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ELECTRICAS



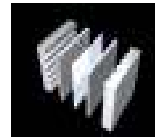
Gerencia de Energías
No Convencionales



Diagnosis of PEMFC operation using EIS

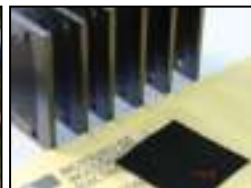
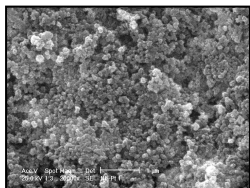
Electrical Research Institute

*Hydrogen and
Fuel Cells Group*



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*International Symposium on
DIAGNOSTIC TOOLS FOR FUEL CELL TECHNOLOGIES
Trondheim, Norway, June 2009*



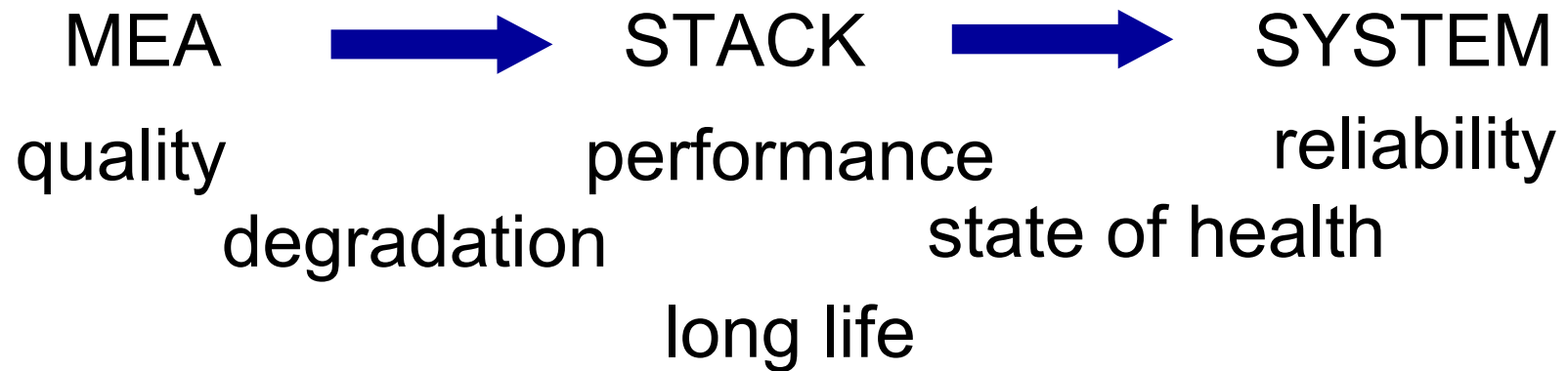


Tecnología de Celdas de Combustible

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Especificaciones Técnicas: CC-IE1k

Parámetro	Descripción
Tipo de Celda de Combustible	PEM
Área activa	50 cm ² (0.6A/cm ²)
Número de Celdas	70 - 75 celdas
Potencia Nominal	1kW (más 200W para auxiliares)
Voltaje de salida (regulado)	48 V d.c. (0.7V/celda)
Corriente de salida	30 A nominal, a 32A pico máximo (2 segundos)
Combustible	hidrógeno puro
Fuente de oxígeno	Aire atmosférico (filtrado)
Temperatura de operación	70°C
Presión de operación	1.0 bar
Embalaje	
Integración	
Elemento clave	
Módulo de operación	
Alimentación	



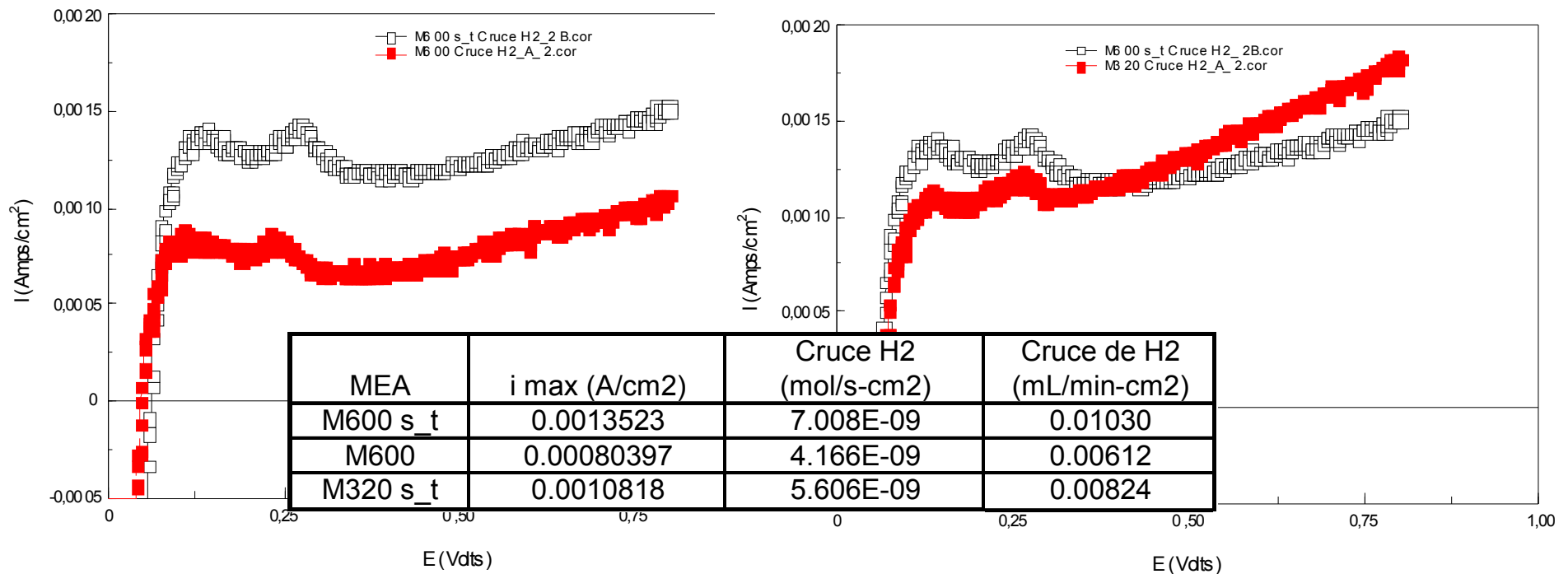


Characterization using d.c. techniques:

voltammetry – electrochem. active area

linear voltammetry – H₂ crossover (int. short circuit)

polarization curves – performance

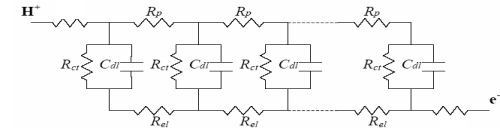
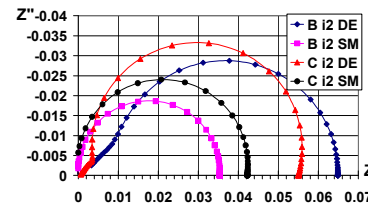




