CONTENT

1. Short information on Eramet
2. Background for Mn-ore agglomeration project - «the NewERA project»
3. Agglomeration options for Mn-ore fines and by-products
4. Mn-ore fines agglomeration test work
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ERAMET IS A FRENCH MINING AND METALLURGICAL GROUP AND A WORLD LEADER IN ITS BUSINESS

- Manganese chemicals and recycling
- Manganese alloys and Tizir titanium dioxide / pig iron
- Alloys powder and transformation plants
- The Norwegian plants are the main part of Eramets Mn-alloy activity
- High purity nickel and alloys melting and transformation plants
- Manganese alloys plant (China)
- SLN-Nickel mines and ferronickel plant (New Caledonia)
- Weda Bay nickel project (Indonesia) – (under study)
- TiZir – Grande Côte (Senegal) ilmenite and zircon mine

- Manganese mine
- Manganese alloys and metal plants
- Maboumine project - niobium and rare earths (under study)
- Manganese mine project (under study)

NyKoSi Agglomeration Seminar, November 2016
ABOUT ERAMET NORWAY AS

A world leading producer of Manganese alloys

- The Porsgrunn and Sauda plants - from Elkem in 1999
- The Kvinesdal plant - from Tinfos in 2008
- Eramet Norway 2015:
  - 517 FTE
  - 4.7 bill NOK in turnover
  - COI ~14%
  - Sales volumes; 493 KT of which refined: ~ 60%
  - El. consumption: 2 TWh
  - CO2 emissions: 800 Ktons
- Capex spendings since 2000:
  - Ca 2,000 mill NOK of which ca 30% = HES

Eramet Norway Sauda
Eramet Norway Porsgrunn
Eramet Norway Kvinesdal

39 MW
38 MW

36 MW
30 MW

29 MW
29 MW
29 MW

HCFeMn 71 KT/y
Ref FeMn 130 KT/y

Ref FeMn 101 KT/y
SiMn 58 KT/y

SiMn & LCSiMn 76 KT/y + 68 KT/y
Sellable production

FeMn
SiMn
Refined FeMn
MOR

HC-slag 180 KT/y

NyKoSi Agglomeration Seminar, November 2016
THE OBJECTIVES OF THE ERAMET NewERA PROJECT

Process efficiency
- Reduce specific energy consumption
- Reduce specific coke consumption
- Increase furnace and refining stability

Reduce variable costs
Increase production
Reduce environmental costs
Reduce future environmental capex
Comply with future demands
Obtain funding support

Resource optimization
- Recover energy, sell electricity
- Utilize waste energy for industrial purposes
- Increase total manganese yield

Environmental footprint
- Reduce CO₂ emissions
- Reduce other emissions
- Reduce depositing
Energy recovery: Gas engines to combust the furnace gases that are currently flared. Engines will produce electricity, hot water for district heating and exhaust gases for the dryer.

Ore drying: A rotary dryer using the hot combusted gas from the gas engines to dry the ore.

Screening: Dried ore will be screened at 3mm. The dried 3-80 mm lumps will be fed directly to the HCFeMn furnace. Fines below 3 mm together with Mn-containing filter dusts and sludges will be agglomerated.

Agglomeration: Roll-press, vibration–compaction or “tableting” are considered to agglomerate the ore fines and dusts.

Waste-to-value: Agglomerate Mn by-product together with Mn-ore fines and recycle to HCFeMn or SiMn furnaces.
WHY DRY AND SCREEN THE ORE?

Reasons:

- Eramet wants to improve the permeability of the furnace charge in order to increase the consumption of the Gabonese ore to benefit from the inherent properties of this ore.

