

University of Stuttgart

Institute of Combustion and Power Plant Technology

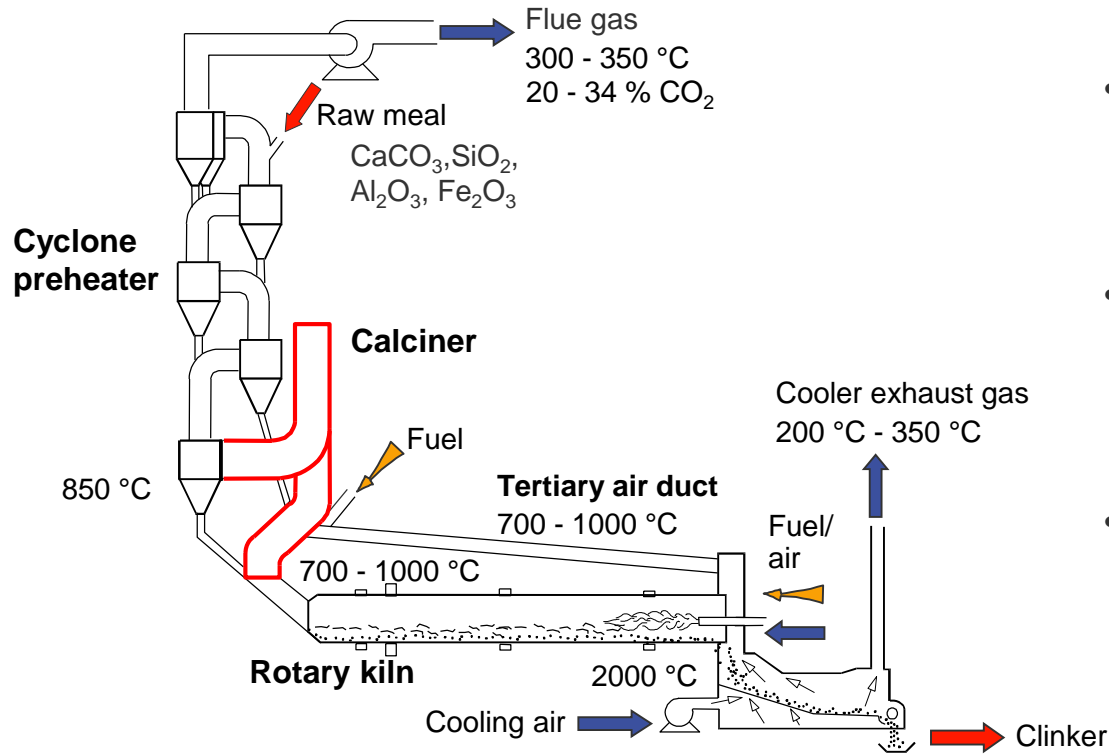
Prof. Dr. techn. G. Scheffknecht

Experimental investigation on emission-free cement production by Calcium Looping post combustion CO₂ capture

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7th HTSLCN Meeting, 4th to 5th September 2017, Luleå