Interest on EIS as applied to Fuel Cells

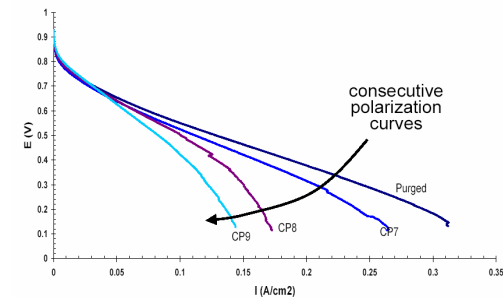
MEA development

- platinum activity follow-up
- bulk membrane resistance
- ionic conductivity at CL (through distributed element model)



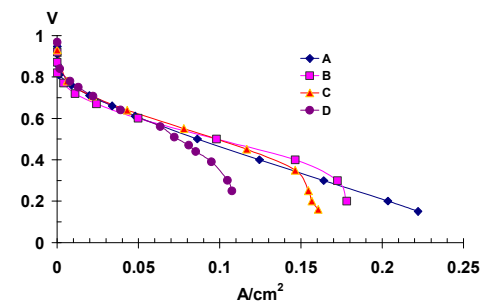
Stack

- sensitivity to operating conditions



Systems control

- Potential flooding/drying detection



Steady-state and transient models

- Combination of experimentally determined kinetic parameters with EIS-determined parameters for PEMFC dynamic model

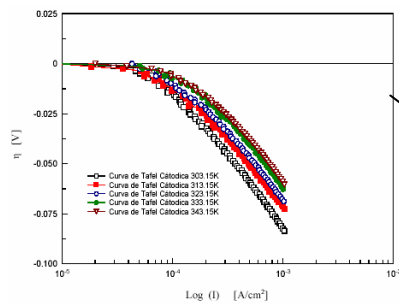


Figura 2. Curvas de Tafel obtenidas experimentalmente para el cátodo de una celda PEM

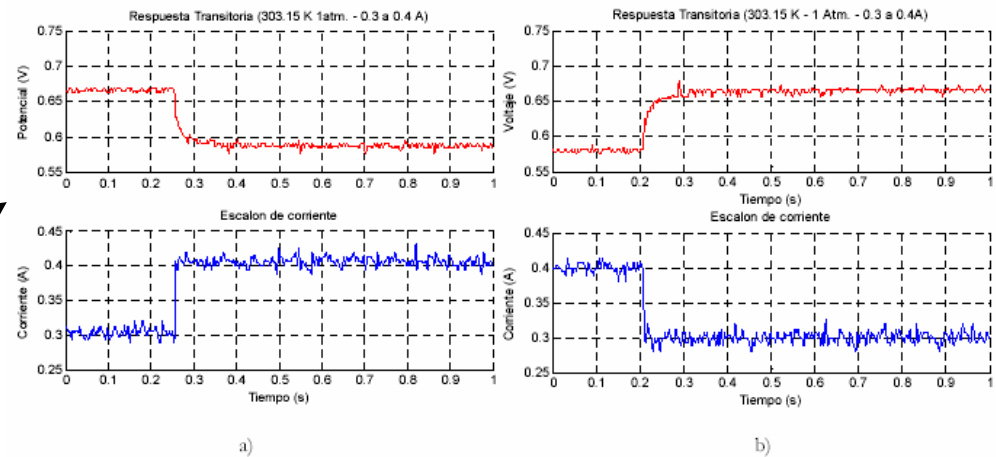
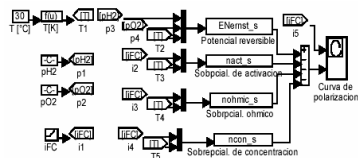
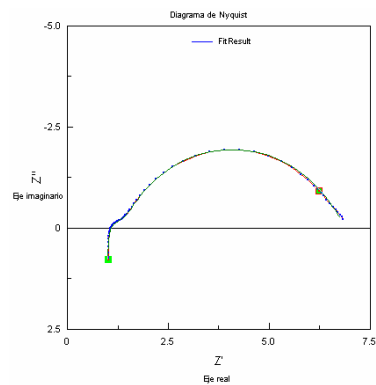


Figura 12. Respuesta transitoria de celda PEM: a) Flanco positivo. b) Flanco negativo

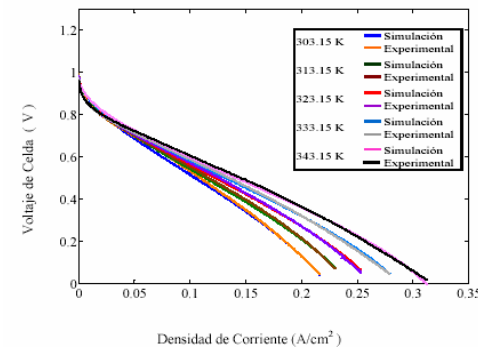


Fig. 3 Comparación de Respuestas (Modeladas vs. Experimentales)



Q = can EIS be used as a diagnostic technique during operation near flooding/drying conditions?