Potential benefits:

- Increase pre-reduction in the furnace.
- Decrease specific electrical energy.
- Decrease specific carbon consumption.
- Increase furnace operating stability and time at full load.
- Increase production.
- Reduce CO₂ footprint.
The agglomeration technique chosen will be dependent on:

- Thermodynamic properties of the agglomerate.
- Raw materials particle size.
- Agglomerate size required.
- Binder.
- Cold and hot strength.
- Reactivity.
- Porosity.
- Capacity.
- Cost.
- Industrially demonstrated on Mn-ores.
### MATERIALS TO BE AGGLOMERATED

<table>
<thead>
<tr>
<th>materials</th>
<th>Particle size</th>
<th>blend</th>
<th>moisture</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ore fines</td>
<td>0-3mm</td>
<td>30%</td>
<td>&lt;2%</td>
</tr>
<tr>
<td>Ore dryer filter dust</td>
<td>&lt;50mm</td>
<td>45%</td>
<td>&lt;2%</td>
</tr>
<tr>
<td>Sludge</td>
<td>&lt;50mm</td>
<td>10%</td>
<td>40%</td>
</tr>
<tr>
<td>Filter dust</td>
<td>&lt;50mm</td>
<td>3%</td>
<td>&lt;2%</td>
</tr>
<tr>
<td>Metallic fines</td>
<td>0-1mm</td>
<td>15%</td>
<td>&lt;2%</td>
</tr>
</tbody>
</table>

The «ore filter dust» is the ore fines captured in the filter after the rotary dryer.
Cold bonded agglomerates containing Gabonese ore are highly oxidised – MnO₂.

Hot bonded Gabonese sinter and indurated pellets have a lower degree of oxidation as the MnO₂ is reduced to lower oxides during the sintering / induration process.

There will be an energy benefit in the furnace from exothermic pre-reduction of highly oxidised ore briquettes compared to sinter and pellets.

Therefore from an energy perspective it is preferable to smelt cold-bonded agglomerates rather than hot-bonded sinter or pellets.

\[
\begin{align*}
\text{MnO}_2 + \frac{1}{2} \text{CO} &= \frac{1}{2} \text{Mn}_2\text{O}_3 + \frac{1}{2} \text{CO}_2 \\
\frac{1}{2} \text{Mn}_2\text{O}_3 + \frac{1}{6} \text{CO} &= \frac{1}{3} \text{Mn}_3\text{O}_4 + \frac{1}{6} \text{CO}_2 \\
\frac{1}{3} \text{Mn}_3\text{O}_4 + \frac{1}{3} \text{CO} &= \text{MnO} + \frac{1}{3} \text{CO}_2
\end{align*}
\]
Different agglomeration techniques require different raw materials sizing:

- Sintering: 1-10mm
- Pelletising: Max 0,2mm
- Briquetting: 0-6mm
- Extrusion: 0-6mm
- Eirich mixer: <1mm

- For briquetting, a combination of fine and course particles will give a stronger briquette. The correct blend can be achieved by screening, extra crushing or blending in other materials. Too much coarse material can weaken the briquette and increase machine wear.

- For pelletising, the <3mm Mn-ore would have to be milled. This increases the agglomeration cost and and therefore pelletising is eliminated.
Adherence to an ideal particle size distribution curve, (eg. Fuller curve), gives the maximum compaction, cold and hot compressive strength in agglomerates.

\[ P_x = \left( \frac{d_x}{d_{\text{max}}} \right)^n \times 100 \]

Where
\( p_x = \% \) passing square aperture size \( d_x \)
\( d_{\text{max}} = \) maximum particle size, mm
\( n = 0.5 \), grading co-efficient for Fuller’s curve

The coefficient of uniformity (CU) indicates the deviation from the Fuller curve, where \( D_{60} \) and \( D_{10} \) are the screen apertures for which 60% and 10% of the sample passes through, respectively.

\[ \text{CU} = \frac{D_{60}}{D_{10}} \]

The CU for the ‘ideal’ Fuller curve is 36, but satisfactory agglomerates are made is CU => 5
AGGLOMERATE SIZE

The agglomerate size is a compromise:

- Agglomerates, ore and coke should have a similar size range to avoid segregation.
- Large agglomerates are more susceptible to thermal decrepitation than small particles.
- Small agglomerates will most likely have a higher CO-gas reactivity (skrinking core model).
- Very small agglomerates may decrease the furnace charge permeability.
- The agglomerate should be <1/3rd the diameter of the charging chutes to prevent blockages.
- Larger agglomerates allow a higher machine productivity.
- Larger agglomerates may experience a smaller compaction pressure at their centre which may result in a more fragile agglomerate.
- The wear on roll press equipment will be greater with smaller briquettes.
- An agglomerate size between 5mm and 60mm is recommended.
The degree of pre-reduction tends to increase as the porosity in the ore or agglomerate increases.

