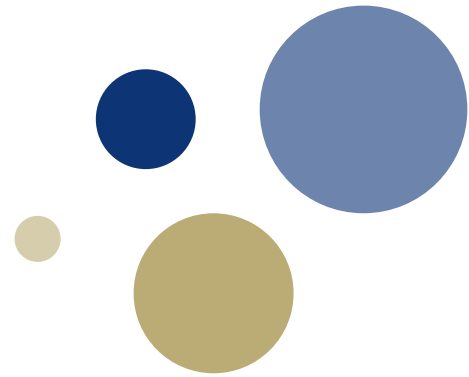




NTNU

Norwegian University of
Science and Technology

S  H₂ IFT

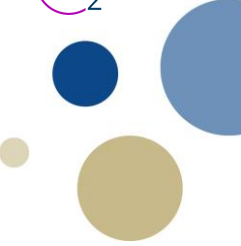
The SH2IFT logo features the letters 'S', 'H₂', and 'IFT' in a blue, sans-serif font. The 'H₂' is enclosed within a magenta circular outline that has a small white circle at the top and a gap at the bottom.

Consequence Analysis of Liquid Hydrogen Tank Explosion

Green Hydrogen Webinar

Federico Ustolin

07.10.2021



Content

- ✿ Introduction on BLEVE and modelling activity
- ✿ Liquid CO₂ explosion experiments
- ✿ BMW safety tests on liquid hydrogen
- ✿ LH₂ BLEVE CFD analysis by using ADREA-HF
 - ✿ ADREA-HF code validation
 - ✿ Simulation of BMW bursting tank test
- ✿ Conclusions

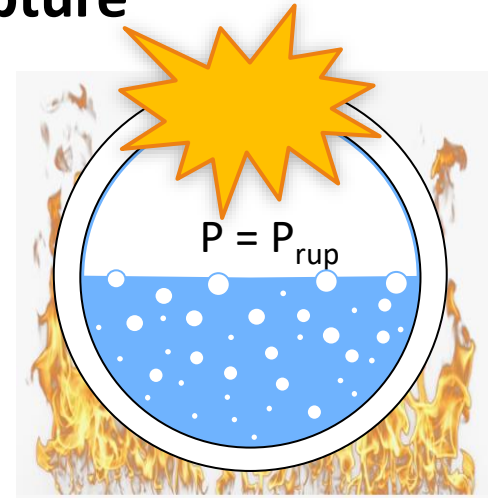
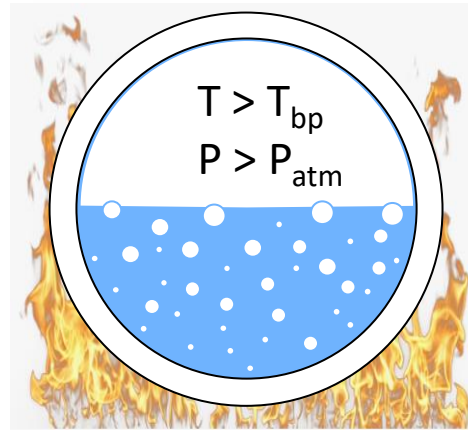
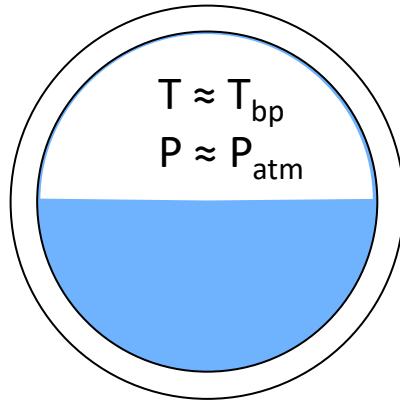
BLEVE

Boiling Liquid Expanding Vapour Explosion:

physical explosion might result from the catastrophic rupture of a tank containing a superheated liquid due to the rapid depressurization

