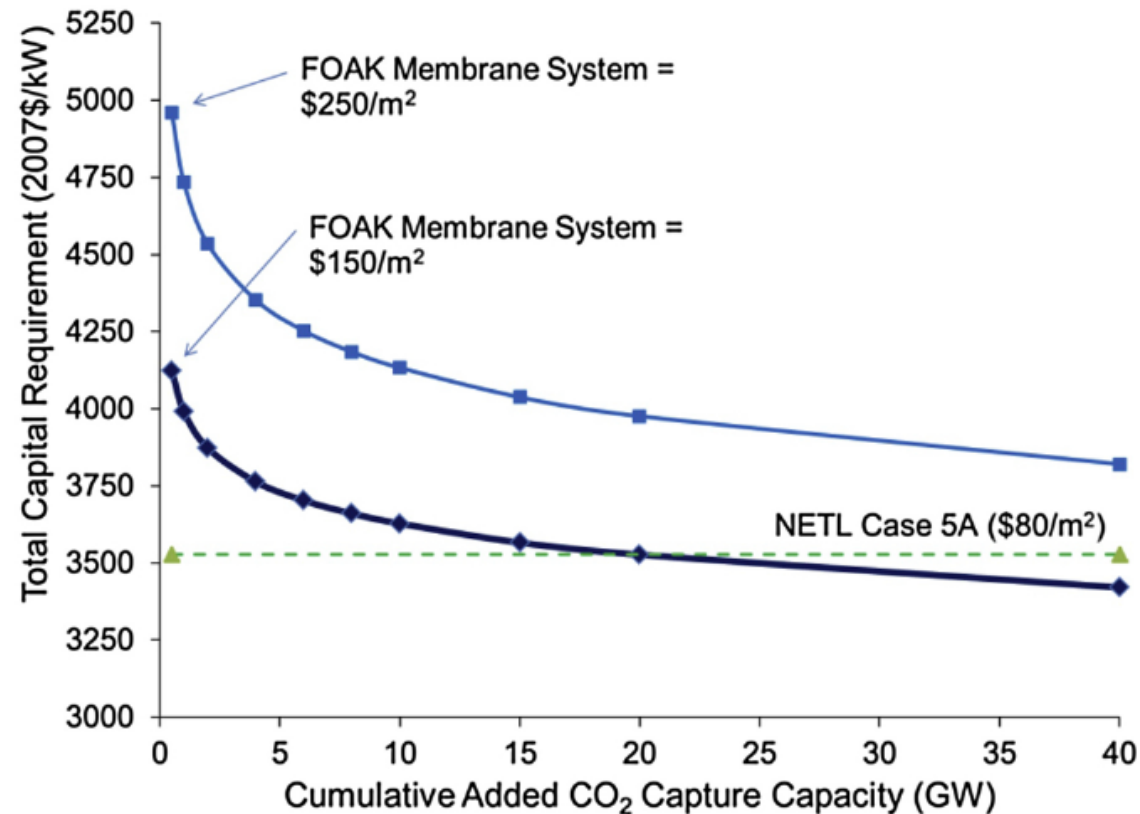
# Improving cost estimates for NOAK plants

Illustrative cost trajectory of an advanced technology from FOAK plant to mature plant, showing the deployment of the technology needed to meet a given cost goal. Note that the FOAK cost represents a plant that reliably meets its design performance measures.



# Improving cost estimates for NOAK plants

Total capital cost of a power plant with two assumed FOAK costs for an advanced membrane-based CO<sub>2</sub> capture system



# Steam and electricity costs for industrial emitters

---

- Steam and electricity supply strategies and costs aren't always carefully evaluated in the case of CO<sub>2</sub> capture from industrial sources
- Especially, steam characteristics (availability, cost and CO<sub>2</sub> intensity ) will strongly depend on supply strategy, energy prices, plant location, potential synergies with the industrial plant and nearby facilities