An agglomerate with a high porosity is desirable - provided it is strong.
WHAT BINDER TO USE?

- **Binder criteria:**
  - Short curing / hardening time without post heat treatment
  - Agglomerate cold and hot strength – transport to the furnace
  - Minimum of unwanted components (slag formation, volatile hydrocarbons / sticky deposits)
  - Easy to handle.
  - Low cost.

- **Organic binders:**
  - Molasses / lime, lignosulphonate, Carboxymethyl cellulose (CMC):
    - ~24 hours hardening time indoors before can be transported.
    - Satisfactory cold and hot strength
    - No slag production

- **Cement (OPC):**
  - Maximum strength is obtained after 2-4 weeks stored under ambient conditions.
  - Cement contributes to slag formation and consumes energy
  - Cement bonded agglomerates tend to break-up on heating.

- **Bentonite:**
  - Low cold strength

*Organic binder are preferred*
<table>
<thead>
<tr>
<th>Technique</th>
<th>material</th>
<th>binder</th>
<th>plant</th>
</tr>
</thead>
<tbody>
<tr>
<td>Sintering (moving grate)</td>
<td>Mn ore fines</td>
<td>none</td>
<td>Eramet Gabon, Eramet China</td>
</tr>
<tr>
<td>Green pelletising</td>
<td>Filter dust from oxygen refining of HCFeMn</td>
<td>10-12% cement</td>
<td>Eramet Sauda, Norway</td>
</tr>
<tr>
<td>Indurated pellets</td>
<td>Ilmenite</td>
<td>Bentonite</td>
<td>Tizir, Norway</td>
</tr>
<tr>
<td>Vibration / compaction</td>
<td>Mn ore fines, filter dusts</td>
<td>10-12% cement</td>
<td>Aaltvedt, Norway</td>
</tr>
<tr>
<td>Roll press briquetting</td>
<td>Mn ore fines</td>
<td>~5% molasses / lime, lignosuphonat, organs</td>
<td>Euroagglo NewERA test work, France</td>
</tr>
<tr>
<td>Eirich mixer</td>
<td>Venturi sludge</td>
<td>blended with filter dusts</td>
<td>Eirich mixer test work, Germany, Norway</td>
</tr>
<tr>
<td>«Tablet» machine</td>
<td>Mn-ore fines</td>
<td>none</td>
<td>Eurotab Go-4-0 test work, France</td>
</tr>
</tbody>
</table>
Typical sinter mix consisted of 1-10mm Mn-ore fines, <6mm coke fines, return sinter fines and flux additives. Materials are pelletised in a rotating drum where moisture additions are made. The raw sinter mix is then layered on the hearth layer to a total depth of about 500mm. Ignition of the coke in the mix is by horizontal burners. Suction is applied beneath the grate to draw in air and propagate the ignition front through the bed. The sinter is discharged from the moving grate into a cooler, then crushed to <75mm.

- Advantages:
  - Industrial operation with Mn-ores
  - Porous, strong product
  - Waste materials can be recycled

- Disadvantages
  - Large capacity
  - High Capex
  - Lost advantage of exothermic reduction of Mn-ore in the furnace

Hot bonding not considered for agglomerating NewERA Mn-ores because of size/capacity and loss of exothermic effect in furnace
Cold bonding process where a mixture of fines and a binder is compressed in a rotary die to form a product with uniform size and shape.

**Advantages:**
- Takes advantage of exothermic pre-reduction of MnO₂ in the furnace
- Molasses /lime, lignosulphonate and organics can be used as binders.
- 0,1-6mm ore particles size, no fine grinding is required.
- Different agglomerate sizes possible.
- Short hardening time with molasses or lignosulphonate.
- No slag formation with molasses, lignosulphonate, organic binders.
- Strong product that can be easily transported.
- Automated process that does not require continuous supervision.
- In industrial operation with Mn-ore fines, chromite fines, steelmill wastes.
- High capacity

**Disadvantages:**
- Strength of briquettes with organic binder over long time?
- Break down products of organic binder in a sealed furnace?

