

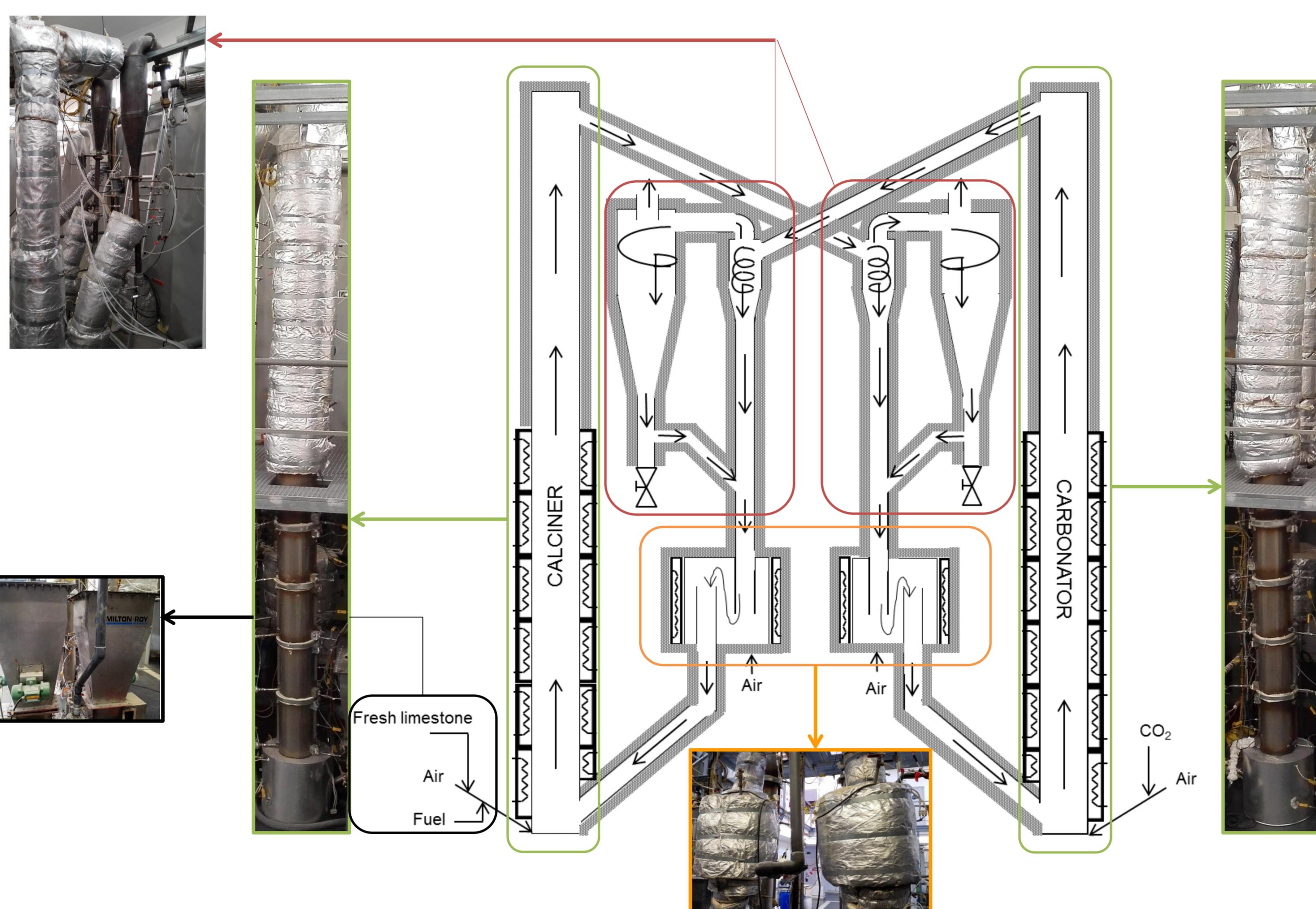
# Screening CO<sub>2</sub> capture test for cement plants using a lab scale Calcium Looping pilot facility.