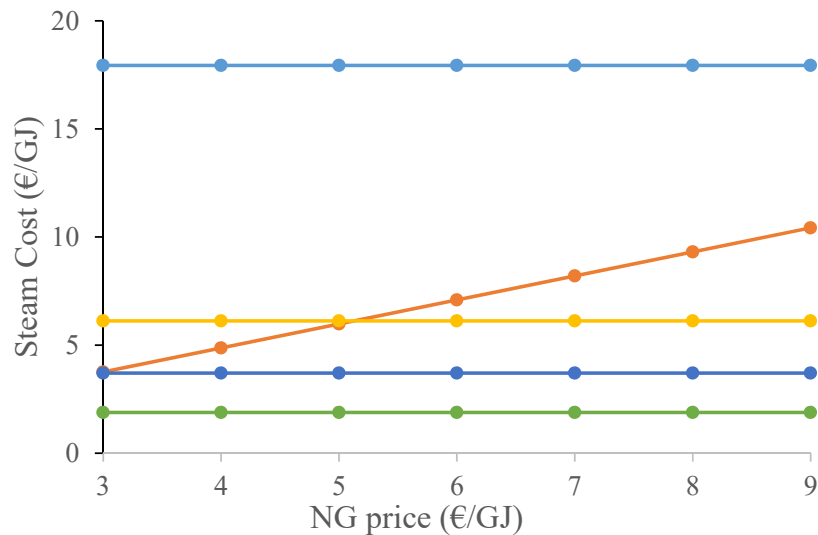
Steam characteristics for different supply strategies for a generic Netherlands-based application  
with an NG price of 6 €/GJ, a coal price of 3 €/GJ and an electricity price of 58 €/MWh

Source	Steam cost (€/GJ)	CO <sub>2</sub> intensity (kgCO <sub>2</sub> /MWh)
Electrical	17.9	313
Natural gas boiler	7.1	205
Coal CHP plant	6.1	458
Steam extraction from an LP Turbine	3.7	175
Waste heat	1.9	0

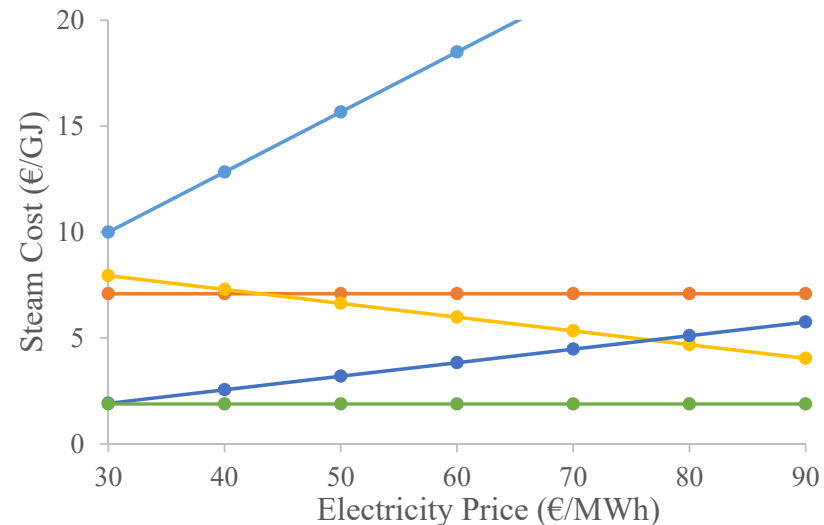


# Steam and electricity cost for industrial emitters

- Impact of energy prices on the cost of each supply strategies, for example:
  - Optimal steam supply depends on energy prices which may also change over time
  - Steam extraction prior to the LP turbine will strongly benefit capture technologies requiring steam
  - Steam from a coal CHP plant becomes cheaper with increasing electricity prices
  - At low electricity price, electrical boilers could become more attractive than NG boilers or CHP plant when taking into account the associated CO<sub>2</sub> emissions