Facts & warnings:

- **EIS highly sensitive to changes within the fuel cell**
- **EIS response is strongly dependent on design**
- **If gradients (heterogeneities) along active area exist, EIS will pick them up**
- **“Dry” and excess of water may coexist in different regions of FC (as well as other effects)**
- **EIS should not be seen as a black or white result but as a color palette (i.e. interpreted as such)**



water dynamics near dry/wet limit

Dehydration Stage: (previously conditioned and purged)

- Tcell = 40 °C
- Cathode: P: 10psi; flow: air 0.5 L/min
- Anode: P= 10psi; gas exit closed
- t = 1hr, EIS for ohmic resistance @ Eoc

Rest Stage (no humidification):

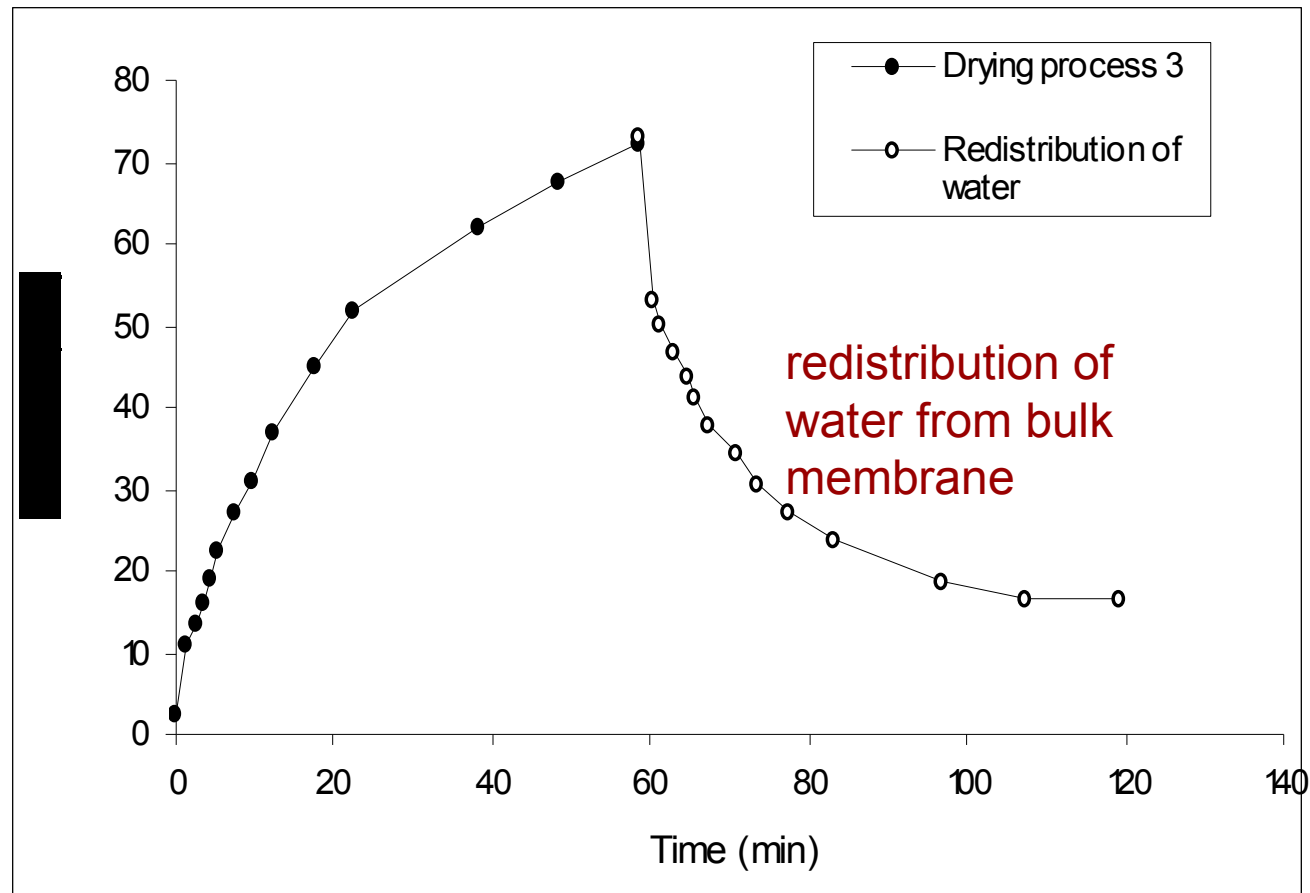
- Tcell = 40 °C
- Cathode, P = 10psi, Flow: air 0 L/min (just after dehydration process)
- Anode, P = 10psi, gas exit closed.
- t = 1hr, EIS for ohmic resistance @ Eoc

MEA: 25cm², Gore, Pt = 0.7 mg/cm², carbon paper, DL = 50μ,
GFF: simple serpentine



