

Intensified post combustion solvent based CO₂ capture using a RPB absorber and rotating regenerator

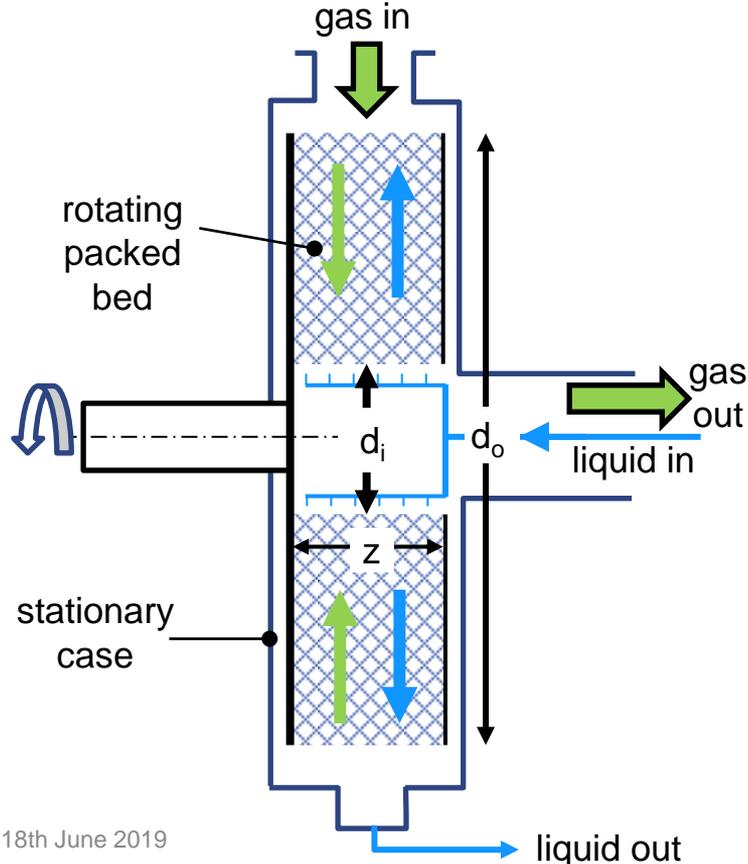
Jonathan Lee, Pierrot Attidekou, Tolu Kolawole, James Hendry
Process Intensification Group, School of Engineering, Newcastle
University, UK.

Robin Schulz, Thomas Rabold
Julius Montz GmbH - Hofstr. 82 - 40723 Hilden, Germany

Talk Outline

- What is a rotating packed bed.
- Carbon capture using rotating packed beds.
- Effect of flow configuration on CO₂ absorption.
- Integrated solvent regenerator and reboiler
- Conclusions
- Future work

What is a Rotating Packed Bed (RPB)?