Chain of events leading to the tank rupture

Valid for
cryogenic
substances

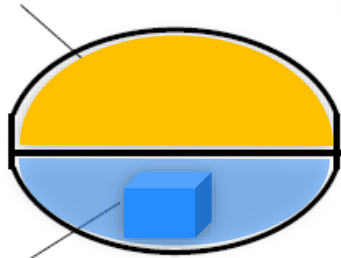


Time



BLEVE

Compressed
Vapor



Liquid

Time

$$P$$

$$T = T_s(P)$$

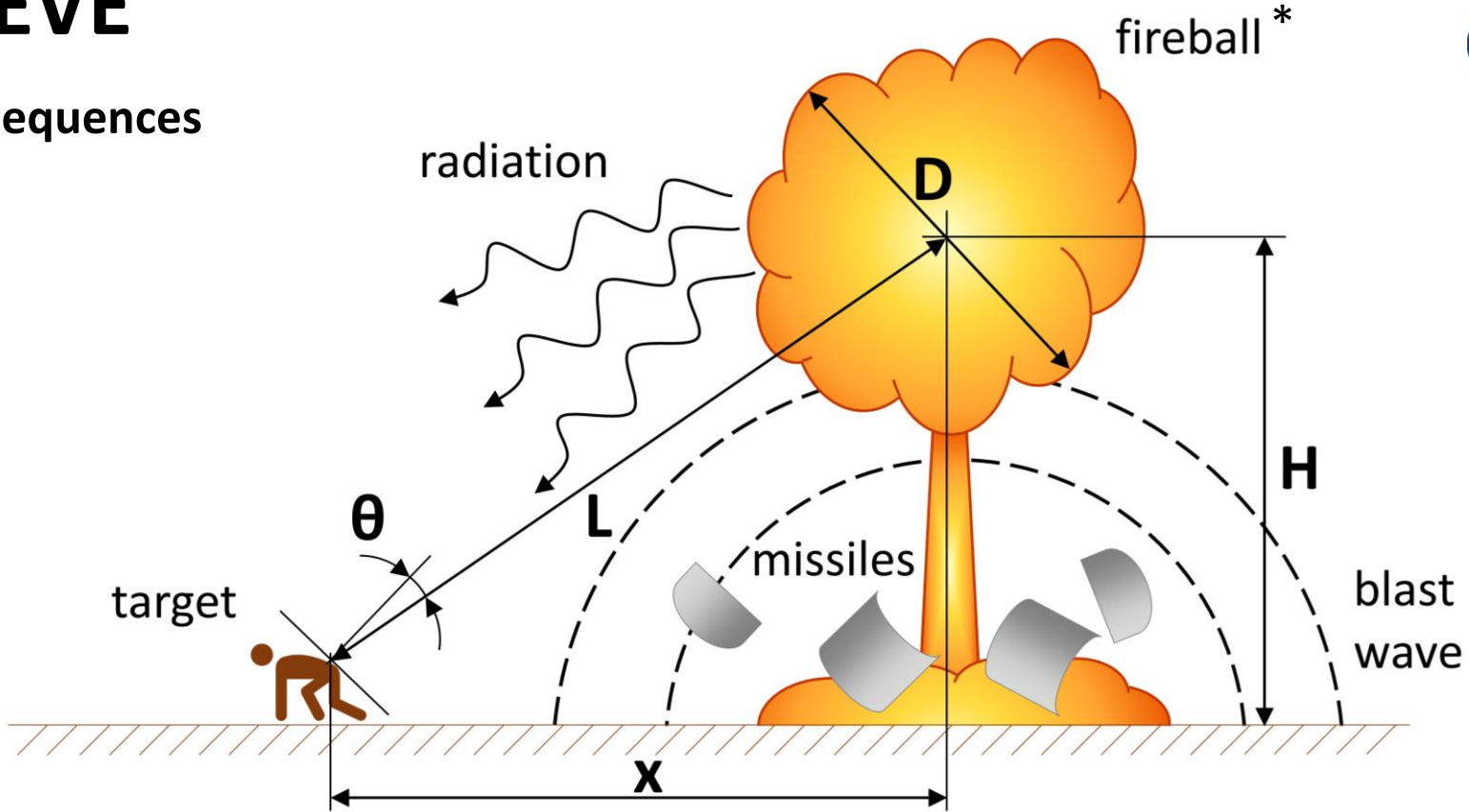
$$h_l = h_l(T)$$

$$h_g = h_g(T)$$

Hot liquid undergoing sudden depressurization in a tank
(adapted from [Casal, 2008])

