



10<sup>th</sup> Trondheim CCS Conference, 18<sup>th</sup>-19<sup>th</sup> June 2019, Trondheim, Norway

# Integration of a flexible Calcium Looping CO<sub>2</sub> capture system in a back-up power plant

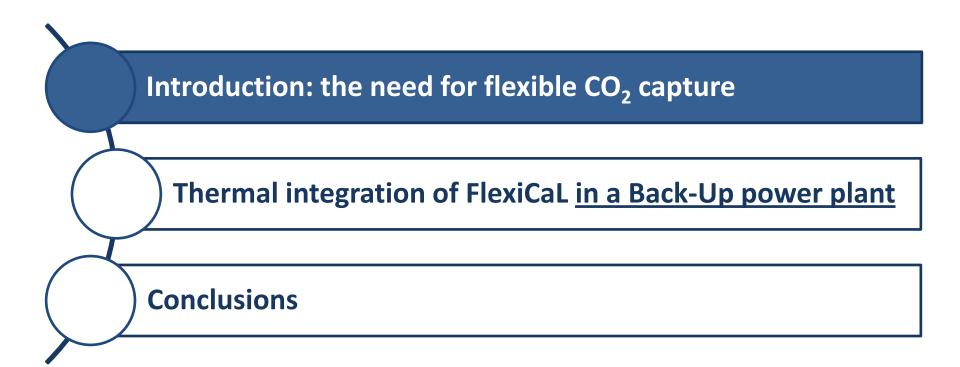
Borja Arias, Yolanda A. Criado, J. Carlos Abanades

Spanish Research Council CSIC-INCAR, Francisco Pintado Fe 26, 33011, Oviedo, Spain

abanades@incar.csic.es



#### **Outline**



## The need for flexible CO<sub>2</sub> capture systems

Fossil fuel power plants undergo flexible operation with load changes, partial load operation or turn off periods due to the increasing amount of renewable energy



#### **PROBLEM:**

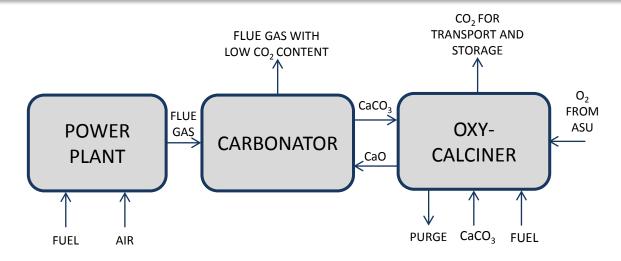
CO<sub>2</sub> CAPTURE TECHNOLOGIES ARE INTEGRATED SYSTEMS WITH LOW FLEXIBILITY AND HIGH CAPITAL INVESTMENT.

OPERATION WITH LOW CAPACITY FACTORS WOULD LEAD TO HIGH CO<sub>2</sub> COST BECAUSE OF WASTE OF CAPITAL

#### Approaches to address flexibility in existing CO<sub>2</sub> capture technologies:

- □ Post-combustion using liquid solvent → Storage tanks of solvent
- □ Oxy-combustion → Cryogenic storage of O<sub>2</sub>
- □ Pre-combustion → Storage of hydrogen/polygeneration