d_i depends on the outlet gas velocity

z depends on the flooding limit at d_i

d_o depends on the mass transfer duty

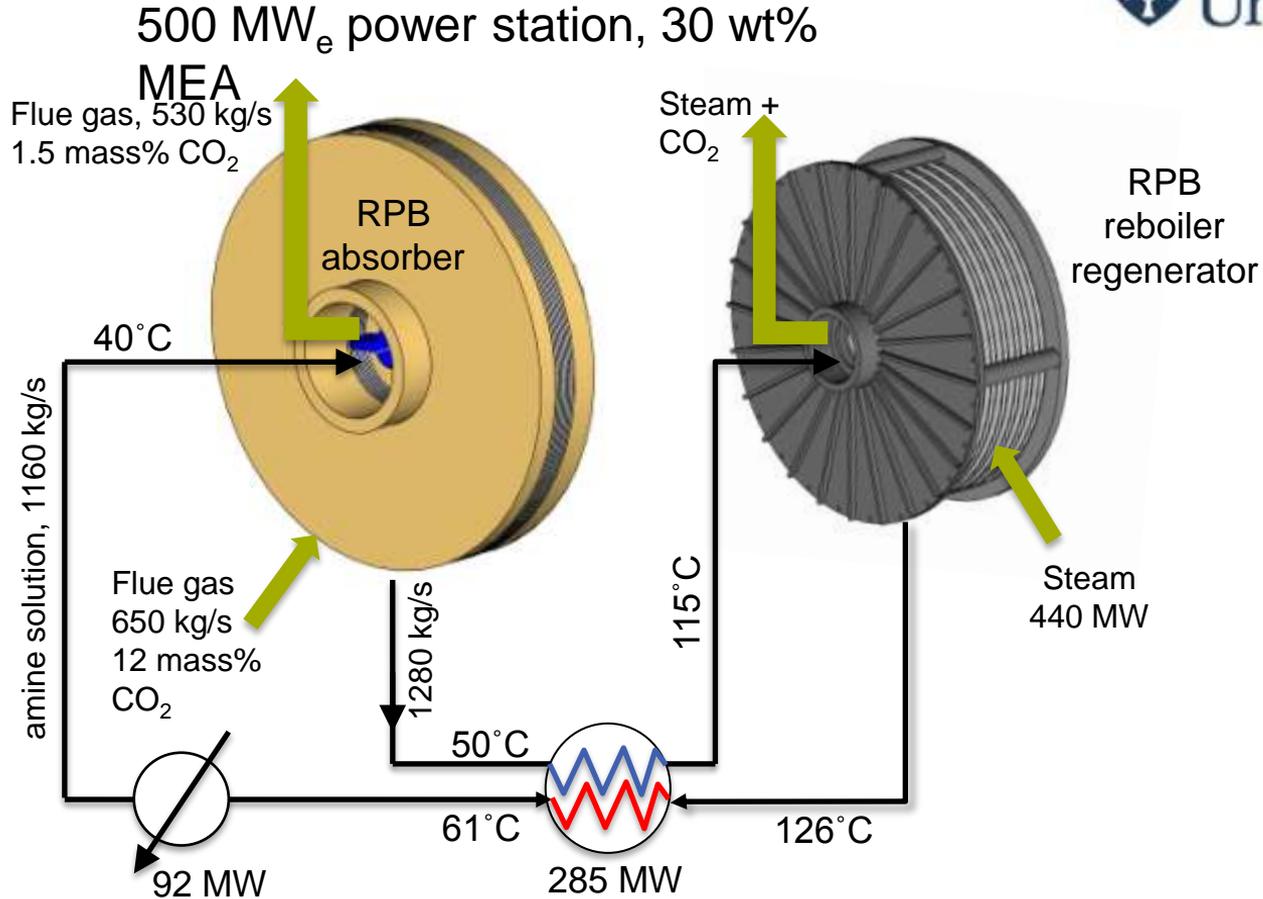
z is comparable to packed column diameter

$d_o - d_i$ is comparable to packed column height

Rotation decreases both z and d_o , and reduces packing volume by 1-2 orders of magnitude