BLEVE

Consequences



*Fireball if substance is flammable and ignition source is present

Modelling activity

Collaboration with **PRESLHY** project partner National Centre for Scientific Research “Demokritos”

Aim of the work: provide critical indications on the BLEVE theory

- CFD analysis of BLEVE for liquid CO₂ (LCO₂) and liquid hydrogen (LH₂) tanks
- Study the dynamic of the blast wave (no combustion)

Liquid CO₂ explosion tests

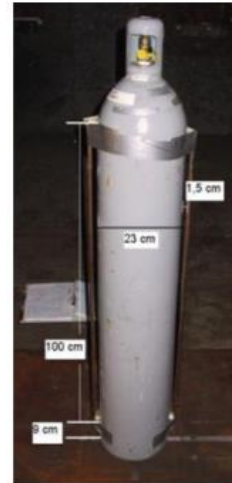
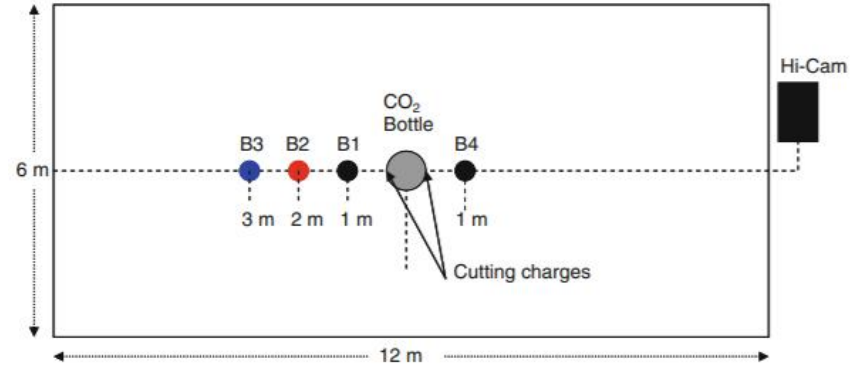
Laboratory for Ballistic Research (TNO
Defence, Security and Safety)

Bunker: 6 × 12 × 4 m

40-l LCO₂ bottle wrecked by explosive:

- D = 0.23 m
- h = 1.37 m
- fd = 95%
- T = 290 K
- P = 5.2 MPa

[van der Voort, M.M., van den Berg, A.C., Roekaerts, D.J.E.M. et al. Blast from explosive evaporation of carbon dioxide: experiment, modeling and physics. Shock Waves 22, 129–140 (2012)]