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## Objective

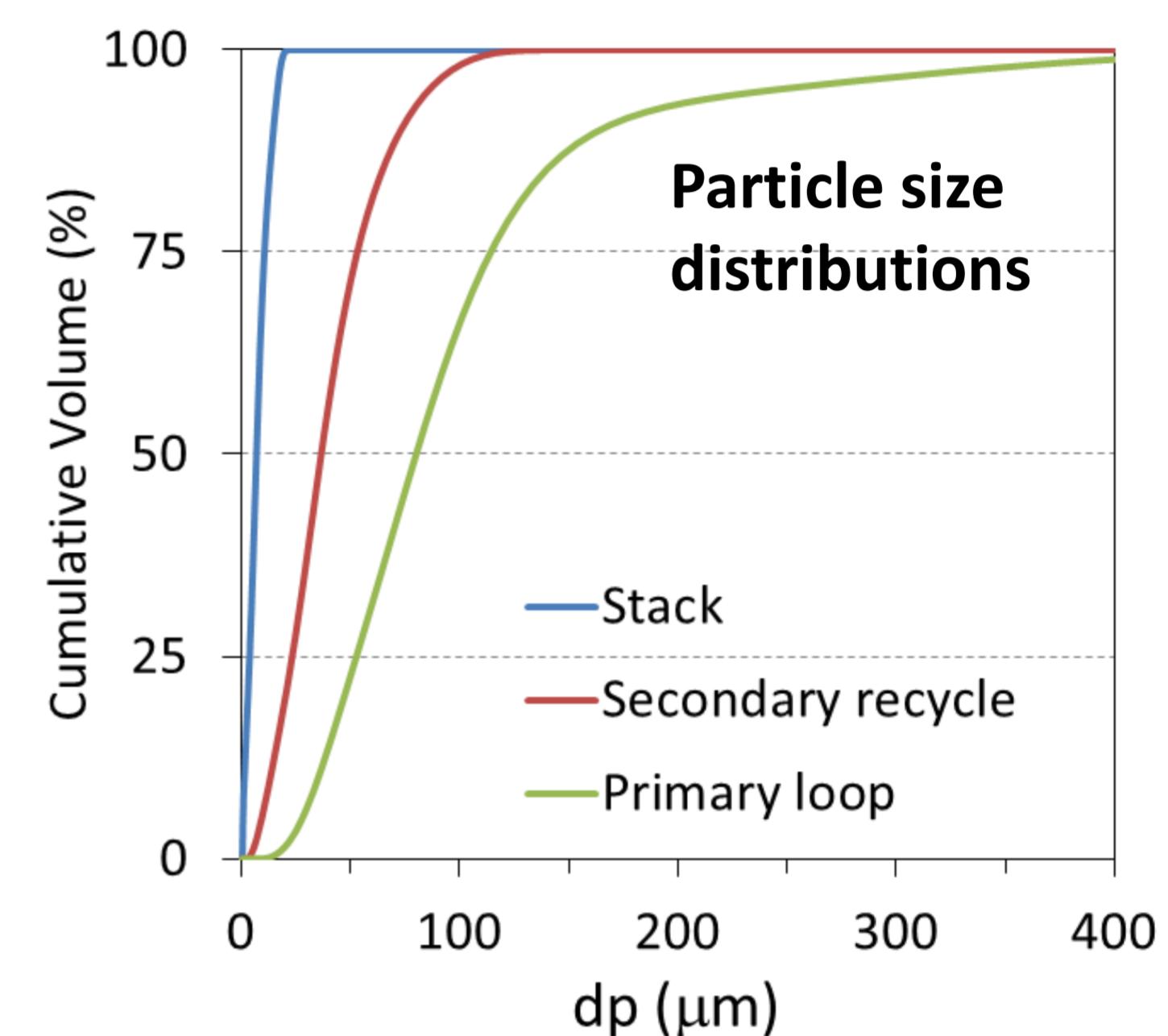
Calcium Looping (CaL) is based on the use of CaO as a regenerable sorbent of CO<sub>2</sub>. The technology has been demonstrated for post-combustion CO<sub>2</sub> capture in power generation at TRL 6-7, but requires detailed testing at closer conditions to those expected in cement applications: higher CO<sub>2</sub> concentrations, higher sorbent activity and lower average particle sizes. We investigate these new operating conditions in a 30 kW<sub>th</sub> CaL pilot in CEMCAP.