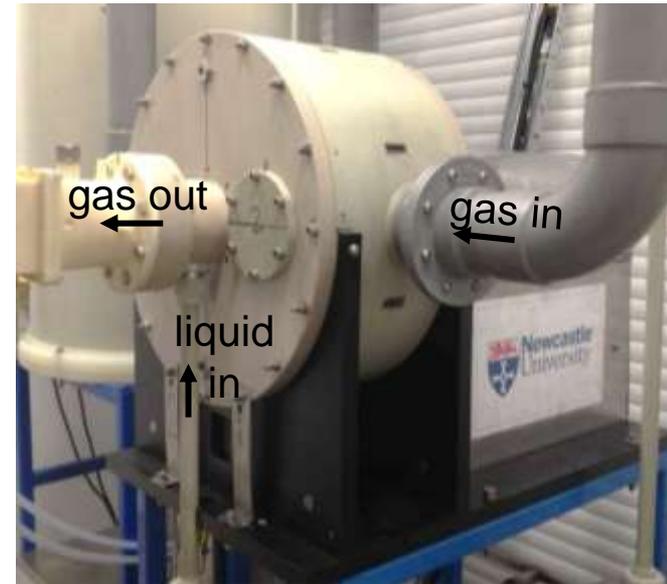
Civil engineering costs eliminated

Carbon Capture Using RPB

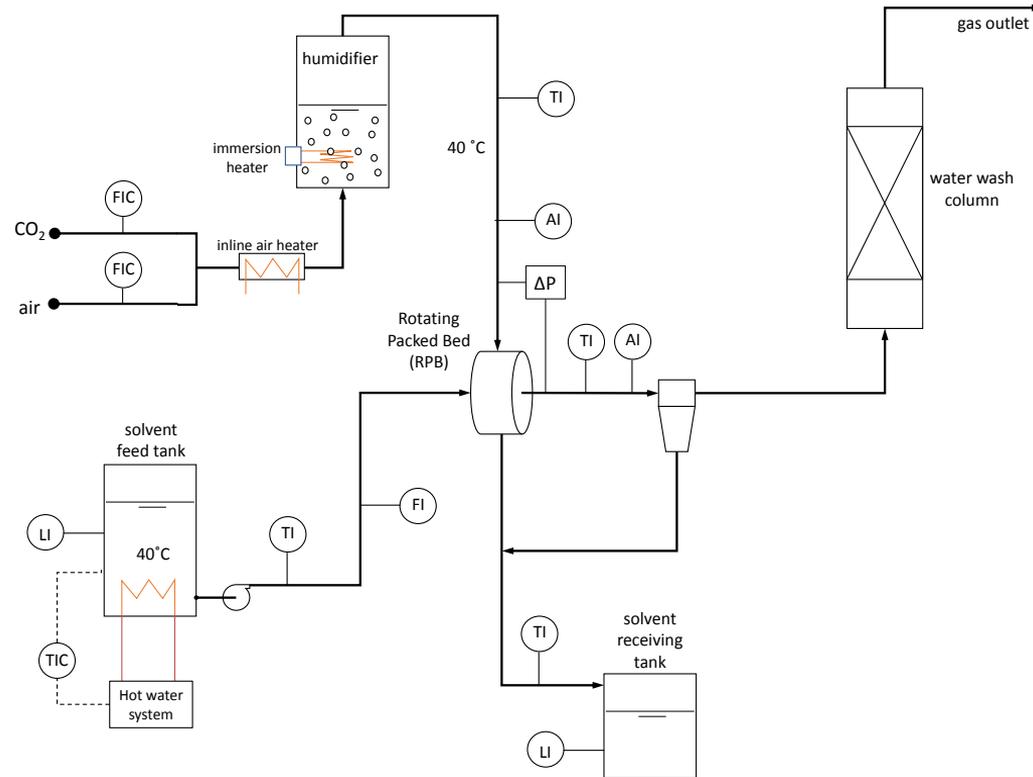


CO₂ Capture Using RPB

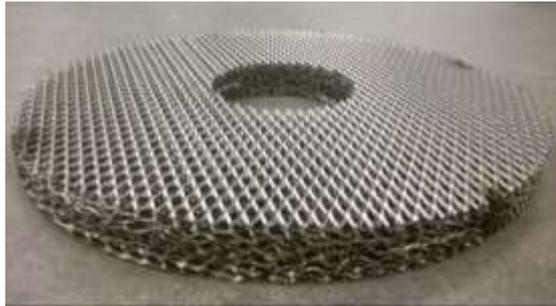
280 mm diameter gas absorption rig



Experimental Setup



Packing Materials



Stack of expanded SS316 mesh sheets

$$a_p = 663 \text{ m}^2 \text{ m}^{-3} \quad \varepsilon = 0.80$$

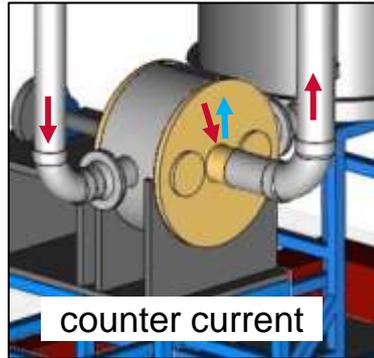


Montz structured packing – first prototype

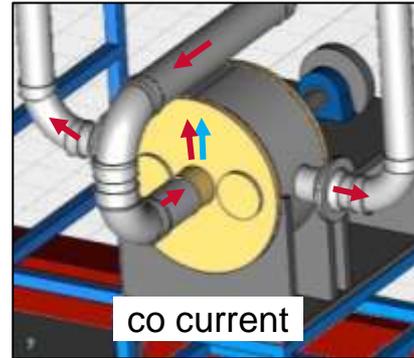
$$a_p = 830 \text{ m}^2 \text{ m}^{-3} \quad \varepsilon = 0.94$$