**Opportunities**
- Recycle by-products together with the Mn-ore fines.
- Composite briquettes of manganese ore fines and coal /coke may prove beneficial due to the exothermic reactions taking place between the higher manganese oxides and volatiles from the coal during heating.
Fines plus cement binder are vibrated then compacted in a multi-cell mold. The green briquettes are then dried and cured for several days. Developed from cement block making process.

Advantages:
- Takes advantage of exothermic pre-reduction of MnO₂ in the furnace.
- 0.1-6mm ore particles size, no fine grinding is required.
- Different agglomerate sizes.
- Strong product
- Automated process that does not require continuous supervision.
- High capacity.
- In industrial operation with Mn-ore fines, steelmill wastes, ...

Disadvantages:
- Long hardening time to peak strength with cement binder.
- Temperate hardening room required?
- Slag formation with cement binder.
- Cement binder tends to break up on heating

Opportunities:
- Use lignosuphonate or molasses as binder?
- Recycle by-products together with the Mn-ore fines.
- Composite briquettes of Mn-ore fines and coal/coke
The machine consists of a mixer, a vacuum chamber and a screw extruder. Ore fines, dusts and sludge s are blended with cement binder and water and compacted, de-aerated by vacuum and forced through a die to make long “sausages”.

**Advantages:**
- Takes advantage of exothermic pre-reduction of MnO₂ in the furnace
- Strong green extrudate due to higher mixture density / vacuum de-aeration.
- Low binder consumption?
- Low capital cost of equipment.
- Ability to make briquettes of different sizes.
- High capacity (15-115mt/h).
- Demonstrated on Mn-ores.

**Disadvantages:**
- Cement binder, slag formation, higher energy consumption.
- Extuder wear.

**Opportunities:**
- Can use wet sludges direct into machine.
HIGH INTENSITY MIXER (EIRICH)

- Fine material is fed into the inclined rotating mixing pan. The combination of rotating pan and fast rotating rotors generate nuclei. The rotation speed is then reduced to increase the size of the granules.

- **Advantages:**
  - Takes advantage of exothermic pre-reduction of MnO₂ in the furnace
  - No binder consumption.
  - OK green strength of granules (>2kg.f/ pellet).
  - Drying improves strength. But may increase dusting.
  - Low capital cost of equipment.
  - Low operating cost.

- **Disadvantages:**
  - Can only agglomerate <0.5mm particles?
  - Transport; some dusting and sticking to silo walls
  - Some curing time / drying is probably needed improve green strength.
  - Relatively small granules size, 1-10mm.
  - Not commercially demonstrated on Mn-ores

- **Opportunities.**
  - Mixer can be used as a pre-treatment step before roll-press or vibration-compaction briquetting.
  - Testwork performed with venturi sludge and filter dusts at Eramet Kvinesdal
Tableting: this technology is not used in the mining and metallurgical industry, but has been developed for the food and pharmaceutical industries. It offers the possibility of agglomerating without using a binder.

- **Advantages:**
  - No / low binder consumption.
  - Takes advantage of exothermic pre-reduction of MnO₂ in the furnace

- **Disadvantages:**
  - High capital cost.
  - Small capacity.
  - Not demonstrated on Mn-ores.
# Choice of Agglomeration Technique for Mn-Ore Fines