## Calcium looping for post-combustion CO<sub>2</sub> capture



#### ADVANTAGES OF CO<sub>2</sub> CAPTURE BY CAL

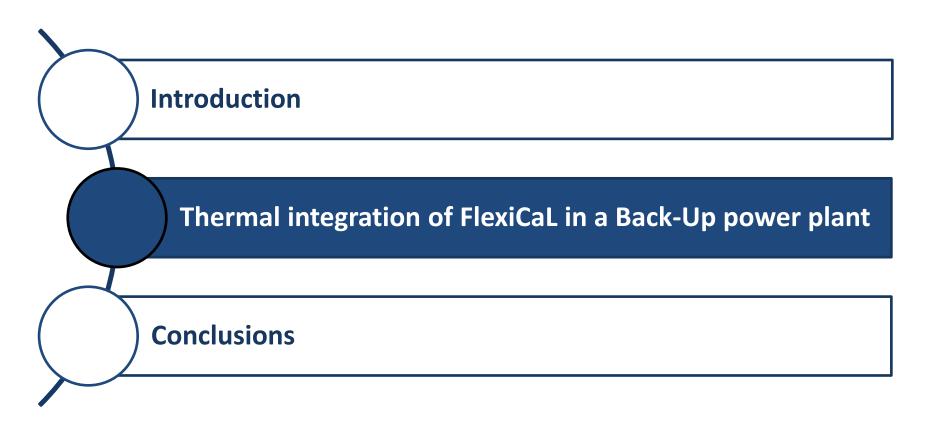
- Based on CFB technology
- □ Low energy penalty → Additional power produced
- □ Use of CaO as sorbent  $\rightarrow$  Rich CaO purge
- ☐ Energy penalties: 6-9 net points
- □ Developed up to TRL 6-7



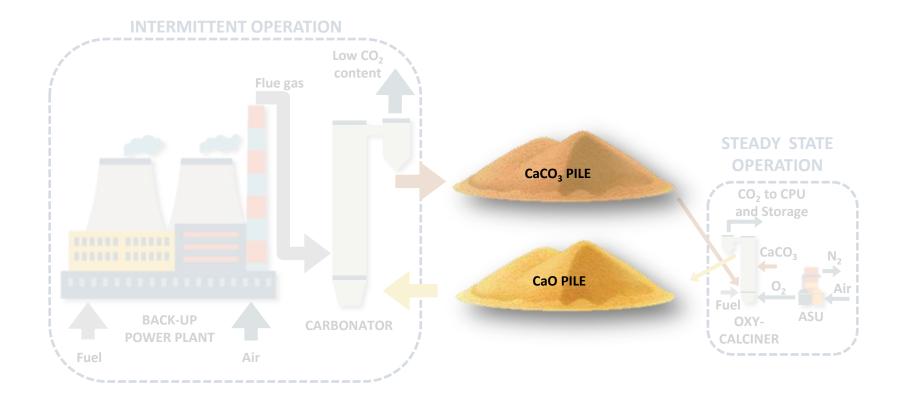
www.flexical.eu

TO IMPROVE THE FLEXIBILITY OF CO<sub>2</sub> CAPTURE BY DEVELOPING NOVEL CALCIUM LOOPING PROCESS INTEGRATED WITH ENERGY STORAGE SYSTEM

#### **Outline**



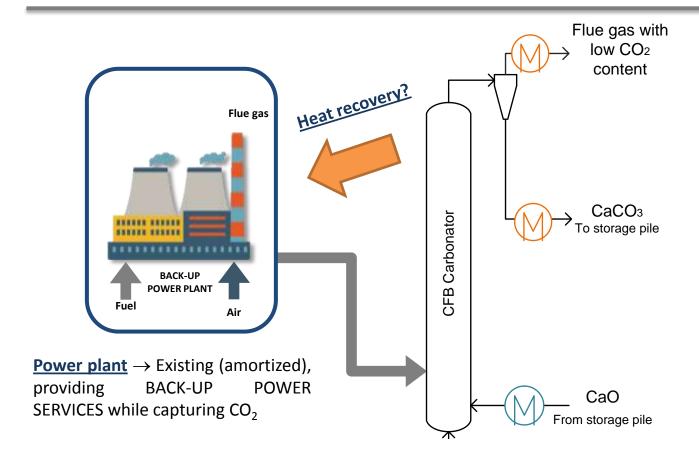
# Flexible CaL for back-up power plants





Calcium looping  $CO_2$  capture system for back-up power plants. Y. A. Criado, B. Arias and J. C. Abanades; *Energy Environ. Sci.*, **2017**, 10, 1994