Gas-liquid flow configurations

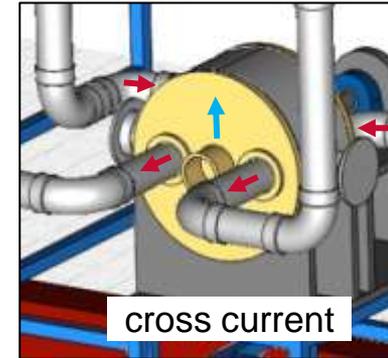
liquid flow  gas flow 



- High $K_G A$
- High ΔP
- High $\text{Power}_{\text{liq}}$



- Low $K_G A$
- Low ΔP
- High $\text{Power}_{\text{liq}}$



- Intermediate $K_G A$
- Low ΔP
- Lower $\text{Power}_{\text{liq}}$

Design of Experiments: 3-level face centered composite

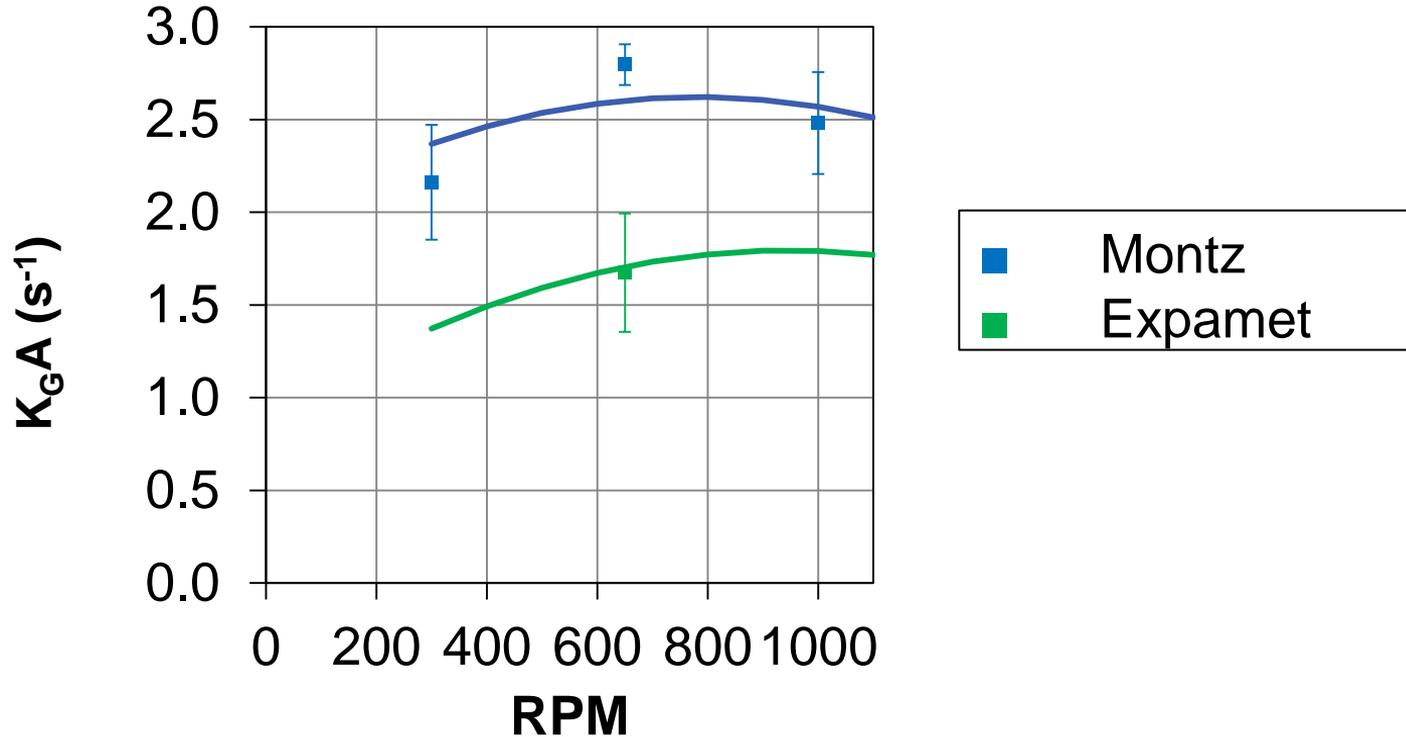
rpm - 300, 650, 1000

$(L/G)_{\text{mass}}$ - 2, 4, 6

MEA - 30%, 50%, 70%

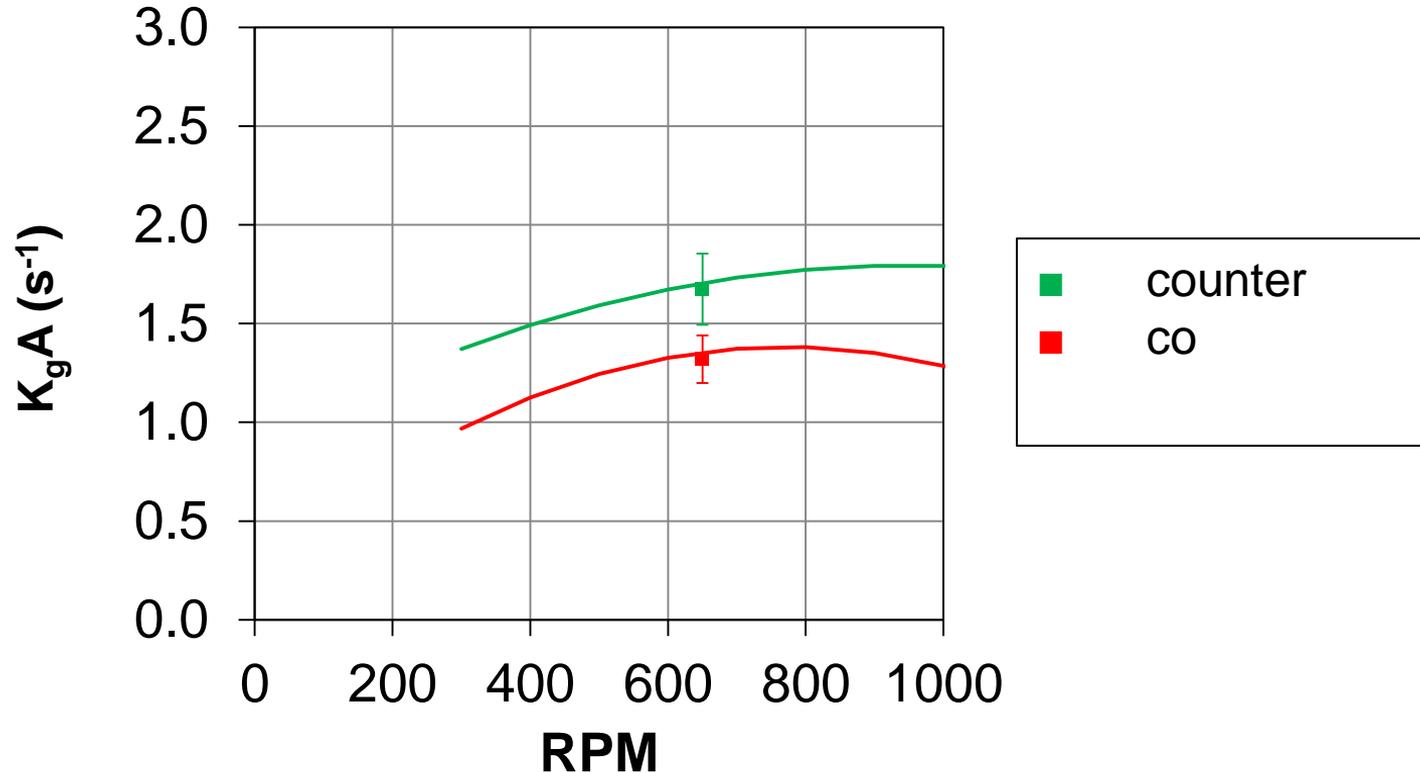
Comparison of Expamet and Montz

30 wt% MEA, $(L/G)_{\text{mass}} = 4$ ratio, counter-current flow