Clinker manufacturing



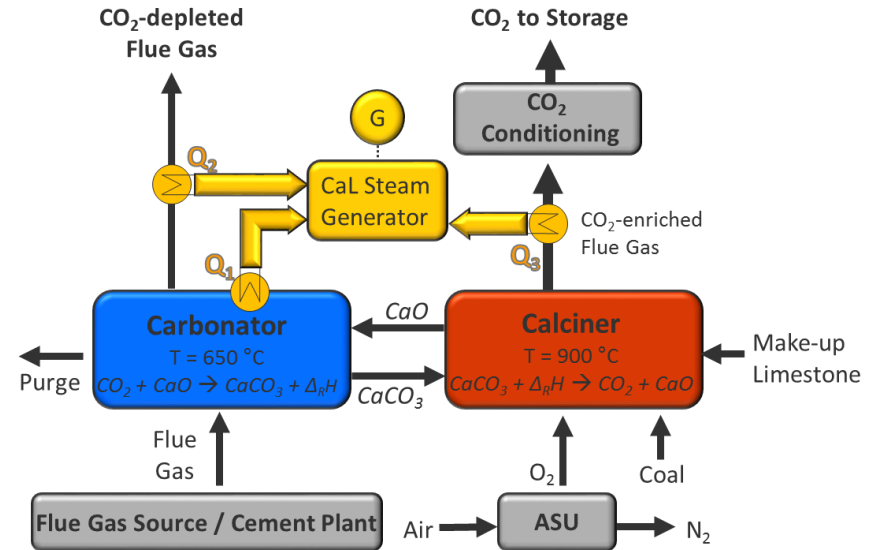
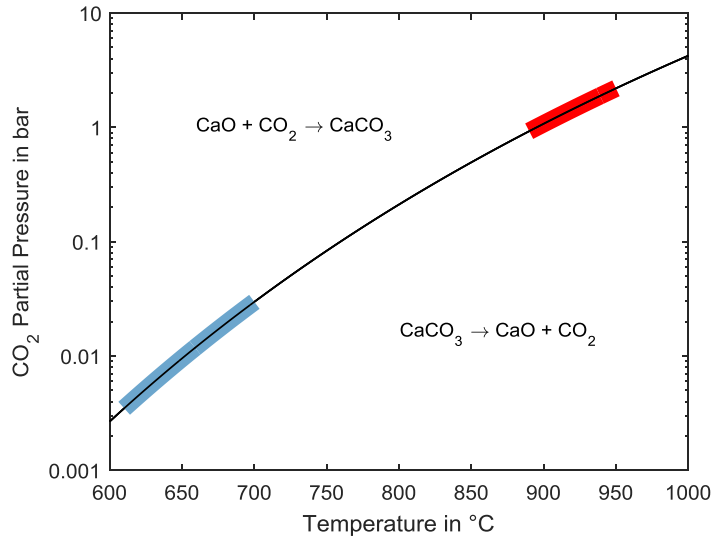
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- Cement production constitute ~5 % of global anthropogenic CO_2 emissions
- CO_2 emissions:
 - 60 % by raw materials
 - 40 % by fuel
- Reduction of CO_2 emissions:
 - 56 % CCS
 - 44 % by increase of energy efficiency, alternative fuels, reduction of clinker share

Calcium – Looping

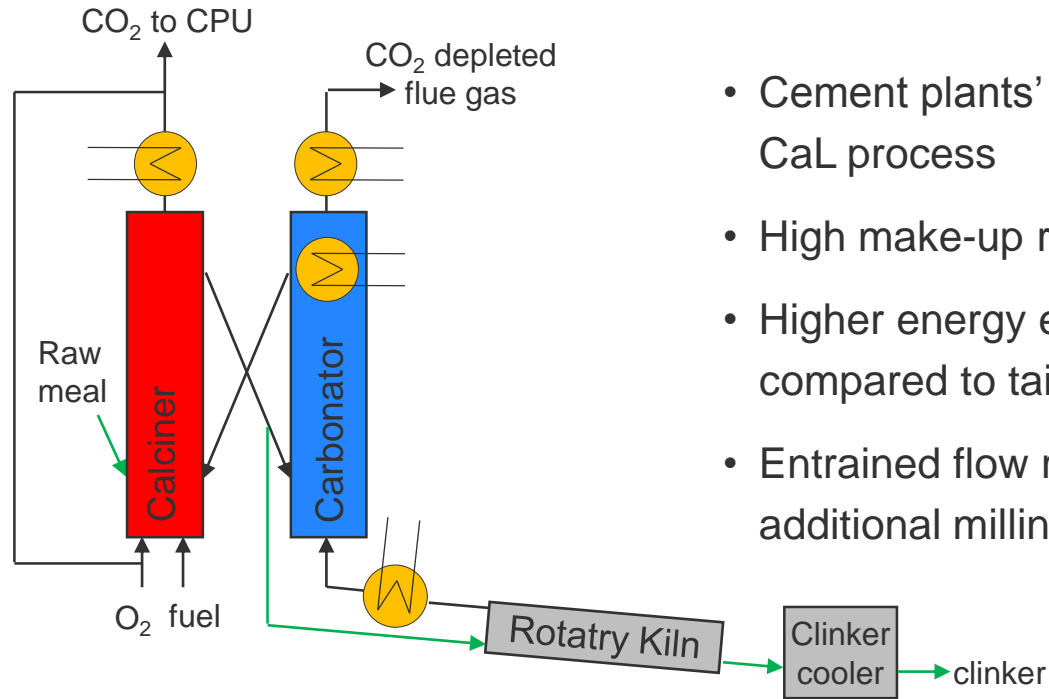
Calcium Looping – General Process Description