## THE 30 kW TEST FACILITY

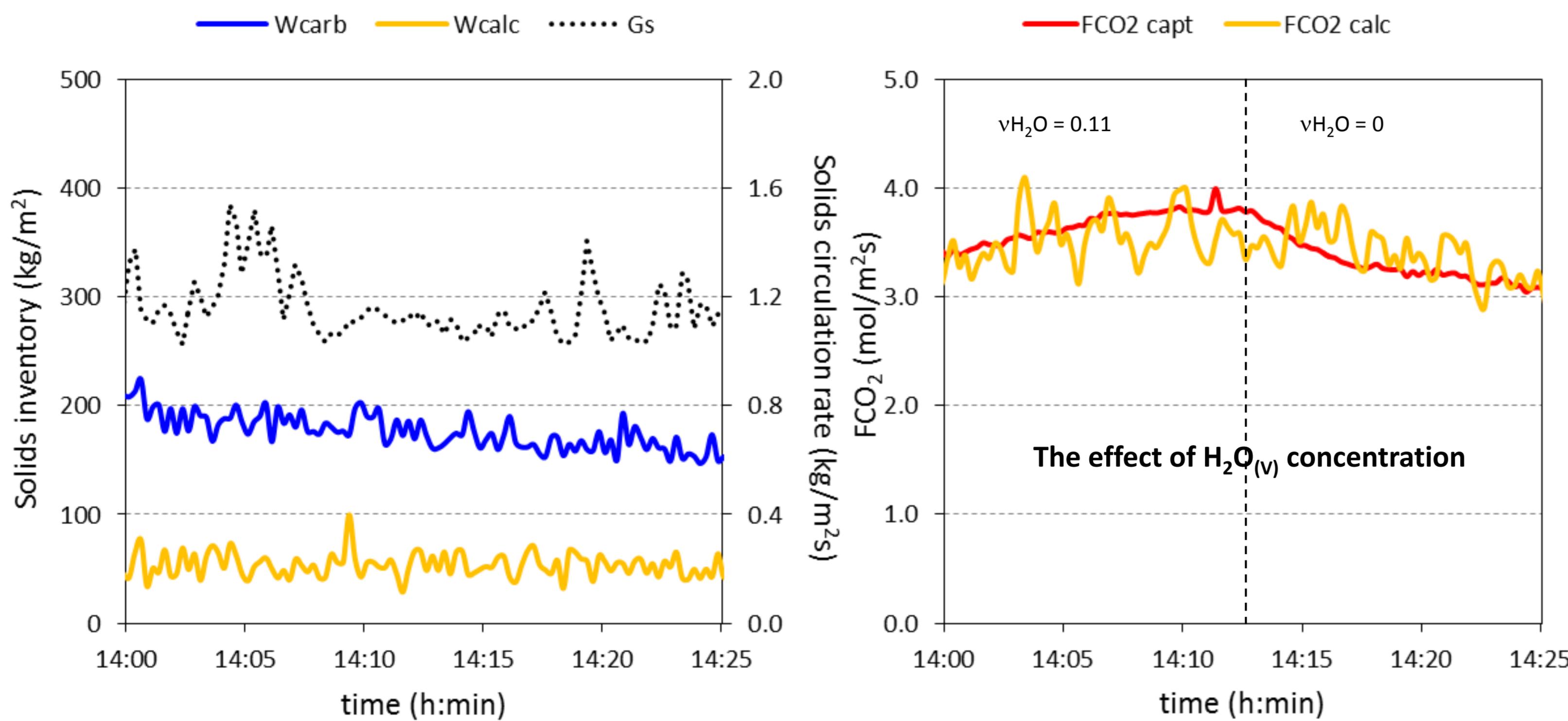