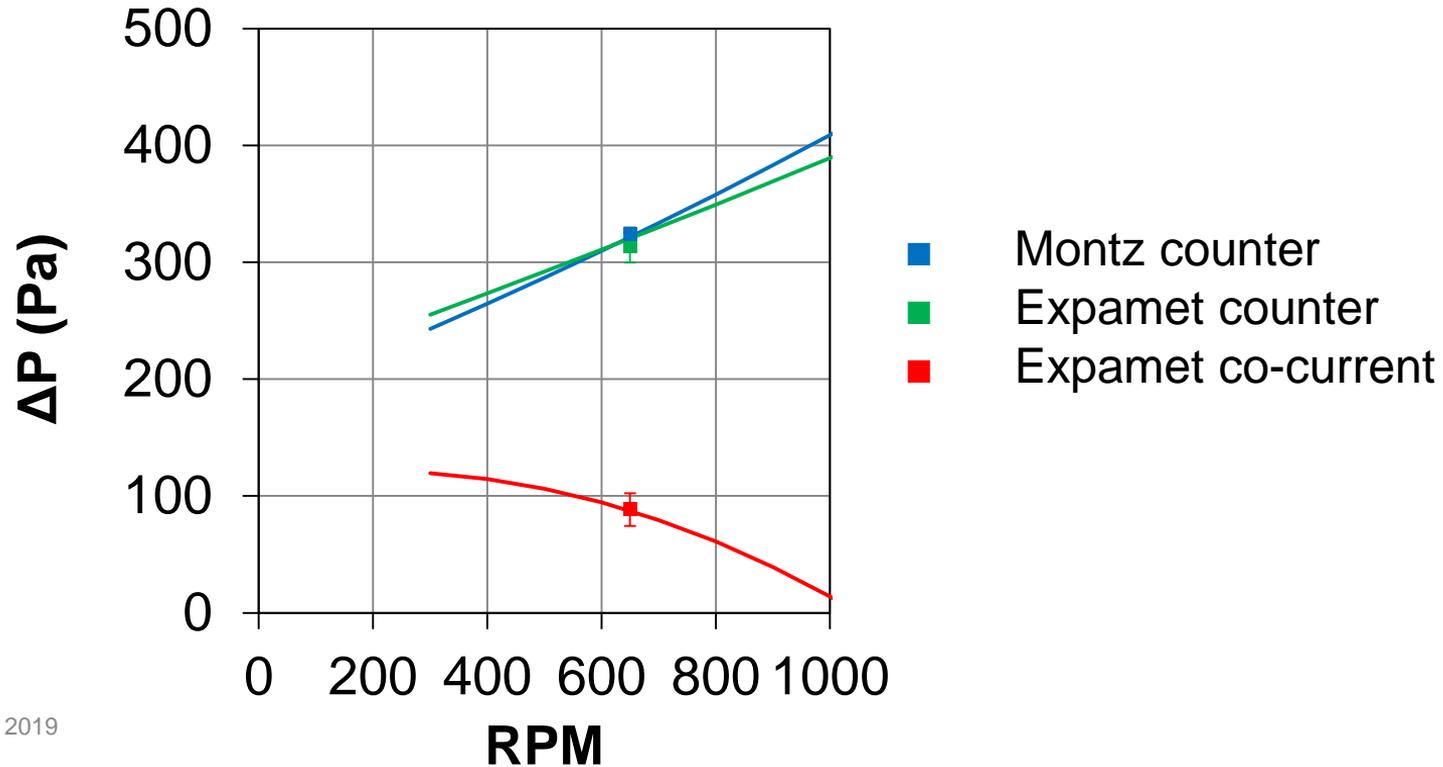
Comparison of Counter and Co Flow

30 wt% MEA, $(L/G)_{\text{mass}} = 4$, Expamet Packing

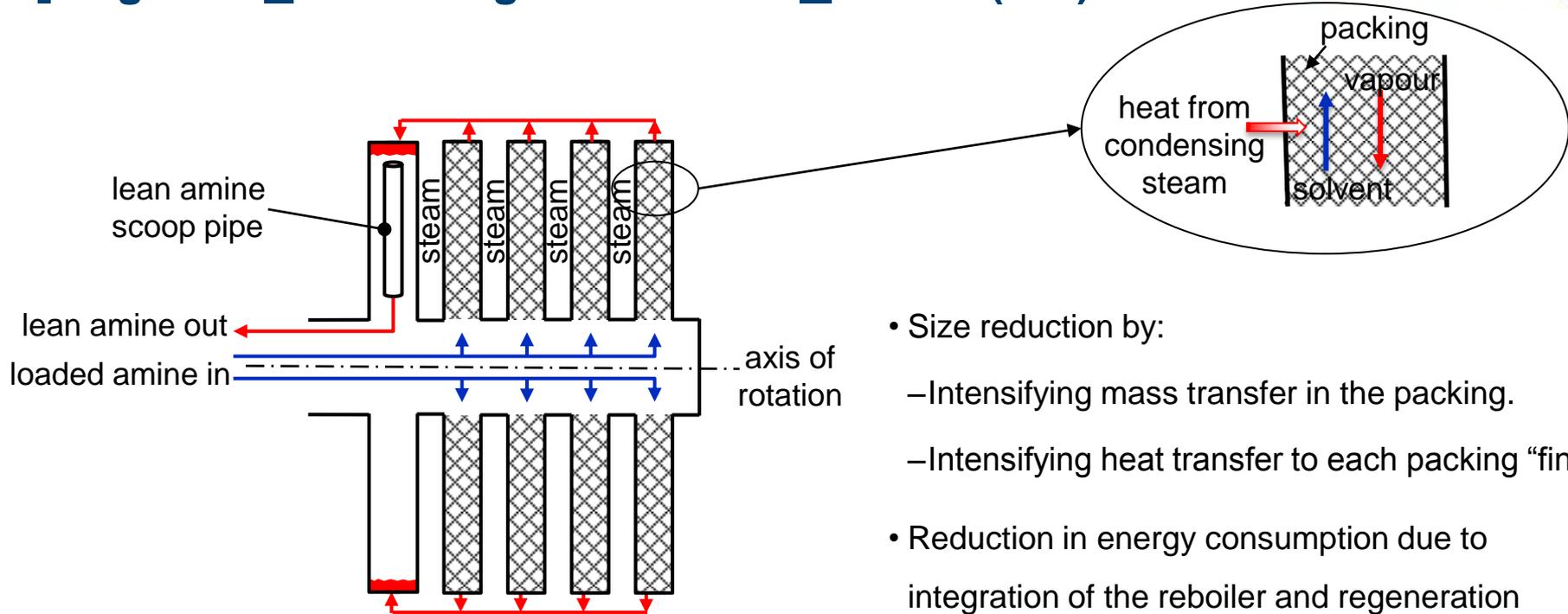


Comparison of Pressure Drop

30 wt% MEA, $(L/G)_{\text{mass}} = 4$

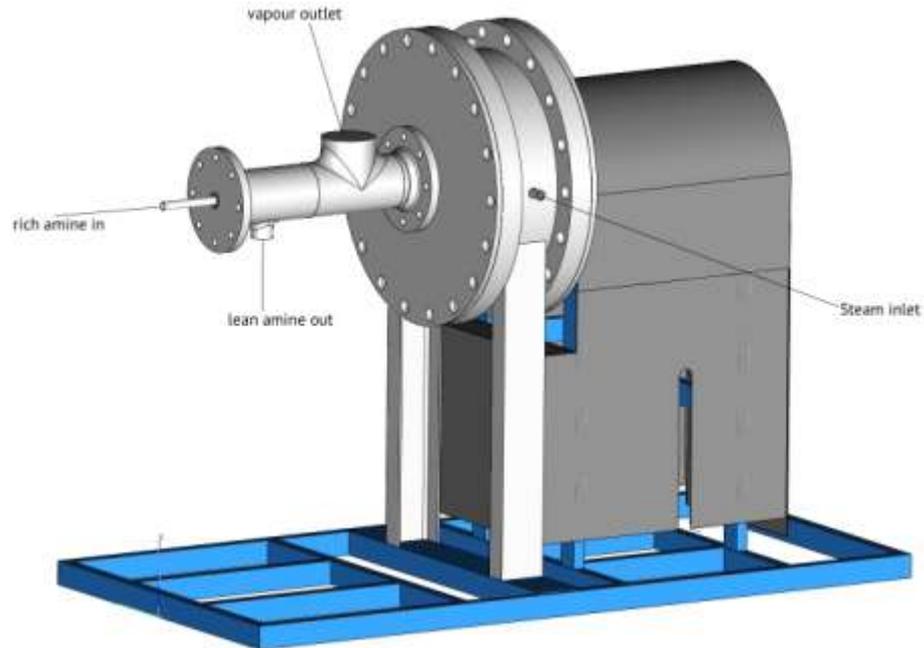