cell's ohmic resistance

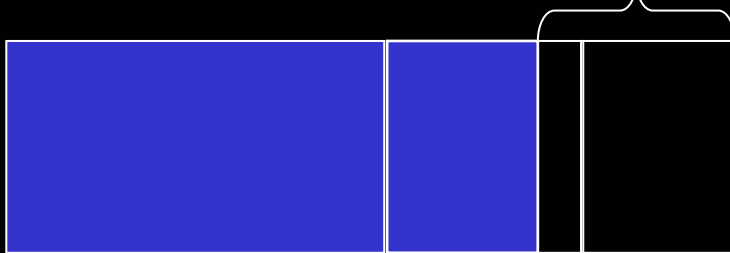
determined by high frequency intercept



*low conductivity final current collectors plates used

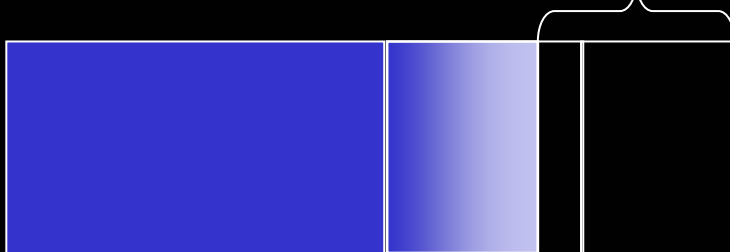


M CL DL



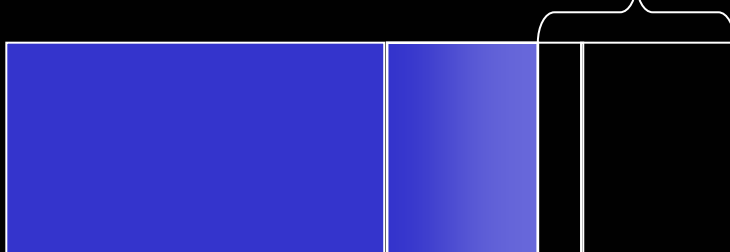
after conditioning

M CL DL



after high air flux
CL w/H₂O gradient

M CL DL



after 1 hr rest
H₂O redistributes in CL



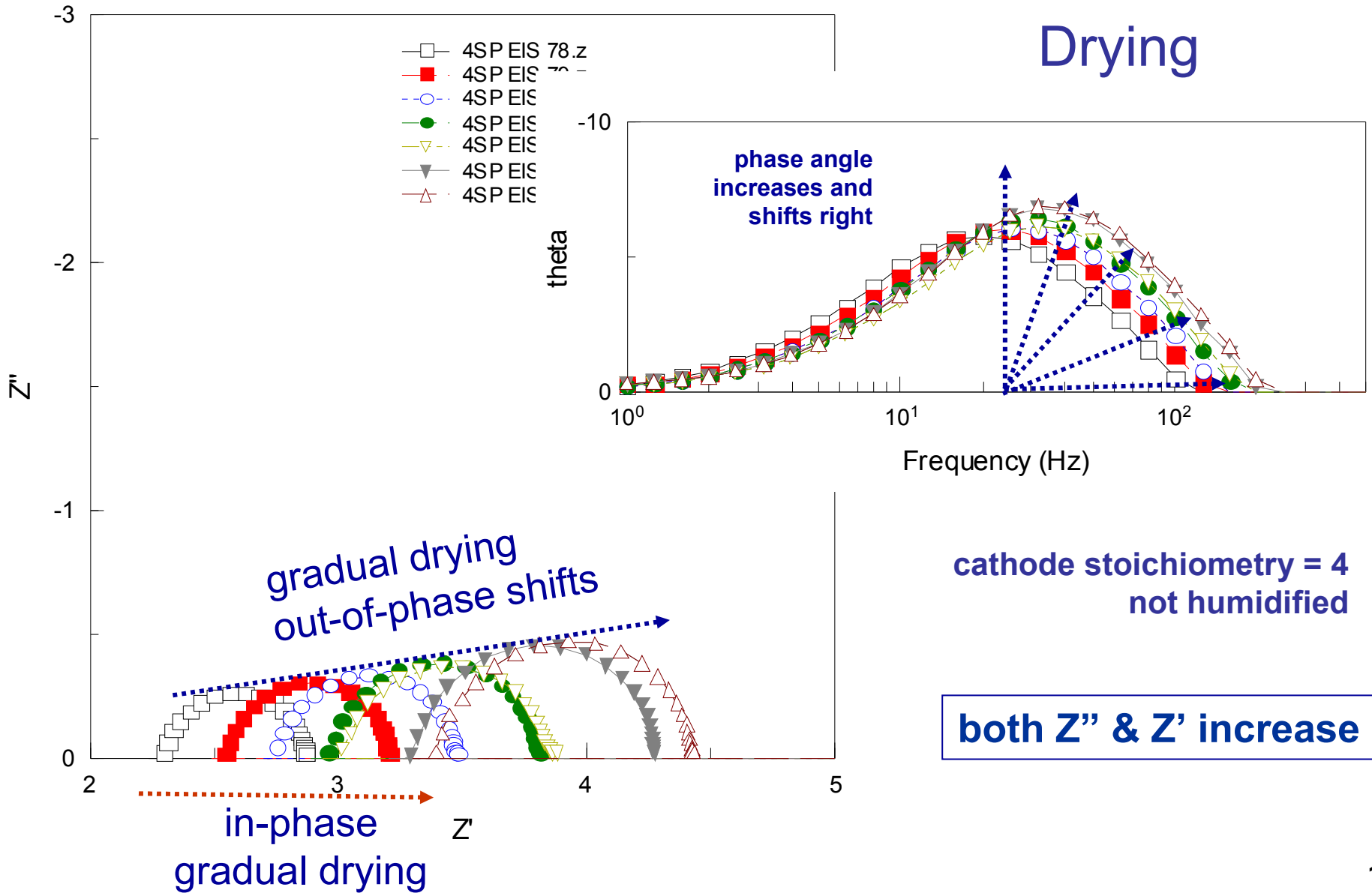
Real life is cruel for EIS:

Practical operating conditions are hardly under steady-state, it depends on specific application and design

Experimental approach:

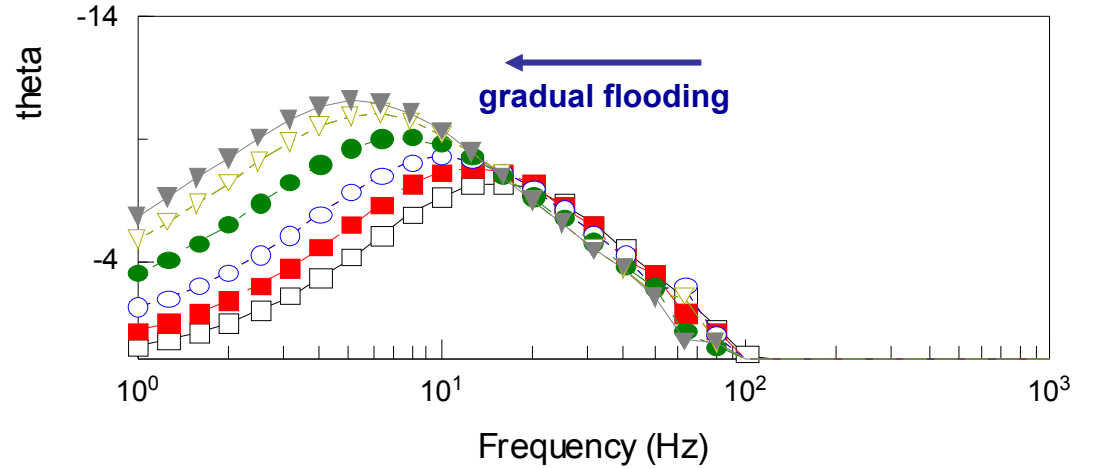
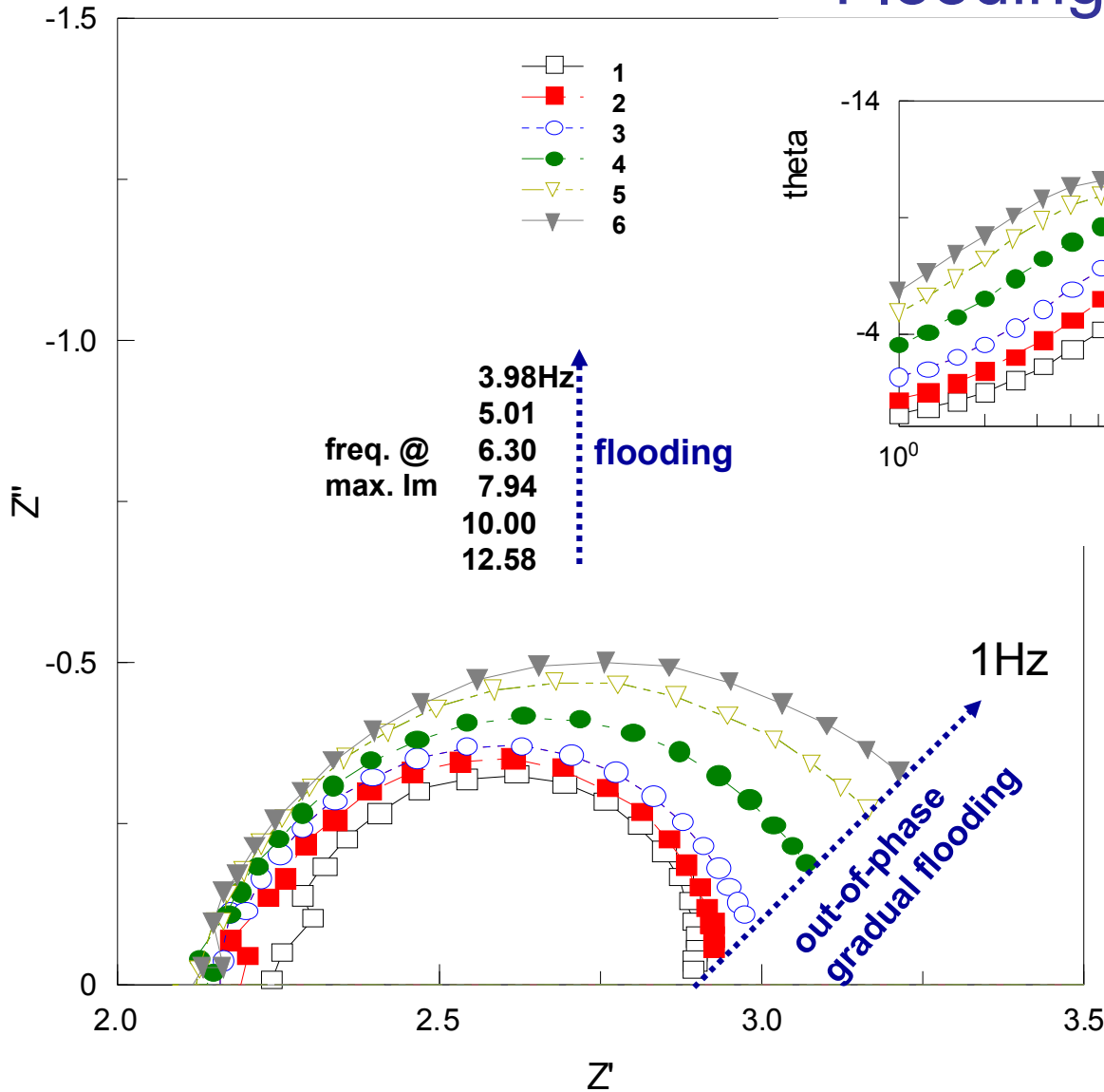
- Initial conditioning
 - Operating near the limit of drying/flooding
 - EIS (1Hz to 1KHz), 10mV ($E_{cell} = 0.4V$)
- low T & stoich's
 - dead ended configuration
 - purge stages
 - dry feeds
 - use of O_2

Own 50 cm² MEA, GFFc = 4ps, GFFa pch. 0.7 mg Pt/cm², Nafion NRE-212. GDL-30-BC (C paper w/MPL). T=343.15 K (70°C) & 69 kPa (10 psi)

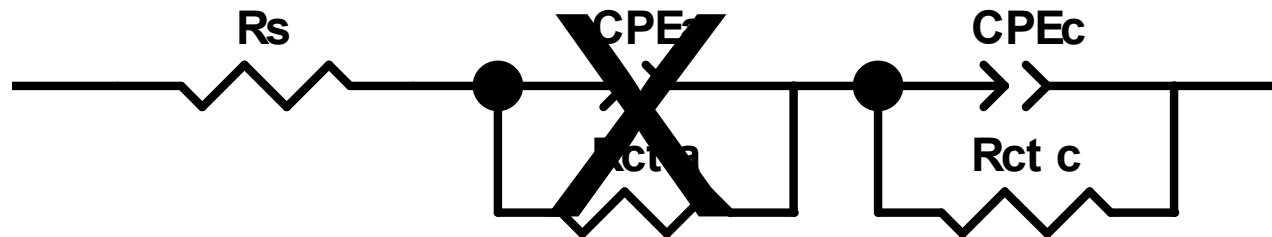




Flooding



EIS: every 20 mins.