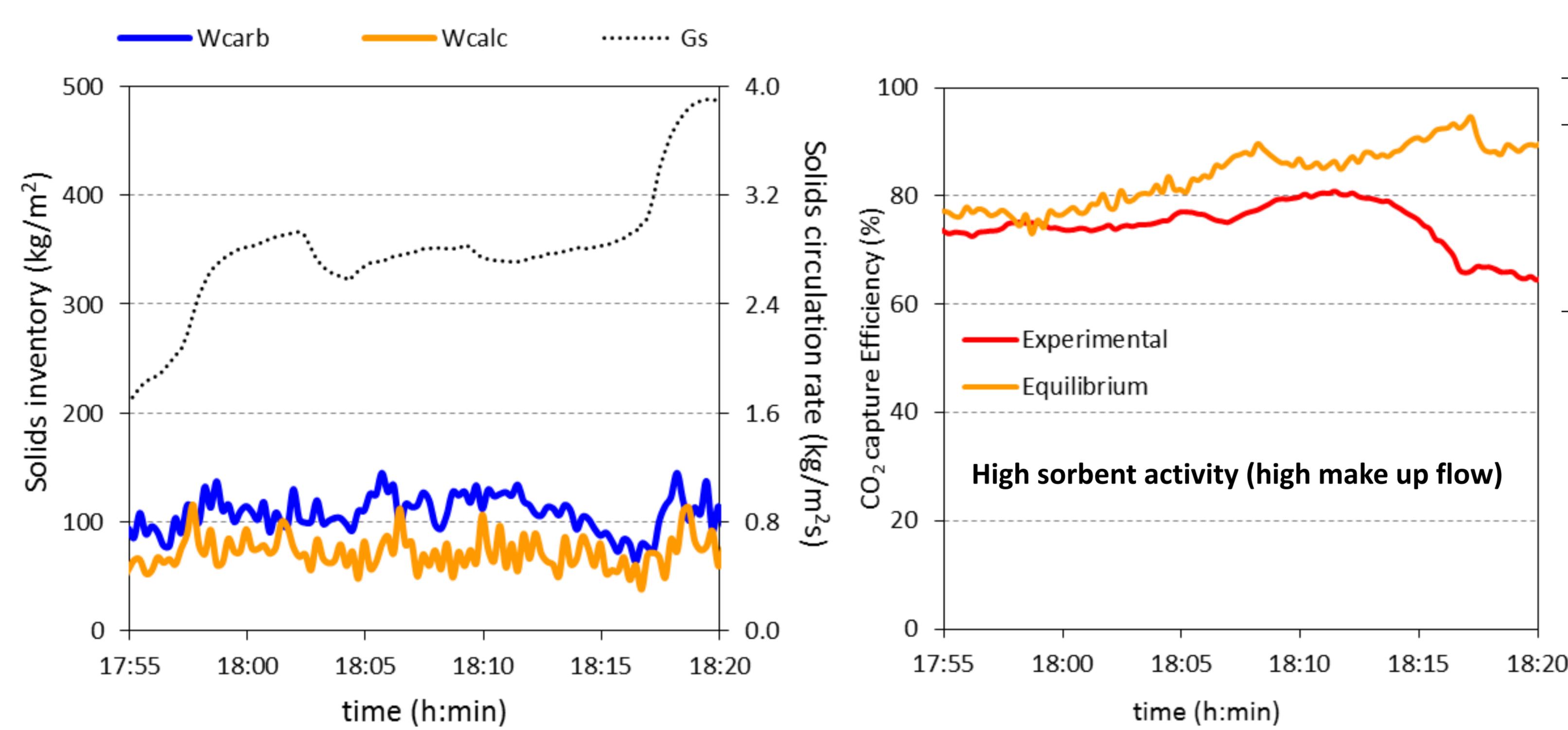