—•— Electrical Boiler  
—•— Coal CHP plant  
—•— Waste heat



—•— Natural gas boiler  
—•— Steam extraction from an LP Turbine

# Steam and electricity cost for industrial emitters

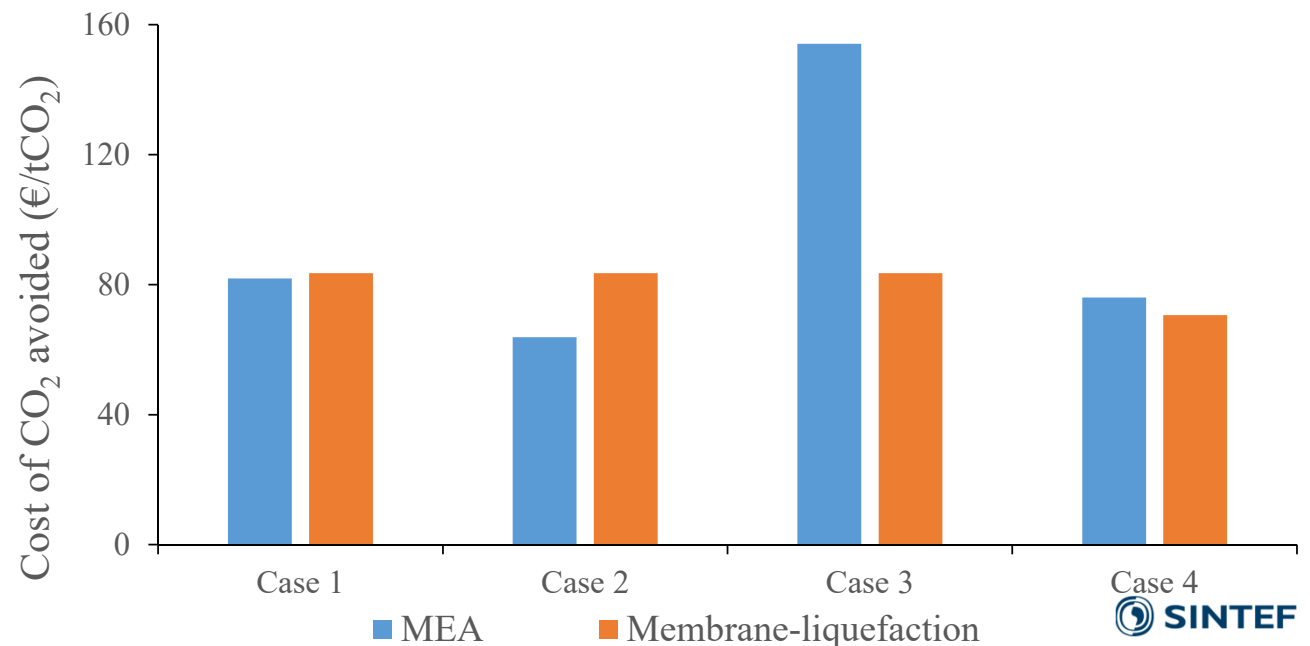
- Illustration of this for a case considering CO<sub>2</sub> capture from a cement plant

- Case 1-3: Steam supply strategy
- Case 4: Steam supply strategy and energy prices

- Heat supply strategy and energy prices will influence:

- The cost performances of a given capture technology
- The comparison of capture technologies
- The design of the CCS system (for e.g. partial capture to allow using only waste heat)