BMW safety tests

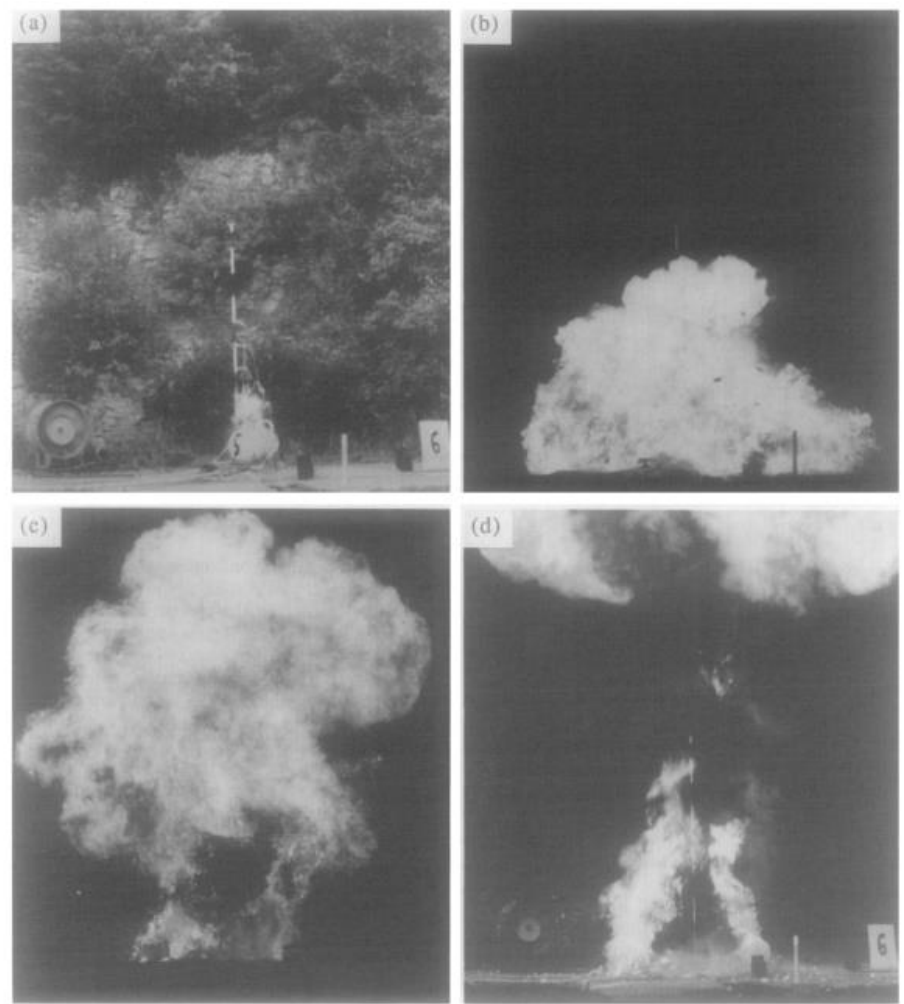
Bursting tank scenario test

Ten single wall vessels insulated with foam and ruptured with explosives:

- $V = 120\text{-l}$
- $P = 0.2 \div 1.5 \text{ MPa}$
- $m_{\text{LH}_2} = 1.8 \div 5.4 \text{ kg}$

Many uncertainties (e.g. filling level, initial temperature, tank dimensions)

[Pehr, K., 1996. Aspects of safety and acceptance of LH2 tank systems in passenger cars. Int. J. Hydrogen Energy 21, 387–395]



g. 3. Development of a fireball. (a) Ignition; (b) 250 ms after ignition; (c) 1250 ms after ignition; and (d) 1800 ms after ignition.

CFD analysis methodology

- CFD code: ADREA-HF
- Homogeneous Equilibrium Model (HEM)
- Raoult's law for ideal mixture
- k-epsilon turbulence model with wall function
- Peng-Robinson and Redlich-Kwong-Mathias-Copeman EoS were tested

The code was validated with the LCO₂ experiments and then employed for the simulation of the LH₂ BMW explosion tests.

CFD analysis methodology

The Navier-Stokes equations, continuity equation, energy equation of the mixture and conservation equation of species. The Favre-averaged equations are (Einstein summation convention is used):

$$\frac{\partial \bar{\rho}}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_i}{\partial x_i} = 0,$$

$$\frac{\partial \bar{\rho} \tilde{u}_i}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_j \tilde{u}_i}{\partial x_j} = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \left(\mu_{eff} \left(\frac{\partial \tilde{u}_i}{\partial x_j} + \frac{\partial \tilde{u}_j}{\partial x_i} \right) \right) + \bar{\rho} g_i,$$

$$\frac{\partial \bar{\rho} \tilde{H}}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_j \tilde{H}}{\partial x_j} = \frac{\partial}{\partial x_j} \left(\frac{\mu_t}{Pr_t} \frac{\partial \tilde{H}}{\partial x_j} \right) + \frac{D\bar{p}}{Dt},$$

$$\frac{\partial \bar{\rho} \tilde{q}_k}{\partial t} + \frac{\partial \bar{\rho} \tilde{u}_j \tilde{q}_k}{\partial x_j} = \frac{\partial}{\partial x_j} \left(\frac{\mu_t}{Sc_t} \frac{\partial \tilde{q}_k}{\partial x_j} \right) + \bar{R}_k, \quad k = 1, \dots, N_{subs},$$