R_s = total ohmic resistance

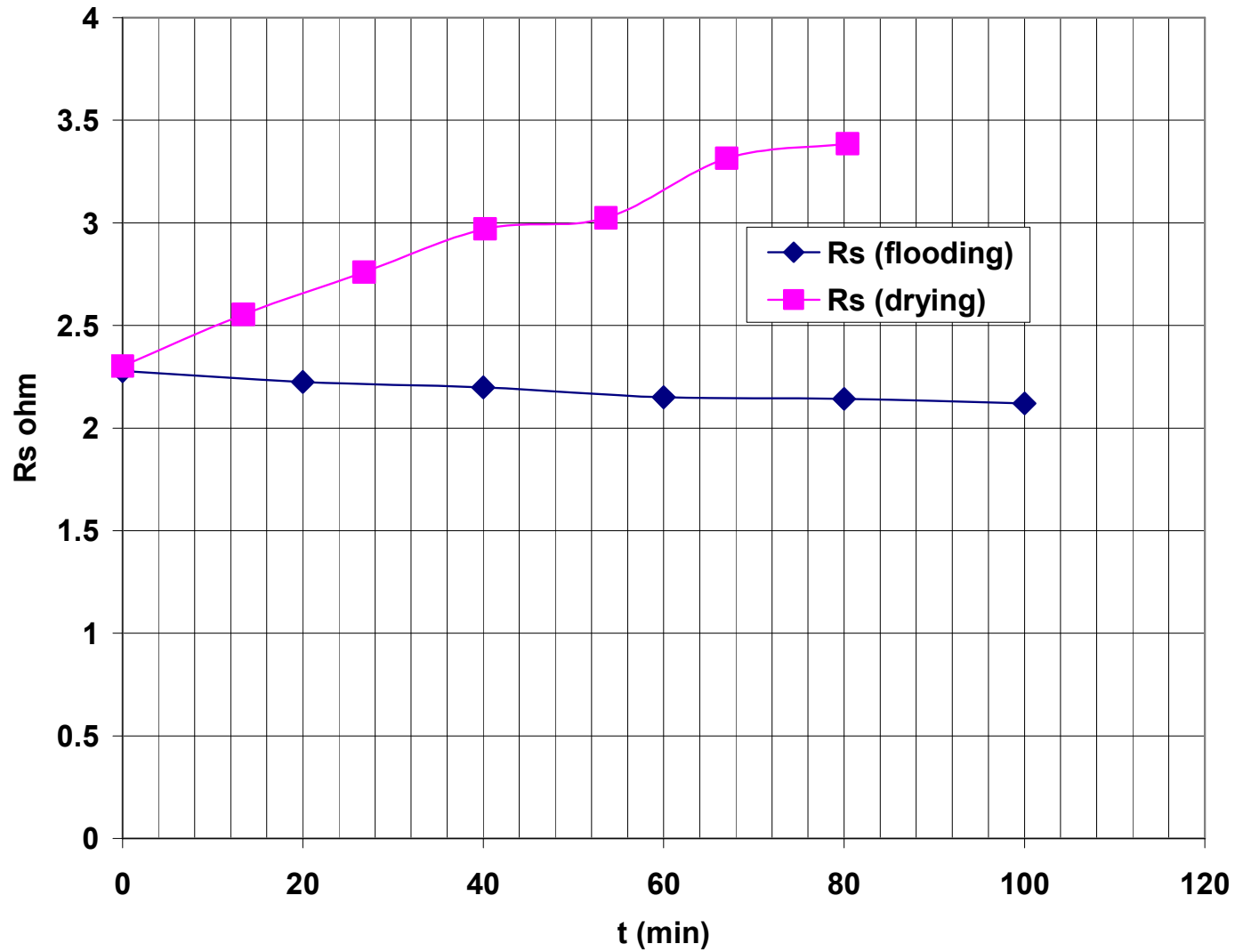
$R_{ct a}$ = anode charge transfer resistance

$CPEa$ = non-ideal double layer capacitance anode

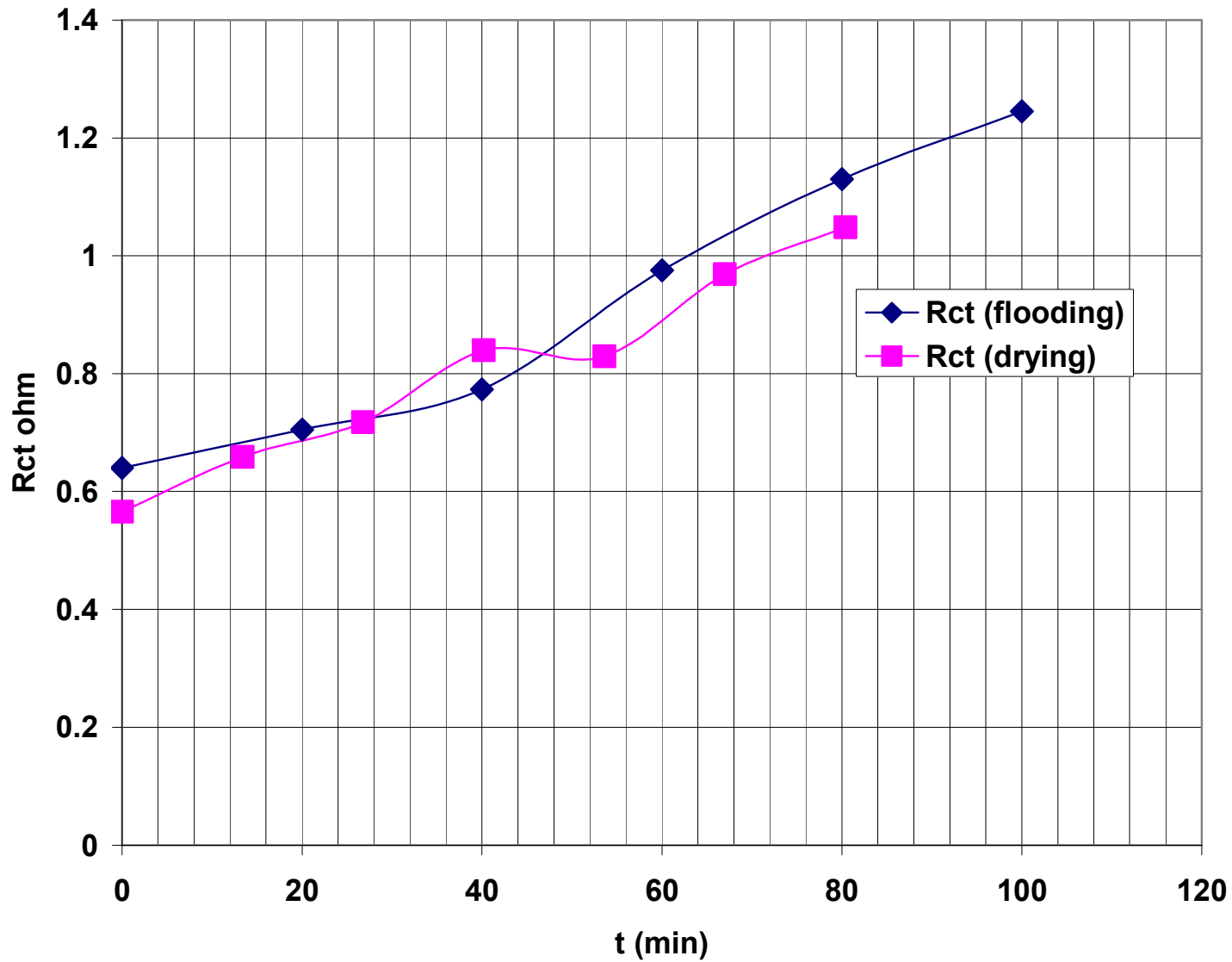
$R_{ct c}$ = anode charge transfer resistance