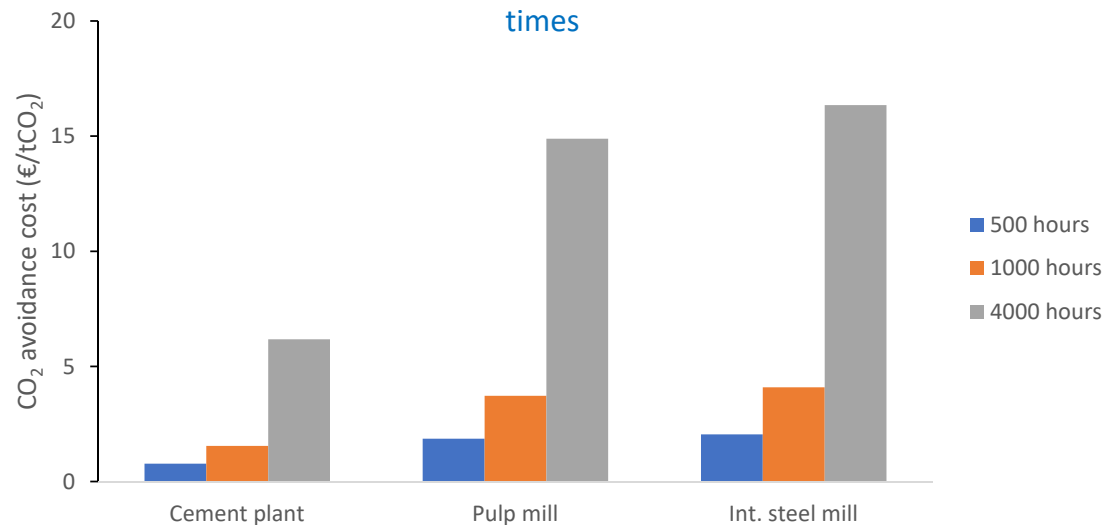
	NG Price (€/GJ)	Electricity Price (€/MWh)	Steam production option
Case 1	6	58	NG gas boiler
Case 2	6	58	Steam extraction
Case 3	6	58	Electric boiler (EU elec. mix)
Case 4	6	30	Electric boiler (Norwegian elec. Mix)



# Retrofitting costs

- Economic impact of production stop
  - Retrofit will result in partial or full-shut downs of the industrial plant
  - Aligning shut-downs with maintenance/upgrade period will reduce this cost
    - May not be enough, especially in the case of capture technologies needing a tight integration with the plant
  - This can have significant impact on the CO<sub>2</sub> avoidance cost but needs to be evaluated carefully

Impact of losing a "10% profit margin" on the CO<sub>2</sub> avoidance cost for different full plant production stop times