Assumption: instantaneous and uniform rupture of tanks in all directions

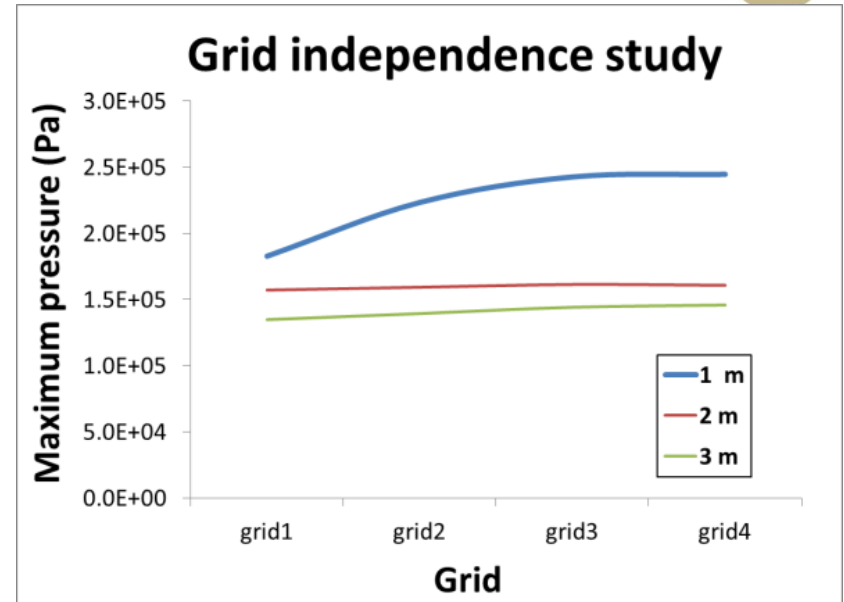
LCO₂ simulation configuration

Initial conditions of the LCO₂ BLEVE simulation (**assumption: 100% LCO₂**)

Pressure (Pa)	Temperature (K)	Density (kg/m ³)	Mass (kg)
5,200,000	289.03	772.54	30.90

Computational meshes (double symmetry along y- and x-axis):

- × Grid 1: 33,792 cells
- × Grid 2: 113,960 cells
- × Grid 3: 265,832 cells
- × Grid 4: 469,560 cells

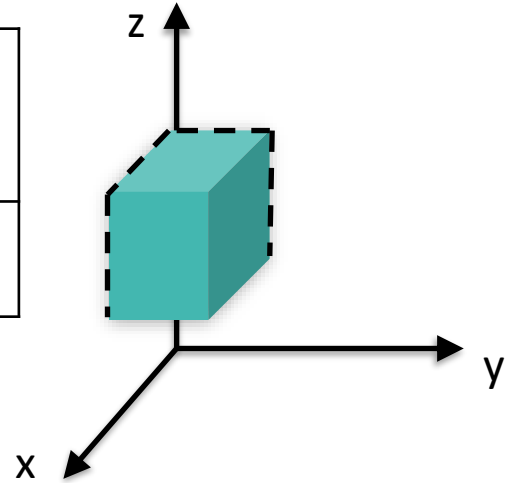


Relative error between grid 3 and 4 $\leq 1\%$ for all three sensors

LH₂ simulation configuration

Characteristics of the simulated LH₂ tank and dimensions of the domain
(double symmetry along y- and x-axis → ¼ tank)

Tank	Volume (litres)	Area (m ²)	Height (m)	Orientation	Tank height (m)	Domain dim. (m)
LH ₂	120	0.177	0.706	Horizontal	1	10 × 10 × 11