$CPEc$ = non-ideal double layer capacitance anode

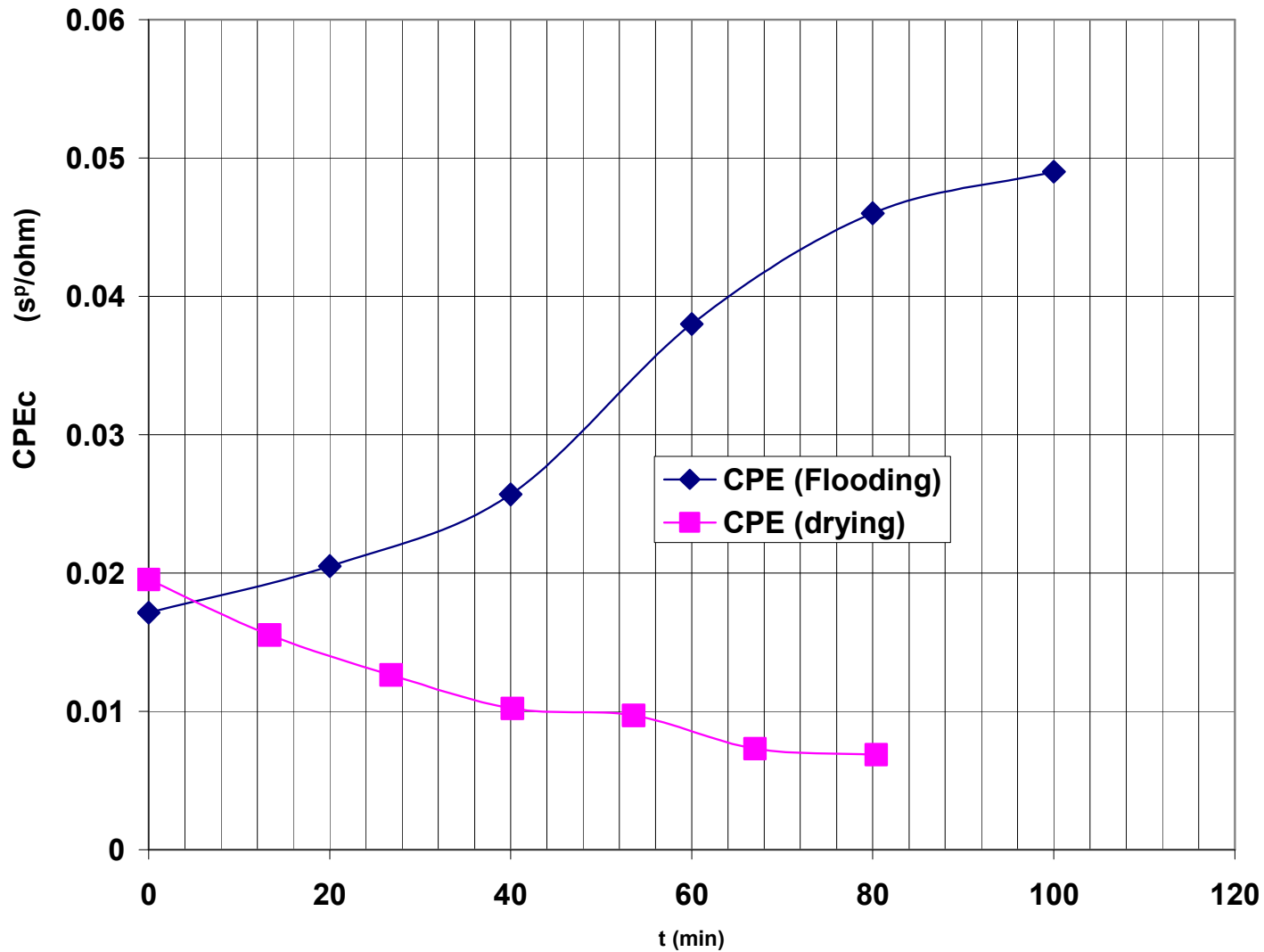
CPE = distributed element, diffusional process