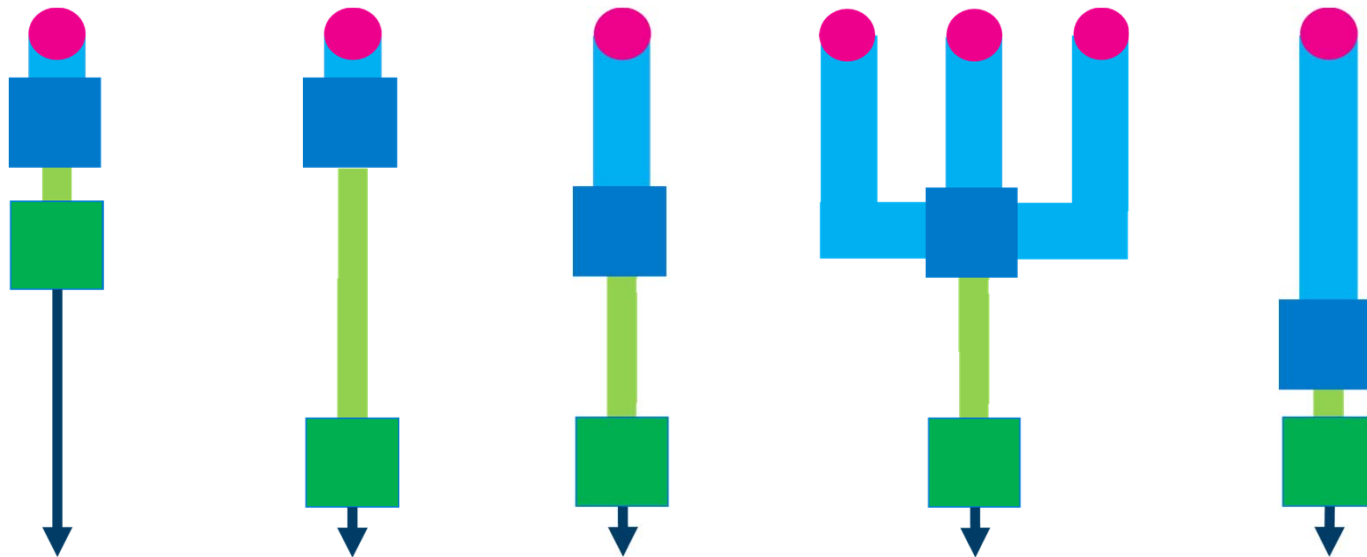


# Retrofitting costs

---

- Space constraints
  - Finding available space for the CO<sub>2</sub> capture unit near the emission sources might be challenging
    - Alternative layouts and configurations could be considered in such cases
    - Most industrial sources have several point sources, each with different qualities and quantities which may result in pooling strategies

Illustration of different layout alternatives that could be considered in space constraint cases



# Retrofitting costs

---

- Space constraints
  - Finding available space for the CO<sub>2</sub> capture unit near the emission sources might be challenging
    - Alternative layouts and configurations could be considered in such cases
    - Most industrial sources have several point sources, each with different qualities and quantities which may result in pooling strategies
- In some cases, these alternative layouts can result in significant and costly transport of the flue gas
  - Flue gas and utilities interconnection costs were evaluated to be in the range of 16-35 €/tCO<sub>2,avoided</sub> for a refinery retrofit in the RECAP study
  - However these costs are often overlooked in many studies
- To help to better account for this, cost of pipeline rack and ducting as a function of flow and distance will be provided in the guideline

# Retrofitting costs

---

- Utilities supply and integration
  - Similar issue as for space availability and ducting
  - Efficient use of spare capacities with the plant
  - Integration with the plant in term of utilities can be challenging
- Impact on product quality
  - Depending on the type, CO<sub>2</sub> capture can have an impact of the product quality of the main plant
    - E.g: oxyfuel with cement
  - Variation in plant product value vs. cost of post-treatment to keep the same product quality
- Flue gas pre-treatment
  - Wide range of possible impurity types and levels for industrial emissions
    - Pre-treatment costs are often not taken into account
    - Pre-treatment could also have additional cost impact, for example in space constraint cases

# Summary

---

- There are still challenges in establishing reliable cost estimates for CCS technologies
- We have initiated a collaborative effort aiming to develop improved cost guidelines on three areas of Techno-Economic Analyses
- These guidelines will support the establishment of more reliable estimates through:
  - Additional or improved methods/approaches
  - Establishment of supporting data and revision, in some case of, commonly used data
  - Raising awareness and guidance on important issues, often ignored in literature but which can be key for cost evaluation
- This work is expected to results in new white paper, building on the first one from the IEAGHG cost group, and several publications

# Towards improved guidelines for cost evaluation of CO<sub>2</sub> capture technologies

Simon Roussanaly<sup>1,\*</sup>, Edward Rubin<sup>2</sup>, Mijndert Van Der Spek<sup>3</sup>, Niels Berghout<sup>4</sup>, George Booras<sup>5</sup>, Tim Fout<sup>6</sup>, Monica Garcia<sup>7</sup>, Stefania Gardarsdottir<sup>1</sup>, Michael Matuszewski<sup>8</sup>, Sean McCoy<sup>9</sup>, Shareq Mohd Nazir<sup>10</sup>, and Andrea Ramirez<sup>11</sup>

<sup>1</sup> SINTEF Energy Research

<sup>2</sup> Carnegie Mellon University

<sup>3</sup> ETH Zürich

<sup>4</sup> International Energy Agency

<sup>5</sup> Electric Power Research Institute

<sup>6</sup> National Energy Technology Laboratory

<sup>7</sup> IEAGHG, Cheltenham

<sup>8</sup> AristoSys, LLC, Contractor to NETL

<sup>9</sup> University of Calgary

<sup>10</sup> Norwegian University of Science and Technology

<sup>11</sup> Delft University of Technology

Corresponding author: [Simon.Roussanaly@sintef.no](mailto:Simon.Roussanaly@sintef.no)