- CO₂ capture by cyclic calcination and carbonation of Calciumcarbonat (CaCO₃)
- High energy efficiency due to high temperature level



Calcium Looping – Cement Plant Integration

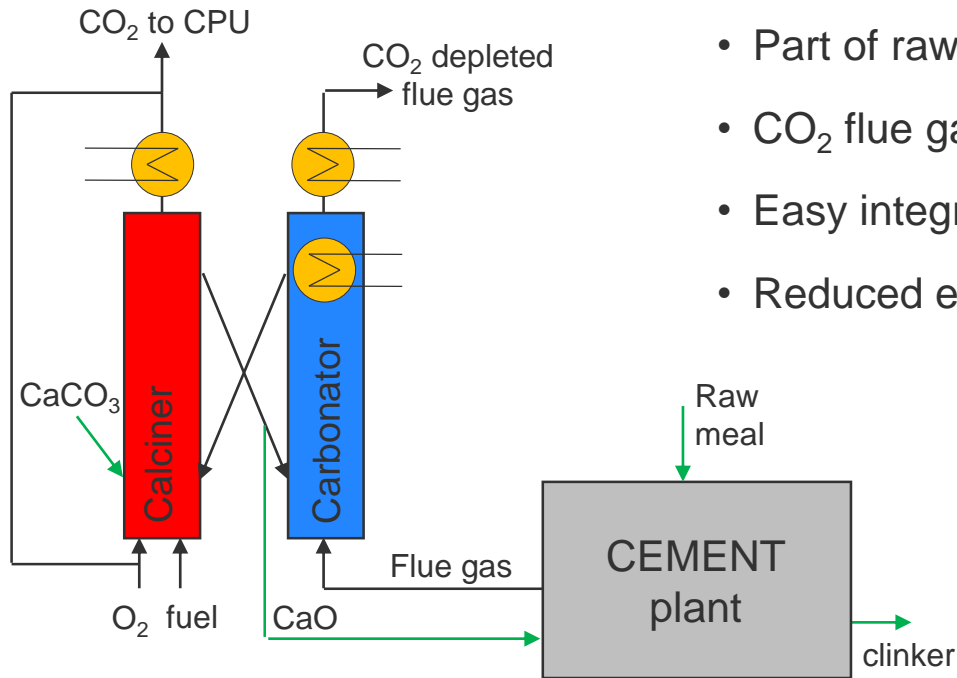
Integrated CaL



- Cement plants' raw meal completely calcined by CaL process
- High make-up ratio realizable
- Higher energy efficiency and higher complexity compared to tail-end
- Entrained flow reactors or CFB reactors with additional milling step if necessary

Calcium Looping – Cement Plant Integration

Tail-end CaL



- Part of raw meal calcined in CaL process
- CO_2 flue gas concentration ~ 20 - 35 %
- Easy integration
- Reduced energy efficiency

Experimental results

Experimental results – Experimental facility

200 – 230 kW_{th} pilot scale facility (3 reactors)

Bubbling bed reactor (1x)