## MAIN FEATURES

- Two CFB reactors ( $h = 6 \text{ m}$ ,  $d_i = 0.1 \text{ m}$ )
- Double recycle loop
- Gas mixtures of CO<sub>2</sub>, air, SO<sub>2</sub>, H<sub>2</sub>O feeds
- 40 Thermocouples, 20 ΔP measurements
- 4 O<sub>2</sub> zirconia probes,
- 2 on-line gas analysers (CO<sub>2</sub>, O<sub>2</sub>, SO<sub>2</sub>, NO<sub>x</sub>)



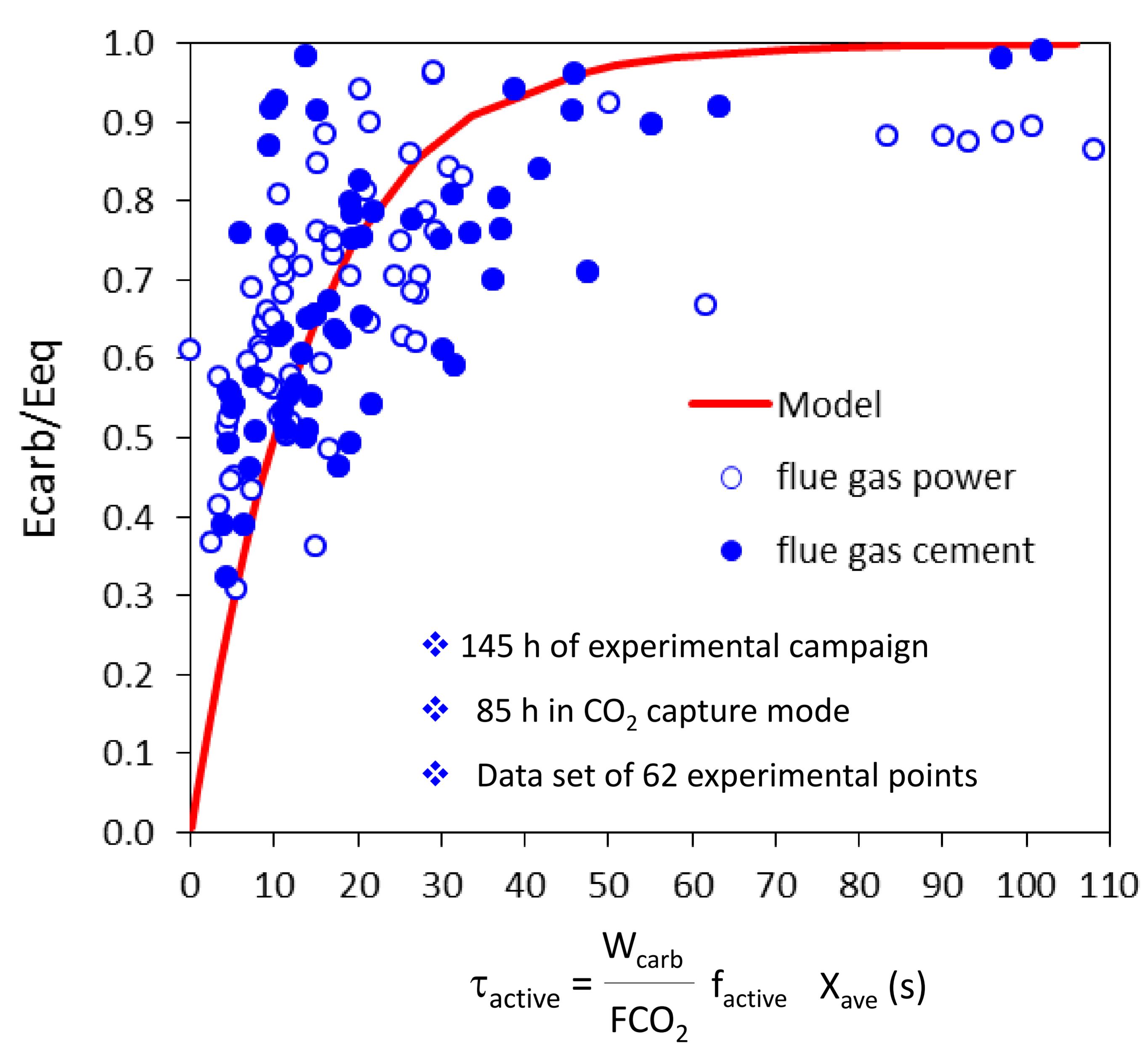
## EXAMPLES OF EXPERIMENTAL RESULTS OF CO<sub>2</sub> CAPTURE



## REACTION MASS BALANCE

### RANGE OF OPERATING CONDITIONS

CARBONATOR			CALCINER		
Carbonator temperature (°C)	T <sub>carb</sub>	620-725	Calciner temperature (°C)	T <sub>calc</sub>	760-920
Carbonator inlet velocity (m/s)	u <sub>carb</sub>	2-3.7	Calciner inlet velocity (m/s)	u <sub>calc</sub>	1.5-3.3
Inlet CO <sub>2</sub> concentration (vol/vol)	v <sub>CO<sub>2</sub></sub>	0.1-0.27	Molar ratio fresh make-up to CO <sub>2</sub>	F <sub>0</sub> /F <sub>CO<sub>2</sub></sub>	0-0.55
Inlet H <sub>2</sub> O concentration (vol/vol)	v <sub>H<sub>2</sub>O</sub>	0-0.12	Solids circulation flowrate (kg/m <sup>2</sup> s)	G <sub>s</sub>	0.9-3.7



## CONCLUSIONS

- High activity material resulting from large make up flows of limestone allow for high CO<sub>2</sub> capture efficiencies despite very low solids inventory in the reactor (100 kg/m<sup>2</sup>).
- Pilot plant and its reactor model behaves with similarly with flue gases from cement than with flue gases from power when using limestone as make up.

## References

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