### CaL for back-up power: integration of the carbonator

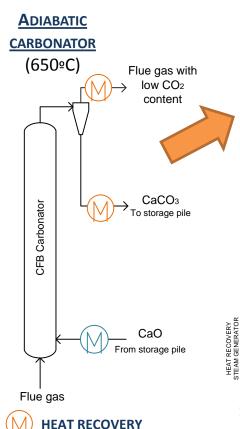


<u>Carbonator</u> (New) is an adiabatic reactor. It is decoupled from the calciner and is fed with stored CaO following the intermittent power plant operation modes





## Thermal integration of the carbonator block



**PRE-HEATING** 

HEAT RECOVERED FROM GAS AND SOLIDS OUTLET STREAMS:

In an additional steam cycle (SC)COE increases for very low CF

Integrated within the power plant steam cycle

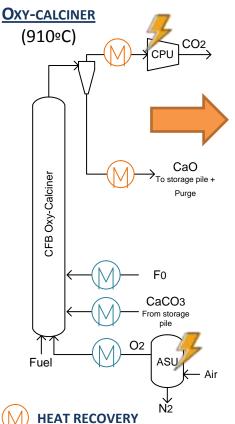
Allows reducing the coal thermal input for the maximum SC capacity  $\rightarrow$  Reduces  $CO_2$  flow  $\rightarrow$  Lower FlexiCal size required

P: Pressure (bar) REHEATER T: Temperature (°C) RH P= 0.05 P= 280.0 T= 31 HP TURBINE IP TURBINE LP TURBINE SH2 T= 447 T= 334 P= 0.9 P= 25.0 ECO BOILER FEED P= 335.0 DNDENSER T= 174 FEEDWATER HEATERS DEAEREATOR LP FEEDWATER HEATERS

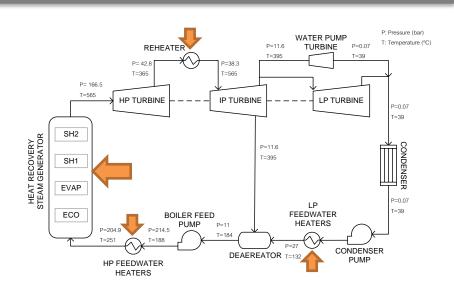
Replace bleedings to HP and LP feedwater heaters:

Reduced modifications in the existing power plant  $\rightarrow$  Low Capex

## Integration of the oxy-calciner block



**HEAT RECOVERED FROM GAS AND SOLIDS OUTLET** STREAMS TO RUN A SMALL **SUBCRITICAL STEAM CYCLE** 





Enough power available as to cover the electricity demand in CPU, ASU and auxiliaries of the oxy-calciner block



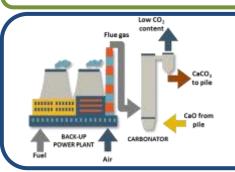


### Results for a case example

#### **MAIN ASSUMPTIONS:**

**Existing power plant:** 350 MW<sub>e</sub> power plant (reference 777 MW<sub>th</sub> for  $\eta$ =45%) operated under **CF=0.1** 

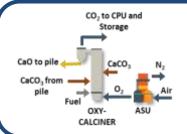
**Calcium looping**: T<sub>Carb</sub>=650°C, T<sub>Calc</sub>=910°C, X<sub>ave</sub>=0.35, E<sub>Carb</sub>=0.9 and E<sub>Calc</sub>=1



- □ 206 MW<sub>th</sub> from the carbonator are recovered in the power plant steam cycle
- □ Thermal power plant input in the back up plant can be reduced by a 12%
- Due to the absence of bleeds there is a certain penalty (~3 net points) on the steam cycle efficiency.