- diameter: 330 mm
- height: 6 m

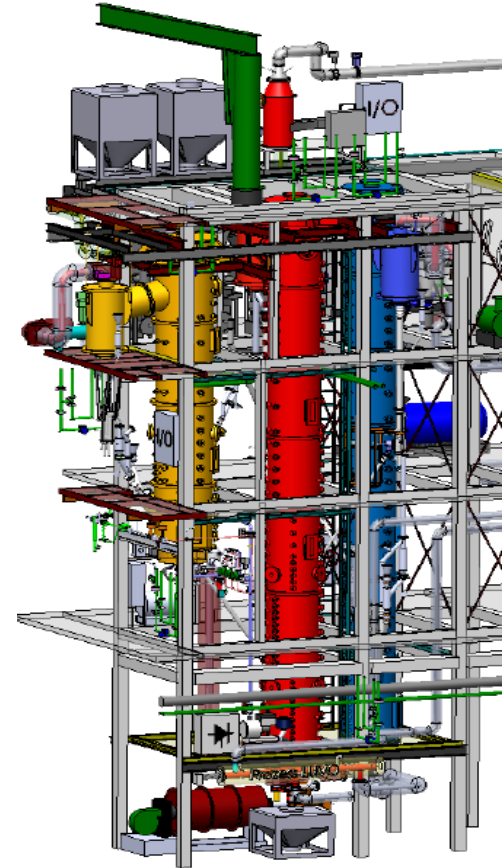
Circulating fluidized bed reactor (2x)

- diameter: 200 mm
- height: 10 m

Possible reactor configuration: CFB-CFB, BFB-CFB

No electrical heating (heated by combustion)

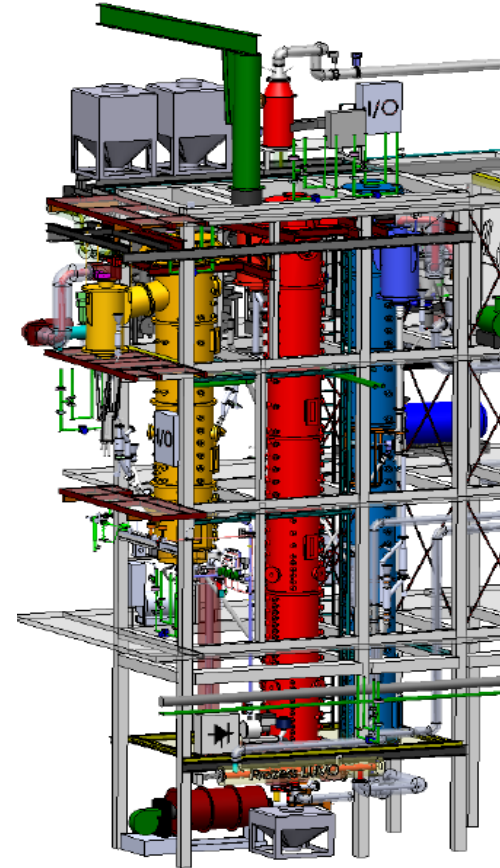
Gas analysis (H₂, CO, CH₄, O₂, CO₂, C_xH_y, SO₂, NO_x)



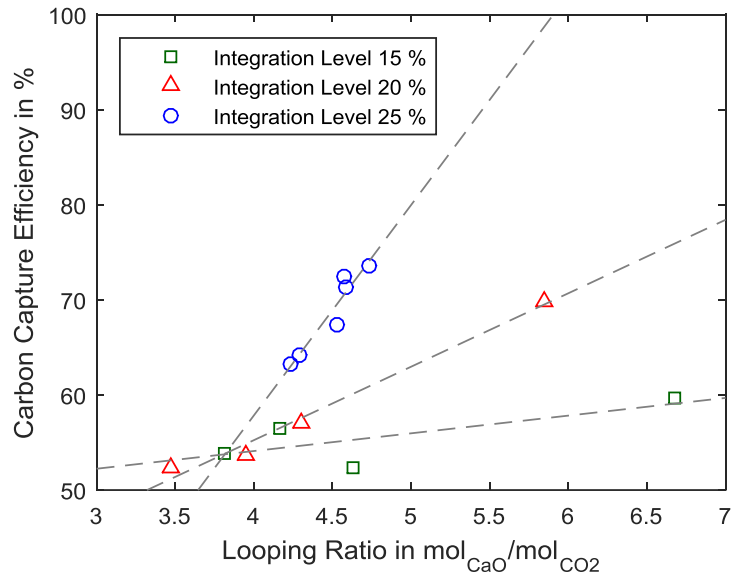
Experimental results – Experimental conditions

