



HFC Meeting

Human Factors in Operational Risk
Management With Focus on Barrier
Management

HSE Experience of Incorporating
Human Reliability into LOPA and SIL
Analysis from an Engineers
Viewpoint

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HSE Experiences of Incorporating Human Reliability into LOPA and SIL Analysis from an Engineers Viewpoint



- Introduction.
- My background.
- Introduction to LOPA.
- Human reliability in LOPA
- Operator involvement in LOPA
- Example Buncefield LOPA operator tasks.
- Human factors issues in LOPA and SIL determination.
- Guidance associated with LOPA and Human Factors.

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My Background



Dr Colin Chambers CEng MIET

- **Background**
 - Degrees in Electronic Systems, Control Engineering and Computer Science.
- **Worked at HSL since 1996**
 - Development of risk assessment methodologies.
 - COMAH safety report technical assessor EC&I.
 - SIL determination assessor & LOPA specialist.
 - Served on Process Safety Leadership Group (PSLG) LOPA sub-group.
 - Helped develop PSLG guidance on LOPA.
 - Member of competent authority (CA) group who assessed all post Buncefield LOPA studies for the UK bulk fuel storage sector.

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Introduction



- My experience of working in HSE and with the UK petrochemical industry is that EC&I engineers and Process Safety engineers have been tasked with determining and reviewing Safety Integrity Levels (SIL) using methods such as Layer Of Protection Analysis (LOPA).
- It is also my experience that many processes within the petrochemical industry rely on operator involvement to perform critical control tasks and implement risk reduction measures.
- This talk presents a brief picture of HSE's experience of how engineers have accounted for human reliability in LOPA used for SIL determination.

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What is LOPA

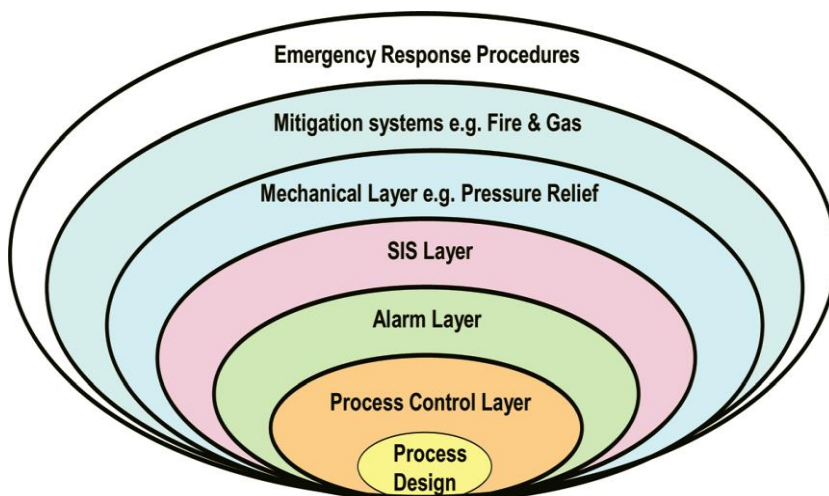


- LOPA can be thought of as a method of assessing the balance between process risk and its risk reduction factors.
- LOPA represents the process safety Onion Layer Model of process risk reduction.
- The output from a LOPA is a mitigated event frequency, which is compared to a target frequency.

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Onion Layer Model: Layers Of Protection



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LOPA rules and their application to operator actions



LOPA rules support the requirements of IEC 61511 for SIL determination and guard against dependent failures.

- Independence.
 - Between independent protection layers (IPL), initiating event (IE) and conditional modifiers (CM) for each initiating event.
- Effectiveness.
 - The IPL is able to prevent the process entering an unsafe state without relying on any other risk reduction measure.
 - Layer completeness – ‘detect – think – do’.
- Auditability.
 - Must be able to demonstrate, with documented evidence, all of the above issues associated with an IPL.