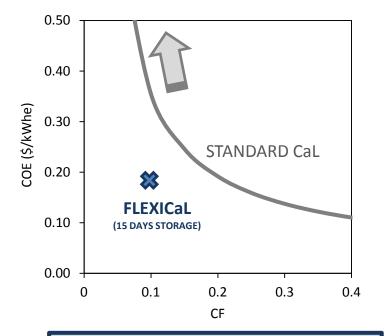


- CaO can be stored at <u>156°C</u> and CaCO<sub>3</sub> at <u>207°C</u>
- □ Between 2000 and 25000 m³ of solids per operation day of the power plant are required
- □ A purge of 0.1 Mton is annually produced



- Only represents an <u>8% of the total thermal capacity</u> (66 MW<sub>th</sub>)
- □ 12.5 MW<sub>e</sub> are produced in the associated steam cycle, being required about 11 MW<sub>e</sub> in the ASU, CPU and auxiliaries
- □ Net OVERALL energy efficiency 28%.
- □ Net energy efficiency DURING PICK POWER with CO<sub>2</sub> capture: 42%

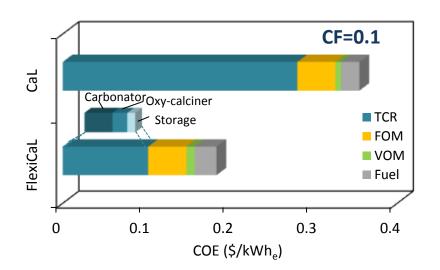
#### Cost analysis for the case example



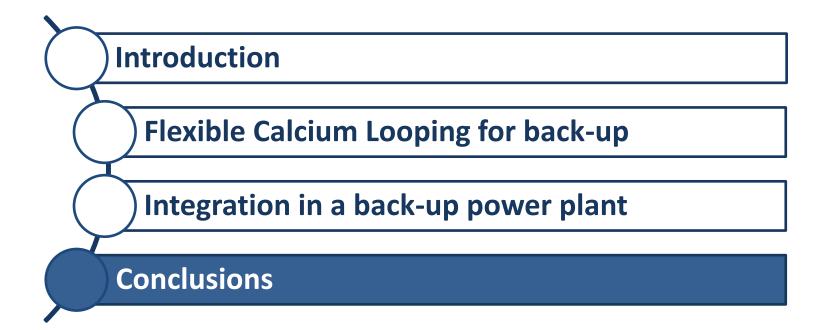
AVOIDANCE COSTS ARE HIGH (190  $\$/t_{co2}$ ) BUT LESS THAN HALF OF THE COST OF AN EQUIVALENT REFERENCE CAPTURE SYSTEM WITH CF=0.1

- Standard CaL (as other "conventional" CO<sub>2</sub> capture technologies) heavily penalized for extremely low capacity factors mainly due to the CAPEX
- Thanks to the reduced oxy-calciner size and the low-cost storage silos costs below 0.2 \$/kWhe are estimated for retrofitting amortized coal power plants with a CF of just 0.1

TECHNOLOGY	TCR (\$/kWe)
Standard CaL	2450
FlexiCaL (15 days storage)	900



#### **Outline**



#### **Conclusions**

- □ Calcium looping is a CO<sub>2</sub> capture technology with a large flexibility potential by its integration with a CaO/CaCO<sub>3</sub> solid storage system, which allows very low CF.
- □ Heat from the carbonator block can be recovered in the existing power plant steam cycle, reducing up to 12% fuel consumption
- Oxy-calciner block can operate in steady state mode. ASU and CPU can be selfsustained power generation from calciner waste heat
- Energy penalty is high (overall net energy efficiency  $\sim$  0.28) but energy is consumed during periods of low power demand, while 0.42 efficiency is retained during Back-up periods with CO<sub>2</sub> capture





10<sup>th</sup> Trondheim CCS Conference, 18<sup>th</sup>-19<sup>th</sup> June 2019, Trondheim, Norway

# Integration of a flexible Calcium Looping CO<sub>2</sub> capture system in a back-up power plant

Borja Arias, Yolanda A. Criado, J. Carlos Abanades

Spanish Research Council CSIC-INCAR, Francisco Pintado Fe 26, 33011, Oviedo, Spain

abanades@incar.csic.es