	Integrated CaL option	Tail-end CaL option
y_{CO_2}	15 %	20 .. 35 %
$\dot{N}_{\text{CaO},0} / \dot{N}_{\text{CO}_2}$	0.6* , 1.0*	0.08 ... 0.34
$\dot{N}_{\text{CaO}} / \dot{N}_{\text{CO}_2}$	8 ... 20	0 ... 9
T_{Calciner}	~ 910 °C	~ 910 °C
$T_{\text{Carbonator}}$	~ 650 °C	~ 650 °C

* limited by experimental facility – actual make up rate of ~ 4 mol_{CaO}/mol_{CO₂}



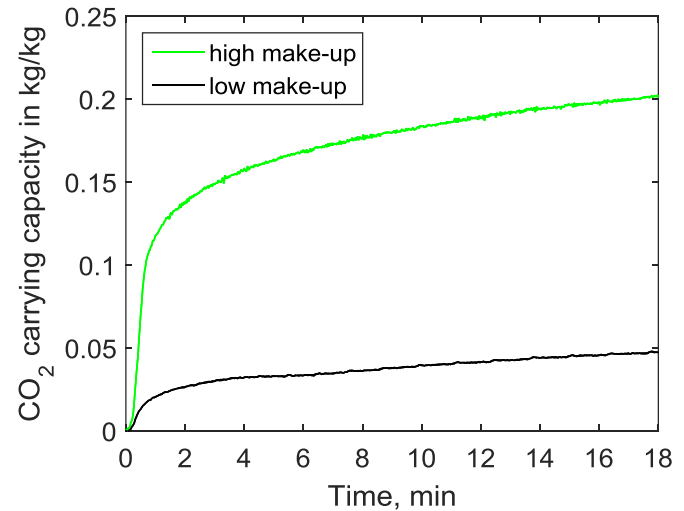
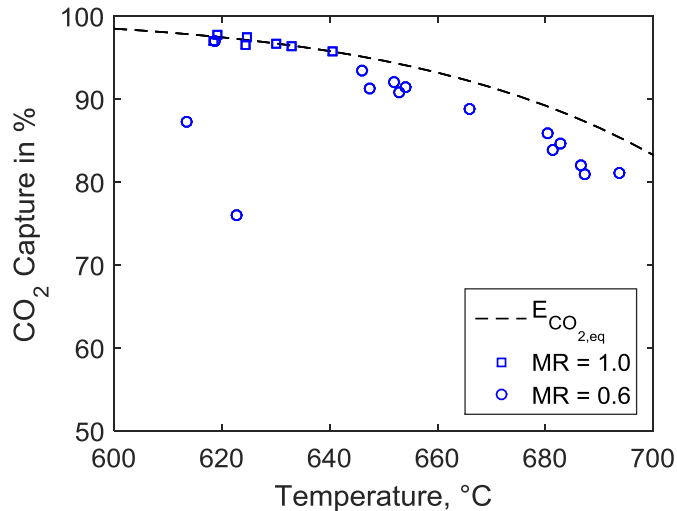
Experimental results – Tail-end CaL Option



- CO₂ capture increases with increasing make-up ratio
- Strong influence of looping ratio upon CO₂ capture in Tail-end configuration
- Influence of looping ratio increases with increasing make-up rate / integration level

Experimental results – Integrated CaL Option

- CO₂ capture was limited by the equilibrium CO₂ capture
- High CO₂ capture rate above 90 % reached
- High sorbent activity due to high make-up flows



Conclusion

Conclusion and Outlook

CaL CO₂ capture:

- Beneficial Calcium Looping operation conditions due to reutilization of sorbent in cement plant
- High CO₂ capture rate >90 % CO₂ capture achieved over a wide range of parameters
- CO₂ capture adjustable by looping ratio, integration level

Tail-end CaL configuration:

- easy to integrated
- reduced energy efficiency
- minor technical uncertainties

Integrated CaL configuration:

- complex integration
- high energy efficiency
- research upon raw meal sorbent performance and entrained flow carbonator sizing

Thank you for your attention!

Acknowledgement

This project has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement no 641185

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Thank you!



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