

Trondheim CCS Conference 2019 June 17 – 19, 2019 – Trondheim, Norway



Advanced MEMBranes and membrane assisted procEsses for pre- and post- combustion CO₂ captuRe

MEMBER

https://member-co2.com/

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I. Introduction



MEMBER project aims to reduce the cost of the Carbon Dioxide capture technologies to fight against the climate change.

MEMBER has been built on the basis of the best materials and technologies developed in three former FP7 projects:

- \succ M⁴CO₂ (Energy efficient MOF-based Mixed Matrix Membranes for CO₂ Capture),
- FluidCELL (Advanced m-CHP fuel CELL system based on a novel bio-ethanol Fluidized bed membrane reformer),
- > ASCENT (Advanced Solid Cycles with Efficient Novel Technologies)

H2020 – Topic addressed:

NMBP-20-2017: High-performance materials for optimizing carbon dioxide capture





2. Project Objectives



The key objective of MEMBER is to demonstrate state-of-the-art CO_2 capture technologies in an industrially relevant environment. To achieve this, MEMBER will scale-up and manufacture advanced materials and prove their added value in terms of sustainability and performance at TRL 6 in novel membrane based technologies for pre- and post-combustion CO_2 capture in power plants as well as in H₂ generation systems with integrated CO_2 capture and meet the targets of the European SET plan.

Two different technological solutions involving advanced materials will be developed and demonstrated at three different end user's facilities:

- > Advanced Mixed Matrix Membranes (MMMs) for pre- and postcombustion CO_2 capture in power plants ($H_2/CO_2 \& CO_2/N_2$ respect.)
- > A combination of metallic hydrogen membranes and CO_2 sorbent integrated into an advanced Membrane Assisted Sorption Enhanced Reforming (MA-SER) process for pure H₂ production with CO₂ capture.





2. Project Objectives



- Prototype A, targeted for pre-combustion capture in power plants using MMMs at the 2MWth biomass gasifier of CENER (Spain) aimed for BIO-CCS demonstration.
- Prototype B targeted for post-combustion capture in power plants using MMM at the 8.8MW CHP facilities of Agroger (GALP, Portugal).
- Prototype C targeted for pure hydrogen production with integrated CO₂ capture using MA-SER at the IFE-HyNor Hydrogen Technology Centre (Norway) under the supervision of ZEG POWER.

| | | O | | / 1 |
|---|------------|--------------------------------|-------------------------|---------------|
| | Technology | CO ₂ Capture [%] | Capture cost [€/ton] | Demo site |
| Pre-comb. Power (IGCC) | MMM | > 90 | < 30 | CENER |
| Post-comb. Power (Coal) | MMM | > 90 | < 40 | GALP |
| H ₂ with integrated CO ₂ capture | MA-SER | > 90 | < 30 | IFE- HYNOR |

Main operation conditions & performance targets for the MEMBER prototypes.

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OBJ. I: MARKET & BUSINESS OBJECTIVES

- > To overcome CCS market barriers with an ambitious set of CCS solutions.
- To take European industrial companies (Materials manufacturers, engineering companies and end users) to a leading position in the CCS market, generating economic growth and job opportunities.

OBJ. 2: ECONOMIC OBJECTIVES

- Compliance with strict cost-effectiveness and performance targets:
 - Pre-combustion Mixed Matrix Membrane system for Power generation
 - Post-combustion Mixed Matrix Membrane system for Power generation
 - Mixed Matrix Membrane materials for MEMBER
 - MA-SER system for pure hydrogen production with integrated CO_2 capture
 - MA-SER materials for MEMBER







OBJ. 3: TECHNICAL OBJECTIVES

- To take to manufacturing development stage (from MRL 4-5 to MRL 6) a portfolio of materials and membranes of MMM technology:
 - Process optimization on pilot production lines (Polymers and MOFs).
 - Scaling production lines for the fine-tuned core material: MOF > 1kg/batch;
 - Scaling up the production of hollow fibres MMMs to >10.000 hollow fibers / batch
 - Scale up the membrane module size to >10 m²
 - Manufacturing of MMM modules for the pre- and post-combustion CO₂ capture in Power Plants
 - 0
- Move from MRL 4-5 to MRL 6 a portfolio of materials of MA-SER technology:
 - Scale up production for core material: Sorbents: 50-100 kg/day; catalyst: 50 kg/batch;
 - o Scaling up the production of Pd-based H_2 membranes to 8 membranes / batch
 - Lifetime Analysis of MA-SER at TRL6
 - Demonstration of compliance with CCS codes and standards. Installations in experimental demo plants to support and provide additional information on product characterization from qualification testing.