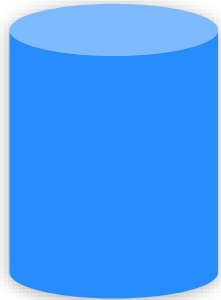


Combustion was not simulated

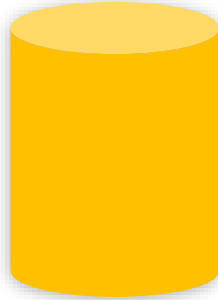
LH₂ simulation configuration

Initial conditions of the LH₂ BLEVE parametric analysis

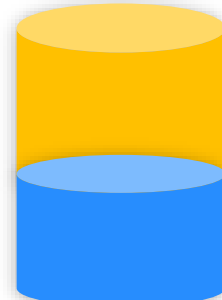
Simulation	Phase and status	Pressure (Pa)	Temperature (K)	Density (kg/m ³)	Mass (kg)
LH2	Saturated L	1,101,325	32.10	42.42	1.27
GH2	Superheated V	1,101,325	32.93	15.00	0.45
LH2-GH2	L and V	1,101,325	32.10, 32.50	42.42 (L), 16.30 (V)	0.77



LH2



GH2

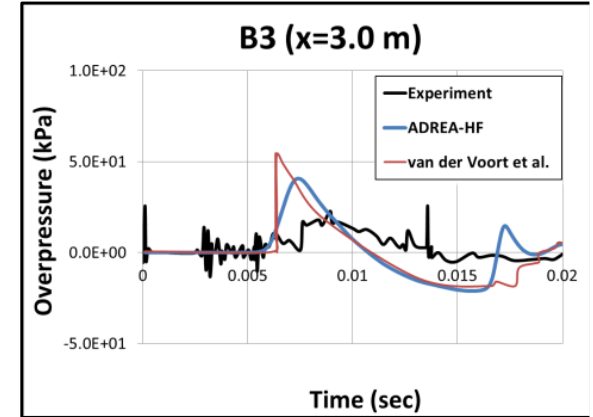
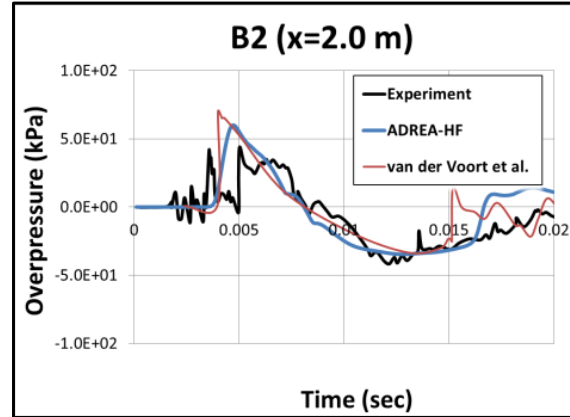
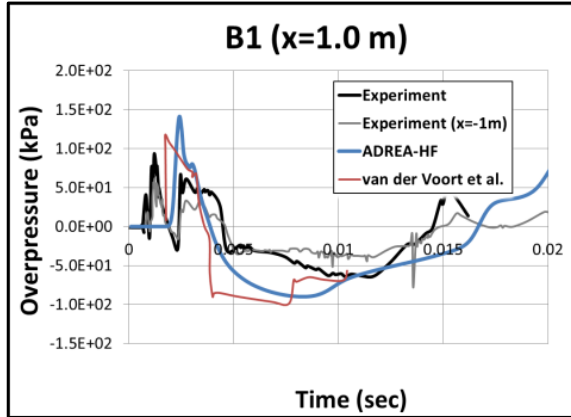