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LOPA limitations with respect to operator involvement



- Requires independence between all layers of protection and the process control system for each initiating event.
 - Operator performs control and risk reduction tasks.
- LOPA is not well suited to complex systems.
 - Significant levels of dependent failure will violate LOPA independence assumptions.
 - Implementing and demonstrating independence of operator and operator tasks is problematic.
 - HSE has in-house human factors specialists who help determine whether independence has been implemented and demonstrated.

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HSE operational guidance for engineers applied to LOPA



- This diagram represents a truly independent layer of protection.
 - What if the operator initiates the final element from another IPL.
 - What if the operator relies on the BPCS sensor and annunciator.
 - What if the operator has other demands on his/her time.
 - LOPA does not consider these ‘what if’s’ so HSE does.
 - Each case above invalidates LOPA rules hence the IPL is not independent, hence HSE would not accept claims for credit in the LOPA.

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Human reliability in LOPA



- Within a LOPA study the assessment of operator contributions to process risk and risk reduction can be performed ‘offline’ using established methods.
 - Human reliability assessments, e.g. HSE is keen to see qualitative task analysis used in conjunction with a human reliability estimation tool such as HEART.
 - Fault tree analysis or reliability block diagram analysis to model failure logic.
- These methods can be used to determine the error rates/probabilities for the initiating events or risk reduction measures.
- There are difficulties in how do we establish whether an operator(s) maintains their estimated initial integrity?

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Human error rates/probabilities in LOPA



- For initiating events/causes in LOPA.
 - Equipment based initiating events use annual equipment failure rate.
 - Operator based initiating events use an annual operator error rate.
- For risk reduction measures (IPL).
 - Equipment based risk reduction measures use PFD_{avg}
 - Average probability of failure on demand.
 - Operator based risk reduction measures HEP.
 - Human Error Probability .

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Simplified error probability calculation used for SIL determination in LOPA



1. $PFD_{avg} = \lambda du \left(\frac{T_i}{2}\right)$
 2. $PFD_{avg}(\text{operator}) \approx \text{HEP?}$
 - HEP is generally considered to be the operator equivalent to PFD_{avg} .
- Where.
 - ' PFD_{avg} ' is the average probability of failure on demand.
 - ' λdu ' is the dangerous undetected failure rate per year.
 - ' T_i ' (hours) is the proof test interval.
 - ' HEP ' is the human error probability per demand.

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Human reliability data quality issues



- Assumptions implicit in data quality.
 - Site and circumstance factors not accounted for, e.g. EPC/PSF .
- Optimistic claims, especially for human reliability.
 - Even historical performance data may not be enough.
- Data sources used.
 - Same process same site historical performance data.
 - Same site similar process historical performance data.
 - Same or similar process historical performance different site.
 - Predicted failure rate from human reliability estimation method such as HEART, THERP etc.
 - Generic data (unsupported published data).

Basic Process control system (BPCS) definition



- A BPCS has been defined as all arrangements required to implement basic process control (PSLG final report).
- This includes operator actions.
- Performance limits placed on the BPCS in IEC 61511.
 - The IEC 61511 performance limit for a BPCS when claimed as an initiating event is 1E-5 dangerous failures per hour.
 - When claimed as a layer of protection a risk reduction factor of less than 10 can be claimed.
 - IEC 61511 references human factors but gives little or no help in how they should be incorporated into LOPA.

Operator as a layer of protection



- The PSLG guidance defined operator crosschecks to formalise operator intervention to address LOPA requirements.
- Operator crosschecks are independent protection layers that are.
 - Designed to prevent initiating events leading to dangerous failures.
 - Independent from the BPCS and from other independent protection layers.
 - Effective in performing the stated task.
 - Be able to detect a hazard and perform an appropriate action – often claims only consider detecting the hazard,
 - Supported by auditable records of their performance,
 - IEC 61511 IPL requirements.