resistive losses increase during drying

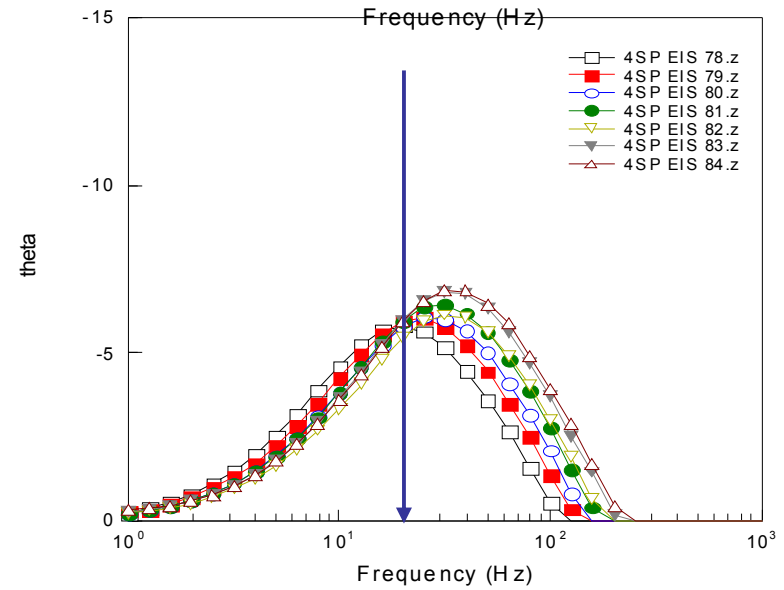
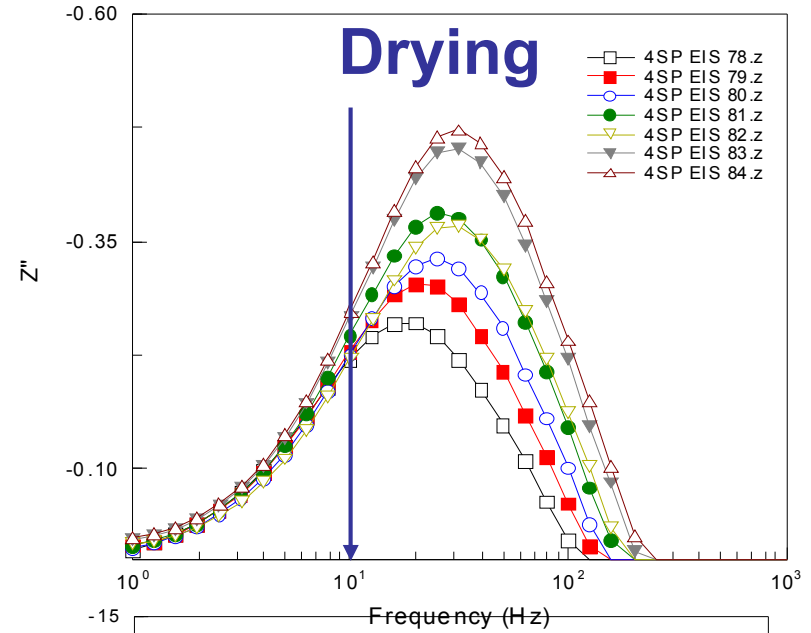
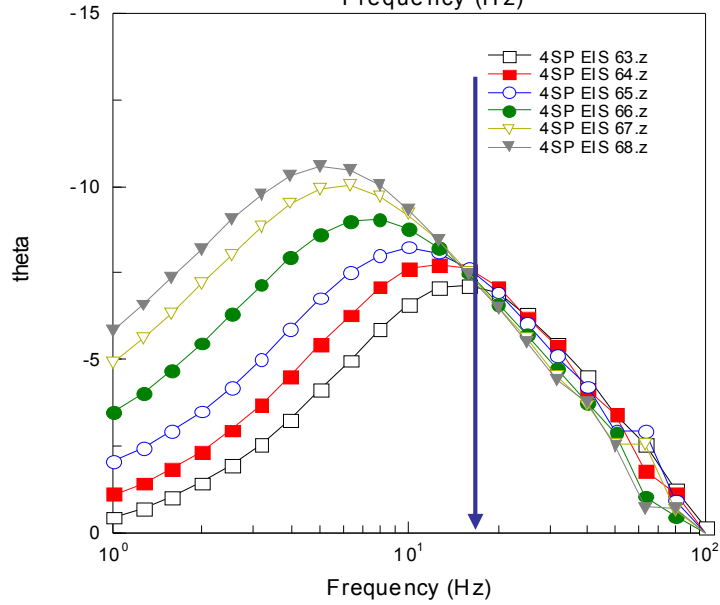
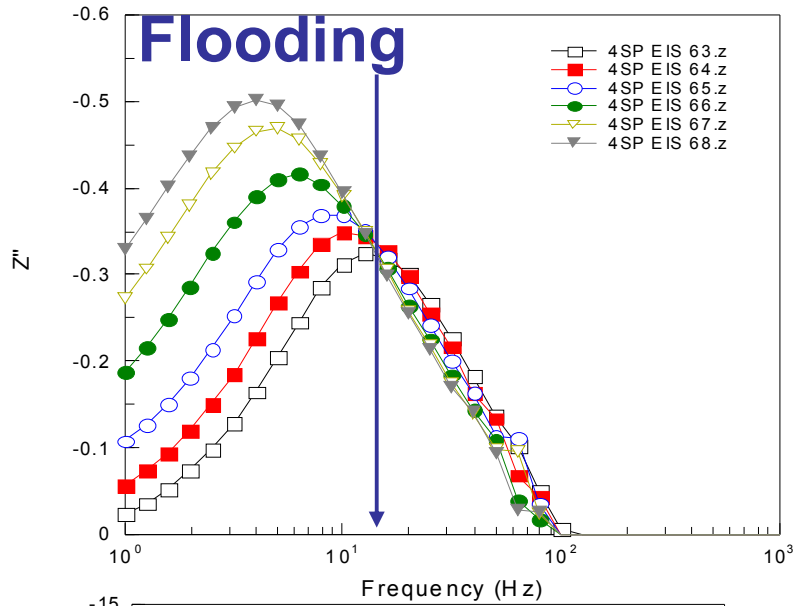


kinetic losses increase during drying and flooding



during drying CPE impedance increases (distributed nature of CL?)

during flooding CPE impedance reduces





Conclusions:

- During drying, both in-phase and out-of-phase impedance content increase
- During flooding only out-of-phase content increases
- For both cases it appears that there is one single frequency threshold ($\sim 10\text{Hz}$) from which out-of-phase content starts to shift to:
 - smaller frequencies for flooding
 - larger frequencies for drying



Phase angle vs. Imaginary content:

- θ seems to better define initial drying/flooding process (one single frequency?)
- θ can be associated with concentration profiles (ac voltammetry?)



Recommendations:

- Minimize FC design effects (ϵ , GFF, GDL, CL, etc.), better base-line during testing
- specific frequencies might be design-dependent: need further studies
- dry/flooding case: **comparison of states** only as a short time forecast
- Different FC sizes might need different approaches for diagnosis
- Isolation of true dry and true flooding conditions is only possible if homogenous internal conditions are achieved
- Structural effects should be studied (carbon support as a conducting grid, i.e. additional capacitance or inductance effects?)



- Properties of components are needed particularly substack layers (i.e. capillary properties, etc.)

For your safety:

This presentation was AH1N1 free...!