LH2-GH2

fd = 37%

ADREA-HF code validation

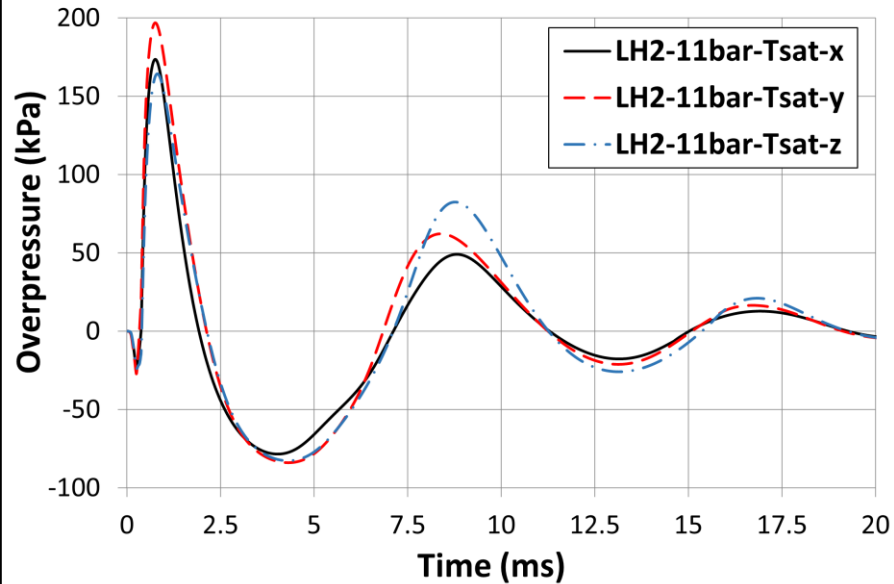
Results of the LCO₂ BLEVE simulations: peak overpressure of the blast wave in three different positions



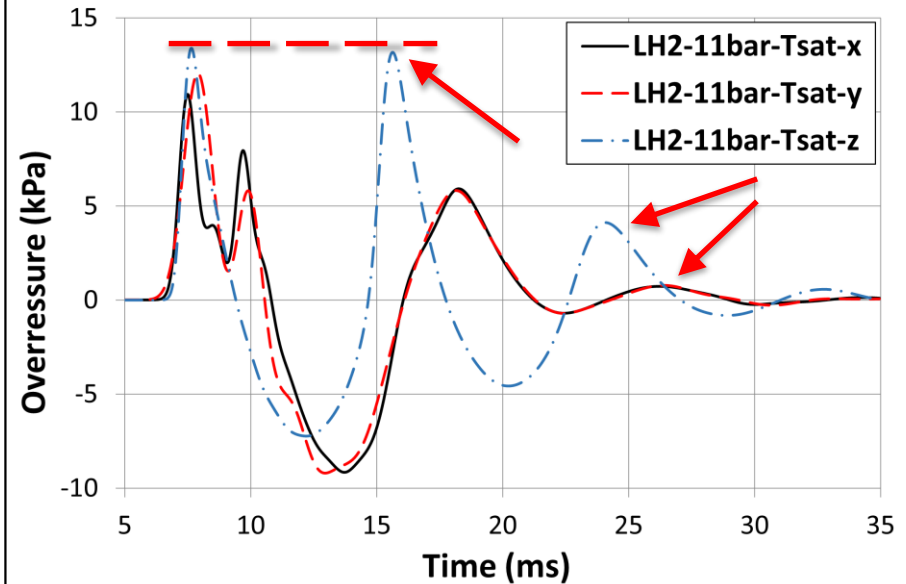
Experimental results are disturbed by the blast wave reflection on the bunker walls