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Buncefield examples of operator tasks assessed by LOPA



- Operator typically performs the following control tasks:
 - calculates tank ullage.
 - line up the relevant tank.
 - check that the correct tank is filling.
 - monitor the tank filling progress.
 - Switch over to next tank in filling sequence for large deliveries.
 - tank fill termination.
 - tank level control valve can be manually/electrically activated.
- Operator performs the following risk reduction tasks:
 - Regularly check tank levels
 - Responds to process alarms
 - Responds to critical alarms

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Buncefield incident UK: Operator tasks before and after



- Pre Buncefield tank filling operations relied on:
 - Operator control of the process.
 - Operator risk reduction measures.
- Post Buncefield tank filling operations relied on:
 - Operator control of the process.
 - Operator risk reduction measures.
 - Electromechanical final layer of protection.

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Operator error analysis problems associated with LOPA



- Only operator considered, not equipment they use.
- Data taken from sources not relevant to situation being considered.
- Task analysis rarely done, so HRA and hence HEP not supported.
- Data taken from published source without considering actual cause of error.
- Uncertainly regarding the definition of a BPCS.
 - Defined in the PSLG final report as 'All equipment and arrangements required to affect normal process control.'

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Assumptions about the operator



- Assumptions made about all parts of the assessment from the process, its operation, the number of persons involved.
- Assumptions can be optimistic or pessimistic and can balance out in the assessment, but this is not acceptable.
- Incorrect assumptions about operator rolls and performance are a significant source of error in a LOPA.
- Erroneous assumptions can be made because the LOPA was desk based.
 - Lack relevant information on how operator tasks are performed and what factors can affect operator.
 - The assessment team might not be representative in terms of relevant experience and expertise.

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Supporting evidence for operator involvement



- Within LOPA studies submitted to HSE supporting evidence, HSE sought includes.
 - Adequate description of the process
 - Adequate description of operator tasks who's failure could lead to a hazardous event occurring.
 - Adequate description of operator based layers of protection and other measures for which credit is claimed.
 - Reference to company procedures, if present, to support expected operator tasks.
- HSE asks can the evidence be verified, to what degree can it be verified – if poorly, then it might not be acceptable.

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Problems when incorporating operator actions within a LOPA



- Engineering standards such as IEC 61511 are based on the quantification of factors used to determine SIL.
 - Hence an engineers need to quantify.
- Concentrating on human reliability estimation numerically can divert focus from identifying barriers to mitigate identified human error possibilities.
- Engineers work to find ways of thinking about operator performance in a similar way to an item of equipment in terms of how their contribution to risk and risk reduction can be estimated.

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Guidance on Human Factors for LOAP and SIL determination



- Process Safety Leadership Group Final (PSLG) report (HSE) – Safety and Environmental Standards for Fuel Storage Sites.
- HSE Operational Guidance. Operator Response within Safety Instrumented Systems in the Chemical, Oil & Gas, and Specialist Industries <http://www.hse.gov.uk/foi/internalops/og/og-00047.htm> PSLG Guidance.
- Engineering Equipment and Materials Users' Association (EEMUA) Publication '191': Alarm Systems – A Guide to Design, Management and Procurement. (ISBN 0 85931 076 0) (Edition 3).
- Contract Research Report 373/2001 – Proposed Framework for Addressing Human Factors in IEC 61508.
- IEC 62508: Guidance on Human Aspects of Dependability (currently draft).

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Conclusions



- This talk has presented an engineers experience of how HSE and industry deal with some common human factors issues in LOPA and SIL determination.
- Industry attempts to find ways of accounting for operator performance and demonstrating this in LOPA studies has been problematic.
- Human reliability data and its applicability by industry has been problematic but is slowly improving.
- An approach has been to use task analysis and HRA methods such as HEART and incorporate the outcome into a LOPA analysis.
- There is guidance out there and HSE contributes to this guidance.
- We as engineers need to be more human factors aware.

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Thank you for listening



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