OBJ. 3: TECHNICAL OBJECTIVES

- Development of a software tool to simulate MEMBER components and CO₂ capture energy performance from the earliest design phases:
 - Module/reactor design and process simulation (at large scale) for full integration of the MMM systems for pre- and post-combustion, and for MA-SER for pure H₂ production with integrated CO₂ capture
 - Development of a model of the MA-SER reformer
 - Validation of the models through demonstration in relevant conditions (demo site)

OBJ. 4: DEMONSTRATION OBJECTIVES

Demonstration of MEMBER systems and related business models in 3 representative demonstration sites across Europe, covering different sectors, membrane based technologies and CO₂ containing streams





3. Main Goals and S&T objectives



OBJ. 5: ENVIRONMENTAL OBJECTIVES

To quantify the environmental impacts of the proposed holistic solutions through life cycle assessment based on 3 case studies throughout Europe

OBJ. 6: SOCIAL OBJECTIVES

Job creation and increase awareness and involvement within the whole social & industrial chain: plant owners, manufacturers, installers, authorities, students, CCS organizations, general public, etc.





4. Partnership





- Multidisciplinary and complementary team.
- I7 partners from 9 countries.
- Industrial oriented (65%):
 - II SME/IND + 6 RTO/HES
- > 7 SMEs (41%) & 4 IND (24%)

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5. Overall approach and methodology



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Inspiring Business







5. Overall approach and methodology



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Inspiring Business



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| # | Main exploitation product/ technologies/ others | | |
|----|--|--|--|
| I | MMM based system for pre-combustion CO ₂ capture | | |
| 2 | MMM based system for post-combustion CO ₂ capture | | |
| 3 | MA-SER system for pure H_2 production with integrated CO_2 capture | | |
| 4 | Advanced polymers for post-combustion MMMs | | |
| 5 | Advanced MOFs for pre- and post-combustion MMMs | | |
| 6 | Advanced MMMs for pre- and post-combustion | | |
| 7 | Advanced sorbents for MA-SER | | |
| 8 | Advanced catalysts for MA-SER | | |
| 9 | Advanced Pd-based H ₂ membranes for MA-SER | | |
| 10 | Software tool for Membrane reactor and SER design. Membrane | | |
| | separation modules | | |
| | Consulting services on LCA of CO ₂ capture | | |





7. Prototype status: Prototype A



System layout selected

- I membrane module system, operating at 4.5 bar Recovery rate 88%; Purity: 98.3%.
- Multi-module systems enhance the hydrogen recovery: 73% (I stage) to 86% (2 stages)
- Lower Permeance reduces the hydrogen separation
- Reduced Selectivity reduces the CO₂ recovery
- System states defined
 - Start-up sequence, normal operation, stand-by, controlled shutdown and emergency shut-down described

> P&ID made

- o Interfaces with gas cleaning system and gasifier defined
- Power consumption estimated
- Information documented in Process Book Prototype A





7. Prototype status: Prototype B



System layout selected

- 2 membrane module system, operating at 8 bar_a
 Membrane area 10 m² and 0.7 m² respectively for module 1 and 2
 Recovery rate >90%; Purity: >90%.
- Reduced Permeance lowers the recovery while purity is not affected
 - An increase in operation pressure can counteract the effect
- Lower Selectivity lowers the CO₂ purity
- System states defined
 - Start-up sequence, normal operation, stand-by, controlled shutdown and emergency shut-down described

P&ID made

- Interfaces with the 8.8 MW CHP facility of Agroger defined
- Power consumption estimated
- Information documented in Process Book Prototype B





7. Prototype status: Prototype C



Process scheme

• The process scheme has been finalised in order to integrate the MA-SER reactor in existing facility at IFE-HyNor premises

MA-SER reactor

- The design of MA-SER reactor has been addressed in order to address the project objective of pure H_2 production with integrated CO_2 capture
- Piping & Instrumentation Diagrams
 - Interfaces with the existing facility at IFE-Hynor premises defined
- Information documented in Process Book Prototype C





Reference Systems, to which MEMBER systems are compared

| | Without capture | With capture |
|---|--|--|
| Pre-combustion | IGCC power plant | IGCC power plant with Selexol absorption |
| Post-combustion | Coal Power Plant | Coal Power Plant with MEA absorption |
| Integrated H ₂ production | Steam reforming process (biomass based scenario) | Steam reforming process with MDEA absorption |





Thank you for your attention



https://member-co2.com/

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