BLEVE blast wave overpressure

0.1 m from tank wall

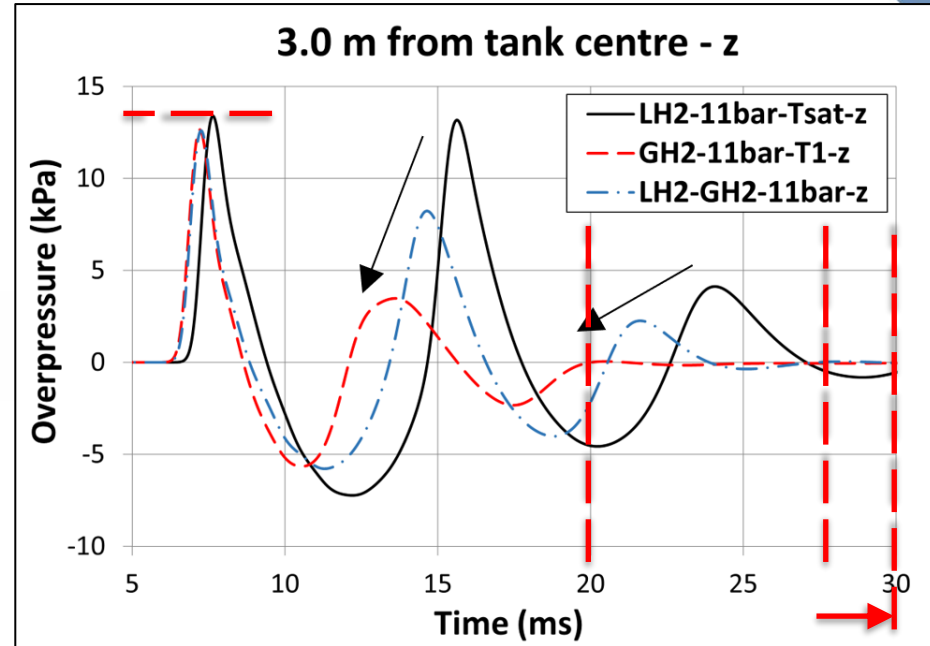
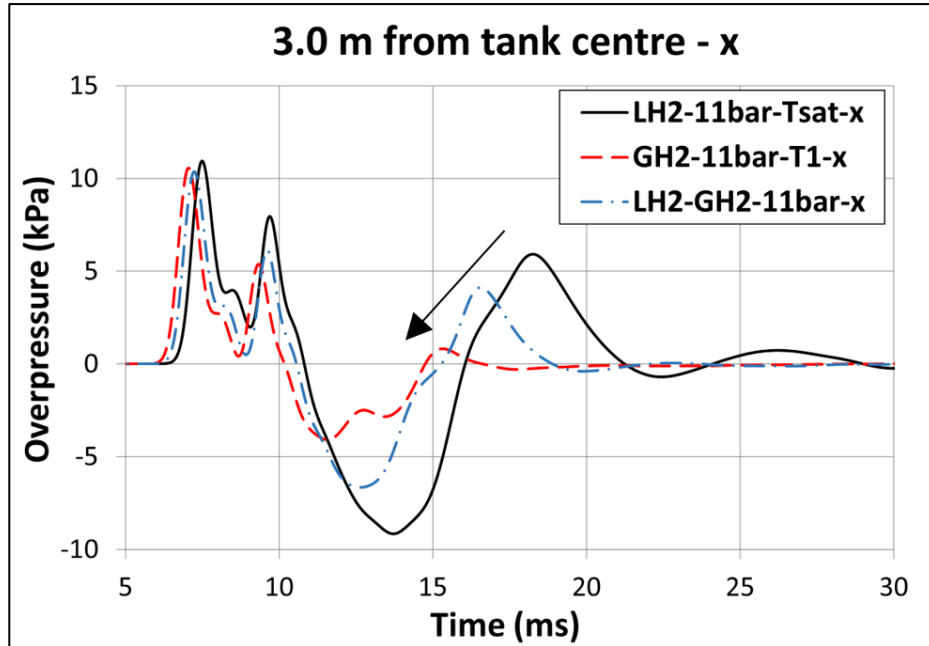


3.0 m from tank centre



Second pressure peak at vertical axis as high as the first one at 3 m from the tank centre

BLEVE blast wave overpressure



- Second pressure peak at horizontal axis decreases with GH2
- Third press peak manifests only when LH2 is initially present
- No large differences in max overpressure yet in explosion duration

Conclusions

- ✿ Differences in the overpressure of the pressure wave along vertical and horizontal axes
- ✿ Both LH₂ or GH₂ contribute to the explosion yield (similar maximum overpressure values)
- ✿ GH₂ simulation produces the shortest explosion, thus the smallest impulse
- ✿ Two pressure peaks for 100% GH₂, while three peaks for the 100% LH₂
- ✿ Maximum overpressure was not mainly affected by the hydrogen mass, while this parameter affects the blast wave impulse.

Thank you for your attention



SH₂I FT

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