Integrated Solvent Regenerator and Reboiler (ISR)

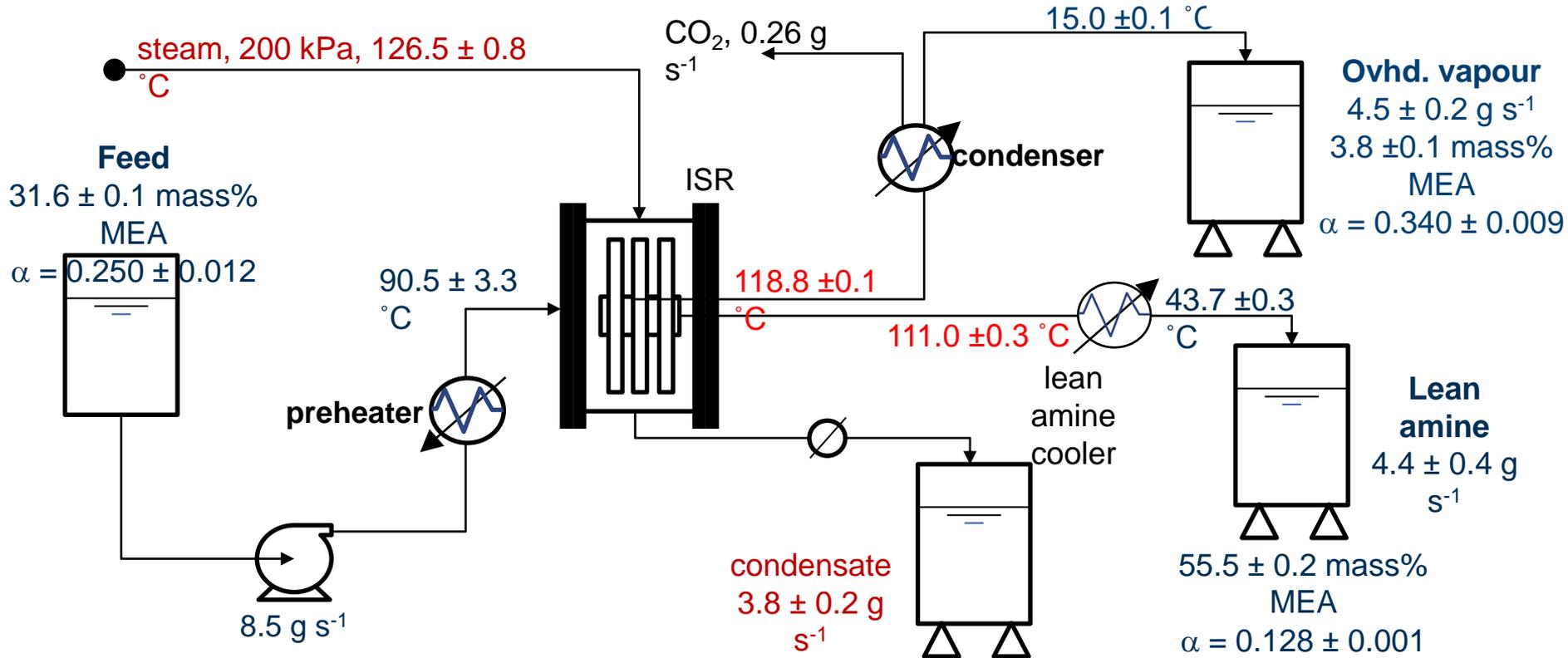


- Size reduction by:
 - Intensifying mass transfer in the packing.
 - Intensifying heat transfer to each packing “fin”.
- Reduction in energy consumption due to integration of the reboiler and regeneration column.