<table>
<thead>
<tr>
<th>Technology</th>
<th>Sinter</th>
<th>Indurated pellets</th>
<th>Roll press briquetting</th>
<th>Vibration compaction</th>
<th>Extrusion</th>
<th>High intensity mixer</th>
<th>Tablet</th>
</tr>
</thead>
<tbody>
<tr>
<td>Equipment capacity</td>
<td>Large</td>
<td>Medium</td>
<td>Medium</td>
<td>Medium</td>
<td>Medium</td>
<td>Small units</td>
<td>Small units</td>
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<tr>
<td>Capital cost</td>
<td>High</td>
<td>High</td>
<td>Medium</td>
<td>Medium</td>
<td>Low</td>
<td>High</td>
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<tr>
<td>Operating cost</td>
<td>Medium</td>
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<td>Low</td>
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<td>Low</td>
<td>Low</td>
<td>Medium</td>
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<tr>
<td>Complexity</td>
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<td>High</td>
<td>Low</td>
<td>Medium</td>
<td>Low</td>
<td>High</td>
<td></td>
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<tr>
<td>Ore particle size</td>
<td>&lt;5mm</td>
<td>&lt;45μm</td>
<td>&lt;3mm</td>
<td>&lt;5mm</td>
<td>&lt;3mm</td>
<td>&lt;5mm</td>
<td></td>
</tr>
<tr>
<td>Product size, mm</td>
<td>5-80mm</td>
<td>10-15mm</td>
<td>50mm</td>
<td>75mm</td>
<td>25mm</td>
<td>&lt;5mm</td>
<td>&lt;10mm</td>
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<tr>
<td>Feed moisture, %</td>
<td>&lt;5%</td>
<td>&lt;5%</td>
<td>&lt;3%</td>
<td>&lt;5%</td>
<td>&lt;25%</td>
<td>&lt;5%</td>
<td>&lt;5%</td>
</tr>
<tr>
<td>Binder</td>
<td>Ceramic</td>
<td>Bentonite, Molasses, ligno</td>
<td>Cement</td>
<td>Gel agent</td>
<td>Cement, Bentonite?</td>
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<td></td>
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<tr>
<td>Post treatment</td>
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<td>None</td>
<td>Drying/curing</td>
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<td>Cold strength</td>
<td>Medium</td>
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<td>High</td>
<td>High</td>
<td>Medium?</td>
<td>Low?</td>
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<tr>
<td>Hot strength</td>
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<td>High</td>
<td>High</td>
<td>Medium</td>
<td>?</td>
<td>?</td>
<td>?</td>
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<tr>
<td>Porosity</td>
<td>High</td>
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<tr>
<td>CO/(\text{MnOx}) Reactivity</td>
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<td>Medium</td>
<td>High</td>
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<td>High?</td>
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<td>Industrial demonstrated</td>
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<td>yes</td>
<td>no</td>
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</tbody>
</table>
Examine:
- Briquetting properties of Mn-ore fines and by-products
- Different binders: molasses, lignosulphonate, Peridur, bentonite, resin
- Binder addition rates: 3 rate, recommended + / -
- Curing time:
- Cold strength
- (Hot strength)
- (CO reactivity)

<table>
<thead>
<tr>
<th></th>
<th>molasses</th>
<th>lignosulphonate</th>
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<tbody>
<tr>
<td></td>
<td>1</td>
<td>2</td>
</tr>
<tr>
<td>% lime</td>
<td>2</td>
<td>4</td>
</tr>
<tr>
<td>% molasses</td>
<td>4</td>
<td>8</td>
</tr>
<tr>
<td>% Lignosulphonate</td>
<td></td>
<td>2</td>
</tr>
<tr>
<td>% Bentonite</td>
<td></td>
<td></td>
</tr>
<tr>
<td>% Peridur</td>
<td></td>
<td></td>
</tr>
<tr>
<td>% Euroagglo resin</td>
<td></td>
<td></td>
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</table>

Euroagglo facility
PRELIMINARY CONCLUSIONS

- **Briquetting technique:** Roll-press briquetting produced acceptable briquettes.
- **Mix:** Possible to make strong briquettes with Mn-ore fines and by-products combined.
- **Cold strength:** Lignosulphonate and molasses /lime gave briquettes with a cold crushing strength of >150kg.f
- **Binder:** preferred binder: lignosulphonate => molasses => resin
- **Binder amount:**
  - Lignosulfonate: a minimum of 4% lignosulfonate is needed, curing time 24h
  - Lime and molasse: a minimum of 3% lime and 6% molasse, curing time of 24h
  - Strength began to deteriorate after longer storage.
  - Optimisation tests are required resin binder and Peridur
- **Ore particle size, <3mm of <5mm.** Does not seem to have a great influence on mechanical properties of briquettes.
- **Hot strength:** briquettes generate less fines on heating than Gabonese ore.
- **CO reactivity:** Briquettes are as reactive as Gabonese ore.
The presented work on agglomeration and particularly «waste-to-value» was made with help from:

- Industrial partners: Eramet Norway, Eramet Research, Eramet Engineering,
- R&D partners: NTNU, Sintef, SFI.
- Financial support: Enova, EU (Go-4-0)
- Test work; Thomas By, student, NTNU.

**Thanks you for your attention!**