Construction of the Pilot Scale Unit



Experimental Setup

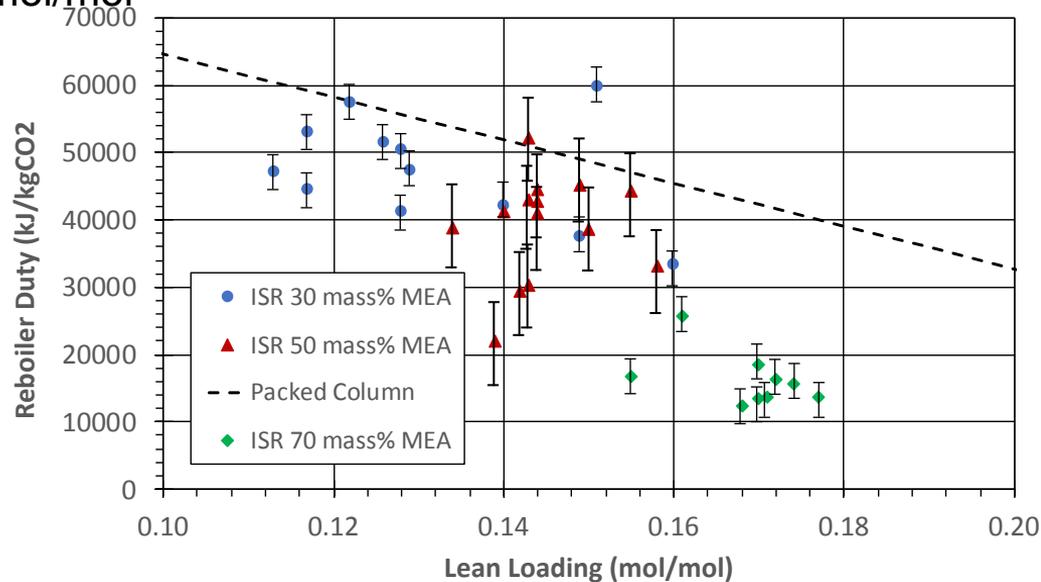


Reboiler Duty as a function of amine strength

Feed at 90 °C
mol/mol

Total reflux

Feed MEA loading = 0.24



- Compare to data of Sakwattanapong (2005)
- 30-50% reduction in loading.
- Reboiler duty decreases with increasing MEA solution strength due to decreasing reflux flow.
- For 30 mass% amine there is a saving of 13% on the reboiler duty compared to a packed column and separate reboiler.

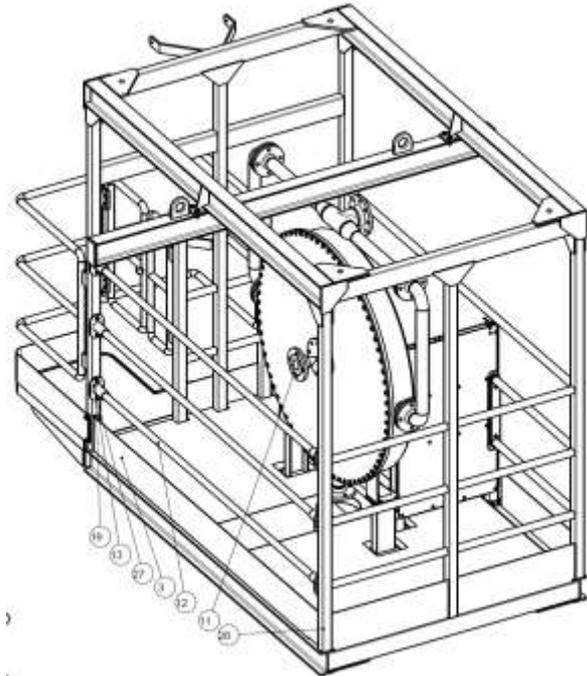
Conclusions

- RPB significantly increases rate of mass transfer compared to a packed column.
- The flow configuration of the absorber has a significant effect on the rate of mass transfer and the pressure drop.
- The reboiler and regenerator columns have been integrated.
- As well as reducing the size of the regenerator and reboiler, integration of the units reduces the reboiler energy use.

Future Work

Project Artemis – Testing of RPB and ISR for 90% capture of CO₂

- Testing to achieve TRL 7.
- Work funded by UK government and CCSL.
- In partnership with University Sheffield.
- Test rig will be sited at CFACT near Sheffield
- RPB Absorber will be commissioned in July 2019.
- ISR will be commissioned in September 2019.



Acknowledgements



EU Horizon 2020 grant
agreement 727503.

EPSRC

Engineering and Physical Sciences
Research Council

Grant Ref. EP/M001458/1



Department for
Business, Energy
& Industrial Strategy



ALSTOM

Lab scale rotating test rigs are available for solvent testing

Questions?